

Effect of Co-B Catalyst Synthesized in Methanol on the Hydrolysis of Sodium Borohydride

Mehmet Sait İZGİ¹, Ömer ŞAHİN¹, Erhan ONAT,² Sabit HOROZ³

ABSTRACT: In this study, the effect of parameters such as treatment time, temperature, amount of catalyst and the NaBH₄ concentration were investigated on the catalytic activity of Co-B catalyst synthesized in methanol and the optimum conditions were determined. The maximum hydrogen generation rate was found as 2200 mLH₂/min.g.catalyst for Co-B catalyst synthesized in methanol while 600 mLH₂/min.g.catalyst was found for Co-B catalyst synthesized in water. The activation energy was found as 34.694 kJ/mol for Co-B catalyst prepared in methanol. Consequently, our results suggest that the cold plasma treatment with different conditions can be used as a promising technique to enhance the catalytic activity of Co-B catalyst prepared in the methanol.

Keywords: Co-B catalyst, cold plasma treatment, methanol, sodium borohydride.

Metanolde Sentezlenen Co-B Katalizörün Sodyum Hidrolizi Üzerine Etkisi

ÖZET: Bu çalışmada, metanol içinde sentezlenen Co-B katalizörünün etkinliğini arttırmak için alternatif bir yöntem olarak soğuk bir plazma yöntemi seçilmiştir. İşlem süresi, sıcaklık, katalizör miktarı ve NaBH₄ konsantrasyonları gibi parametrelerin Co-B katalizörün katalitik aktivitesi üzerindeki etkisi araştırılmış ve optimum koşullar belirlenmiştir. Maksimum hidrojen üretim oranı, metanolde sentezlenen Co-B katalizörü için 2200 mLH₂/min.g. katalizör olarak bulunurken, suda sentezlenen Co-B katalizörü için 600 mLH₂/min.g. katalizör olarak bulunmuştur. Metanolde hazırlanan Co-B katalizörü için aktivasyon enerjisi 34.694 kJ/mol olarak belirlenmiştir. Sonuç olarak, sonuçlarımız, farklı koşullardaki soğuk plazma işleminin, metanolde hazırlanan Co-B katalizörünün katalitik aktivitesini arttırmak için umut verici bir teknik olarak kullanılabileceğini göstermektedir.

Anahtar Kelimeler: Co-B katalizörü, soğuk plazma işlemi, metanol, sodyum borhidür.

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INTRODUCTION

Hydrogen can be produced using a wide variety of techniques without the emission of pollutants and greenhouse gases, and as technology improves, production costs are targeted to reach levels comparable to other sources. Nowadays, hydrogen is produced by catalytic conversion from natural gas or hydrolysis of water. However, these methods are not fast enough and flexible for portable PEM fuel cells. For this reason, small-scale hydrogen generator systems, which can quickly supply pure hydrogen, are gaining importance (Fakeeha et al., 2016; Ismaev et al., 2016; Izgi et al., 2017; Gupta et al., 2005; Balat, 2008; Niwa et al., 2012).

Chemical hydrides which are stable, non-combustible, and non-toxic in nature, have 10.8% of hydrogen storage capacity (Sahin et al., 2015; Liang et al., 2008; Qiming et al., 2012). Sodium borohydride (NaBH_4) is one of these chemical hydrides. The hydrolysis of NaBH_4 with water was shown by Schlesinger et al (Schlesinger et al., 1953).

Heterogeneous and homogeneous catalysts such as Ni (Ingersoll et al., 2007), Co (Fernandes et al, 2009), Co-B (Izgi, 2015), Co-B-Cr (Izgi et al., 2015), Co-Cu-B (Izgi et al., 2016), Co-B-P (Sahin et al., 2016) and Co-B-F (Cho et al., 2007) were used to carry out the process of NaBH_4 . Unlike the homogeneous catalysts, the heterogeneous catalysts have some advantages such as longer operation of catalyst, easy separation of catalyst from the sodium meta-borate (NaBO_2) solution, and there is no formation of other byproducts apart from NaBO_2 during the process (Fakeeha et al, 2016; Saka et al., 2015; Benitez et al, 1997; Isha et al., 2012;). Among these catalysts, the Co-B is a good candidate for hydrogen generation owing to its high activity and low cost (Krishann et al., 2009; Ozdemir et al., 2013; Coskuner et al., 2014).

Generally, the water has been used as solvolytic agent for generation hydrogen from the hydrolysis of NaBH_4 . However, during past decades, some reports showed that methanol can be used as solvolytic solvent as an alternative to the use of water (Schlesinger et al., 1953; Fernandes et al., 2009; Ocon et al., 2013; Kim et al., 2004).

In our present study, the methanol was used as solvolytic agent for generation hydrogen from the hydrolysis of NaBH_4 for the first time. Before the cold plasma treatment was applied, 10% of NaOH concentration was determined as the most efficient concentration of NaOH on the NaBH_4 hydrolysis of the Co-B catalyst synthesized in the methanolic medium. The effect of parameters such as treatment time, temperature, amount of catalyst and the NaBH_4 concentration were investigated on the catalytic activity of Co-B catalyst and the optimum conditions were determined. The Co-B catalyst was characterized by XRD, SEM, BET and FTIR measurements. Consequently, the results suggest that the methanol can be used as an alternative solvent to increase the activity of Co-B catalyst.

MATERIAL AND METHOD

Preparation

The chemical reduction method was used to synthesize Co-B catalyst for production of hydrogen from sodium borohydride solutions. $\text{CoCl}_2 \cdot 6\text{H}_2\text{O}$ as Co source and NaBH_4 as B source were utilized for preparation of Co-B catalyst in the methanol. In typical the chemical reduction method; After about 1.25 g of $\text{CoCl}_2 \cdot 6\text{H}_2\text{O}$ was dissolved in 50 mL of methanol, this solution, which was placed in a 250 mL three-necked balloon, was cooled to about 2-4 °C and 1.25 g of sodium borohydride dissolved in methanol was slowly added drop wise with vigorous stirring. Once a black precipitate was obtained, it was washed several times with absolute ethanol to remove foreign substances in the precipitate. The final product was dried in N_2 at 110 °C for 8 hours to obtain Co-B catalyst.

The cold plasma treatment was applied on the Co-B catalyst after the synthesis process was completed. The effect of parameters such as treatment time (0, 10 min, 20 min, and 30 min), temperature (30 °C, 40 °C, 50 °C and 60 °C), and amount of catalyst (0.0125g, 0.025g, 0.05g, 0.75g, 0.25g) were investigated on the catalytic activity of Co-B catalyst and the optimum conditions were determined.

Characterization

X-ray diffraction (XRD on a Bruker D8 Advance X-ray diffractometer with Cu K α source and scanning electron microscope (SEM) (JEOL JSM 5800) were used to analyze structural and morphological properties, respectively. The porous properties of catalyst were examined using N₂ adsorption

studies. The measurements were carried out on Micromeritics ASAP 2000 with adsorptive and desorptive apparatus and the Co-B catalyst were pretreated in vacuum at 350 °C for 20 h before the measurements. The surface area was calculated from the isotherms using the Brunauer Emmette Teller (BET) equation.

RESULT AND DISCUSSIONS

Effect of Solvent Type

In this study, methanol and water were used as the reducing medium for the Co-B catalyst. The reason of using different solvents is to see how

different solvent environments affect the catalytic activity and particle size of the catalyst. The time-dependent change in hydrogen gas volumes obtained using these catalysts in the hydrolysis of NaBH₄ catalysts is given in Figure 1.

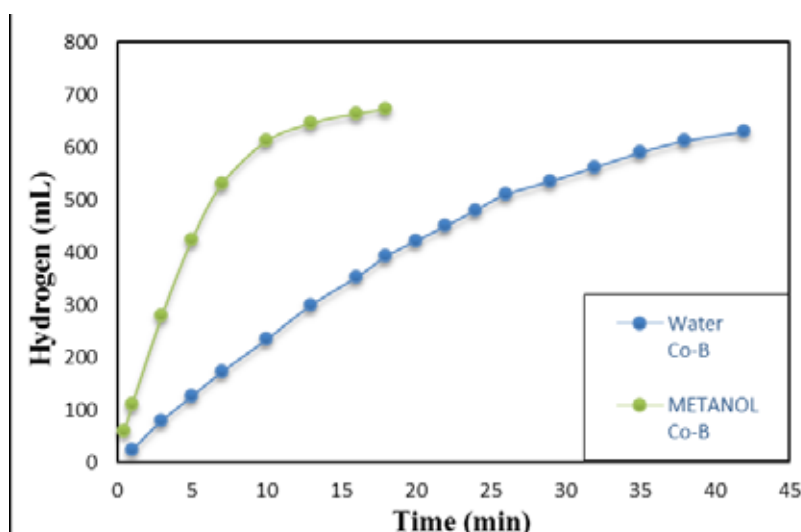


Figure 1. The effect of solvent type on the hydrolysis of NaBH₄ with Co-B catalyst synthesized in different solvents (NaOH concentration: 10%, catalyst amount: 25 mg, NaBH₄ concentration: 2.5%, reaction temperature: 30 °C).

As can be seen in Figure 1, when methanol was used as the reducing medium of the reaction catalyst, the reaction was completed in 20 minutes with the same temperature and amount of catalyst while water was used as the solvent, the hydrolysis with the catalyst obtained was completed in 40 minutes. Thus, it has been determined that the most effective catalyst for the hydrolysis of NaBH₄ is the Co-B catalyst synthesized in the methanol environment.

Effect of NaOH Concentration

Since NaBH₄ spontaneously degrades, NaOH should be used to stabilize the environment. In this regard, NaOH was used at different concentrations in the initial environment of hydrolysis to provide stability of the NaBH₄. The most effective NaOH concentration on the NaBH₄ hydrolysis of the Co-B catalyst synthesized in the methanolic medium was determined to be 10% as shown in Figure 2.

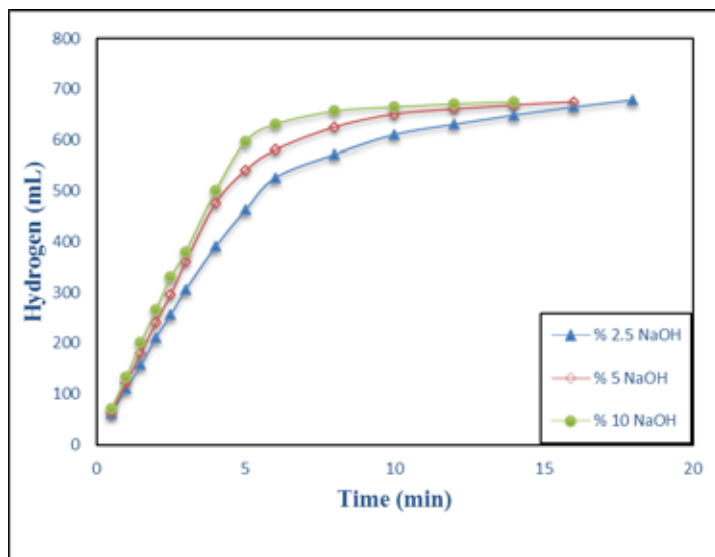


Figure 2. Effect of Co-B catalyst synthesized in methanol in NaBH_4 hydrolysis at different NaOH concentrations (30 °C, 2.5% NaBH_4 , 25 mg of catalyst, 10 mL of solution).

Effect of different amounts of Co-B catalyst

The data for experiments in which the effect of different amounts of catalyst (12.5-75 mg) on the hydrolysis of NaBH_4 was examined with the Co-B catalyst

synthesized in the methanolic medium being the same as the variables used in previous experiments (NaOH concentration, NaBH_4 percentage, temperature, solution volume) are given in Figure 3.

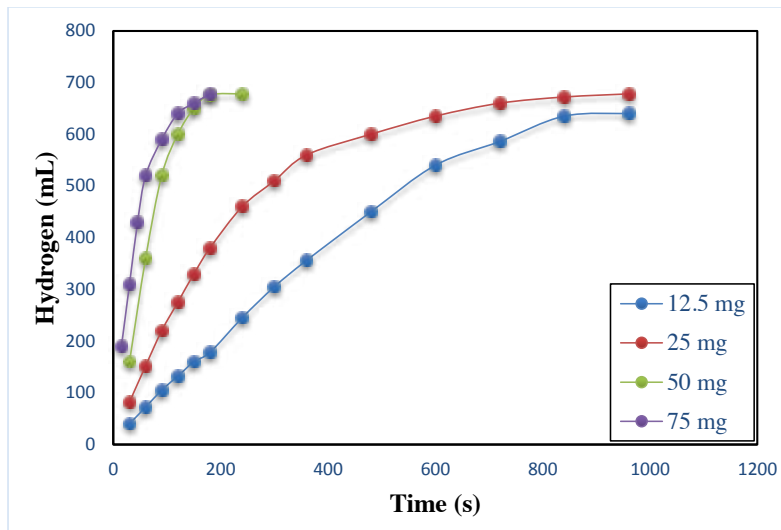


Figure 3. Effect of different catalyst amounts of Co-B catalyst synthesized in methanol on NaBH_4 hydrolysis (30 °C, 2.5% NaBH_4 , 10% NaOH, 10 mL solution).

As shown in Figure 3, hydrolysis of the NaBH_4 completed in a shorter time with the increasing amount of catalyst. It can be explained that there is no connection between the amount of catalyst and the rate of hydrogen production. It can be said that only the amount of NaBH_4 per unit catalyst is caused by the reduction in the NaBH_4

concentration, depending on the amount of catalyst that is increasing; This depends on the increasing amount of catalyst.

Effect of NaBH_4 Concentration

Figure 4 demonstrates effect of NaBH_4 concentration on the hydrolysis of NaBH_4 .

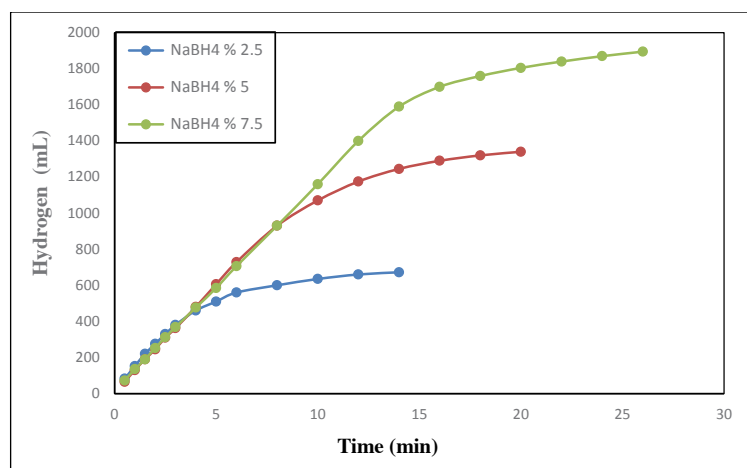


Figure 4. Effect of sodium borohydride concentrations on NaBH₄ hydrolysis with Co-B catalyst synthesized in methanol (NaOH concentration: 10%, catalyst amount: 25 mg, reaction temperature: 30 °C).

As the NaBH₄ concentration rises, the rate of hydrogen production steadily increases. The possible reason for this is related to the hydrogen content in NaBH₄. With increasing NaBH₄ concentration, the hydrogen content is risen and accordingly the hydrogen production rate is increased.

Hydrogen production at different NaBH₄ concentration confirms this interpretation. Because the rate of hydrogen production at 2.5% NaBH₄ concentration was 1920 mLH₂/min.g.catalyst while the rate

of hydrogen production at 7.5% concentration was 3116 mLH₂/min.g.catalyst.

Effect of Reaction Temperature”

As can be seen in Figure 5, the NaBH₄ hydrolysis reaction rate of the Co-B catalyst at different temperatures increases as the temperature of the solution medium increases with the same amount of catalyst and the same NaBH₄ concentration. It was observed that the change of the hydrogen gas volume with time is not linear at different temperatures.

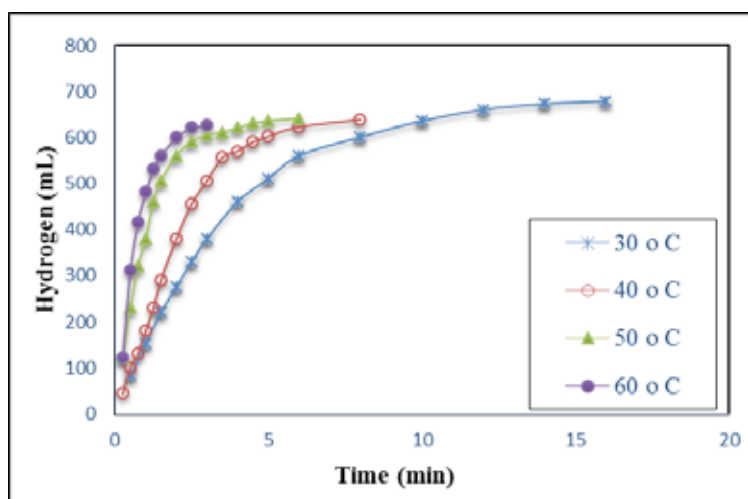


Figure 5. Effect of temperatures on hydrolysis of NaBH₄ with Co-B catalyst synthesized in methanolic medium (NaOH concentration: 10%, catalyst amount: 25 mg, NaBH₄ concentration: 2.5%).

The degree of reaction was determined by applying the first-order kinetic model to the effect of the behavi-

or of the Co-B catalyst synthesized in the methanolic medium on NaBH₄ hydrolysis.

$$-r_{\text{NaBH}_4} = -\frac{dC_{\text{NaBH}_4}}{dt} = kC_{\text{NaBH}_4} \quad (1)$$

If the Equation 1 was integrated, the rate of hydrogen production shown in Equation 2 was obtained.

$$\ln\left(\frac{C_{\text{NaBH}_4}(t=0)}{C_{\text{NaBH}_4}(t=t)}\right) = kt \quad (2)$$

Kinetic evaluation was performed for 30 °C, 40 °C, 50 °C and 60 °C using the Equation 2. Figure 6 indicates the variation between concentrations of NaBH₄ obtained at different temperatures and time and it was

observed that the change is linear. This shows us how the values of the first order and the reaction rate constants are suitable.

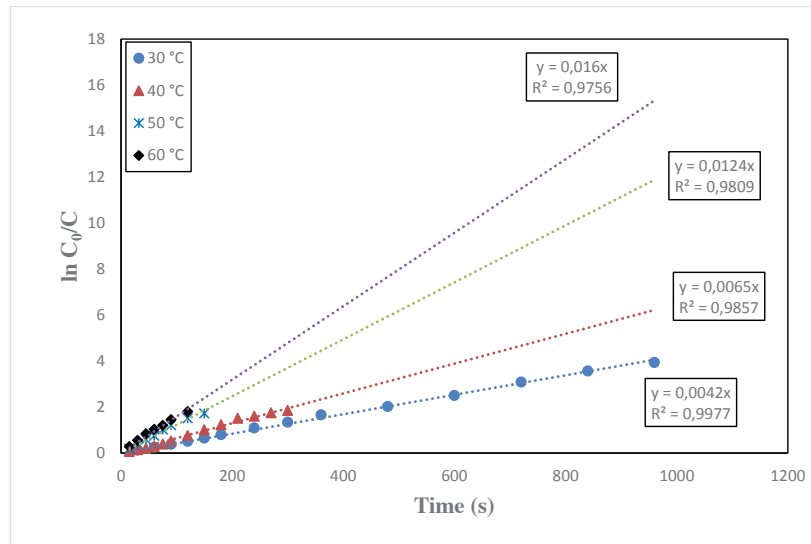


Figure 6. The first order reaction kinetics (10 mL solution, 2.5% NaBH₄, 25 mg catalyst, 10% NaOH) of Co-B catalyst synthesized in the methanolic medium.

Using the reaction rate constants obtained at different temperatures, the Arrhenius equation was deter-

mined using Equations 3 and 4 to find the activation energy for the hydrolysis reaction.

$$k = A \cdot e^{-\frac{Ea}{RT}} \quad (3)$$

If both sides (ln) are taken in order to linearize Equation 3

$$\ln k = \ln A - \frac{Ea}{RT} \quad (4)$$

When the 1/T graph was plotted against the ln k values according to Equation 4, the activation energy was found from the slope of the line

obtained in Figure 7. According to these values obtained, the activation energy was determined as 34.694 kJ/mol.

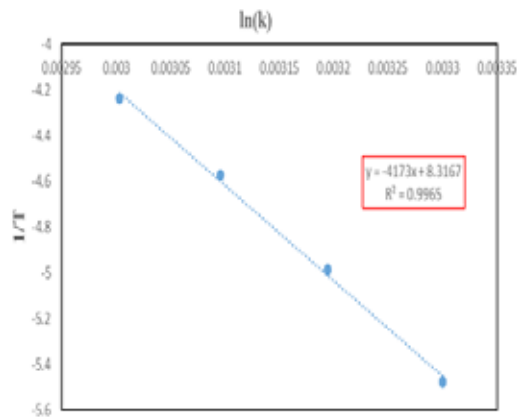


Figure 7. According to first order kinetic reaction, Arrhenius equality for the Co-B catalyst synthesized in methanol.

Characterization of Co-B catalyst synthesized in methanol and water environments

The characterization of the Co-B catalyst synthesized in water and methanol mediums was determined by BET, SEM, XRD and FT-IR analyzes, respectively.

BET characterization of Co-B catalyst

As is known, one of the important parameters affecting catalyst activity and performance is the surface area of the catalyst. Physical adsorption and desorption analyzes of our synthesized catalysts were also carried out. Only BET surface areas are given from these obtained values. The BET surface area of the Co-B catalyst synthesized with purified water was 148.248 m² / g

while the BET surface area synthesized in the methanol environment was 40.067 m² / g. The micropores for the catalyst constitute an important part of the inner surface. Macropores are needed as a transmitter to ensure that the correct diffusion is faster than micropores. The obtained results are SEM shown in Figure 8.

SEM characterization of Co-B catalyst

Figure 8 shows SEM images of Co-B catalyst synthesized in pure water and methanol. Compared to SEM images, it is clear that the grain structure is reduced with methanol. At the same time, the catalyst synthesized with methanol turns into a more regular structure and reduces agglomeration, which prevents the crystallization of the catalyst.

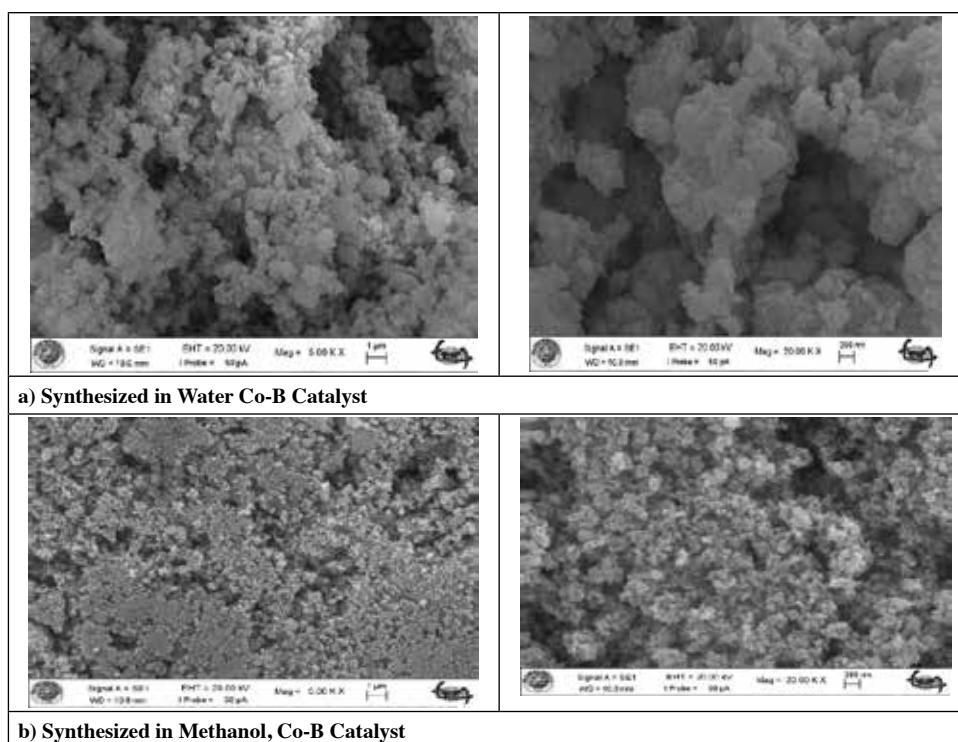


Figure 8. SEM images (a) Co-B catalyst synthesized with pure water (b) Co-B catalyst synthesized with methanol.

XRD analysis of Co-B catalyst

As shown in Figure 9, the Co-B catalyst synthesized in pure water or methanolic environment exhibits an amorphous structure in XRD analysis.

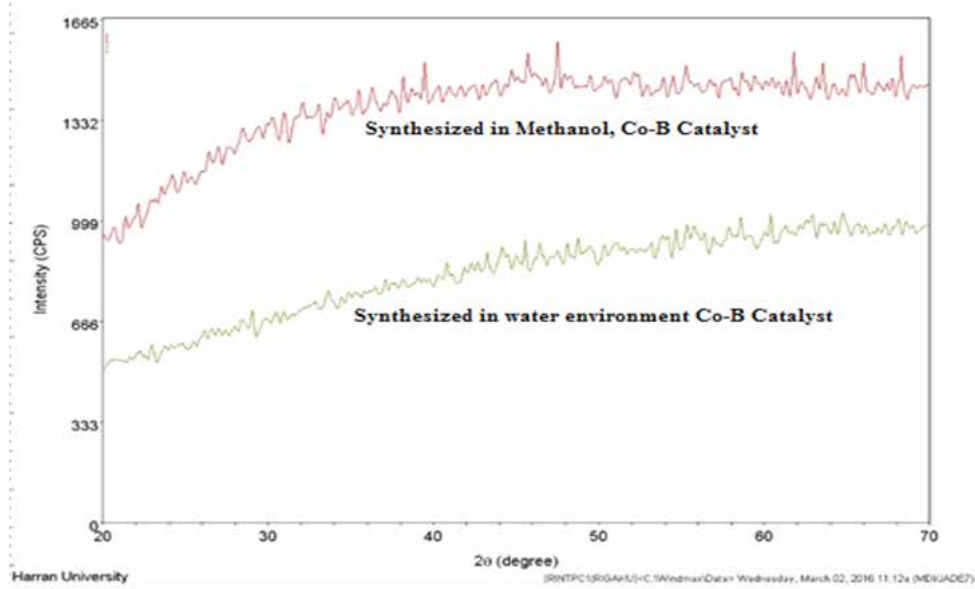


Figure 9. XRD of (a) Co-B catalyst synthesized with pure water (b) Co-B catalyst synthesized with methanol.

FT-IR spectroscopy of Co-B catalyst

Figure 10 indicates the FT-IR results for the Co-B catalyst. As seen in the figures, there is no structural change in the synthesis of Co-B catalyst in pure water and methanol environments. As a result, it can be conc-

luded that when the the Co-B catalyst is synthesized with methanol in order to increase the catalytic activity of the Co-B catalyst, only the number of micro- and meso pores of the catalyst, which does not deteriorate its chemical structure, can be increased.

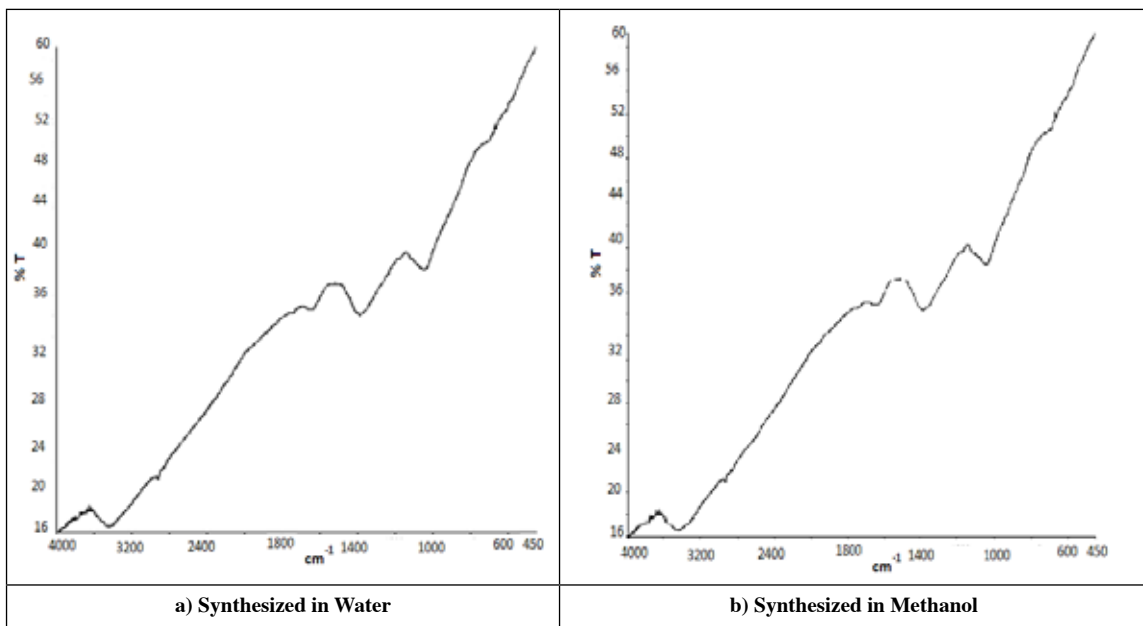


Figure 10. IR spectra of (a) Co-B catalyst synthesized with pure water (b) Co-B catalyst synthesized with methanol.

CONCLUSIONS

Co-B catalyst was successfully synthesized in water and methanol for generation hydrogen from the hydrolysis of NaBH_4 . The effect of solvolytic agent on the activity of Co-B catalyst was investigated and it was observed that the hydrogen production rate of hydrolysis reaction of NaBH_4 with Co-B catalyst prepared in the methanol is completed in shorter time compare to one is synthesized in the water. The cold plasma treatment was applied on the Co-B catalyst which was prepared in methanol solvent. Before the cold plasma treatment was applied, 10% of NaOH concentration was determined as the most efficient concentration of NaOH on the NaBH_4 hydrolysis of the Co-B catalyst synthesized in the methanolic medium. The effect of parameters such as treatment time, temperature, amount of catalyst and the NaBH_4 concentration were investigated on the catalytic activity of Co-B catalyst and the optimum

conditions were determined. The hydrogen generation rate of Co-B catalyst synthesized in methanol is $2200 \text{ mLH}_2/\text{min.g.catalyst}$, while the value of the catalyst synthesized in pure water is $600 \text{ mLH}_2/\text{min.g.catalyst}$. At the same time, the initial rates of these values at $t = 0$ were $4635 \text{ mLH}_2/\text{min.g.catalyst}$ in methanol and the hydrogen production rate of Co-B catalyst in pure water was $1063 \text{ mLH}_2/\text{min.g.catalyst}$ at $t = 0$. The activation energy was determined as 34.694 kJ/mol for Co-B catalyst prepared in methanol. It can be concluded that the cold plasma treatment may be used in the hydrogen generation from hydrolysis of NaBH_4 in the presence of Co-B catalyst prepared in methanol.

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