



## Extractive Desulfurization Using Piperidinium Based Ionic Liquids with Lewis Acids

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**Abstract:** This work includes the preparation of ionic liquid 1,4-dimethylpiperidinium iodide [MMPip]I and its salts with ferric chloride as Lewis acid in different molar proportions [MMPip]I/nFeCl<sub>3</sub> (n=1,2,3). The prepared compounds were diagnosed by spectroscopic and physical methods such as <sup>1</sup>H-NMR, FT-IR, elemental analysis (CHN) and other techniques. The thermal stability of these compounds was studied to use in the extractive desulfurization process (EDS). The efficiency of these compounds in removing sulfur compounds from the petroleum model was examined using dibenzothiophene (DBT) with a concentration of 1000 ppm dissolved in the solvent of normal hexane. The results showed that the compounds used had an acceptable efficiency of up to 30% despite using medium amounts of the extracted agent relative to the oil model; these compounds have a promising future in extractive sulfur removal processes.

**Keywords:** Piperidine ionic liquids, desulfurization, thermal study, lewis acid.

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### INTRODUCTION

Desulfurization is one of the chemical processes used to remove sulfur from raw materials in industry or final products. These processes are critical because they provide a large portion of the sulfur used in other fields and other sulfur-free materials to reduce toxic and polluting emissions to the environment, such as SO<sub>x</sub> emissions that cause acid rain (1-3). The fuel refining process necessarily requires the removal of sulfur from the oil hardships. The Environmental Protection Agency has imposed global restrictions on the specifications of the fuels used in transportation (EPA)(4). The optimum allowable sulfur content in diesel and gasoline is 15-30 ppm, which was previously 500 ppm in most countries, and is now being reduced to 10 ppm (5). Thus, one of the critical processes in oil refineries is the removal of sulfur from oil. The price of oil production is determined by the sulfur content, which influences the price of crude oil and processing costs (1, 6-8).

Ionic liquids (ILs) with a high distribution coefficient for sulfur compounds, a low cross solubility for hydrocarbons, a low viscosity, and a fast separation phase after mixing and extraction are ideal. Unfortunately, natural ionic fluids perform less efficiently in liquid-liquid extraction for typical sulfur compounds such as dibenzothiophene (DBT). However, ionic liquids have a high distribution coefficient. In mixtures, the distribution coefficient is somewhat low; in other words, liquids are not ideal solvents for extraction desulfurization, especially with heavy oil, and the (EDS) process efficiency is lower. Because oxidizing sulfur compounds have a much higher distribution coefficient, the efficiency of the ionic liquid extraction process increases if organic sulfur compounds have previously been oxidized to sulfoxides and sulfonates (9-11).

Desulfurization by extracting fuel with ionic liquids instead of conventional organic solvents is an exciting alternative to extremely clean diesel oils. The use of different ionic liquids have been investigated within (EDS) (cations such as



removal ratio was done by using absorption to create a standard calibration curve and determine the wavelength ( $\lambda_{\max} = 285 \text{ nm}$ ) at the highest absorption intensity, as shown in Figure 5. The percentage of sulfur removed was calculated through the following relationship:

$$S_{\text{removal}} \% = \frac{\text{Conc.i} - \text{Conc.t}}{\text{Conc.i}} \times 100$$

Where  $\text{Conc.i}$  = initial concentration of sulfur (1000 ppm) represented by concentration of organic sulfur compound (DBT),  $\text{Conc.t}$  = sulfur concentration at certain time in a specific conditions (DBT) concentration.

### Characterization and analysis data

Several physical and spectral methods were used; the  $^1\text{H-NMR}$  was investigated by Bruker Avance DPX 400 MHz using  $\text{DMSO-d}_6$  as solvent. Trio-1000 equipment was used for mass spectroscopy; the elemental analysis was investigated by Flash EA 1112 Series Thermo Electron Corporation. The FT\IR measured by JASCO Canvas 4200, Avanta 2.02 software for atomic absorption by SensAA GCB scientific equipment system. METTLER Toledo TGA\ DSC used for thermal analysis at 30-950 °C with a ramping heat rate of 10 °C/min under air, STARE evaluation software. The sulfur content was measured by Shimadzu UV-Vis 1800 spectrometer at ( $\lambda_{\max} = 285 \text{ nm}$ ). Table (1) shows some physical properties of prepared compounds.

**Table 1:** Some physical properties of prepared compounds.

No.	Compound	Conductivity*	m.p. °C	Color
1	[MMPip]I	100	85	Off white
2	[MMPip]I/FeCl <sub>3</sub>	90	70	Brown
3	[MMPip]I/2FeCl <sub>3</sub>	90	68	Dark brown
4	[MMPip]I/3FeCl <sub>3</sub>	90	68	Dark brown

\* Conductivity ( $\text{ohm}^{-1} \cdot \text{mol}^{-1} \cdot \text{cm}^2$ ) at (25 °C) and ( $10^{-3} \text{ M}$ ) by using water as solvent

## RESULTS AND DISCUSSION

### Characterization data

The characterization of the cation in the ionic liquids [MMPip]<sup>+</sup> by  $^1\text{H-NMR}$  ( $\text{DMSO-d}_6$ , 400 MHz):  $\delta 0.9409$  (3H-CH<sub>3</sub>, d,  $J = 11.52 \text{ Hz}$ ),  $\delta 1.6512$  (5H-CH<sub>2</sub>CH<sub>2</sub>, m),  $\delta 2.7547$  (3H-CH<sub>3</sub>, s),  $\delta 3.0718$  (4H-2CH<sub>2</sub>, m),  $\delta 8.2942$  (1H-NH, br).

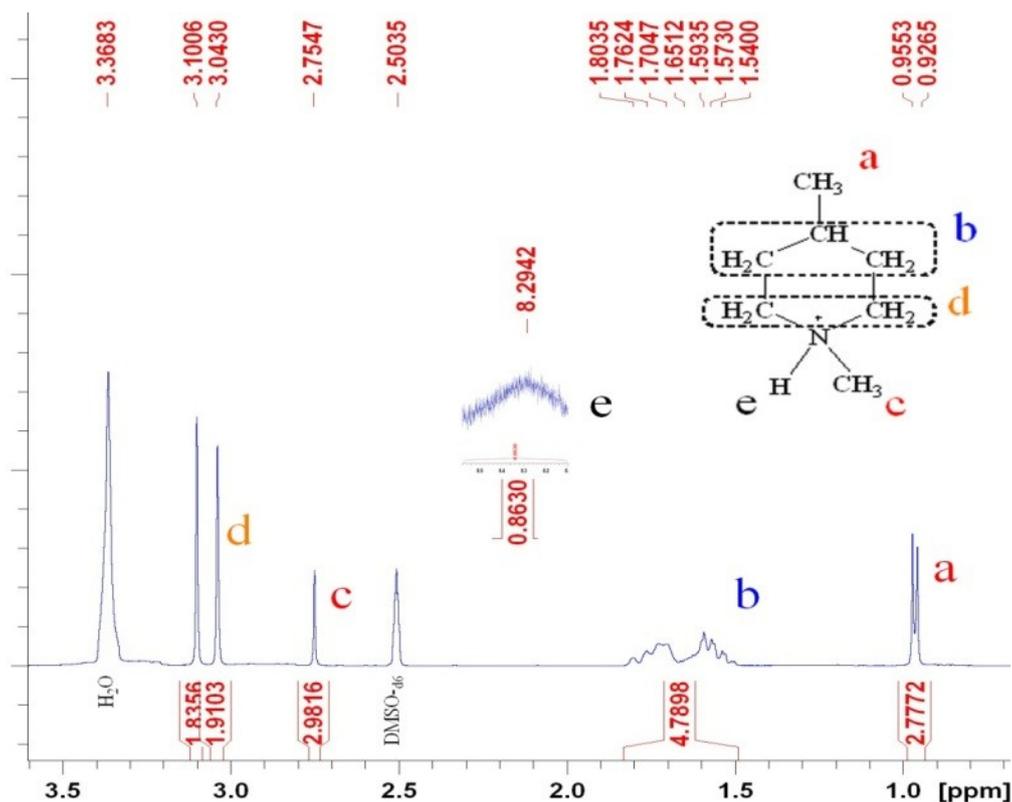
[MMPip]I (**1**) Anal. Calcd. for  $\text{C}_7\text{H}_{16}\text{IN}$ : C, 34.87; H, 6.69; N, 5.81. Found: C, 35.89; H, 6.84; N, 5.61.

[MMPip]I/FeCl<sub>3</sub> (**2**) Anal. Calcd. for  $\text{C}_7\text{H}_{16}\text{Cl}_3\text{FeIN}$ : C, 20.85; H, 4.00; Cl, 26.37; Fe, 13.85; N, 3.47.

Found: C, 19.25; H, 3.76; Cl, 27.66; Fe, 14.65; N, 3.22.

[MMPip]I/2FeCl<sub>3</sub> (**3**) Anal. Calcd. for  $\text{C}_7\text{H}_{16}\text{Cl}_6\text{Fe}_2\text{IN}$ : C, 14.87; H, 2.85; Cl, 37.61; Fe, 19.75; N, 2.48. Found: C, 13.05; H, 2.66; Cl, 39.05; Fe, 21.55; N, 2.22.

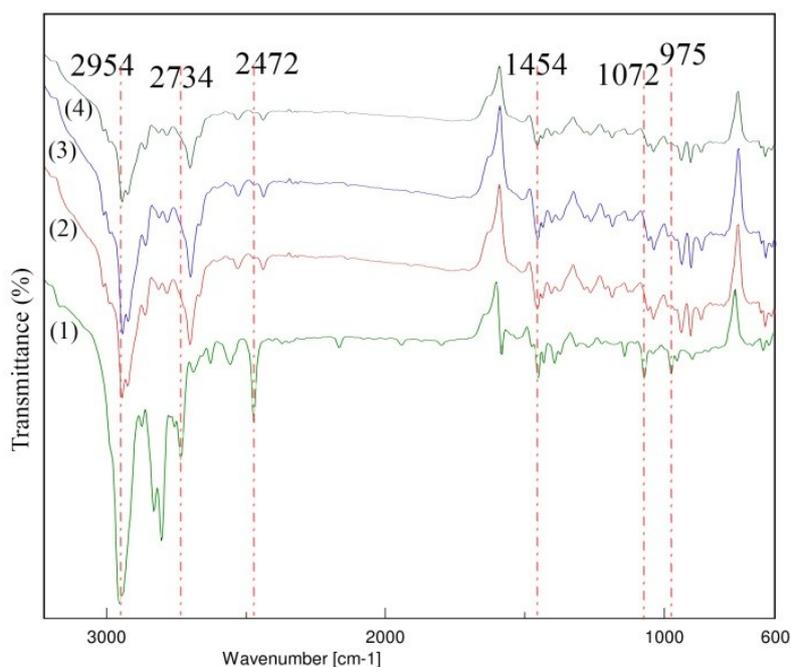
[MMPip]I/3FeCl<sub>3</sub> (**4**) Anal. Calcd. for  $\text{C}_7\text{H}_{16}\text{Cl}_9\text{Fe}_3\text{IN}$ : C, 11.55; H, 2.22; Cl, 43.84; Fe, 23.02; N, 1.92. Found: C, 9.75; H, 1.98; Cl, 42.76; Fe, 24.25; N, 1.75. Figure 1 shows the  $^1\text{H-NMR}$  of [MMPip]I (**1**).



**Figure 1:** The  $^1\text{H-NMR}$  of [MMPip]I (1) (400 MHz,  $\text{DMSO-d}_6$ ).

The infrared spectrum measured the ionic liquid (organic salt) and the ionic liquid mixture with  $\text{FeCl}_3$ . The results showed that the presence of Lewis acid makes slight displacements of some bands, and it may change the band's intensity (26-28). For example, a band appeared at  $975\text{ cm}^{-1}$  due to the in-plane bending frequency of the (C-H) group and is shifted to a lower position when ferric chloride is

present (20, 29). The bands observed at  $1072\text{ cm}^{-1}$ ,  $1454\text{ cm}^{-1}$  belong to (C-N str. or C-C str.) and (C-H, scissoring bending) respectively (20, 30). The other bands investigated are  $2472\text{ cm}^{-1}$  ( $\text{N}^+\text{-CH}_3$  str.),  $2734\text{ cm}^{-1}$  ( $\text{N}^+\text{-H}$  str.),  $2954\text{ cm}^{-1}$  (C-H symmetric str.). Figure 2 shows the IR spectra of ILs systems (20).



**Figure 2:** IR spectra of the IL systems: (1) [MMPip]I; (2) [MMPip]I/ $\text{FeCl}_3$ ; (3) [MMPip]I/ $2\text{FeCl}_3$ ; (4) [MMPip]I/ $3\text{FeCl}_3$ .

**Thermal study data**

The thermal stability of [MMPip]I and its mixtures with ferric chloride was studied. A noticeable decrease in the melting point of compounds containing ferric chloride was revealed. The study was under thermal conditions (30-950 °C) and a temperature rampage rate (15 °C/min). The results showed that the ionic liquid [MMPip]I is stable at temperatures up to 250 °C; as shown in Figure 3, the thermal degradation process occurs in one main

stage (21, 31, 32). Although the presence of ferric chloride increases the presence of moisture water in the compound, as the results showed, the moisture water loses by cycling to 110 °C. Thus, the [MMPip]I/nFeCl<sub>3</sub> compounds have two main stages of thermal degradation. However, all mixes are relatively stable at the temperature of experimental conditions of the process (EDS). Figure 4 shows the thermal gravimetric analysis of the compounds.

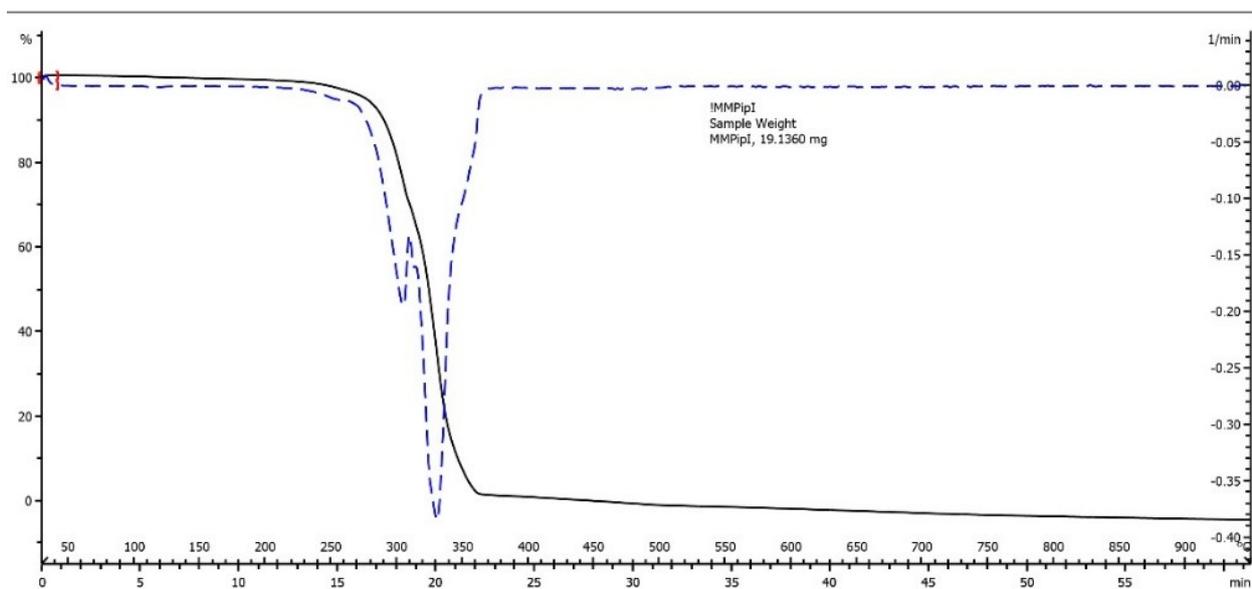


Figure 3: TGA and DTA of [MMPip]I.

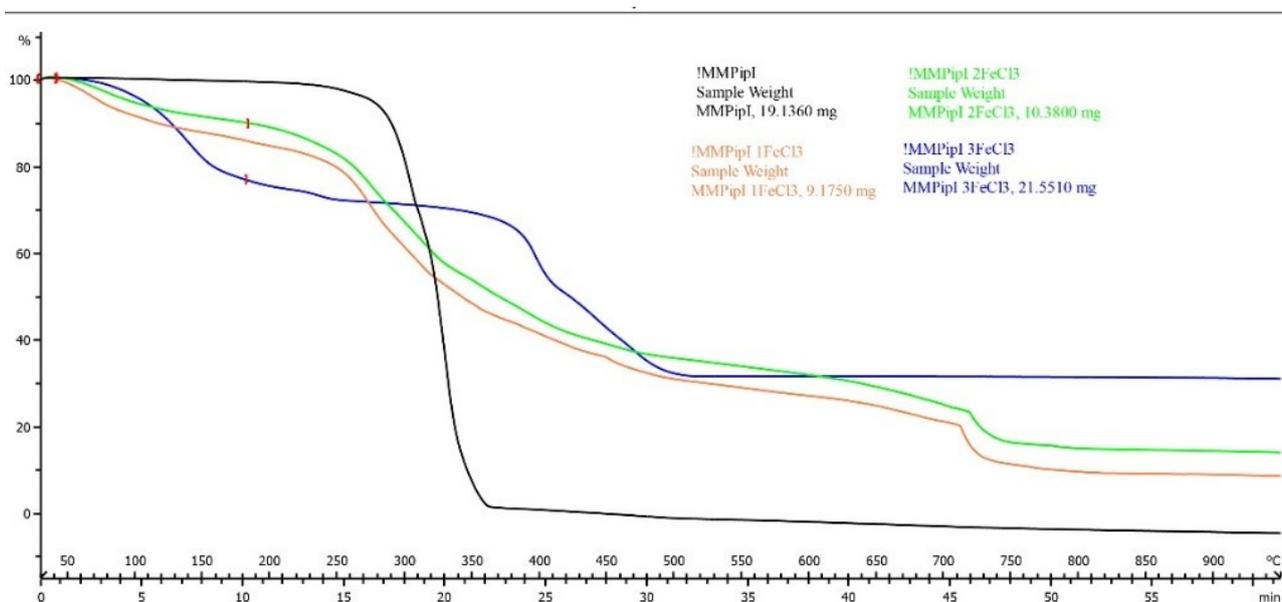


Figure 4: TGA analysis of [MMPip]I and its FeCl<sub>3</sub> mixtures.

**Data for desulfurization analysis**

Completing the standard curve by measuring the compound (DBT) absorbance for several standard

concentrations (250, 500, 750, and 1000 ppm), as shown in Figure 5.

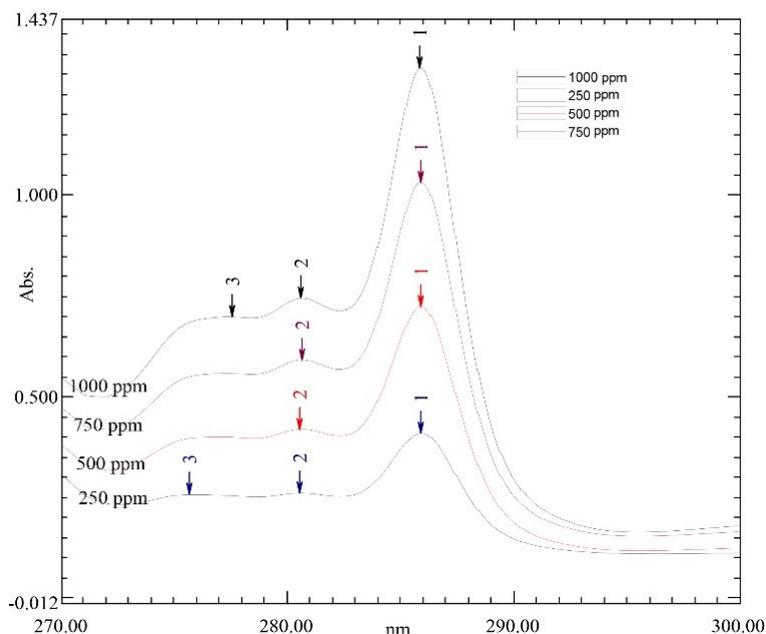


Figure 5: DBT absorbance with different concentrations.

The optimum conditions for the (EDS) process were determined by treating the model oil with prepared compounds for extraction at multiple temperatures (15, 30, 45 °C) using a fixed weight of the extracted materials (0.05 g) and 30 minutes. The results showed an increase in the removal efficiency with an increase in temperature. These results have good similarities to the literature (18, 20, 33), noting that there was no significant increase in efficiency when the temperature was increased from 30 °C to 45 °C, and it is preferable to use the laboratory temperature because it is more controllable, as shown in Figure 6. After stabilizing the temperature,

the optimum time was verified under 30 °C and using the weight of the extracted substance (0.05 g). The results showed that the removal process increases with the increase of time, which have slightly different from the literature (20), and there is no significant difference between 60 minutes and 90 minutes, as the equilibrium is almost stable after 60 minutes and as illustrated in Figure 7. Finally, the efficiency was tested using many different weights, as the results showed that with the increase in the amount of extracted material, the extraction efficiency increases Figure 8.

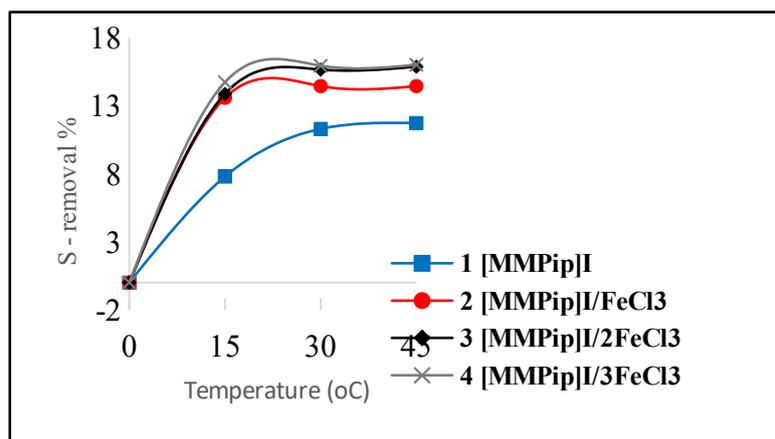
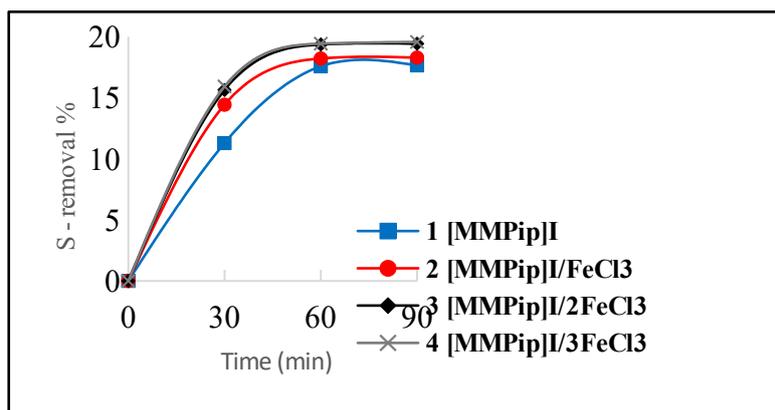
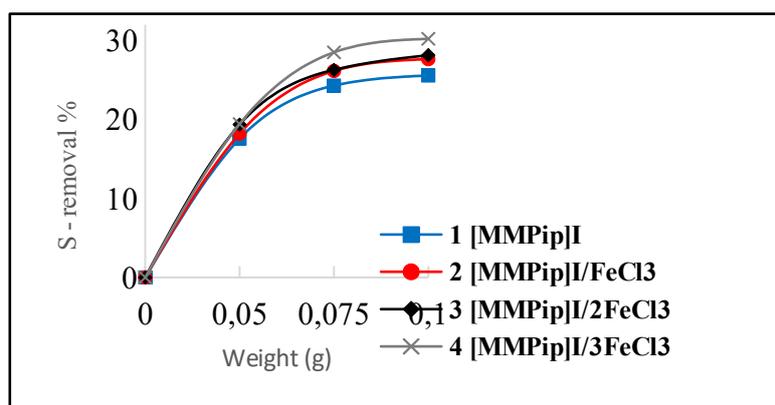


Figure 6: Effect of temperature: extractant used 0.05 g, 30 min.



**Figure 7:** Effect of time: extractant used 0.05 g, 30 °C.



**Figure 8:** Effect of extractant weight: 60 min, 30 °C.

Through these results, it is noted that the increase in temperature from 30 °C to 45 °C and the increase in the time for the extraction process after 60 minutes does not significantly affect the efficiency of the extraction process, while the increase in the weight of the extracted material (ionic liquid or ionic liquid containing Lewis acid) is more considerable and more clearly. By comparing the results, we find that the highest percentage of sulfur removal is when using 0.1 g of compound (I), which is rather good when compared to efficiency results of up to 100%, but by using high amounts of the extracted substance to the oil model (18, 20). It also noted that the efficiency of the removal ratio increases with the increase in the ratio of ferric chloride to the ionic liquid, which is consistent with the published research (19, 34, 35).

The proposed mechanism for the extraction of organic sulfur compounds is through the interactions between the  $n$  electrons of organic sulfur compounds (DBT) with  $n$  electrons of the ionic liquid and their interaction with the metallic element in Lewis acid (36, 37). The results showed that ionic liquid mixed with Lewis acid has a higher extraction efficiency than the ionic liquid alone and higher than the use of Lewis acid alone, and the extraction process is more selective for aromatic sulfur compounds (17, 20, 21).

## CONCLUSION

The pyridinium base's ionic liquid and salt were prepared with ferric chloride as Lewis acid, and their efficiency was tested in extracting the organic sulfur compounds from the petroleum model. It was found that the best extraction factor among the compounds used is [MMPip]I/3FeCl<sub>3</sub>, where the percentage of sulfur removal from the oil model was (30%) under the optimal conditions (10 mL of model oil of 1000 ppm DBT, 0.1 g of extractant, 60 min at 30 °C). Compared with the previous work, these results are considered promising due to the use of acceptable quantities of the extracted agent relative to the quantity of the oil model used. It also noticed that the extraction efficiency increased with the increase in Lewis acid (ferric chloride) ratio to the ionic liquid under the same experimental conditions for the extraction process.

## ACKNOWLEDGEMENT

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## Extractive Desulfurization Using Piperidinium Based Ionic Liquids with Lewis Acids

Assim A. Sabah<sup>1\*</sup>

### Supporting Information

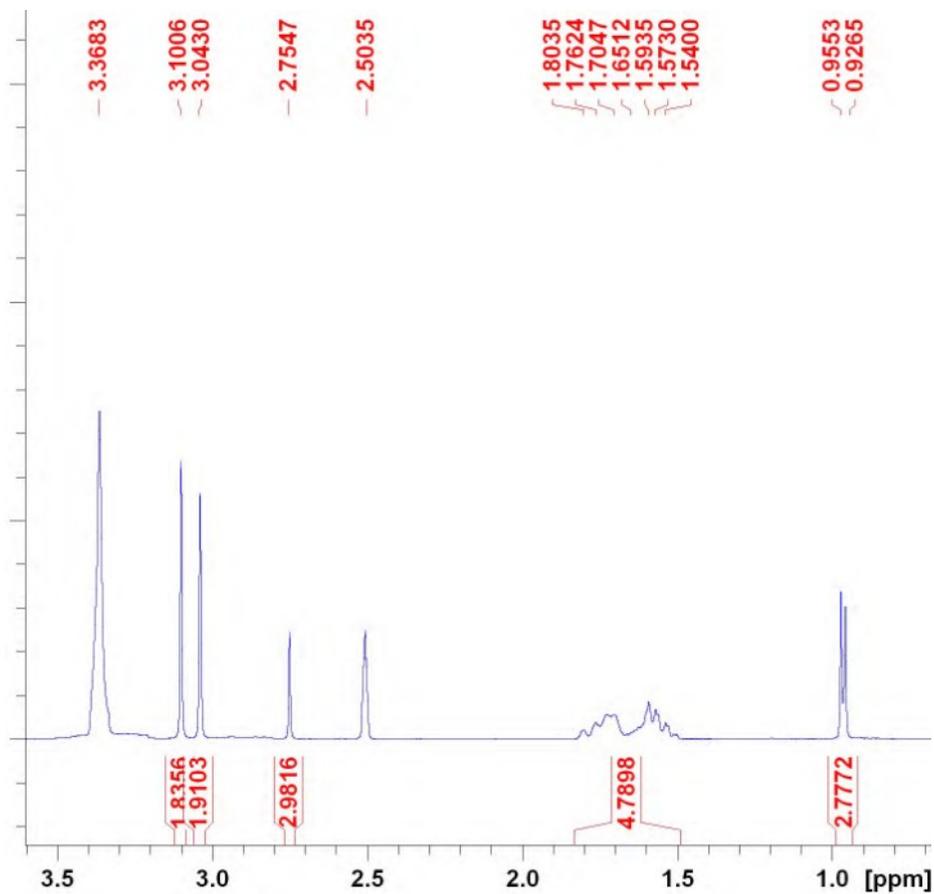


Figure S1: <sup>1</sup>H-NMR of [MMPip]I ionic liquids.

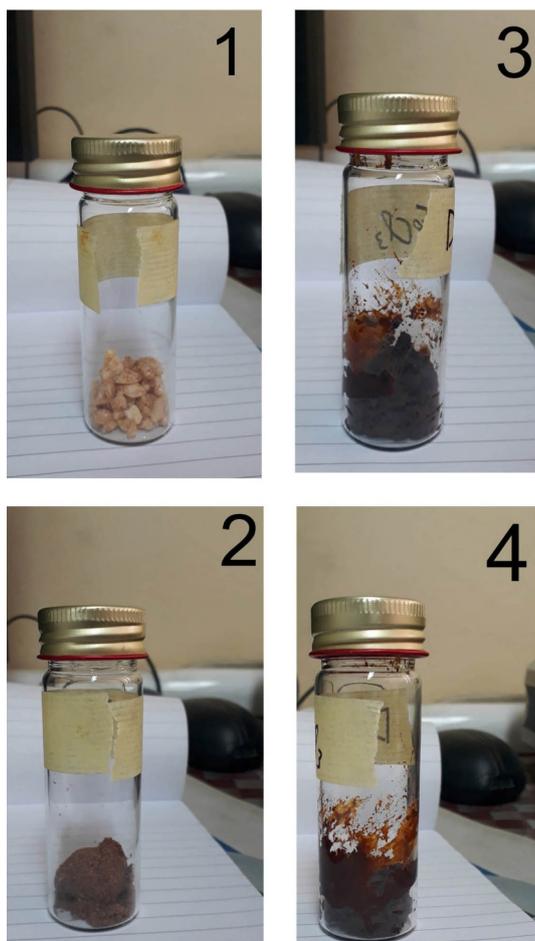


Figure S2: Pictures of the prepared compounds.

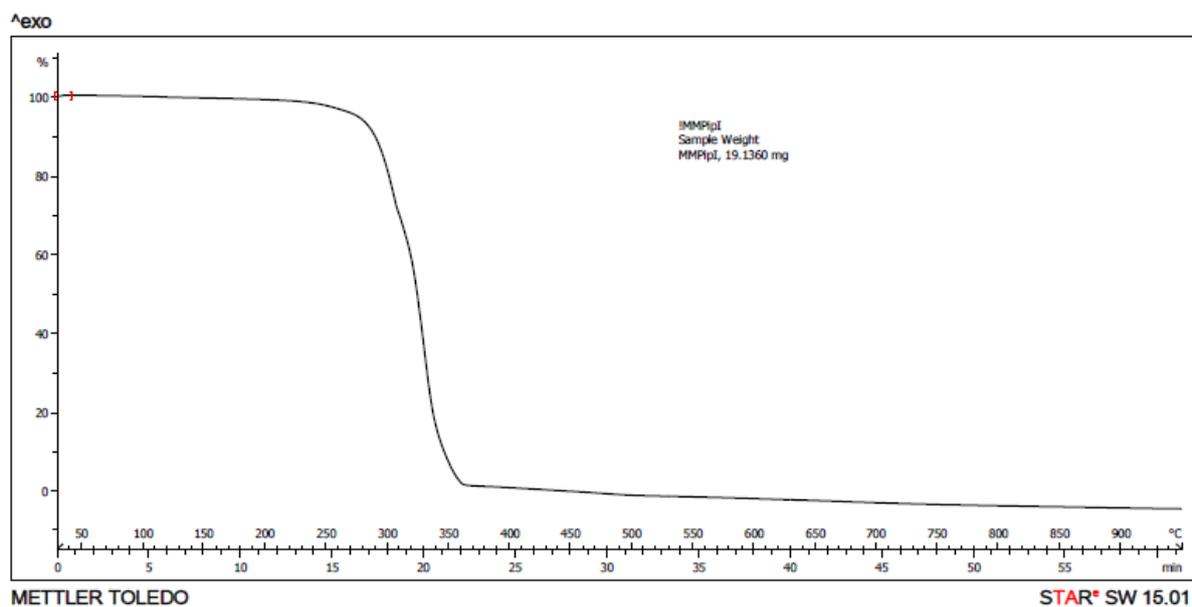


Figure S3: TGA analyses of [MMPip]I ionic liquids.

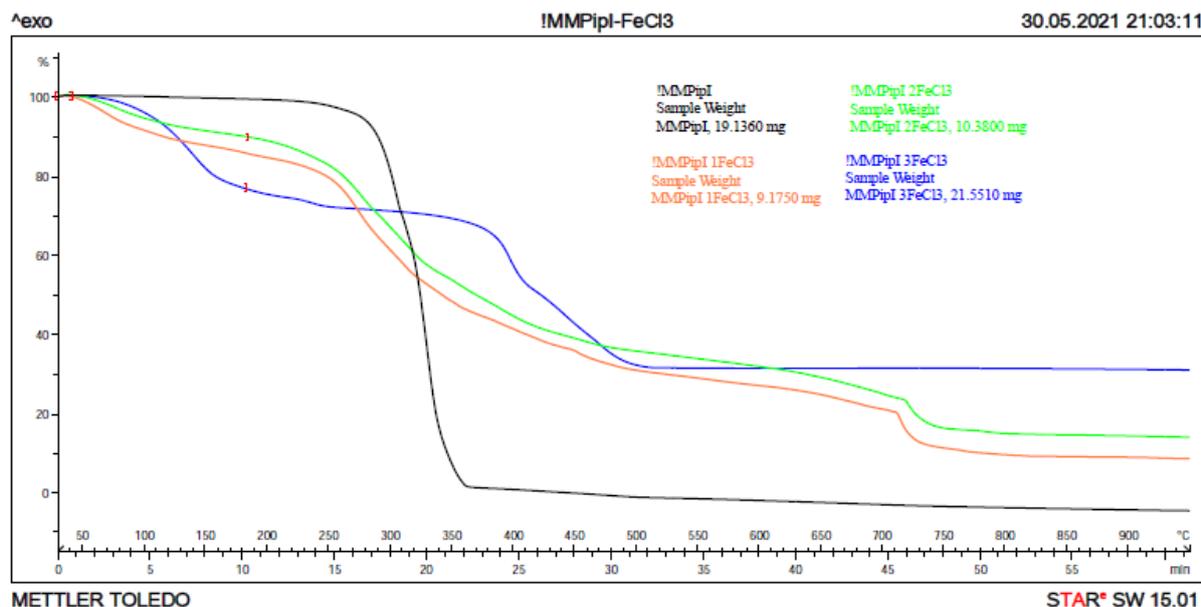


Figure S4: TGA analysis of prepared compounds.

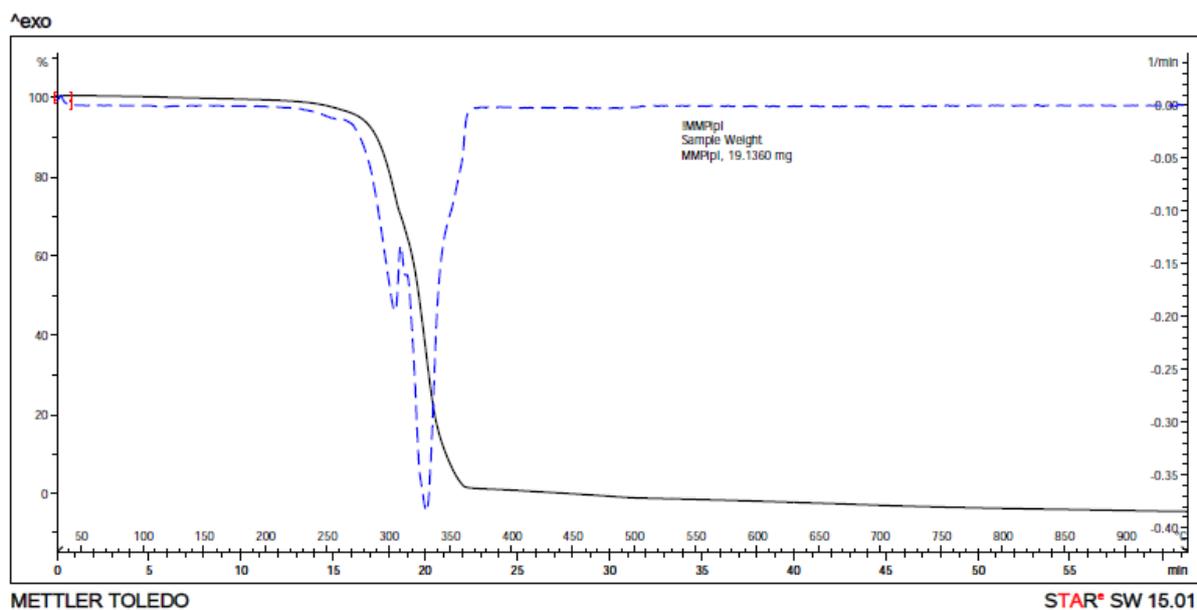


Figure S5: TGA and DTA analyses of [MMPip]I ionic liquids.

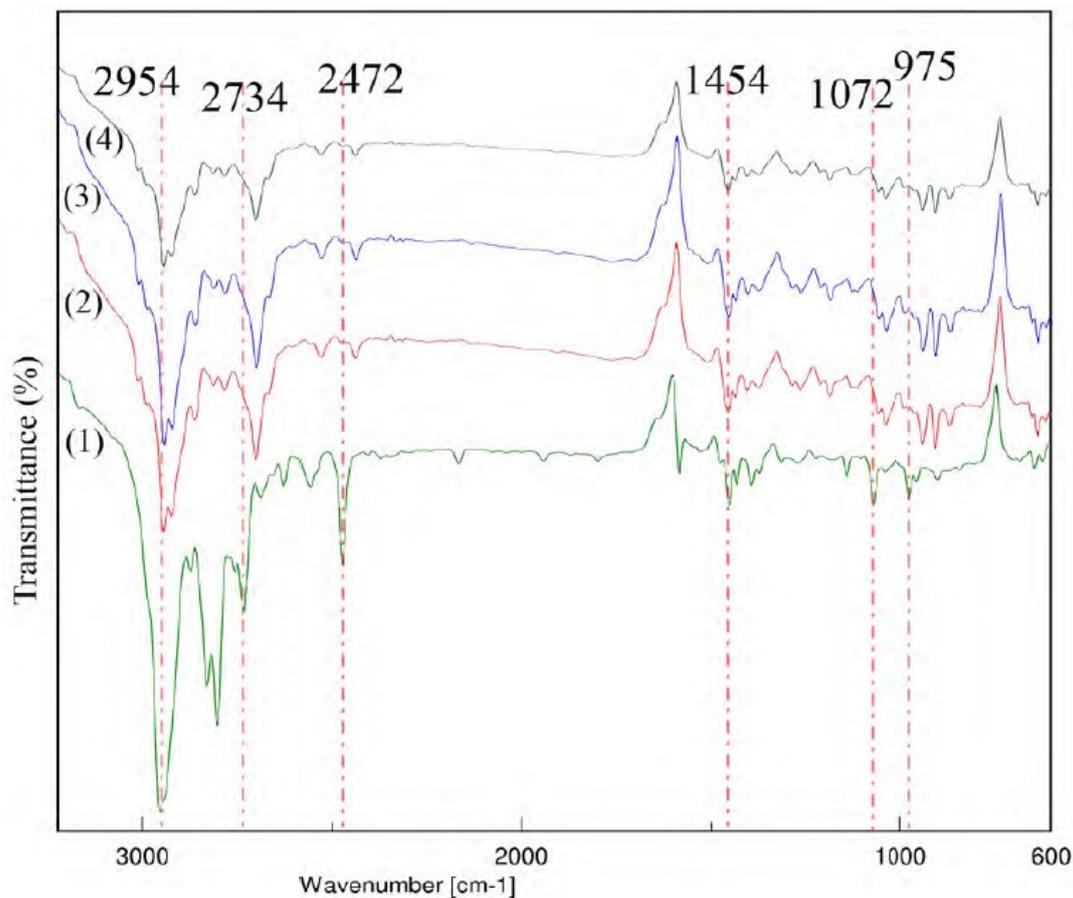


Figure S6: FT-IR spectrum of prepared compounds.

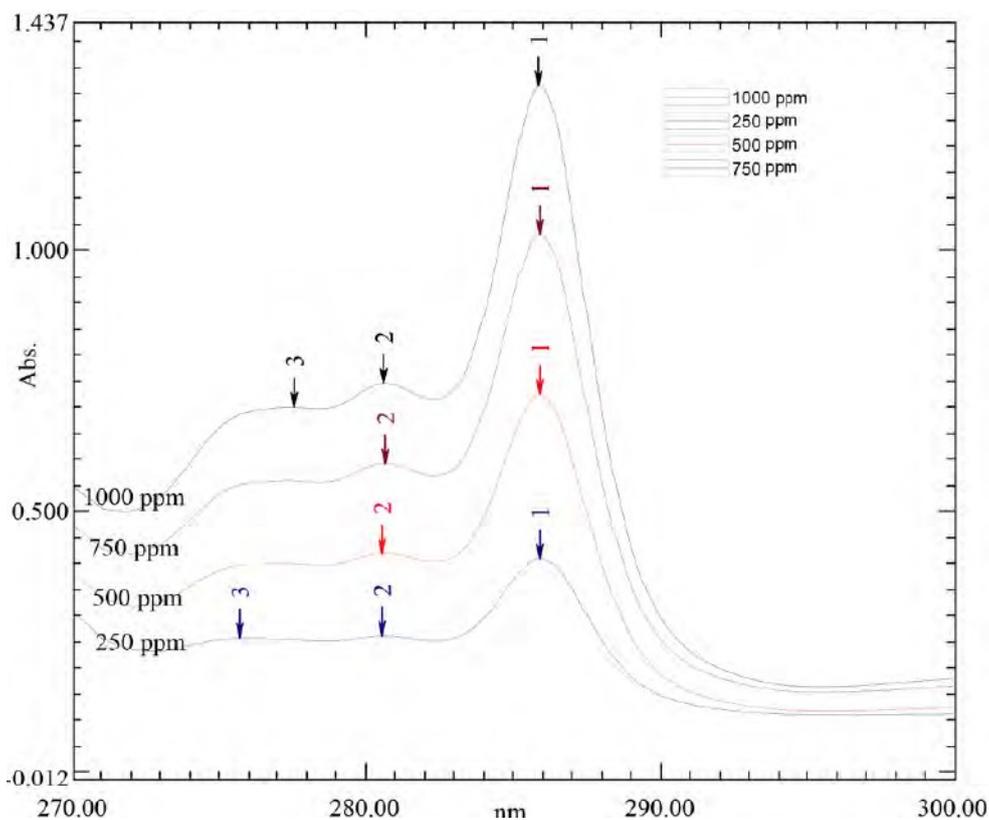
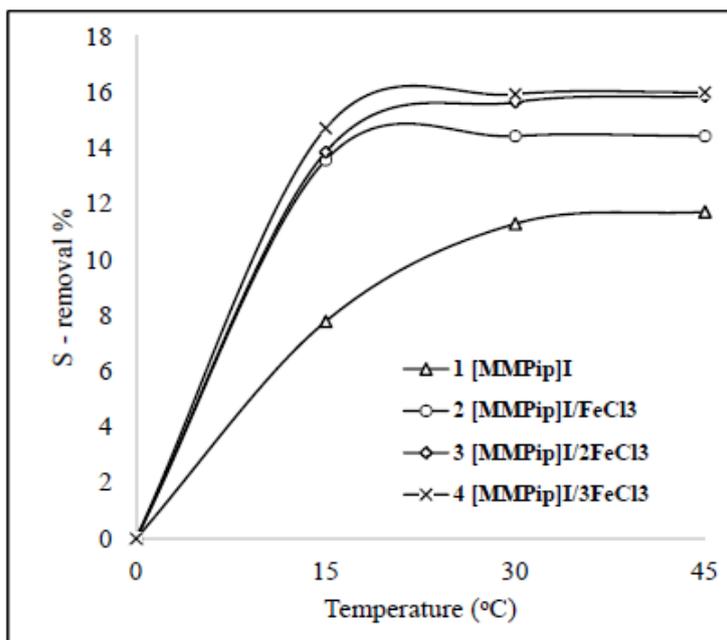
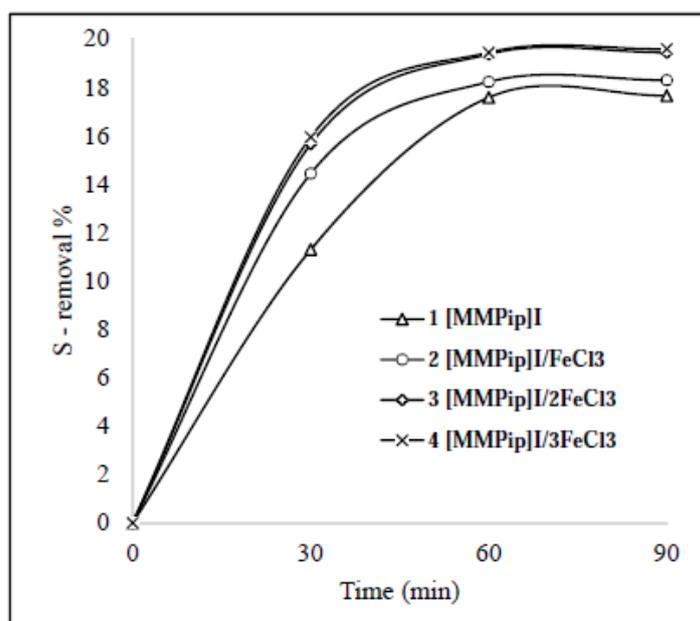


Figure S7: Calibration curve standard solutions spectrum.



**Figure S8:** Effect of temperature: extractant used 0.05 g, 30 min.



**Figure S9:** Effect of time: extractant used 0.05g, 30 °C.

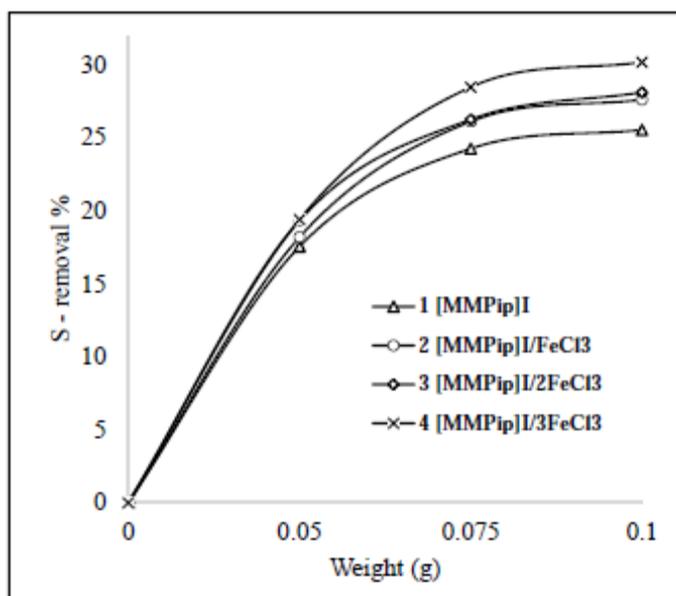


Figure S10: Effect of extractant weight: 60 min, 30 °C.

Data Set: 250 - RawData

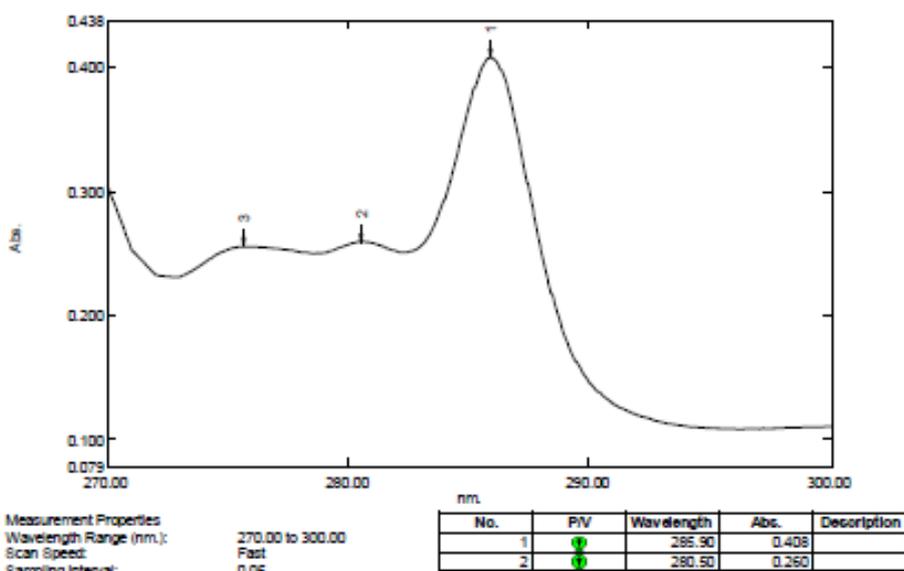


Figure S11: UV- Spectrum peak pick report of 250 ppm of DBT stranded solution.

Data Set 500 - RawData

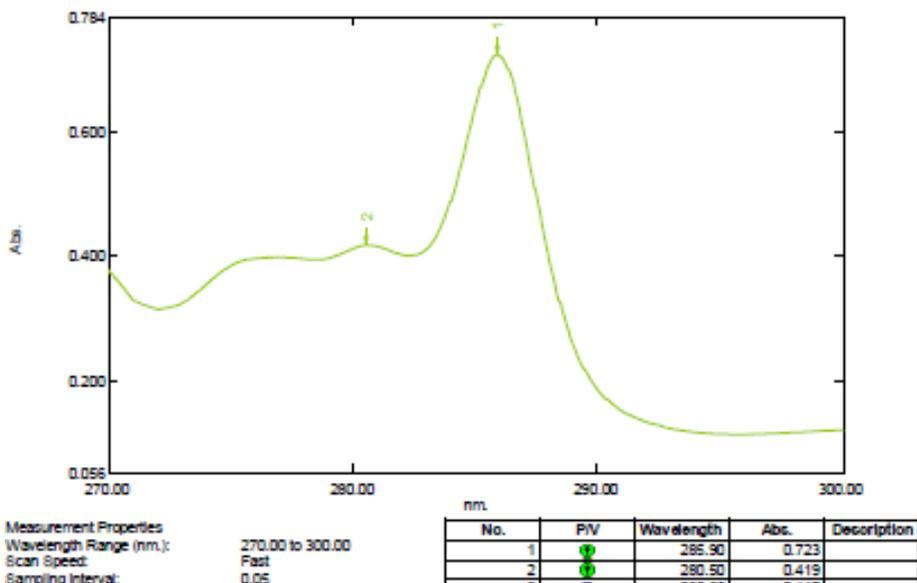


Figure S12: UV- Spectrum peak pick report of 500 ppm of DBT stranded solution.

Data Set 750 - RawData

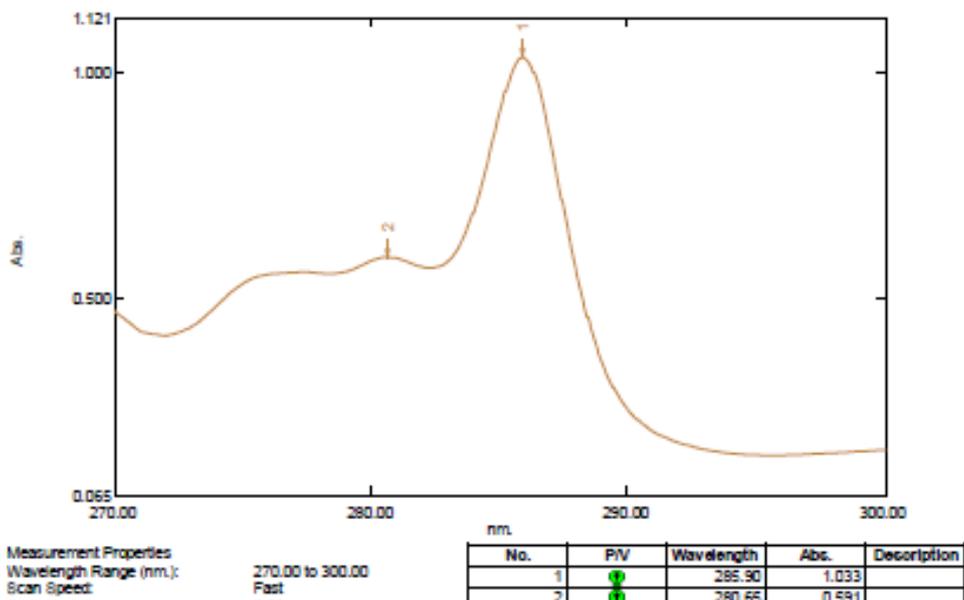


Figure S13: UV- Spectrum peak pick report of 750 ppm of DBT stranded solution.

Data Set: 1000 - RawData

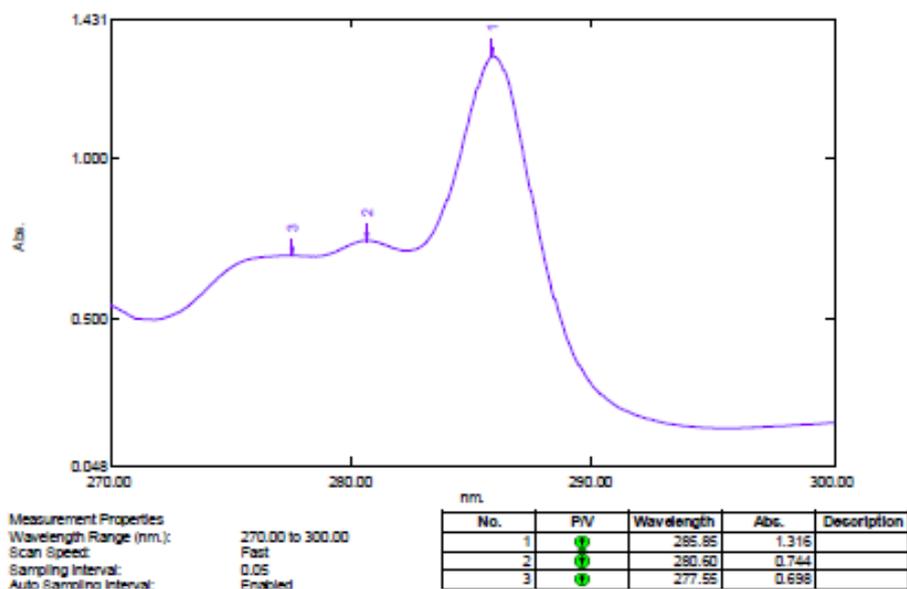


Figure S14: UV- Spectrum peak pick report of 1000 ppm of DBT stranded solution.

Data Set: 001- 1- 15c- 0.05g- 30 min - RawData

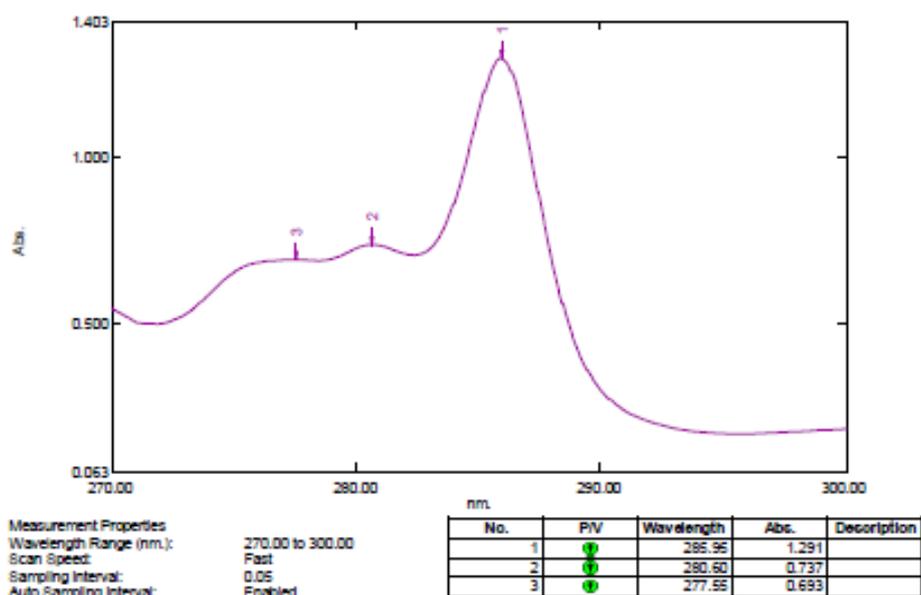
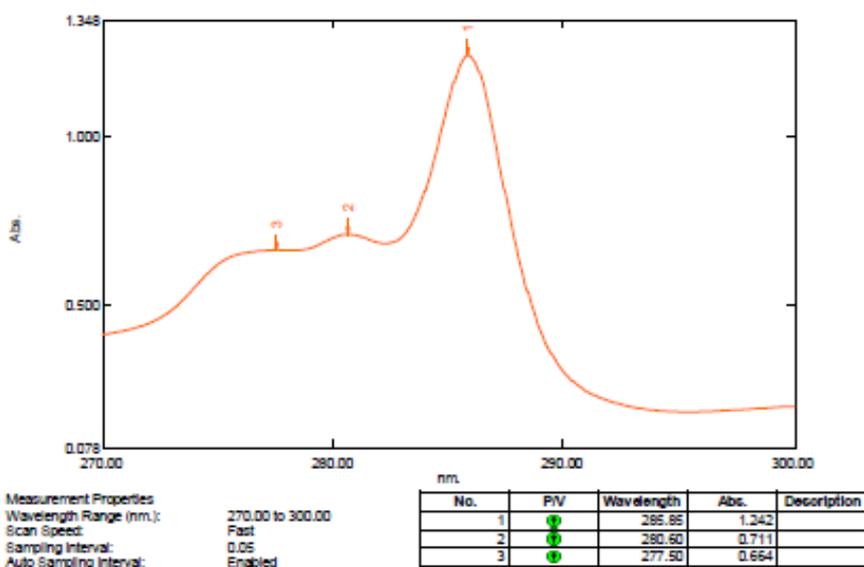


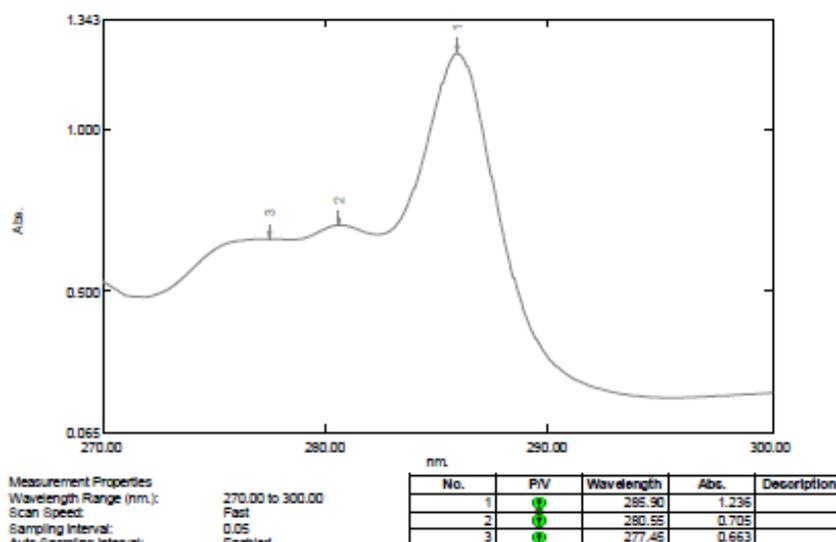
Figure S15: UV- Spectrum peak pick report of extractive desulfurization condition: extractant (1), at 15 °C, weight of extractant 0.05 g, time = 30 min.

Data Set 002- 1- 30c- 0.05g- 30 min - RawData

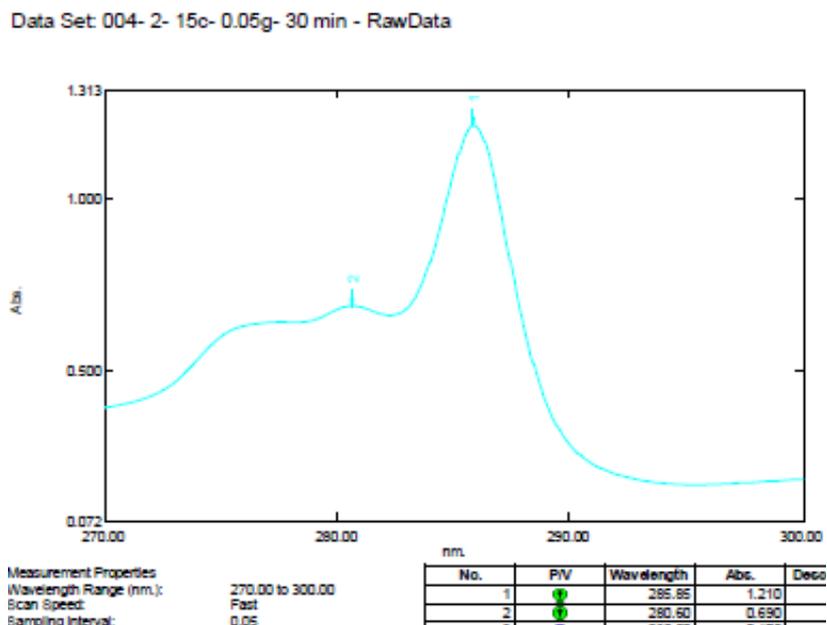


**Figure S16:** UV- Spectrum peak pick report of extractive desulfurization condition: extractant (1), at 30 °C, weight of extractant 0.05 g, time = 30 min.

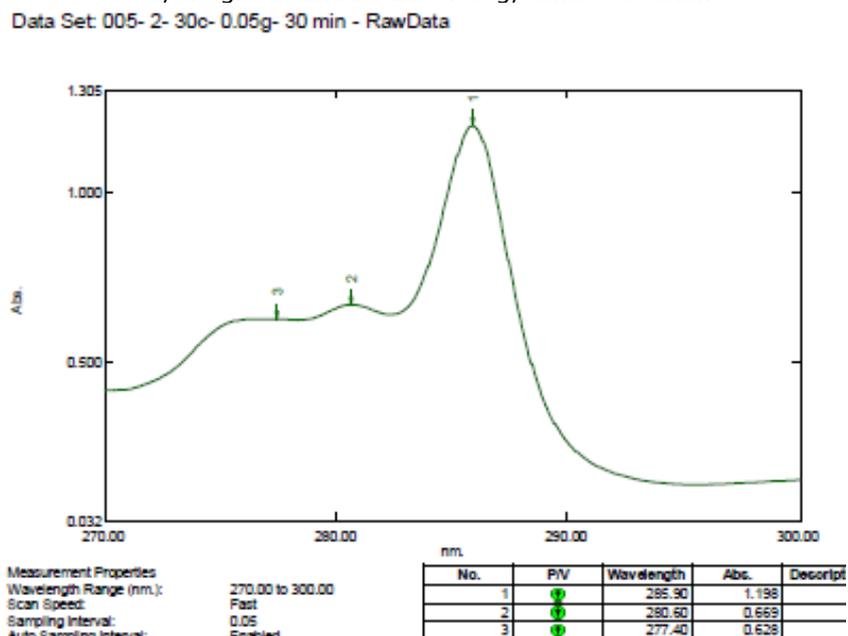
Data Set 003- 1- 45c- 0.05g- 30 min - RawData



**Figure S17:** UV- Spectrum peak pick report of extractive desulfurization condition: extractant (1), at 45 °C, weight of extractant 0.05 g, time = 30 min.



**Figure S18:** UV- Spectrum peak pick report of extractive desulfurization condition: extractant (2), at 15 °C, weight of extractant 0.05 g, time = 30 min.



**Figure S19:** UV- Spectrum peak pick report of extractive desulfurization condition: extractant (2), at 30 °C, weight of extractant 0.05 g, time = 30 min.

Data Set 006- 2- 45c- 0.05g- 30 min - RawData

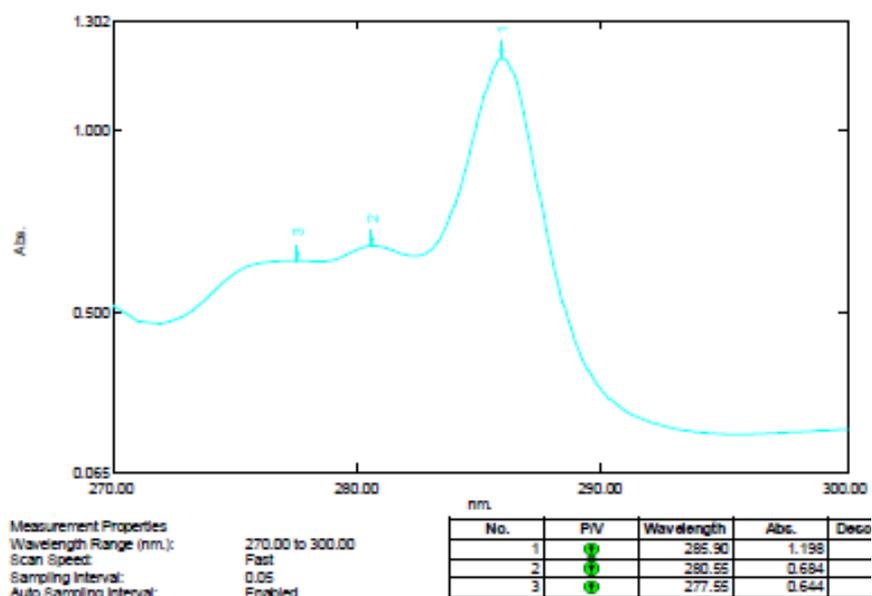


Figure S20: UV- Spectrum peak pick report of extractive desulfurization condition: extractant (2), at 45 °C, weight of extractant 0.05 g, time = 30 min.

Data Set 007- 3- 15c- 0.05g- 30 min - RawData

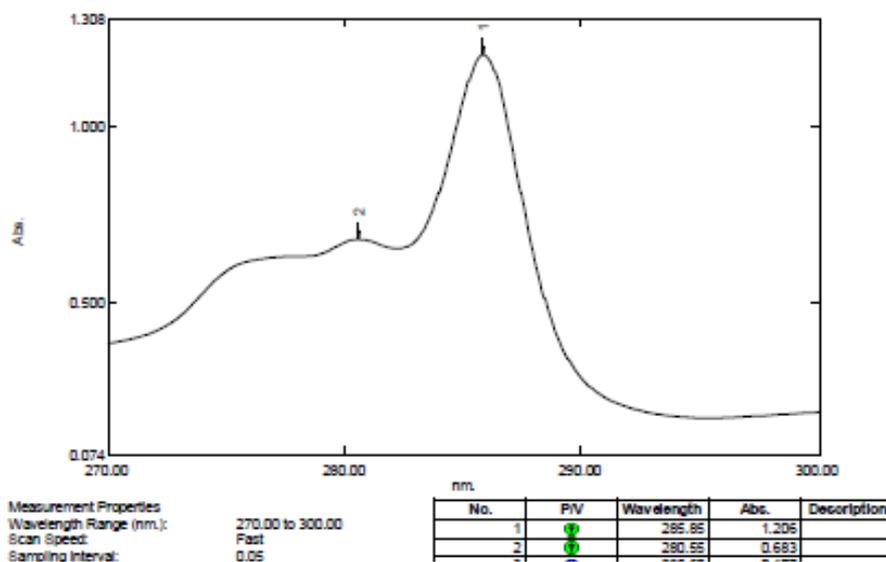
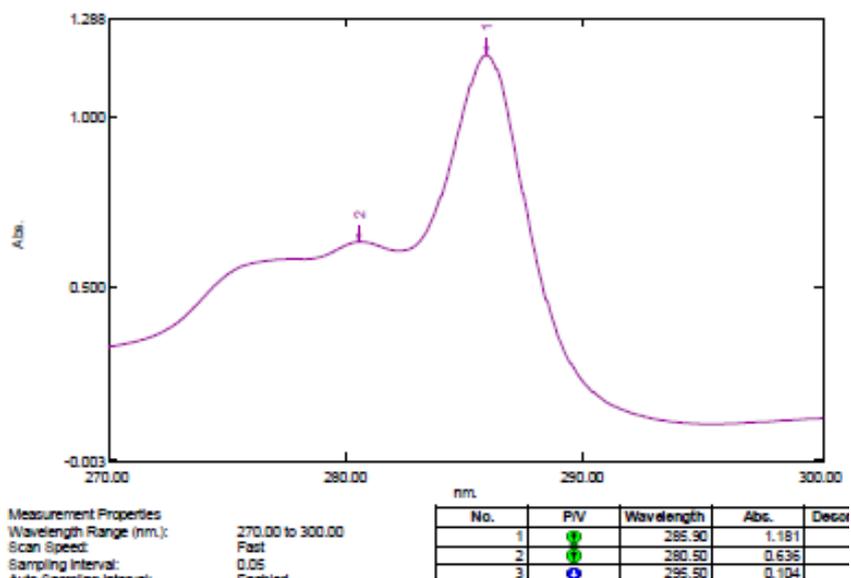


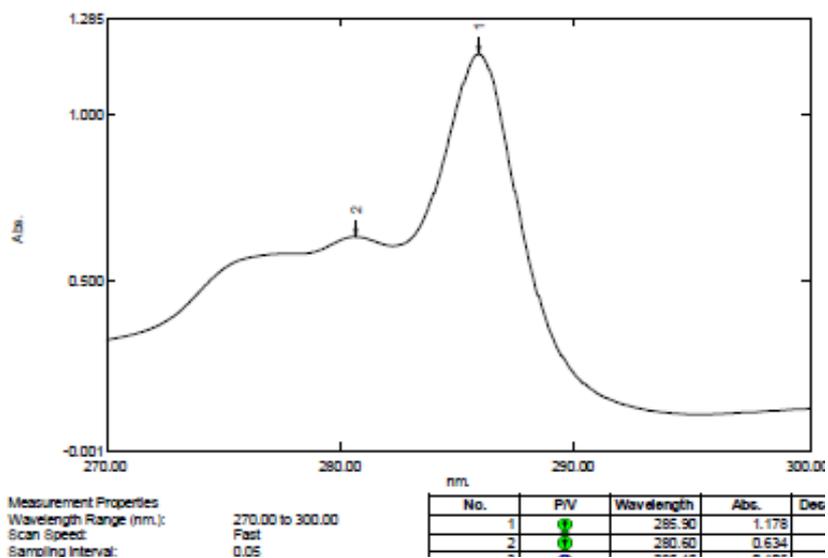
Figure S21: UV- Spectrum peak pick report of extractive desulfurization condition: extractant (3), at 15 °C, weight of extractant 0.05 g, time = 30 min.

Data Set 008- 3- 30c- 0.05g- 30 min - RawData

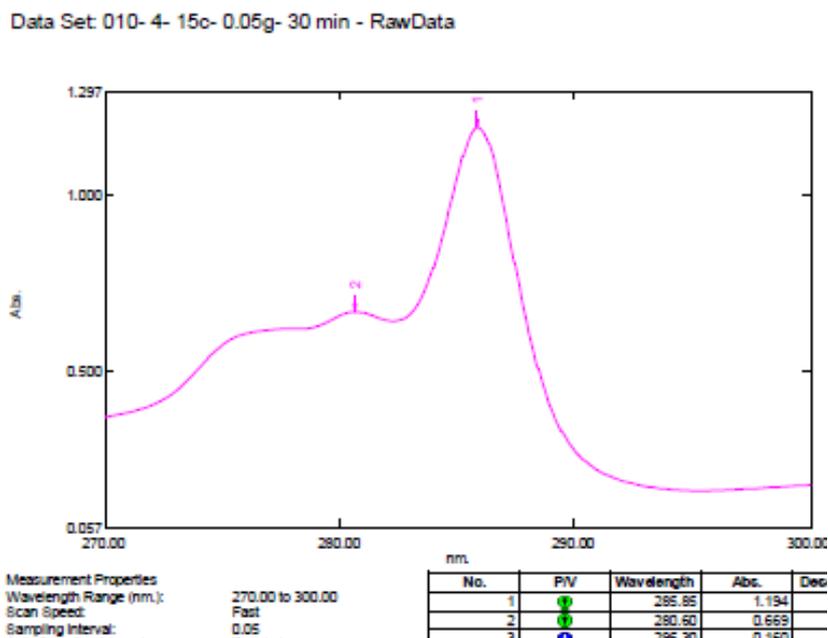


**Figure S22:** UV- Spectrum peak pick report of extractive desulfurization condition: Extractant (3), at 30 °C, weight of extractant 0.05 g, time = 30 min.

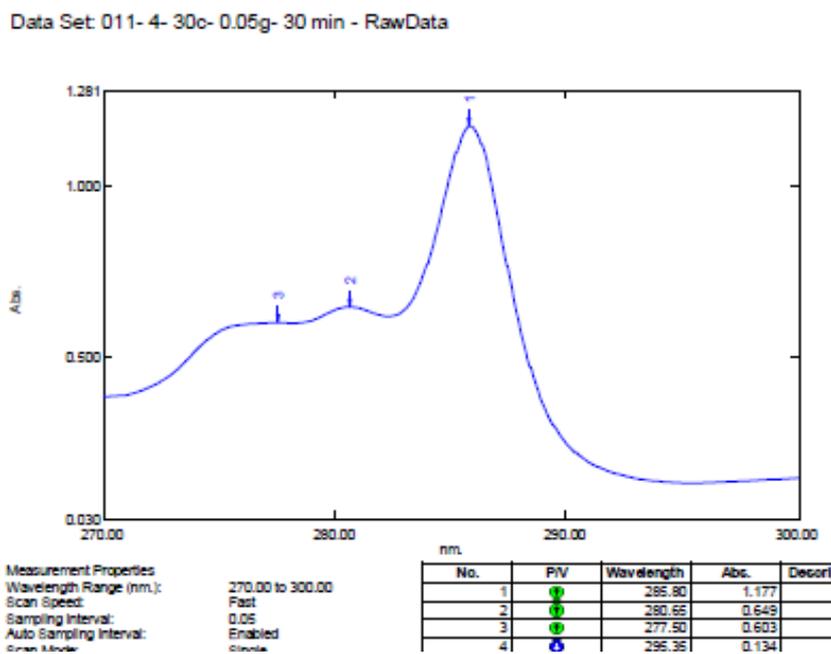
Data Set 009- 3- 45c- 0.05g- 30 min - RawData



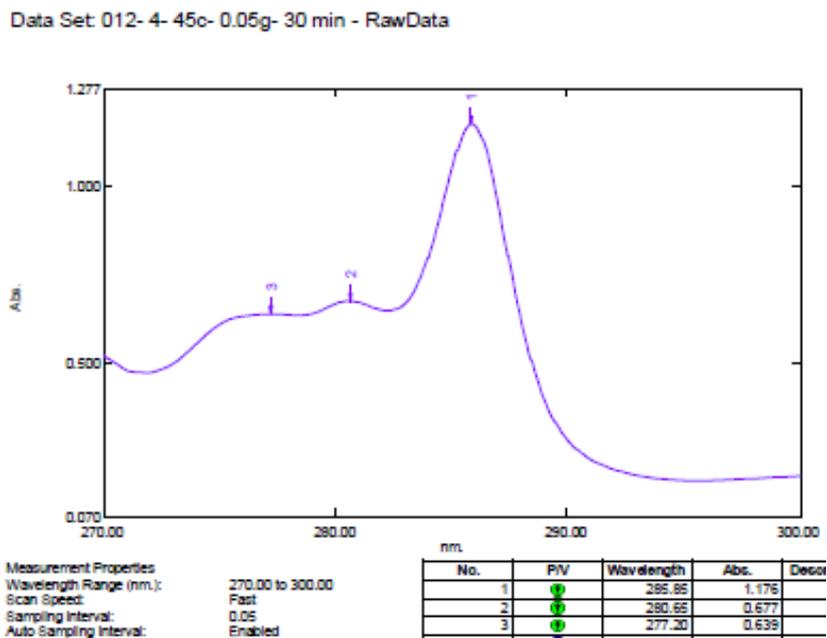
**Figure S23:** UV- Spectrum peak pick report of extractive desulfurization condition: extractant (3), at 45 °C, weight of extractant 0.05 g, time = 30 min.



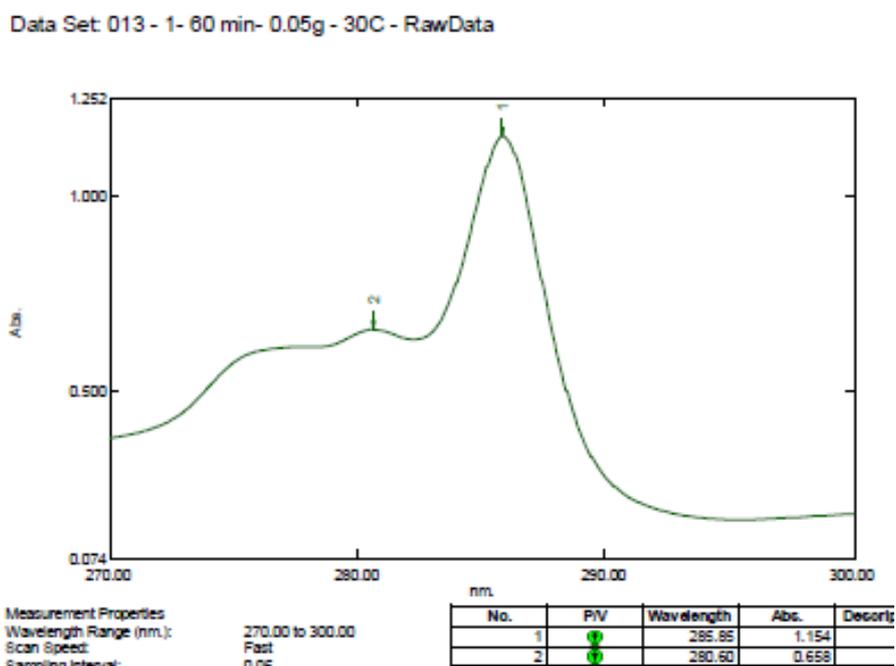
**Figure S24:** UV- Spectrum peak pick report of extractive desulfurization condition: extractant (4), at 15 °C, weight of extractant 0.05 g, time = 30 min.



**Figure S25:** UV- Spectrum peak pick report of extractive desulfurization condition: extractant (4), at 30 °C, weight of extractant 0.05 g, time = 30 min.

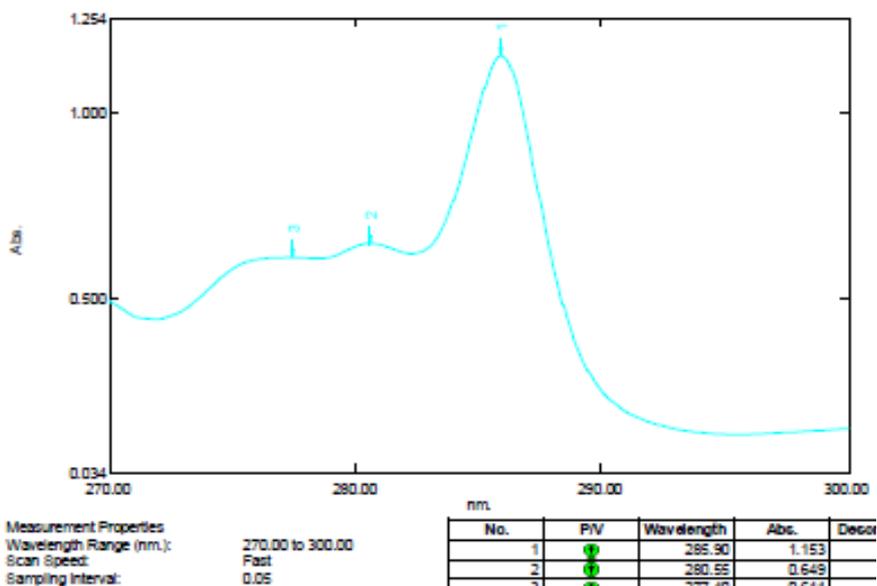


**Figure S26:** UV- Spectrum peak pick report of extractive desulfurization condition: extractant (4), at 45 °C, weight of extractant 0.05 g, time = 30 min.



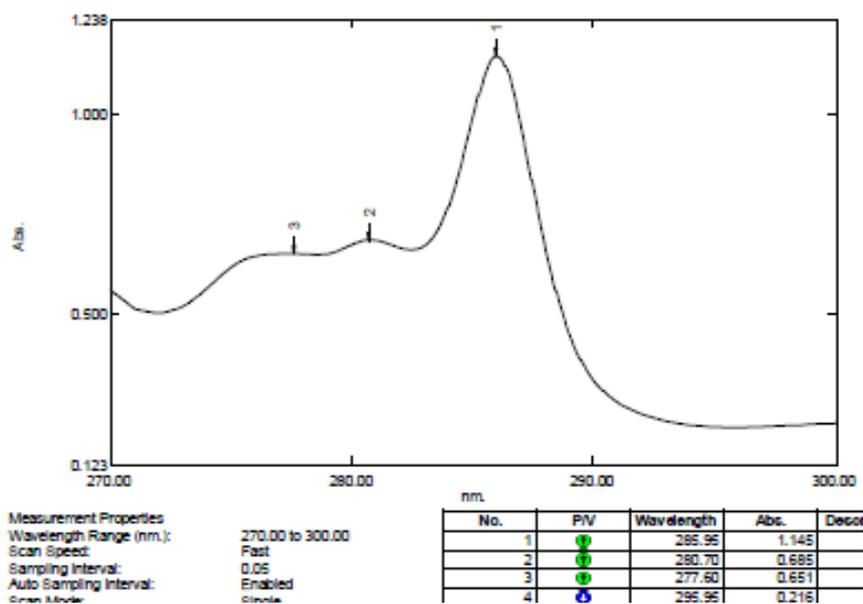
**Figure S27:** UV- Spectrum peak pick report of extractive desulfurization condition: extractant (1), at 30 °C, weight of extractant 0.05 g, time = 60 min.

Data Set: 014 - 1- 90 min- 0.05g - 30C - RawData



**Figure S28:** UV- Spectrum peak pick report of extractive desulfurization condition: extractant (1), at 30 °C, weight of extractant 0.05 g, time = 90 min.

Data Set: 015 - 2- 60 min- 0.05g - 30C - RawData



**Figure S29:** UV- Spectrum peak pick report of extractive desulfurization condition: extractant (2), at 30 °C, weight of extractant 0.05 g, time = 60 min.

Data Set 016 - 2- 90 min- 0.05g - 30C - RawData

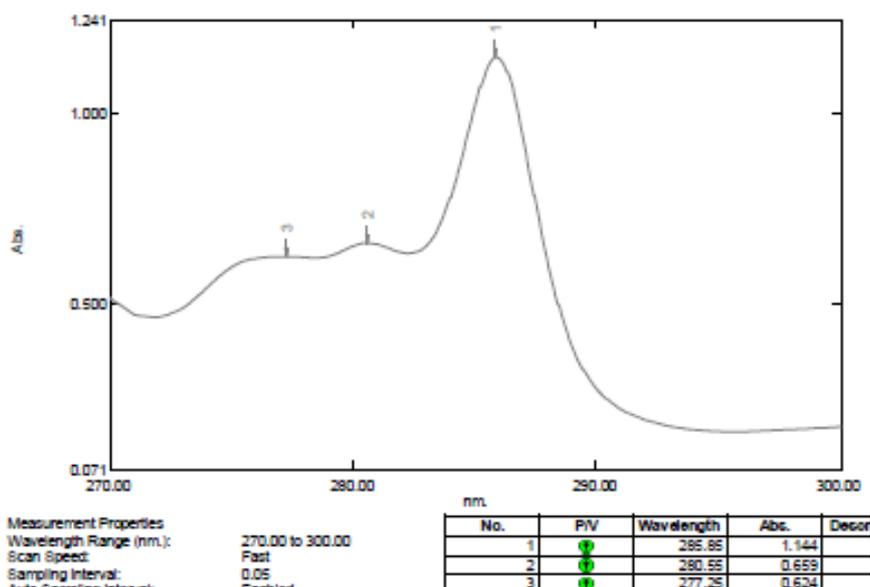


Figure S30: UV- Spectrum peak pick report of extractive desulfurization condition: extractant (2), at 30 °C, weight of extractant 0.05 g, time = 90 min.

Data Set 017 - 3- 60 min- 0.05g - 30C - RawData

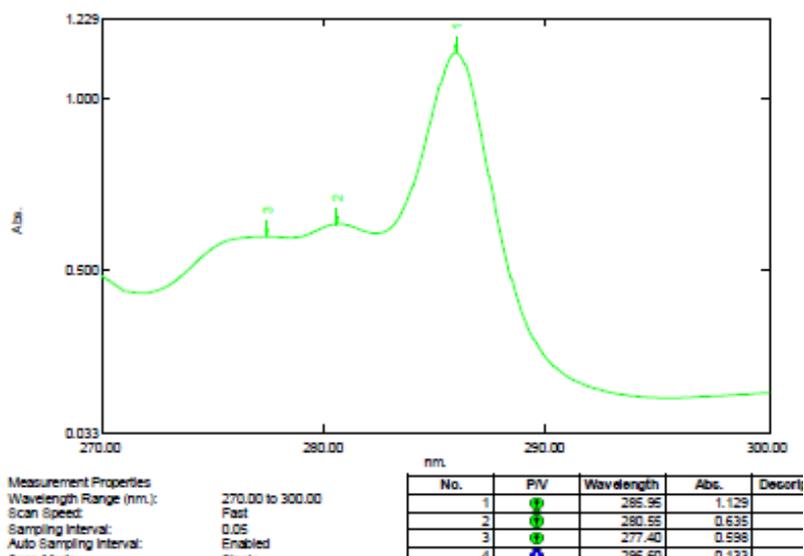
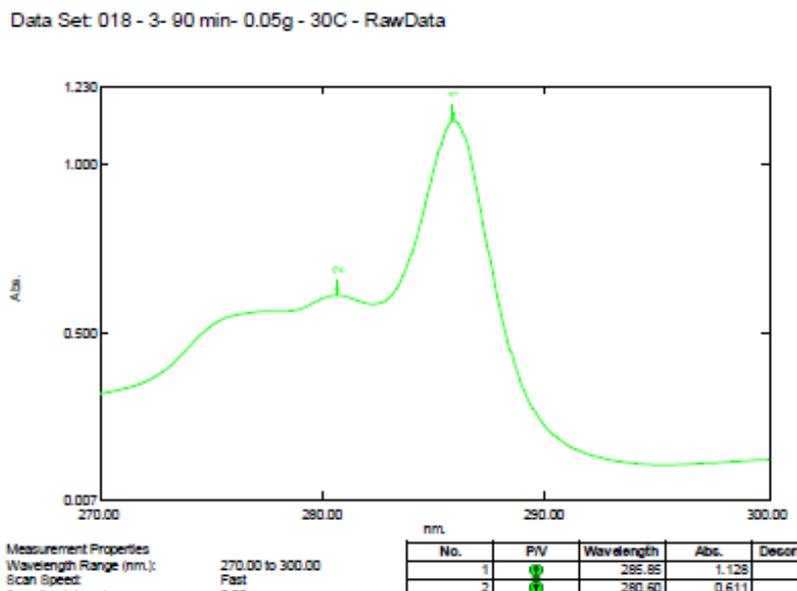
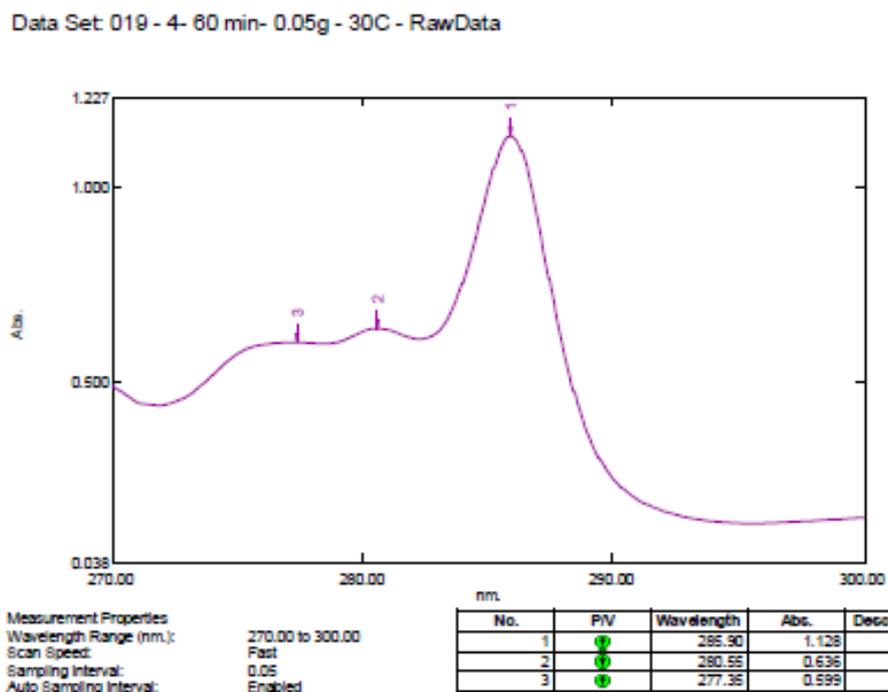


Figure S31: UV- Spectrum peak pick report of extractive desulfurization condition: extractant (3), at 30 °C, weight of extractant 0.05 g, time = 60 min.

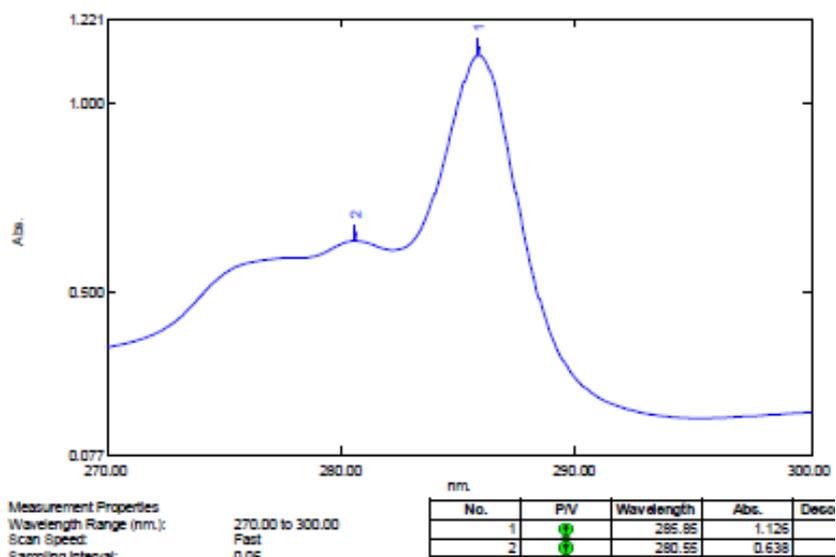


**Figure S32:** UV- Spectrum peak pick report of extractive desulfurization condition: extractant (3), at 30 °C, weight of extractant 0.05 g, time = 90 min.



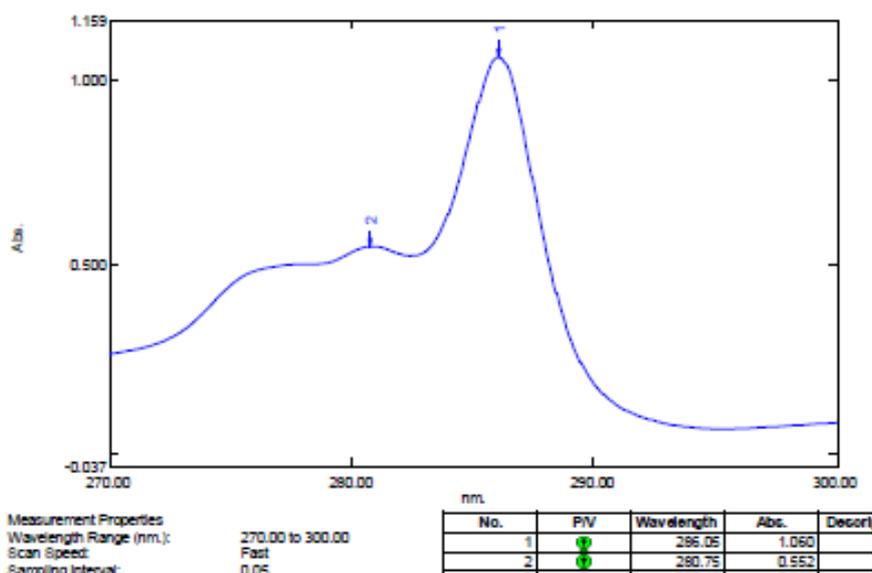
**Figure S33:** UV- Spectrum peak pick report of extractive desulfurization condition: extractant (4), at 30 °C, weight of extractant 0.05 g, time = 60 min.

Data Set 020 - 4- 90 min- 0.05g - 30C - RawData

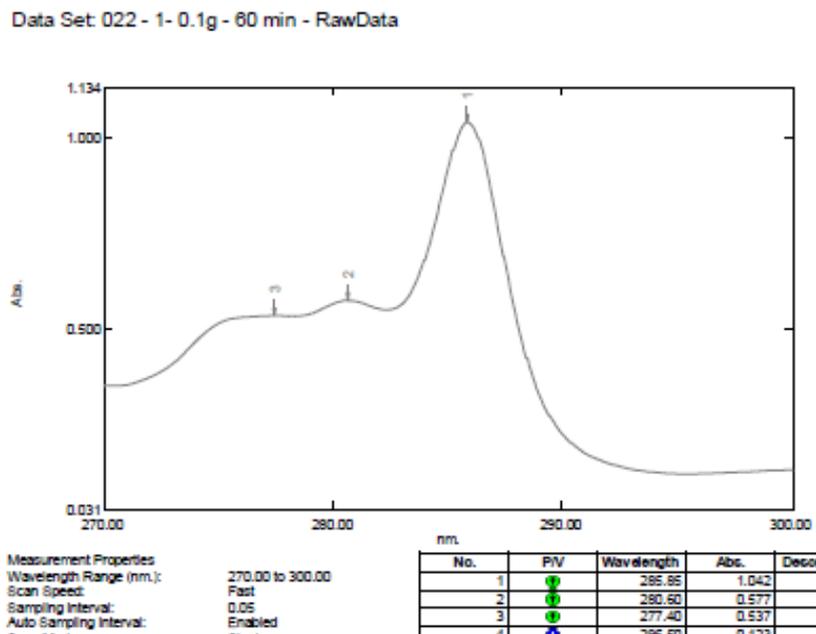


**Figure S34:** UV- Spectrum peak pick report of extractive desulfurization condition: extractant (4), at 30 °C, weight of extractant 0.05 g, time = 90 min.

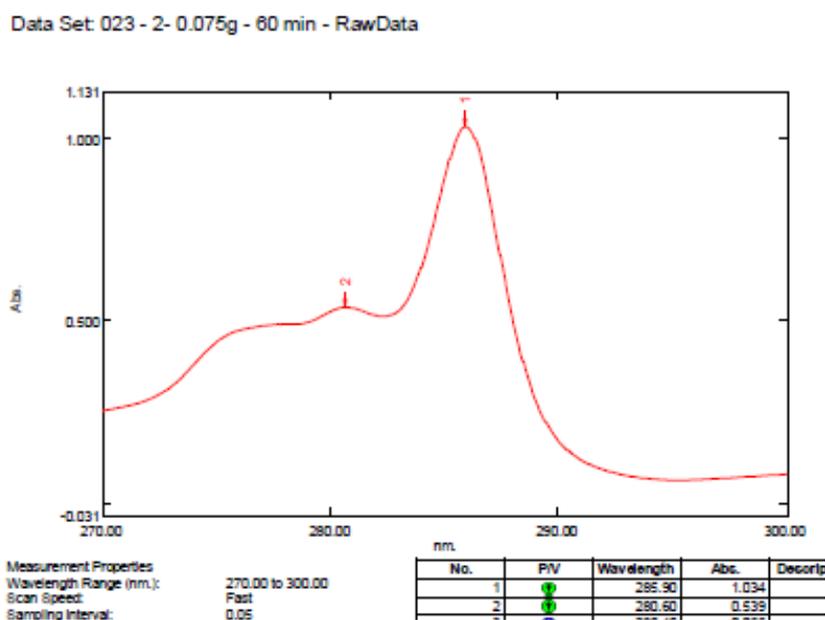
Data Set 021 - 1- 0.075g - 60 min - RawData



**Figure S35:** UV- Spectrum peak pick report of extractive desulfurization condition: extractant (1), at 30 °C, weight of extractant 0.075 g, time = 60 min.

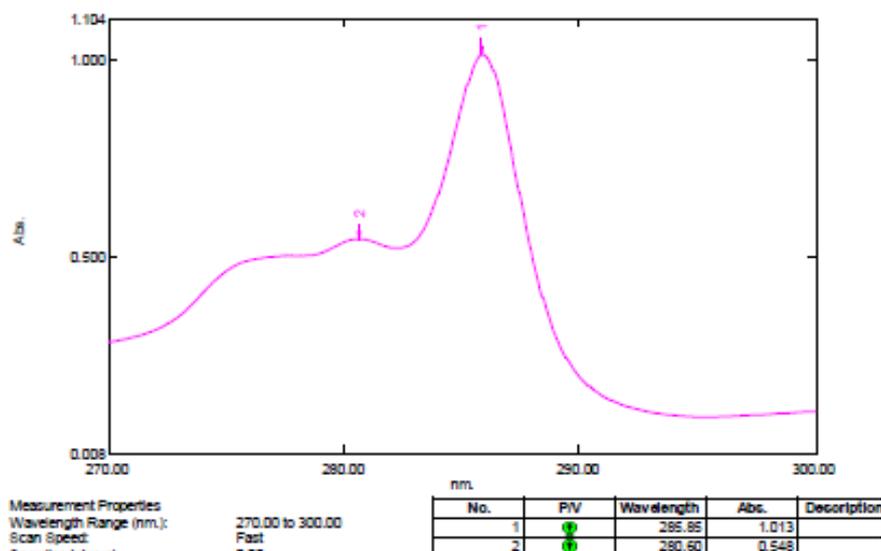


**Figure S36:** UV- Spectrum peak pick report of extractive desulfurization condition: extractant (1), at 30 °C, weight of extractant 0.1 g, time = 60 min.



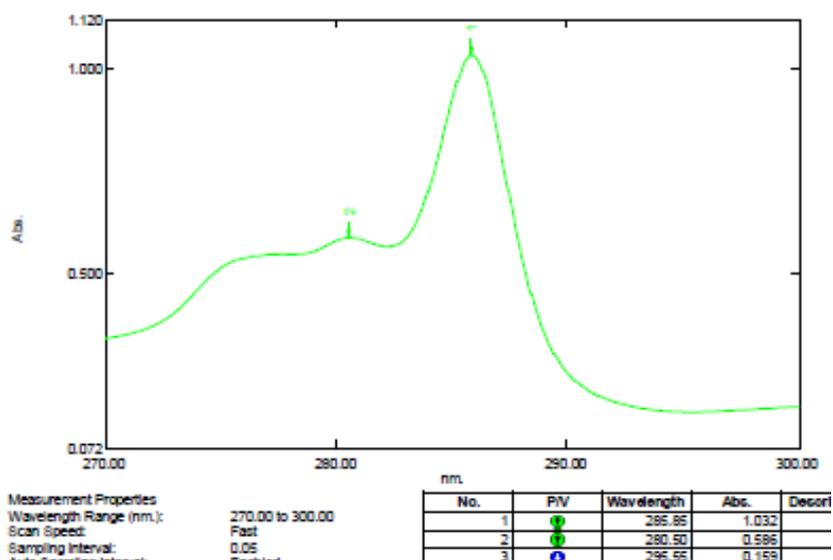
**Figure S37:** UV- Spectrum peak pick report of extractive desulfurization condition: extractant (2), at 30 °C, weight of extractant 0.075 g, time = 60 min.

Data Set 024 -2- 0.1g - 60 min - RawData

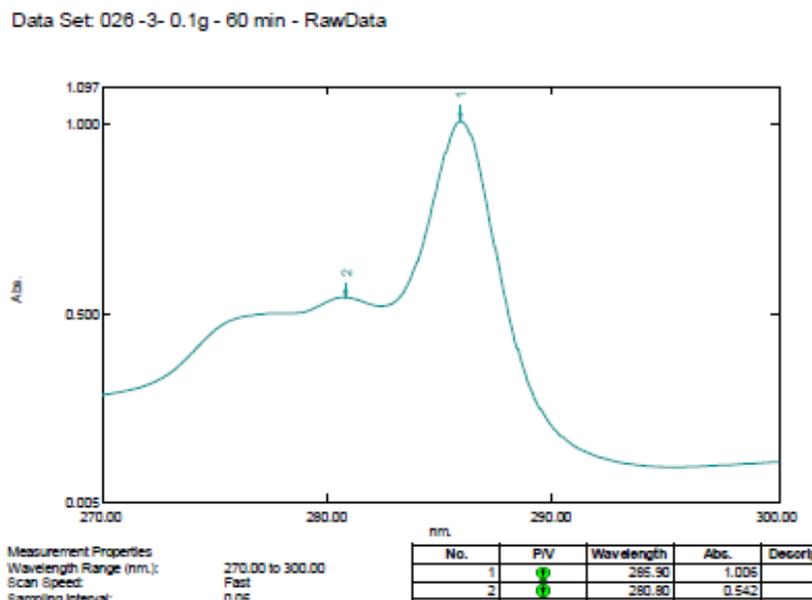


**Figure S38:** UV- Spectrum peak pick report of extractive desulfurization condition: extractant (2), at 30 °C, weight of extractant 0.1 g, time = 60 min.

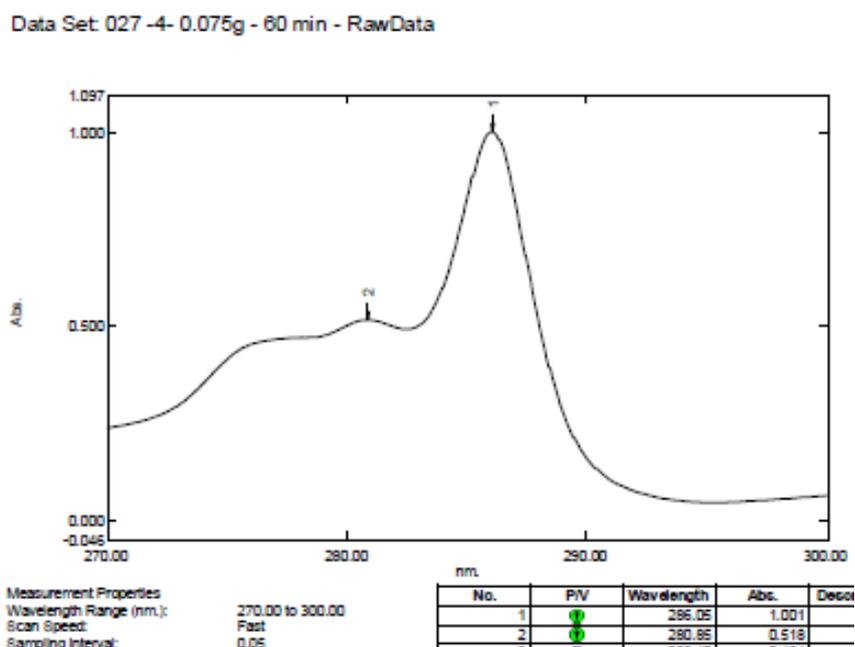
Data Set 025 -3- 0.075g - 60 min - RawData



**Figure S39:** UV- Spectrum peak pick report of extractive desulfurization condition: extractant (3), at 30 °C, weight of extractant 0.075 g, time = 60 min.

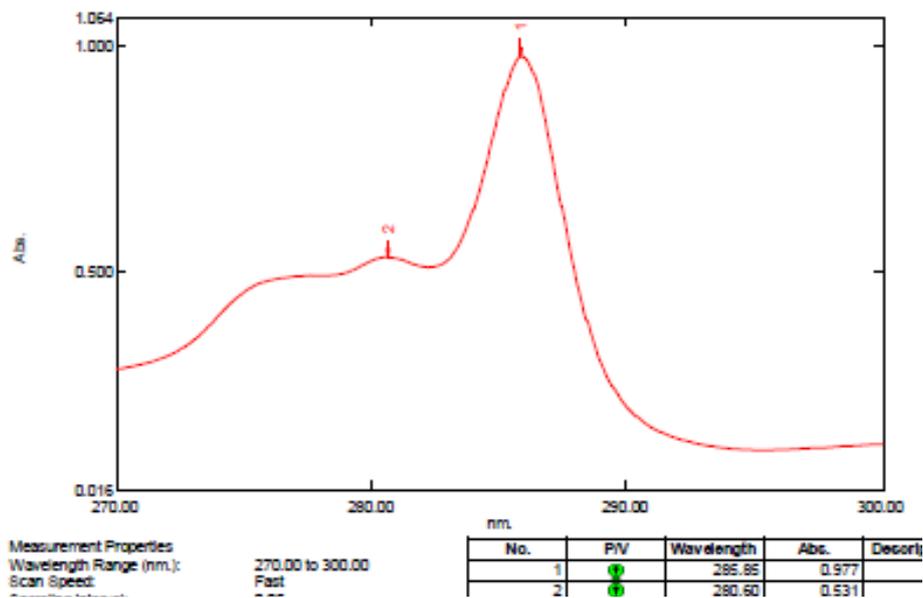


**Figure S40:** UV- Spectrum peak pick report of extractive desulfurization condition: extractant (3), at 30 °C, weight of extractant 0.1 g, time = 60 min.



**Figure S41:** UV- Spectrum peak pick report of extractive desulfurization condition: extractant (4), at 30 °C, weight of extractant 0.075 g, time = 60 min.

Data Set: 028 -4- 0.1g - 60 min - RawData



**Figure S42:** UV- Spectrum peak pick report of extractive desulfurization condition: extractant (4), at 30 °C, weight of extractant 0.1 g, time = 60 min.

