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**Research Paper / Makale**

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**Adsorption of Cr(VI) Ions on Magnetite Nano-Particles (Fe<sub>3</sub>O<sub>4</sub>):  
Kinetic and Thermodynamic Studies**

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**Abstract:** This article intends to investigate the kinetic and thermodynamic properties of adsorption process of hexavalent chromium [Cr(VI)] ions on magnetite nano-particles (Fe<sub>3</sub>O<sub>4</sub>, MNPs). In accordance with this purpose, MNPs were synthesized by chemical co-precipitation method and characterized by FTIR, TEM and VSM methods at first. After that, a series of adsorption experiments were performed for removal of Cr(VI) ions from aqueous media by MNPs. Finally, thermodynamic and kinetic properties of Cr(VI) adsorption on MNPs were investigated. Mean particle size and magnetization saturation (Ms) of synthesized MNPs were about 15 nm and be 75 emug<sup>-1</sup>, respectively. Under optimum adsorption conditions, adsorption capacity and Cr(VI) removal percentage were found to be 33.45 mg/g and 88%, respectively. According to calculated thermodynamic parameters after adsorption experiments, Cr(VI) adsorption process was a result of endothermic reactions. Langmuir and Freundlich isotherm models were investigated and it was observed that the removal of Cr(VI) could be better described by the Langmuir model. Kinetic investigations showed that the pseudo-second-order model have a better description of the Cr(VI) adsorption.

**Keywords:** Nano magnetite; Cr (VI); Adsorption isotherm; Adsorption kinetics; Adsorption thermodynamic.

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**Cr(VI) İyonlarının Manyetit Nano-Partikülleri (Fe<sub>3</sub>O<sub>4</sub>) Üzerine  
Adsorpsiyonu: Kinetik ve Termodinamik Çalışmalar**

**Özet:** Bu çalışmada, hegzavalent krom [Cr(VI)] iyonlarının manyetit nano-partikülleri (Fe<sub>3</sub>O<sub>4</sub>, MNP) ile adsorpsiyonu prosesinin kinetik ve termodinamik özelliklerinin araştırılması amaçlanmıştır. Bu amaç doğrultusunda, ilk olarak kimyasal ikili çöktürme tekniği kullanılarak MNP sentezlendi ve elde edilen ürünler FTIR, TEM ve VSM gibi metotlar ile karakterize edildi. Daha sonra, sulu ortamdan Cr(VI) iyonlarının giderilmesi için MNP ile bir dizi adsorpsiyon deneyleri yapıldı. Son olarak da Cr(VI) iyonlarının MNP ile adsorpsiyonu prosesinin kinetik ve termodinamik çalışmaları yapıldı. Sentezlenen nano-partiküllerin ortalama tene boyutunun 15 nm ve mıknatıslanma doyunluğunun da 75 emug<sup>-1</sup> olduğu tespit edildi. Optimum adsorpsiyon şartlarında, adsorpsiyon kapasitesi ve Cr(VI) giderim yüzdesi sırasıyla 33.45 mg/g ve %88 olarak hesaplandı. Adsorpsiyon deneyleri sonrası hesaplanan termodinamik parametrelere göre MNP ile Cr(VI) adsorpsiyonu endotermik reaksiyonların sonucu oluşan bir proses olduğu söylenebilir. Langmuir ve Freundlich izoterm modelleri araştırıldı ve adsorpsiyon prosesinin Langmuir modeli ile daha iyi açıklanabilir olduğu tespit edildi. Kinetik araştırmalar sonucunda ise MNP ile Cr(VI) iyonlarının adsorpsiyonu için sözde-ikinci-derece kinetik model ile daha iyi bir açıklama getirilebilir.

**Anahtar kelimeler:** Nano manyetit; Cr(VI); Adsorpsiyon kinetiği; Adsorpsiyon termodinamiği.

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## 1. Introduction

Chromium is a heavy metal which has toxic effect and used in various applications such as chromium-plating, production of chromium alloys or metals, leather, ceramic, glass, paint and ink industries [1, 2]. Hexavalent chromium [Cr(VI)] and trivalent chromium [Cr(III)] are two main forms of chromium most occurring in the aquatic environment. Most of the components of Cr(VI) has been reported to be toxic and carcinogenic [3, 4]. Unlike other chromium components, Cr(VI) is soluble in water and therefore its transportation and participation to living organisms are much more likely. According to the World Health Organization (WHO) standards, maximum allowable Cr(VI) concentration in drinking waters is 0.05 mg/l [5-7]. Thus, the amount of chromium content in the waste waters which have dangerous effect on living beings should be reduced to a minimum level before releasing in to the environment.

Magnetite nano-particles (MNPs) are of great interest as a new adsorbent in recent years to remove heavy metals from waste waters which have some advantageous properties such as high surface area and high magnetic sensitivity [8]. With these features, MNPs have high adsorption capacity for heavy metals and easily separable by an external magnetic field from aqueous media. Furthermore, MNPs are also used for some specific applications such as drug delivery, magnetic field-assisted cancer therapy, magnetic resonance imaging and sensing. These applications require that the nanoparticles are superparamagnetic with sizes smaller than 20 nm to have uniform physical and chemical properties.

In this study, adsorption technique which is economic, efficient and easier technique for application was used to remove Cr(VI) ions from aqueous media by MNPs. After adsorption experiments kinetic and thermodynamic properties of Cr(VI) adsorption by MNPs were investigated.

## 2. Materials and Methods

### 2.1. Materials

Iron(III) chloride (FeCl<sub>3</sub>.6H<sub>2</sub>O, >98%), iron(II) chloride (FeCl<sub>2</sub>.4H<sub>2</sub>O, >99%), hydrochloric acid (HCl, %35-37 GR), sodium hydroxide (NaOH, 96%), sulphuric acid (H<sub>2</sub>SO<sub>4</sub>, 95-97%), potassium dichromate (K<sub>2</sub>Cr<sub>2</sub>O<sub>7</sub>), acetone (C<sub>3</sub>H<sub>6</sub>O) and ethanol (C<sub>2</sub>H<sub>5</sub>OH, 99.7%) were purchased from Merck. Ammonium hydroxide (NH<sub>4</sub>OH, 28-30%) and 1,5-Diphenylcarbazide (DPC, C<sub>13</sub>H<sub>14</sub>N<sub>4</sub>O) were purchased from Sigma Aldrich.

A stock solution of 500 mg/l Cr(VI) was prepared by dissolving of 1.414 gr K<sub>2</sub>Cr<sub>2</sub>O<sub>7</sub> with 1000 ml distilled water. 1.5-DPC (0.5%) solution was used for UV measurements and prepared by dissolving of 0.25 gr 1.5-DPC with 50 ml acetone. 6 N sulphuric acid solution was prepared by adding 8.33 ml H<sub>2</sub>SO<sub>4</sub> (98%) into 50 ml distilled water to be used to pH adjustments at UV measurements.

MNPs with an average particle size of 15 nm were synthesized according to our previous report using chemically co-precipitation technique [9].

### 2.2. Adsorption Experiments

Batch adsorption experiments were performed in a 100 ml erlenmayer flask with 50 ml Cr(VI) solution of known concentration and desired amount of adsorbent. The mixture was stirred using a GFL-1086 shaking water bath at 175 rpm. After that the adsorbent was taken from solution by

magnetic separation using a magnet and the solution analyzed for the residual Cr(VI) determination by Shimadzu UV-1240 spectrophotometer. Figure 1 shows a schematic summary of adsorption and Cr(VI) determination experiments.

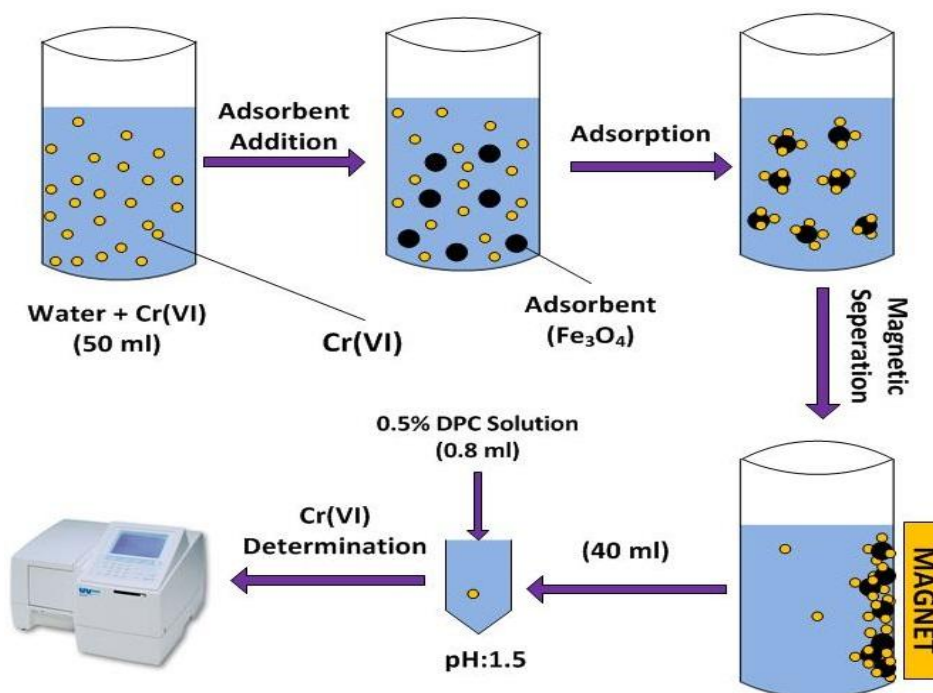


Figure 1. Schematic illustration of adsorption process and Cr(VI) determination experiments.

The percentage removal of Cr(VI) and amount of adsorption at equilibrium,  $q_e$  (mg/g), were calculated by using following Equations 1 and 2.

$$\text{Removal}(\%) = \frac{C_i - C_e}{C_i} 100 \quad (1)$$

$$q_e = \frac{C_i - C_e}{m} V \quad (2)$$

where  $C_i$  and  $C_e$  are initial and final concentration of Cr(VI) (mg/l) in the solution, respectively.  $V$  is the volume (l) of tested solution and  $m$  is the mass of used adsorbent (g).

### 2.3. Determination of Cr(VI) Ions

The amount of Cr(VI), remained in solution after adsorption experiments, was determined using UV-vis spectrophotometer and the used method is as follows; 40 ml of sample was taken in a beaker and 3 ml of 6 N  $\text{H}_2\text{SO}_4$  was added into the solution to decrease the pH of the solution under 2. Then 0.8 ml of 0.5% DPC solution was added in the mixture. After waiting 5 minutes, the UV measurements were performed [10].

### 3. Results and Discussion

#### 3.1. Adsorbent Characterization

Figure 2 shows the XRD pattern of MNPs. Large peaks show nano-crystalline and sharp peaks show the high degree of crystalline structure [11]. As can be seen in the figure, crystalline diffraction peaks with  $2\theta$  at  $30.1^\circ$ ,  $35.4^\circ$ ,  $43.2^\circ$ ,  $53.9^\circ$ ,  $57.2^\circ$  and  $62.7^\circ$  correspond to the characteristic planes [(220), (311), (400), (422), (511), (440)] of cubic spinel Fe<sub>3</sub>O<sub>4</sub>, respectively (JCPDS No. 01-071-6336).

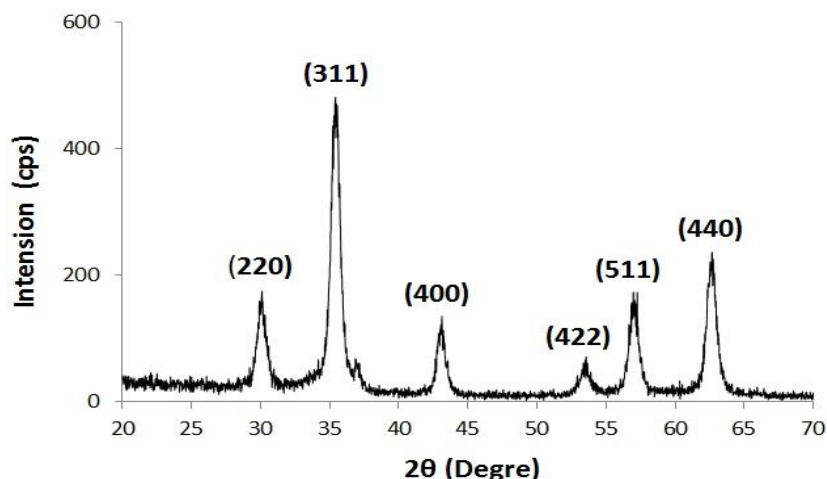


Figure 2. XRD pattern of MNPs

Mean crystallite size and lattice constant of MNPs were calculated according to the Scherrer's formula given in the Equations 3 and 4, respectively. The calculated results are demonstrated in the Table 1.

$$D_{XRD} = \frac{k \lambda}{\beta \cos(\theta)} \quad (3)$$

$$\alpha = d_{hkl} [h^2 + k^2 + l^2]^{1/2} \quad (4)$$

where  $k$  is the particle shape factor (0.89 for magnetite),  $\lambda$  is the X-ray wavelength (0.15406 nm),  $\beta$  is the full width at half height of the diffraction peak (radian),  $\theta$  is the Bragg diffraction angle ( $17.75^\circ$ ),  $d_{hkl}$  is the crystal plane space ( $d_{hkl} = \lambda/2\sin\theta$ ) and  $h, k, l$  are the Miller index.

Table 1. Structural XRD parameters obtained for (3 1 1) basic plane.

| $2\theta$ (der) | $\beta$ (der) | $D_{XRD}$ (nm) | $\alpha$ (nm) | $d_{hkl}$ (nm) |
|-----------------|---------------|----------------|---------------|----------------|
| 35.42           | 0.734         | 11.24          | 0.8397        | 0.2532         |

TEM images of the MNPs were shown in Figure 3. The average size of MNPs was estimated to be 15 nm and MNPs has approximately spherical shape as seen in the figure.

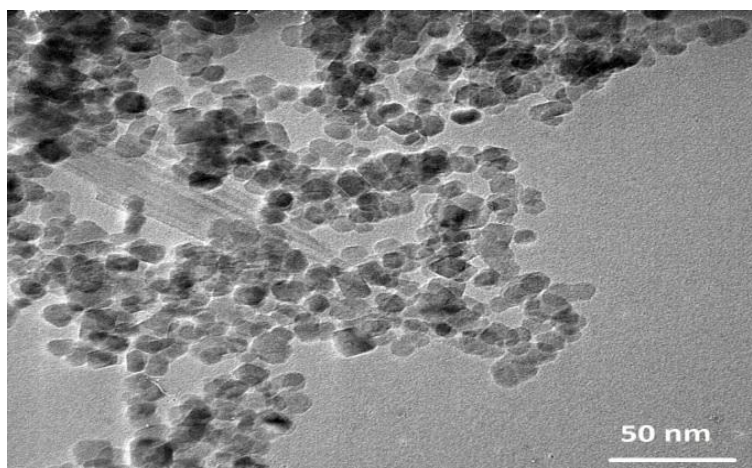


Figure 3. TEM micrograph of MNPs.

Magnetization curve of synthesized MNPs is given in the Figure 4. Magnetization saturation ( $M_s$ ) of MNPs was found to be  $75 \text{ emu g}^{-1}$ . Additionally, the magnetization curve has gone through exactly the origin of magnetization graph. This means that the synthesized MNPs show superparamagnetic behavior at room temperature because of not exhibiting hysteresis, coercivity and remanence [12].

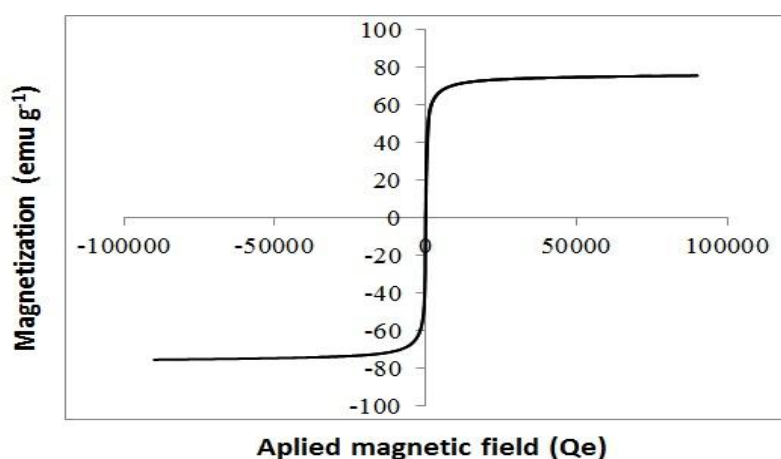


Figure 4. Magnetization curve of MNPs.

### 3.2. Adsorption Kinetics

Figure 5 shows the change in adsorption capacity for 5-25 mg/l initial Cr(VI) concentrations and times up to 150 minutes. As it is expected, a rapid increasing of the adsorption capacity was shown in the first stage and then slowed down until it reaches the equilibrium time. The adsorption capacity increased from 17.4 mg/g to 24.9 mg/g when percentage removal decreased from 87.5% to 62.2% by increasing of the initial Cr(VI) concentration from 10 mg/l to 20 mg/l. This situation can be explained by the mass transfer rate resulted from growing driving force [13]. Additionally, the curves reaches an equilibrium at 90 minutes and initial Cr(VI) concentration has no effect on the equilibrium time. According to these results, it can be said that the adsorption of Cr(VI) on the surface of MNPs is monolayer [14].

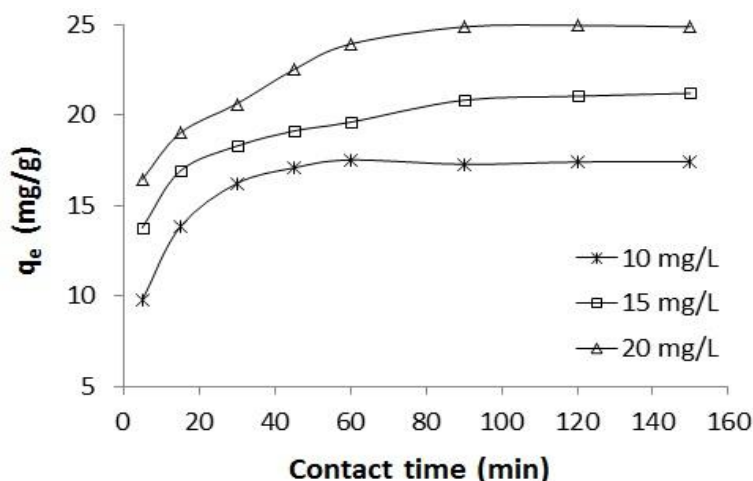


Figure 5. Effect of contact time and initial Cr(VI) concentration on the removal of Cr(VI) by MNPs (adsorption conditions: amount of adsorbent, 0.5gL<sup>-1</sup>; temperature, 25 °C; pH, 3).

In order to investigate the adsorption mechanism, the data were fitted to pseudo-first-order and pseudo-second-order kinetic models. Linear forms of first and second order models were given in the Equations 5 and 6, respectively [15].

$$\log(q_e - q_t) = \log(q_e) - \frac{k_1}{2.303}t \tag{5}$$

$$\frac{t}{q_t} = \frac{1}{h} + \left(\frac{1}{q_e}\right)t \quad (h=k_2q_e^2) \tag{6}$$

k<sub>1</sub>/2.303 and log(q<sub>e</sub>) values were found from slope and intercept of the plot of log(q<sub>e</sub>-q<sub>t</sub>) versus t (Figure 6a). 1/q<sub>e</sub> and 1/k<sub>2</sub>q<sub>e</sub><sup>2</sup> values were found from slope and intercept of the plot of t/q<sub>t</sub> versus t (Figure 6b). The obtained reaction rate constants (k<sub>1</sub> and k<sub>2</sub>), adsorption capacities (mg/g) and R<sup>2</sup> values are shown in the Table 2.

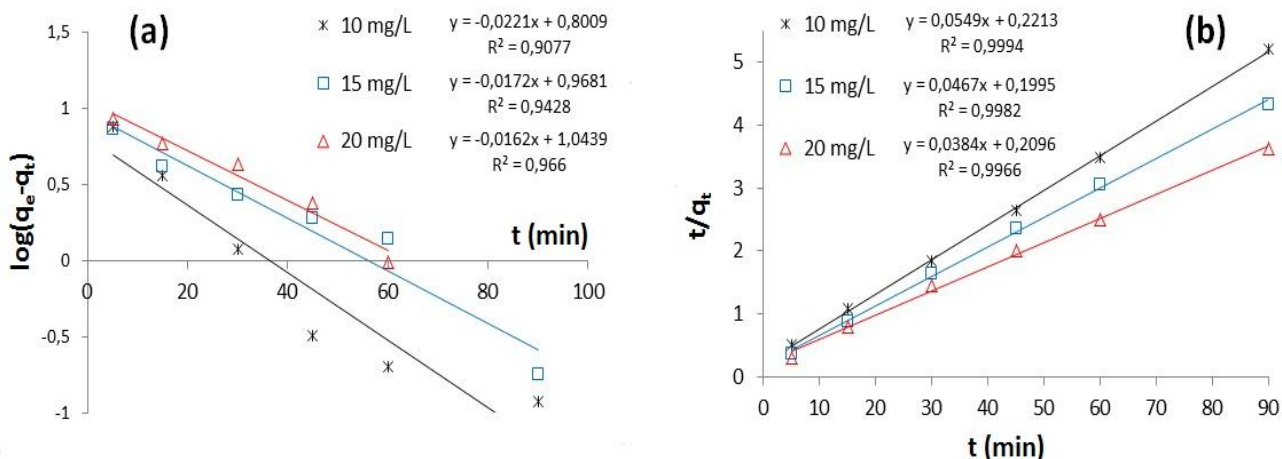


Figure 6. Kinetic models for adsorption of Cr(VI) by MNPs; (a) pseudo-first-order kinetic model, (b) pseudo-second-order kinetic model.

According to Table 2, the calculated adsorption capacities (q<sub>e,cal</sub>) from pseudo-second-order model are very close to the experimental adsorption capacity (q<sub>e,exp</sub>) values. When viewed correlation coefficients, the pseudo-second-order model (R<sup>2</sup>: 0.997–0.999) have a better description of the

Cr(VI) adsorption compared to pseudo-first-order model ( $R^2$ : 0.908–0.966). Therefore, it is clear that adsorption of Cr(VI) on the MNPs follows the pseudo-second-order kinetic model.

Table 2. Kinetic parameters for adsorption of Cr(VI) onto the Fe<sub>3</sub>O<sub>4</sub> NPs.

| C <sub>0</sub><br>(mg/l) | q <sub>e,exp</sub><br>(mg/g) | Pseudo-first-order      |                              |                | Pseudo-second-order        |                              |                |
|--------------------------|------------------------------|-------------------------|------------------------------|----------------|----------------------------|------------------------------|----------------|
|                          |                              | k <sub>1</sub> , (1/dk) | q <sub>e,cal</sub><br>(mg/g) | R <sup>2</sup> | k <sub>2</sub><br>(g/mgdk) | q <sub>e,cal</sub><br>(mg/g) | R <sup>2</sup> |
| 10                       | 17.4                         | 0.0509                  | 6.32                         | 0.908          | 0.01363                    | 18.21                        | 0.999          |
| 15                       | 21.0                         | 0.0396                  | 9.29                         | 0.943          | 0.01094                    | 21.41                        | 0.998          |
| 20                       | 24.9                         | 0.0373                  | 11.06                        | 0.966          | 0.00704                    | 26.04                        | 0.997          |

### 3.3. Adsorption Thermodynamic

Effect of temperature on Cr(VI) removal as a function of initial chromium concentration is illustrated in the Figure 7. As seen clearly from figure, the adsorption capacity (mg/g) increased with increasing of temperature and this result indicates that the adsorption of Cr(VI) on MNPs is an endothermic process.

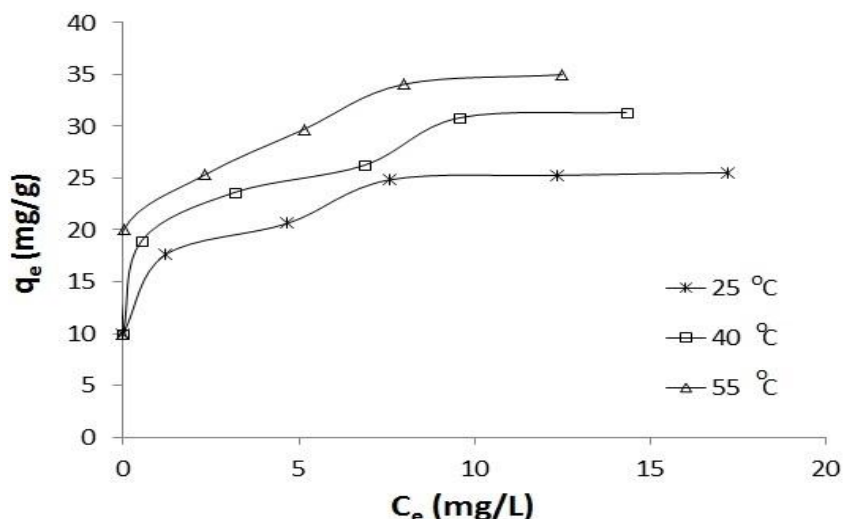


Figure 7. Effect of temperature on the removal of Cr(VI) by MNPs (adsorption conditions: initial concentration of Cr(VI), 10 mg/l; contact time, 90 min; adsorbent concentration, 0.5g/L<sup>-1</sup>; pH, 3)

Thermodynamic parameters which Gibbs free energy ( $\Delta G^0$ ), enthalpy change ( $\Delta H^0$ ) and entropy change ( $\Delta S^0$ ) can be calculated according to Equations 7-9.  $-\Delta H^0/R$  and  $\Delta S^0/R$  values were found from slope and intercept of the plot of  $1/T$  versus  $\ln K_c$  given in the Figure 8.

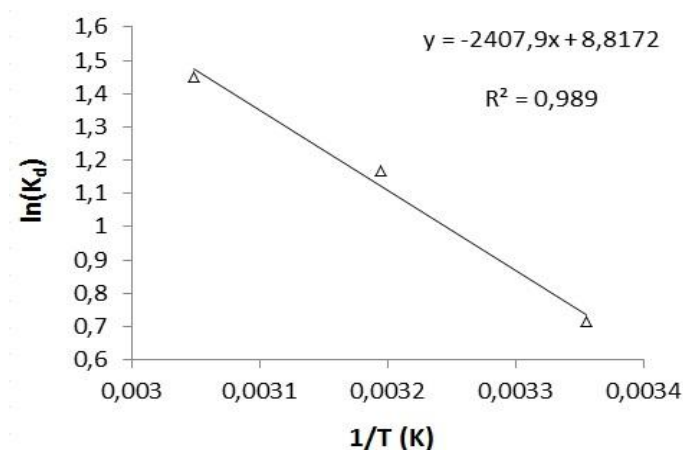


Figure 8. Van't Hoff plot for Cr(VI) adsorption by MNPs.

Thermodynamic parameters are shown in the Table 3. Negative  $\Delta G^{\circ}$  shows that the adsorption process is spontaneous and feasible, positive  $\Delta H^{\circ}$  values are a result of endothermic reactions and the negative values of  $\Delta S^{\circ}$  indicate a decreased randomness at the solid/solution interface during the adsorption process.

$$K_c = C_{\text{ads}} / C_e \quad (7)$$

$$\Delta G^{\circ} = -RT \ln K_d \quad (8)$$

$$\ln K_c = \frac{\Delta S^{\circ}}{R} - \frac{\Delta H^{\circ}}{RT} \quad (9)$$

where  $K_c$  is the equilibrium constant,  $C_e$  is the equilibrium concentration in solution (mg/l) and  $C_{\text{ads}}$  is the solid phase concentration at equilibrium (mg/l),  $R$  is the gas constant (8.314 J/mol K) and  $T$  is the absolute temperature (K).

Table 3. Thermodynamic parameters for adsorption of Cr(VI) by MNPs.

| Temperature (°C) | $\Delta G^{\circ}$ (J mol <sup>-1</sup> ) | $\Delta H^{\circ}$ (J mol <sup>-1</sup> ) | $-\Delta S^{\circ}$ (J mol <sup>-1</sup> K <sup>-1</sup> ) |
|------------------|-------------------------------------------|-------------------------------------------|------------------------------------------------------------|
| 25               | -1772.82                                  |                                           |                                                            |
| 40               | -3042.42                                  | 23449.9                                   | 84.0                                                       |
| 55               | -3960.79                                  |                                           |                                                            |

### 3.3. Adsorption Isotherms

Figure 9 shows the adsorption isotherms of Cr(VI) removal by MNPs at temperatures 25°C, 40°C and 55°C. Langmuir and Freundlich models were employed to investigate the isotherm data. The linearized Langmuir isotherm model is represented by Equation 10 [16]. Dimensionless separation factor ( $R_L$ ) which given by Equation 11 is essential for Langmuir model to define the favorability of an adsorption process [15]. The linear form of Freundlich model is expressed by Equation 12 [18].

$$\frac{C_e}{q_e} = \frac{1}{q_m \cdot b} + \frac{1}{q_m} C_e \quad (10)$$



$$R_L = \frac{1}{1 + (b \cdot C_0)} \tag{11}$$

$$\ln(q_e) = \ln(K_f) + \frac{1}{n} \ln(C_e) \tag{12}$$

where  $q_m$  (mg/g) is the maximum adsorption capacity,  $b$  (l/mg) is the Langmuir constant,  $K_f$  and  $1/n$  constants are related to the adsorption capacity and intensity of adsorption, respectively.

$1/q_m$  and  $1/q_m b$  values were found from slope and intercept of the plot of  $C_e/q_e$  versus  $C_e$  (Figure 9a) and  $1/n$  and  $\ln(K_f)$  values were found from slope and intercept of the plot of  $\ln(C_e)$  versus  $\ln(q_e)$  (Figure 9b). The isotherm constants and correlation coefficients are shown in the Table 4 and according to the correlation coefficients ( $R^2$ ), adsorption isotherms of the used adsorbent for removal of Cr(VI) could be better described by the Langmuir model than by the Freundlich model.

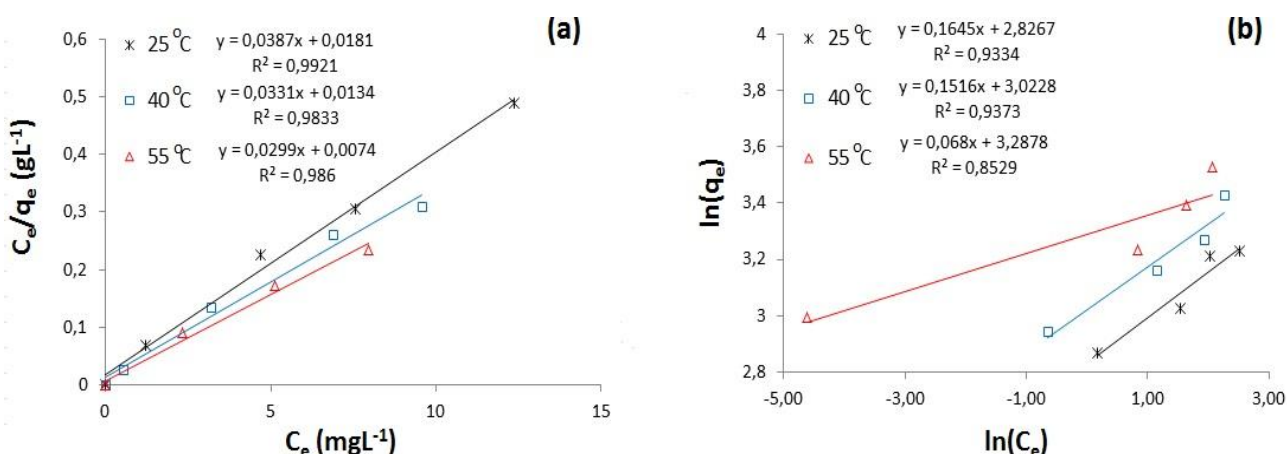


Figure 9. Linear forms of Langmuir (a) and Freundlich (b) isotherms.

As a result we can say that the adsorption of C(VI) ions on MNPs was happened in monolayer. Namely, adsorption occurs on the specific homogeneous areas of adsorbent surface and each of these areas is occupied by only one metal ion, more of these ions cannot be adsorbed. The maximum capacity of adsorbent ( $q_m$ ) which in the range of 25.84-33.45 mg/g was calculated from the Langmuir plots. Additional, increased adsorption capacity with increasing of the temperature proved the endothermic reactions of adsorption process. The equilibrium parameter ( $R_L$ ) was found to be in the range  $0 < R_L < 1$  shown in the Table 4. This proves that the adsorption process is favorable as desired level [2].

Table 4. Langmuir and Freundlich isotherm constants for adsorption of Cr (VI) by MNPs.

| Temperature<br>(°C) | Langmuir constants |           |       |       | Freundlich constants |       |       |
|---------------------|--------------------|-----------|-------|-------|----------------------|-------|-------|
|                     | $q_m$ (mg/g)       | $b$ (l/g) | $R_L$ | $R^2$ | $K_f$ (mg/g)         | $n$   | $R^2$ |
| 25                  | 25.84              | 2.14      | 0.045 | 0.992 | 16.89                | 6.08  | 0.933 |
| 40                  | 30.21              | 2.47      | 0.039 | 0.983 | 20.55                | 6.60  | 0.937 |
| 55                  | 33.45              | 4.04      | 0.024 | 0.986 | 26.78                | 14.71 | 0.853 |

#### 4. Conclusion

Fe<sub>3</sub>O<sub>4</sub> nano-particles (MNPs) have been shown to be an effective adsorbent for removal of Cr(VI) ions from aqueous media. Electrostatic attraction forces between Cr(VI) ions and MNPs play a key role for this adsorption process. Maximum Cr(VI) adsorption capacity was found to be 33.45 mg/g with 88% removal at pH 3.0. Thermodynamic calculations showed that the Cr(VI) adsorption by MNPs is endothermic and spontaneous in nature. The adsorption data were fitted well with Langmuir isotherm and the kinetics of the adsorption followed the pseudo-second-order model. According to these results, MNPs can be used as an effective adsorbent for removal of Cr(VI) ions from industrial waste waters. Additionally, we can say that the magnetic separation of MNPs from solution is more rapid, simpler and more effective than other solid-liquid separation techniques.

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