



## Use of Pitzer's model to calculate thermodynamic properties of aqueous electrolyte solutions of sulfuric acid

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**Abstract:** Over this study we calculated the coefficients of activity of different species and the concentration in the presence of H<sup>+</sup> ion when H<sub>2</sub>SO<sub>4</sub> is alone in solution. The coefficient of average activity was calculated using the model of Pitzer. The constants of dissociation of these reactions were calculated from the values of the free standard energies. The reaction reaches a balance while producing H<sup>+</sup>, HSO<sub>4</sub><sup>-</sup> and SO<sub>4</sub><sup>2-</sup>. The research reported here concentrated on the effect of some important operational parameters on dissolution process. The parameters were investigated and their ranges are as follows: initial molality ranging from 0.001 to 5 mol.kg<sup>-1</sup> and temperatures between 25 and 200°C. Fortran 90 (Mathematical formula translating system) was used to perform all mathematical calculations. The numerical code can be used to calculate the molarity of ion H<sup>+</sup> of an aqueous solution of sulfuric acid. The objective of the present work is to optimize the parameters of leaching such as activity of sulfuric acid on the dissociation phenomena.

**Keywords:** Leaching, Pitzer, activity, dissociation, molality.

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## 1. INTRODUCTION

Several test were conducted to develop models to represent the thermodynamic properties of the solutions of electrolyte. The coefficient of average activity was calculated using the model of Pitzer (1-3). The pitzer ion interaction model, similar to the virial equation used for non-ideal gases, has proved to be the most accurate thermodynamic model up to moderate concentrations in aqueous solutions (4,5).

Pitzer et al. (6-8) developed a model for calculation of the properties of the electrolytes starting from a semi numerical models and an improved analysis of the model of DEBYE HUCKEL.

This model links the intermolecular forces and the distribution of the ions to the osmotic pressure and takes into account the influence of forces with short distance in the binary interactions. The expressions of the coefficient of activity and the osmotic coefficient are deduced from the equation of the excess free energy of GIBBS. The obtained equations are analogous to those of GUGGENHEIM.

Pitzer’s model is capable of precisely forecasting activity and enthalpy provided that the variation of the parameters with temperature are recognized. This variation has been calculated for some electrolytes (9-11).

Zomaitis et al. suggested to admit the parameters to be constant and to consider the influence of temperature only on the DEBYE-HUCKEL (12).

The mixing terms for ions with same sign but with unequal magnitude are not included in the Pitzer ion interaction, Harvie et al. have found these terms (13).

Archer discovered that an ion strength reliant third virial parameter describing the combined interactions between two similar cations and anion or vice versa (14).

Pitzer et al. introduced a Margules type equation to model aqueous solutions up to a pure salt (15).

Sippola found out that only four parameters with a simple temperature dependency in enough to present the osmotic and activity coefficients (16).

Knopf et al. were found to be extrapolate the measured osmotic coefficient within a maximum deviation of 0.01 (17).

The aim of our work was to optimize leaching parameters such as the activity of sulfuric acid. We developed from fortran 90 a program, for simulating this process and predicting its

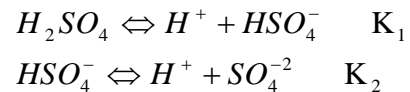
performance. This numerical code is based on the mathematical description of the detailed physical and chemical phenomena occurring.

## 2. METHODS

### 2.1. Thermodynamic Model

The Pitzer thermodynamics model is used extensively to describe the interactions between dissolved ions and solvents (18).

In water, Sulfuric acid is separated according balances (19-22).



The dissociation constants of these reactions are calculated from the values of the standard free energy of species considered.

The equilibrium constant is linked to the standard free energy of the reaction by the relation VAN’T HOFF:

$$\frac{\Delta G^0}{T} = -RT \ln K$$

he just:

$$K_1 = e^{\left( -\frac{\Delta G_{HSO_4^-}^0 - \Delta G_{H_2SO_4}^0}{RT} \right)} = 80.72$$

$$K_2 = e^{\left( -\frac{\Delta G_{SO_4^{2-}}^0 - \Delta G_{HSO_4^-}^0}{RT} \right)} = 0.0125$$

K: equilibrium constant

$\Delta G^0$  : standard free energy

T: Temperature (K)

R: Gas constant  $Jmol^{-1}K^{-1}$

The high values of the equilibrium constant  $K_1$ , translated into strong shift in the balance towards the formation of  $HSO_4^-$  and  $H^+$ . We admit that in the future the first dissociation  $H_2SO_4$  is total. Only the second equilibrium dissociation will be taken into account ( $HSO_4^- \rightleftharpoons H^+ + SO_4^{2-}$ ).

Pitzer et al. gives value perceptibly different  $k_2$ . It adopts the value 0.0105, which corresponds to a compromise (6).

An application of Pitzer ’s expression for estimating the coefficient of activity for a mixture of electrolytes to the couple of ions  $H^+$  and  $SO_4^{2-}$  in the presence of ions  $HSO_4^-$  gives:

$$\ln(\gamma_{H_2SO_4}) = 2f^\gamma + \frac{4}{3}m_1B_{H_1} + \frac{1}{3}(4m_2 + 2m_H)B_{H_2}^{(0)} + \frac{1}{3}(8m_2 + 2m_H)m_H C_{H_2} + 2m_1m_H B'_{H_1}$$

$\gamma_i$ : Activity coefficient of a component  $i$   
 $f^\gamma$ : the derivative of the Debye-Huckel term  
 $m_i$ : Molale concentration of component  $i$   
 $B_{ij}$ : Pitzer binary interaction parameters  
 $C_{ij}$ : Pitzer ternary interaction parameter  
 $HSO_4^-$  is indexed by 1  
 $SO_4^{2-}$  is indexed by 2

Because the molecule  $H_2SO_4$  was supposed to be made of two ions  $H^+$  and  $SO_4^{2-}$ , then we have:

$$\ln \gamma_{H_2SO_4} = \frac{1}{3}(2 \ln \gamma_H + \ln \gamma_{SO_4}),$$

Hence;  $3 \ln \gamma_{H_2SO_4} = \ln(\gamma_H^2 \gamma_{SO_4})$

The computed exploratory Pitzer showed that  $B_{H_2}^{(1)}$  had a negligible effect on the determination of the activity coefficient, expressing  $\beta_{H_2}$  in those circumstances is tantamount to match.  $\beta_{H_2}$  and  $B_{H_2}^{(0)}$ . On the other hand, good results are obtained either with the combination  $B_{H_2}^{(0)}$  and  $C_{H_2}$ , or combination  $C_{H_1}$  and  $C_{H_2}$ , but the first was raised slightly better and has been adopted. It follows  $C_{H_1} = 0$ .

The term  $B'_{H_2}$  is void because it represents the derivative compared to the ionic strength of a term  $B_{H_2}^{(0)}$  independent  $I$ .

This method ensures the relation:

$$\ln(\gamma_H^2 \gamma_{SO_4}) = 6f^\gamma + 4m_1B_{H_1} + (4m_2 + 2m_H)B_{H_2}^{(0)} + (8m_2 + 2m_H)m_H C_{H_2} + 6m_1m_H B'_{H_1}$$

Now let us apply the expression of the coefficient of activity for a mixture of electrolytes to the couple of ions  $H^+$ ,  $HSO_4^-$  in the presence of ions  $SO_4^{2-}$ .

The species  $H_2SO_4$  being supposed constitute of the ions  $H^+$  and  $HSO_4^-$ , one thus has:

$$\ln \gamma_{H_2SO_4} = \frac{1}{2} \ln \gamma_H \ln \gamma_{HSO_4^-}$$

with;  $\ln \gamma_H \ln \gamma_{HSO_4^-} = 2f^\gamma + 2(m_1 + m_H)B_{H_1} + 2m_2B_{H_2}^{(0)} + 4m_2m_H C_{H_2} + 2m_1m_H B'_{H_1}$

The former relationships must be compatible with the balance of dissolution. Hence the expression of the product of the coefficients of activity is as follows:

$$\begin{aligned} \ln(\gamma_H^2 \gamma_{SO_4^-} - \ln \gamma_{H^+} \gamma_{HSO_4^-}) &= \ln\left(\frac{\gamma_H^+ \gamma_{SO_4^-}}{\gamma_{HSO_4^-}}\right) \\ &= 4f^\gamma + 2(m_1 - m_H)B_{H_1} + 2(m_2 \\ &\quad + m_H)B_{H_2}^{(0)} \\ &\quad + 2(2m_2 + m_H)B_{H_2}^{(0)} + 2(2m_2 + m_H)m_H C_{H_2} + 4m_1m_H B'_{H_1} \end{aligned}$$

where:

$$\begin{aligned} \frac{\gamma_H^+ \gamma_{SO_4^-}}{\gamma_{HSO_4^-}} &= \exp(4f^\gamma + 2(m_1 - m_H)B_{H_1} + 2(m_2 + m_H)B_{H_2}^{(0)} \\ &\quad + 2(2m_2 + m_H)B_{H_2}^{(0)} + \\ &\quad 2(2m_2 + m_H)m_H C_{H_2} + 4m_1m_H B'_{H_1}) \end{aligned}$$

At weak concentrations, the molality is close to the concentration on the basis of the second balance of the dissolution of the  $H_2SO_4$ .

The concentration of the sulfate ions in the solution makes it possible to write the following relationship:

$$m = m_1 + m_2 \text{ therefore } m_2 = m - m_1$$

According to Pitzer we have:

$$m = \frac{1000C}{1000\rho - MC}$$

$m$ : Molality  
 $C$ : concentration  
 $M$ : Molar mass  
 $\rho$ : Density

On the other hand, because of the electric neutrality of the solution  $m_H = m_1 + 2m_2$

$$\text{From where } m_1 = 2m - m_H$$

The constant of equilibrium of dissociation of the  $H_2SO_4$  is then:

$$k_2 = \frac{[H^+][SO_4^{2-}]}{[HSO_4^-]} \cdot \frac{\gamma_H \gamma_{SO_4}}{\gamma_{HSO_4}} = \frac{m_H m_2}{m_1} \cdot \frac{\gamma_H \gamma_2}{\gamma_1}$$

with;  $m_H = \frac{\frac{K_2 m_1}{m_2}}{\left(\frac{\gamma_H \gamma_2}{\gamma_1}\right)}$

An average coefficient of activity  $\gamma^\pm$  can be defined by assuming that the  $H_2SO_4$  is completely dissociated. The following relationship:  $4\gamma_\pm^3 m^3 = \gamma_H^2 \gamma_{SO_4} m_H^2 m_2$  allows to calculate the average coefficient of activity  $\gamma^\pm$ .

Indeed, the molality of ions  $H^+$  was determined and one calculates  $(\gamma_H^2 \gamma_{SO_4})$  as follows:

$$\begin{aligned} \ln(\gamma_H^2 \gamma_{SO_4}) &= 6F^\gamma + 4m_1B_{H_1} + (4m_2 + 2m_H)B_{H_2}^{(0)} + (8m_2 \\ &\quad + 2m_H)m_H C_{H_2} + 6m_1m_H B'_{H_1} \end{aligned}$$

with; 
$$C_{H_2} = \frac{C_{H_2}^Y}{2^{\frac{3}{2}}}$$

$$f^Y = A^Y \left( \frac{I^{\frac{1}{2}}}{1 + 1.2I^{\frac{1}{2}}} + \frac{2}{1.2} \ln(1 + 1.2I^{\frac{1}{2}}) \right)$$

$$A^Y = 0.0000043T^2 + 0.002709T + 0.583022$$

I: ionic strength  
 A<sup>Y</sup>: DEBYE-HÜCKEL parameter  
 T: Temperature (K)  
 The temperature T is given in Kelvin

$$B_{H_1} = B_{H_1}^{(0)} + \frac{B_{H_1}^{(1)}}{2I} (1 - (1 + 2I^{\frac{1}{2}})e^{(-2I^{\frac{1}{2}})})$$

$$B'_{H_1} = \frac{B_{H_1}^{(1)}}{2I^2} (1 - (1 + 2I^{\frac{1}{2}} + 2I)e^{(-2I^{\frac{1}{2}})})$$

$$C_{H_2} = \frac{C_{H_2}^Y}{2^{\frac{3}{2}}}$$

For an aqueous sulfuric solution, the ionic species involved are: H<sup>+</sup>, HSO<sub>4</sub><sup>-</sup> and SO<sub>4</sub><sup>2-</sup>.

Therefore; 
$$I = \frac{1}{2}m_H + \frac{1}{2}m_1 + \frac{1}{2}m_2 \cdot 2^2$$

Pitzer provides the following equations, depending on the temperature (8):

$$k_2 = e^{-14.0321 + \frac{2825.2}{T}}$$

$$B_{H_1}^{(0)} = 0.05584 + \frac{46.040}{T}$$

$$B_{H_1}^{(1)} = -0.65758 + \frac{336.514}{T}$$

$$B_{H_2}^{(0)} = -0.32806 + \frac{98.607}{T}$$

$$C_{H_2} = 0.25333 - \frac{63.124}{T}$$

### 2.2. Optimization of Model Parameters

The model of Pitzer was applied to calculate the average coefficients of activity and the molality in ion H<sup>+</sup> of an aqueous solution of sulfuric acid. To this purpose, the numerical code for solving equations is written (in FORTRAN 90). The program can be used to calculate the molality of ion H<sup>+</sup> of an aqueous solution of H<sub>2</sub>SO<sub>4</sub> of an initial molality ranging from 0.001 to 5 mol.kg<sup>-1</sup> at temperatures between 25 and 200°C.

### 3. RESULTS

The term  $\ln \frac{Y_H Y_2}{\gamma_1}$  involved in the expression of the constant of dissolution depends on the molality mH of ion H<sup>+</sup>. An iterative calculation is done by fixing an initial molality mH superior than the initial molality in sulfuric acid. The following equations allow the calculation of a new value of the molality.

A comparison test between the previous and newly calculated value refining the result with an accuracy of 10<sup>-5</sup> mol.kg<sup>-1</sup>.

$$m_1 = 2m - m_H$$

$$m_2 = m - m_1$$

and;

$$m_H = \frac{\frac{K_2 m_1}{\gamma_1}}{\left( \frac{Y_H Y_2}{\gamma_1} \right)}$$

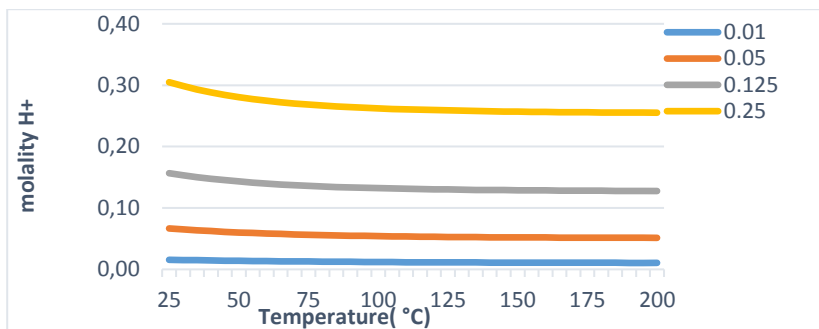
Figure 1 gives the molality in ions H<sup>+</sup> for different temperatures with molalities in H<sub>2</sub>SO<sub>4</sub> lying between 0.01 and 0.25 mol kg<sup>-1</sup>.

Figure 2 provides the molality in ions H<sup>+</sup> for different temperature with molalities in H<sub>2</sub>SO<sub>4</sub> from 0.5 to 5 mol.kg<sup>-1</sup>.

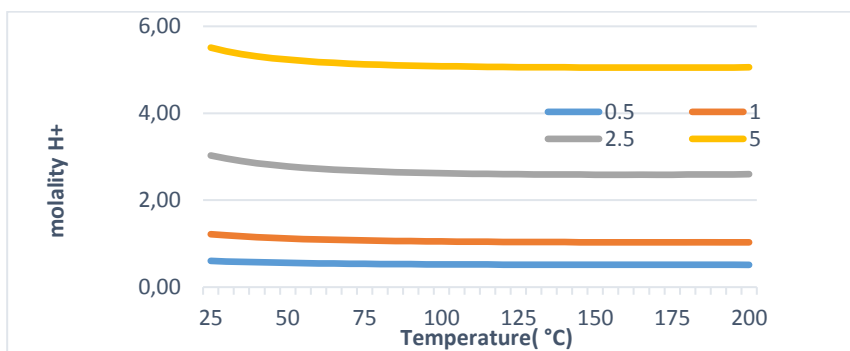
For molality higher than 1 mol.kg<sup>-1</sup> and temperatures within 170-200°C, the molality in ion H<sup>+</sup> passes by a minimum.

Figure 3 shows the molality of H<sup>+</sup> as a function of the molarity of H<sub>2</sub>SO<sub>4</sub> dependence shows between the two molalities whatever the temperature.

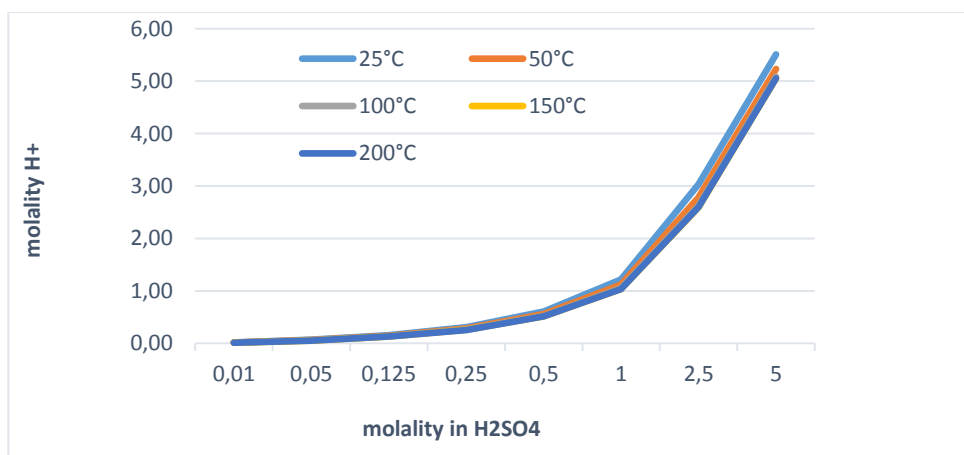
It can be noted that the temperature does not any influence on the calculated molality in ion H<sup>+</sup> as a function of the molality in H<sub>2</sub>SO<sub>4</sub> at 25°C.



**Figure 1:** Molality in H<sup>+</sup> versus the temperature for sulfuric aqueous solutions from 0.01 to 0.25 mol kg<sup>-1</sup>.



**Figure 2:** Variation in molality of H<sup>+</sup> as a function of the temperature for sulfuric aqueous solutions in the range of 0.5 to 5 mol.kg<sup>-1</sup>.



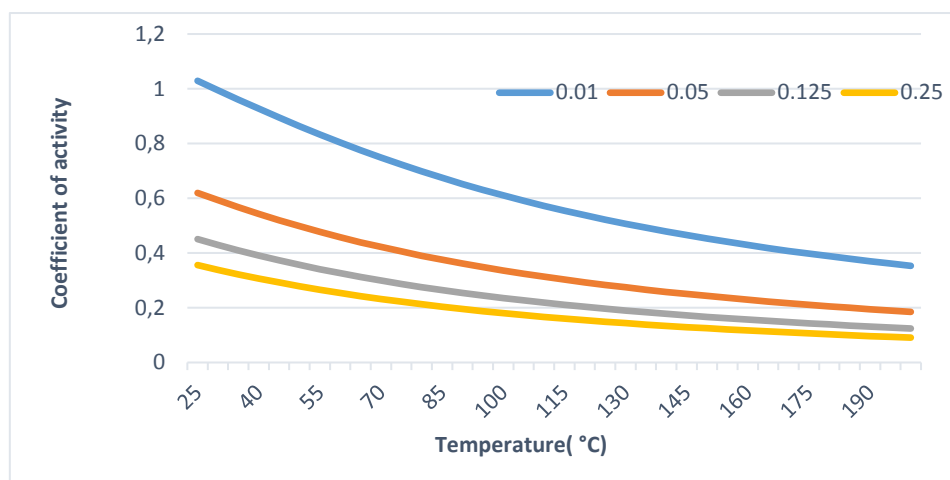
**Figure 3:** Variation in molality of H<sup>+</sup> versus of that of sulfuric acid at various temperatures.

Let  $m$  be the stoichiometric concentration in sulfuric acid, and  $m_H$  the concentration in ion H<sup>+</sup> in equilibrium.

The expression giving the balance of the sulfate ions can be written as:

$$m_H^3 + k_1 m_H^2 + (k_1 k_2 - m k_1) m_H - 2 k_1 k_2 = 0$$

The solving of this cubic equation in  $m_H$  gives a concentration in ion H<sup>+</sup> at equilibrium for 25 °C approximately with a concentration of ions H<sup>+</sup> equals to 0.135M. The stoichiometric concentration  $m$  being equal to 0.125M.



**Figure 4:** Evolution of the activity coefficient of the  $\text{H}_2\text{SO}_4$  as a function of the temperature between 0.01 and 0.25.

The comparison with the value extracted from Figure.1 for the same stoichiometric concentration gives a value of the concentration in ion  $\text{H}^+$  equal to 0.1566519M i.e. a difference of 16.038% compared to the value of this same concentration obtained without taking into account the activities.

Figure 4 gives the values of the activity coefficient of the  $\text{H}_2\text{SO}_4$  in dependence of the temperature for the molalities ranging from 0.01 to 0.25  $\text{mol.kg}^{-1}$ . Whatever the molality, the coefficient of activity  $\gamma_{\pm}$  for the  $\text{H}_2\text{SO}_4$  decreases when the temperature increases.

#### 4. CONCLUSION

In the temperature range considered: 25 to 200°C, this study allows the determination of concentration in ion  $\text{H}^+$  and the coefficients of activity of different kinds of the  $\text{H}_2\text{SO}_4$  alone in solution. In an aqueous solution of  $\text{H}_2\text{SO}_4$ , the species reacting are  $\text{H}^+$ ,  $\text{HSO}_4^-$  and  $\text{SO}_4^{2-}$ . We can consider that the  $\text{H}_2\text{SO}_4$  with the two kinds of anions  $\text{HSO}_4^-$  and  $\text{SO}_4^{2-}$  and the cations  $\text{H}^+$ , constitute a mixed electrolyte for the equation of Pitzer.

The solving of the expression giving the balance of the sulfate ions gives a concentration in ion  $\text{H}^+$  at equilibrium for 25 °C approximately with a concentration of ions  $\text{H}^+$  equals to 0.135M. The stoichiometric concentration  $m$  being equal to 0.125M. The comparison with the value extracted from figure for the same stoichiometric concentration gives a value of the concentration in ion  $\text{H}^+$  equal to 0.1566519M i.e., a difference of 16.038% compared to the value of this same concentration obtained without taking into account the activities.

It can be noted that the temperature does not any influence on the calculated molality in ion  $\text{H}^+$  as a function of the molality in  $\text{H}_2\text{SO}_4$  at 25°C.

For molality higher than 1  $\text{mol.kg}^{-1}$  and temperatures within 170-200°C, the molality in ion  $\text{H}^+$  passes by a minimum.

The coefficient of activity  $\gamma_{\pm}$  for the  $\text{H}_2\text{SO}_4$  decreases when the temperature increases.

The calculation results are in good agreement with those found in literature.

#### 5. REFERENCES

- Campbell DM, Millero FJ, Roy R, Roy L, Lawson M, Vogel KM, et al. The standard potential for the hydrogen-silver, silver chloride electrode in synthetic seawater. *Mar Chem.* 1993 Dec 1;44(2-4):221–33. Available from: [<DOI>](#)
- Waters JF, Millero FJ. The free proton concentration scale for seawater pH. *Mar Chem.* 2013 Feb 20;149:8–22. Available from: [<DOI>](#)
- Clegg SL, Whitfield M. A chemical model of seawater including dissolved ammonia and the stoichiometric dissociation constant of ammonia in estuarine water and seawater from  $-2$  to  $40^\circ\text{C}$ . *Geochim Cosmochim Acta.* 1995 Jun 1;59(12):2403–21. Available from: [<DOI>](#)
- Chihara K, Suzuki; Finlayson M, Knaebel BA, Hill; Knoblauch FB, Mitchell K, Shendalman; Shendalman LH, et al. An NRTL model for representation and prediction of deviation from ideality in electrolyte solutions compared to the models of Chen (1982) and Pitzer (1973). *AIChE Journal [Internet].* 1985 Mar 1 [cited 2023 May 23];31(3):392–9. Available from: [<URL>](#)
- Ball F -X, Planche H, Fürst W, Renon H. Representation of deviation from ideality in

concentrated aqueous solutions of electrolytes using a mean spherical approximation molecular model. *AICHE Journal* [Internet]. 1985 Aug 1 [cited 2023 May 23];31(8):1233–40. Available from: [<URL>](#)

6. Pitzer KS, Roy RN, Silvester LF. Thermodynamics of Electrolytes. 7. Sulfuric Acid. *J Am Chem Soc* [Internet]. 1977 [cited 2023 May 23];99(15):4930–6. Available from: [<URL>](#)

7. Pitzer KS, Mayorga G. Thermodynamics of electrolytes. III. Activity and osmotic coefficients for 2-2 electrolytes. *J Solution Chem* [Internet]. 1974 Jul [cited 2023 May 23];3(7):539–46. Available from: [<URL>](#)

8. Bradley DJ, Pitzer KS. Thermodynamics of electrolytes. 12. Dielectric properties of water and Debye-Hückel parameters to 350 °C and 1 kbar. *Journal of Physical Chemistry* [Internet]. 1979 [cited 2023 May 23];83(12):1599–603. Available from: [<URL>](#)

9. Rogers PSZ, Pitzer KS. High-temperature thermodynamic properties of aqueous sodium sulfate solutions. *Journal of Physical Chemistry* [Internet]. 1981 [cited 2023 May 23];85(20):2886–95. Available from: [<URL>](#)

10. Pitzer KS, Raton B, Arbor A, London B. Activity Coefficients in Electrolyte Solutions 2nd Edition. Available from: [<URL>](#)

11. Greenberg JP, Møller N. The prediction of mineral solubilities in natural waters: A chemical equilibrium model for the Na-K-Ca-Cl-SO<sub>4</sub>-H<sub>2</sub>O system to high concentration from 0 to 250°C. *Geochim Cosmochim Acta*. 1989 Oct 1;53(10):2503–18. Available from: [<DOI>](#)

12. Zemaitis Jr JF, Clark DM, Rafal M, Scrivner NC. Handbook of Aqueous Electrolyte Thermodynamics: Theory & Application. Available from: [<URL>](#)

13. Harvie CE, Weare JH. The prediction of mineral solubilities in natural waters: the Na-K-Mg-Ca-Cl-SO<sub>4</sub>-H<sub>2</sub>O system from zero to high concentration at 25° C. *Geochim Cosmochim Acta*. 1980 Jul 1;44(7):981–97. Available from: [<DOI>](#)

14. Archer DG. Thermodynamic Properties of the NaCl+H<sub>2</sub>O System I. Thermodynamic Properties of NaCl(cr). Aqueous Sodium Chloride Solutions *Journal of Physical and Chemical Reference Data* [Internet]. 1992 [cited 2023 May 23];21:15. Available from: [<DOI>](#)

15. Pitzer KS, Simonson JM. Thermodynamics of multicomponent, miscible, ionic systems: Theory and equations. *Journal of Physical Chemistry* [Internet]. 1986 [cited 2023 May 23];90(13):3005–9. Available from: [<URL>](#)

16. Sippola H. Critical evaluation of the 2nd dissociation constants for aqueous sulfuric acid. *Thermochim Acta*. 2012 Mar 20;532:65–77. Available from: [<DOI>](#)

17. Thermodynamic Dissociation Constant of

the Bisulfate Ion from Raman and Ion Interaction Modeling Studies of Aqueous Sulfuric Acid at Low Temperatures | *The Journal of Physical Chemistry A* [Internet]. [cited 2023 May 23]. Available from: [<URL>](#)

18. Pitzer KS. Activity Coefficients in Electrolyte Solutions. Activity Coefficients in Electrolyte Solutions. 2018 May 4;

19. Que H, Song Y, Chen CC. Thermodynamic Modeling of the Sulfuric Acid–Water–Sulfur Trioxide System with the Symmetric Electrolyte NRTL Model. *J Chem Eng Data* [Internet]. 2011 Apr 14 [cited 2023 May 23];56(4):963–77. Available from: [<DOI>](#)

20. Sippola H. Thermodynamic modelling of concentrated sulfuric acid solutions. *Calphad*. 2012 Sep 1;38:168–76. Available from: [<DOI>](#)

21. Sippola H, Taskinen P. Thermodynamic properties of aqueous sulfuric acid. *J Chem Eng Data* [Internet]. 2014 Aug 14 [cited 2023 May 23];59(8):2389–407. Available from: [<URL>](#)

22. Bouchkira I, Latifi AM, Khmar L, Benjelloun S. Global sensitivity based estimability analysis for the parameter identification of Pitzer's thermodynamic model. *Reliab Eng Syst Saf*. 2021 Mar 1;207:107263. Available from: [<DOI>](#)

