

INVESTIGATION OF LORENTZ FORCE EFFECT ON STEADY NANOFLUID FLOW AND HEAT TRANSFER THROUGH PARALLEL PLATES

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ABSTRACT

In this paper Lorentz force effect on steady fluid flow and heat transfer of nanofluid is examined. The nanofluid is transported through horizontal parallel plates with magnetic flux of uniform density acting perpendicular to the plates. The effects of thermo-fluidic parameters such as Schmidt number, viscosity and magnetic parameter on flow and heat transfer are presented. Other important heat and mass transfer parameters such as Nusselt and Sherwood numbers practically relevant were also studied. Obtained results from analytical solutions shows quantitative increase of Magnetic parameter varied within the range of 1-4 depicts increasing temperature distribution. Also results when compared with past literatures forms good agreement. Therefore study provides a good emphasis for the advancements of Nano fluidics such as micro mixing, friction reduction, energy conservation, and biological samples.

Keywords: *Steady Flow, Nanofluid, Horizontal Plates, Lorentz Force, Homotopy Perturbation Method*

INTRODUCTION

The transport of fluid through parallel surfaces has become increasingly high in most industrial and manufacturing applications today such as power transmission, polymer processing and heat exchangers. Owing to its efficient flow and heat transfer of fluids to its required destination. As energy pricing has become a significant factor in determining the mode of fluid transport, the need to manage heat transfer efficiently as led to renewed effort by scientist and engineers to research into more efficient ways of managing energy. In efforts to enhance heat transfer Abu Nada et al. [1] studied heat transfer under natural convection in horizontal concentric annuli using nanoparticles to increase heat transfer effect on the fluid flow. Heat transfer and flow over stretching sheet was investigated by Cortell [2] where study outcome reveals the influence of radiation on flow while Ellahi et al. [3] presented heat transfer of non-Newtonian fluid through two coaxial cylinders with porous media using variable viscosity, effect of heat transfer on nanoparticle under the influence of magnetism is analyzed. Mixed convection of nanofluid flow through square cavities where analyzed by Garoosi et al. [4-5] under two phase simulation without and with external heating where results show the effect of buoyancy on cavity flow. Shortly after Garoosi et al. [6] Investigated nanofluid flow in heat exchangers adopting the Buongiorno model of numerical technique, they discovered that at low Rayleigh number heat transfer decreases. Brownian motion and thermophoresis effects on slip flow of alumina/water were investigated by Malvandi and Ganji [7] where they showed effects of Nanoparticle concentration on heat transfer. Heat transfer over stretching surface was studied by Mehmood and Ali [8] presenting a three dimensional analytic solution employing the homotopy analysis method. Rashidi et al. [9] analyzed entropy generation in a rotating porous disk under steady flow condition considering the influence of magnetism with results revealing effect of entropy on temperature distribution. Rashidi et al. [10] in the bid to control wake and vortex shedding later considered heat transfer around a porous obstacle. Convective surface boundary condition was used by Shehzad et al. [11] to study three dimensional flow of Jeffery fluid presenting velocity and temperature distribution using series solutions obtained from non-linear equations. Later Shehzad et al. [12-13] investigated thermal radiative effects on mixed convection of thixotropic fluid, results reveal numerical values of wall shear and heat transfer rate. Flow and heat transfer in a rotating system was investigated by Sheikholeslami et al. [14] between stretching sheet and porous surface, discussing the effects of thermo-fluidics on flow and heat transfer. Two phase simulation of nanofluid was also investigated by Sheikholeslami et al. [15] using heat line model analyzing the effect of magnetism on heat and mass transfer.

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In recent years the need to improve the thermal conductivity of fluids as led to the addition of nanoparticles into base fluid, owing to the fact that nanoparticles have higher thermal conductivities, which enhances the overall energy transport during fluid flow. Therefore this creative approach has been widely adopted by researchers in the study of flow and heat transfer [16-39]. Nanofluid displays characteristics of high heat transfer and enhanced flow character due to high thermal conductivity of nanoparticles which makes them potentially useful in medical, fuel cells and microelectronic processes.

Approximate analytical methods of solutions applied by researchers in study of the fluid flow include the perturbation method (PM), homotopy analysis method (HAM), homotopy perturbation method (HPM), adomian decomposition method (ADM) and Differential transformation method (DTM) [39-43]. Methods such as PM are limited owing to the problems of weak nonlinearities and artificial perturbation parameter which may be non-existent in practical sense. The need to find an initial condition to satisfy the boundary condition makes methods such as DTM requires computational tools such as Matlab, Maple or Mathematica in handling a solution of large parameters resulting to large computational cost and time. Lack of rigorous theories for determining the initial approximation of the HAM, its auxiliary function and parameter restricts the HAM. Also the problem of finding the adomian polynomials makes the ADM not attractive to researchers. However the homotopy perturbation method been a relatively simplistic method of solving nonlinear, coupled equations due to its highly successive and accurate approximation making it a favourable analytical technique to researchers.

Motivated by past research works, the homotopy perturbation method (HPM) is used to investigate Lorentz force effect which is a resistive magnetic force type on steady nanofluid flow and heat transfer conveyed through horizontal parallel plates.

MODEL DEVELOPMENT AND ANALYTICAL SOLUTION

Here nanofluid flows through parallel plates held horizontally against each other under steady flow condition. The plates are held at a distance h , where the x axis is along the plate and the y axis is perpendicular which is described in the physical model of problem Figure 1. The nanofluid flow along the x axis which is normal to the plate with an angular velocity. A uniform magnetic flux acts perpendicular to the axis of flow, such that the plates is held by equal but opposite force which fixes its position at reference $(0, 0, 0)$ i.e. its position remains the same. The formulation of the model development of the nanofluid is developed with respect to the above conditions following the assumptions that the fluid is incompressible, radiation heat transfer is negligible and two component mix is in thermal equilibrium. Therefore the governing equations of the system can be described as:

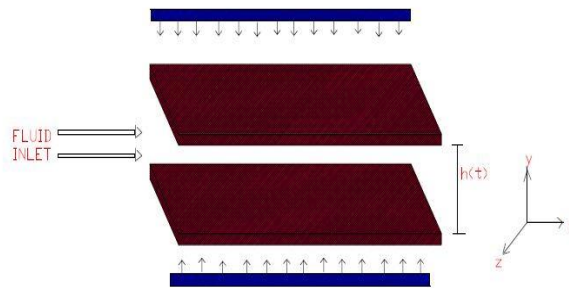


Figure 1. Physical model of problem

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0 \quad (1)$$

$$\rho_f \left(u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} \right) = -\frac{\partial p^*}{\partial x} + \mu \left(\frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} \right) - \sigma B_0^2 u \quad (2)$$

$$\rho_f \left(u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} \right) = -\frac{\partial p^*}{\partial y} + \mu \left(\frac{\partial^2 v}{\partial x^2} + \frac{\partial^2 v}{\partial y^2} \right) \quad (3)$$

$$u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} = \alpha \left(\frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} \right) + \frac{(\rho C p)_p}{(\rho C p)_f} x \left[D_B \left\{ \frac{\partial C}{\partial x} \frac{\partial T}{\partial x} + \frac{\partial C}{\partial y} \frac{\partial T}{\partial y} \right\} + (D_T / T_C) \left\{ \left(\frac{\partial T}{\partial x} \right)^2 + \left(\frac{\partial T}{\partial y} \right)^2 \right\} \right] \quad (4)$$

$$u \frac{\partial C}{\partial x} + v \frac{\partial C}{\partial y} = D_B \left(\frac{\partial^2 C}{\partial x^2} + \frac{\partial^2 C}{\partial y^2} \right) + \left(\frac{D_T}{T_0} \right) \left\{ \frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} \right\} \quad (5)$$

Taking boundary conditions as:

$$u = ax, v = 0, T = T_h, C = C_h \quad \text{at } y=0 \quad (6)$$

$$u = 0, v = 0, T = T_0, C = C_0 \quad \text{at } y=h \quad (7)$$

With the dimensionless parameters stated in the nomenclature, the dimensionless equations are given as [37]:

$$\frac{d^4 f}{d\eta^4} - R \left(\frac{df}{d\eta} \frac{d^2 f}{d\eta^2} + f \frac{d^2 f}{d\eta^2} \right) - M^2 \frac{d^2 f}{d\eta^2} = 0 \quad (8)$$

$$\frac{d^2 \theta}{d\eta^2} + \text{PrRf} \frac{d\theta}{d\eta} + Nb \frac{d\theta}{d\eta} \frac{d\phi}{d\eta} + Nt \left(\frac{d\theta}{d\eta} \right)^2 = 0 \quad (9)$$

$$\frac{d^2 \phi}{d\eta^2} + RScf \frac{d\phi}{d\eta} + \frac{Nt}{Nb} \frac{d^2 \theta}{d\eta^2} = 0 \quad (10)$$

Taking appropriate boundary condition as:

$$f = 0, \frac{df}{d\eta} = 1, \theta = 1, \phi = 1 \quad \text{at } \eta=0 \quad (11a)$$

$$f = 0, \frac{df}{d\eta} = 0, \theta = 0, \phi = 0 \quad \text{at } \eta=1 \quad (11b)$$

Important characteristics of flow, heat and mass transfer for practical relevance are reduced to skin friction, Nusselt and reduced Sherwood number which can be defined as:

$$C_{fr} = f''(1) \text{ where } C_{fr} = \frac{H^2 \sqrt{1 - \alpha t} \text{Re}_r}{r^2} C_f \quad (12a)$$

$$Nur = -\theta'(1) \text{ where } Nur = \sqrt{1 - \alpha t} Nu \quad (12b)$$

$$shr = -\phi'(1) \text{ where } shr = \sqrt{1 - \alpha t} sh \quad (12c)$$

where $\text{Re}_r = \frac{r\alpha H}{2\nu}$ is the local squeeze Reynolds number.

Principles of Homotopy Perturbation Method

The following equation is considered in explaining the fundamentals of the homotopy perturbation method [38]:

$$A(u) - f(r) = 0 \quad r \in \Omega \quad (13)$$

Utilizing the boundary condition:

$$B(u, \frac{\partial u}{\partial \eta}) = 0 \quad r \in \Gamma \quad (14)$$

A is the general differential operator, B is the boundary operator, f(r) is the analytical function and Γ is the boundary domain of Ω . Separating A into two components of linear and nonlinear terms L and N respectively. The Eq. (13) is reconstructed as:

$$L(u) + N(u) - f(r) = 0 \quad r \in \Omega \quad (15)$$

Homotopy perturbation structure takes the form:

$$H(v, p) = (1 - p)[L(v) - L(u_0)] + P[A(v) - f(r)] = 0 \quad (16)$$

where $v(r, p) : \Omega \times [0, 1] \rightarrow R$

In Eq. (16) $P \in (0, 1)$ is the embedding parameter and U_0 is taken as the initial term that satisfies boundary condition. The power series of Eq. (16) can be expressed therefore as:

$$v = v_0 + P v_1 + P^2 v_2 + P^3 v_3 + \dots \quad (17)$$

Most appropriate solution for the problem takes the form:

$$u = \lim_{p \rightarrow 1} (v_0 + P v_1 + P^2 v_2 + P^3 v_3 + \dots) \quad (18)$$

Application of the Homotopy Perturbation Method

The homotopy perturbation method (HPM) which is an analytical scheme for providing approximate solutions to the ordinary differential equations, is adopted in generating solutions to the coupled ordinary nonlinear differential equation. Upon constructing the homotopy, the Eqs. (8)- (10) can be expressed as:

$$H_1(p, \eta) = (1-p) \left[\frac{d^4 f}{d\eta^4} \right] + p \left[\frac{d^4 f}{d\eta^4} - R \left(\frac{df}{d\eta} \frac{d^2 f}{d\eta^2} + f \frac{d^2 f}{d\eta^2} \right) - M^2 \frac{d^2 f}{d\eta^2} \right] \quad (19)$$

$$H_2(p, \eta) = (1-p) \left[\frac{d^2 \theta}{d\eta^2} \right] + p \left[\frac{d^2 \theta}{d\eta^2} + PrRf \frac{d\theta}{d\eta} + Nb \frac{d\theta}{d\eta} \frac{d\phi}{d\eta} + Nt \left(\frac{d\theta}{d\eta} \right)^2 \right] = 0 \quad (20)$$

$$H_3(p, \eta) = (1-p) \left[\frac{d^2 \phi}{d\eta^2} \right] + p \left[\frac{d^2 \phi}{d\eta^2} + RScf \frac{d\phi}{d\eta} + \frac{Nt}{Nb} \frac{d^2 \theta}{d\eta^2} \right] = 0 \quad (21)$$

Taking the appropriate boundary condition as:

$$f = 0, \frac{df}{d\eta} = 1, \theta = 1, \phi = 1 \text{ at } \eta=0 \quad (22a)$$

$$f = 0, \frac{df}{d\eta} = 0, \theta = 0, \phi = 0 \text{ at } \eta=1 \quad (22b)$$

Taking power series of velocity, temperature and concentration fields yields:

$$f = P^0 f_0 + P^1 f_1 + P^2 f_2 + \dots \quad (23)$$

$$\theta = P^0 \theta_0 + P^1 \theta_1 + P^2 \theta_2 + \dots \quad (24)$$

$$\phi = P^0 \phi_0 + P^1 \phi_1 + P^2 \phi_2 + \dots \quad (25)$$

Substituting Eq. (23) into (20) and selecting at the various order yields:

$$P^0 : \frac{d^4 f_0}{d\eta^4} \quad (26)$$

$$P^1 : \frac{d^4 f_1}{d\eta^4} - \frac{d^2 f_0}{d\eta^2} M + R \frac{d^2 f_0}{d\eta^2} f_0 - \frac{d^2 f_0}{d\eta^2} \frac{df_0}{d\eta} \quad (27)$$

$$P^2 : \frac{d^4 f_2}{d\eta^4} - \frac{d^2 f_1}{d\eta^2} M + R \frac{d^2 f_0}{d\eta^2} f_1 + \frac{d^2 f_1}{d\eta^2} f_0 - \frac{df_0}{d\eta} \frac{d^2 f_1}{d\eta^2} - \frac{df_1}{d\eta} \frac{d^2 f_0}{d\eta^2} \quad (28)$$

Substituting Eq. (24) into (21) and selecting at the various order yields:

$$P^0 : \frac{d^2 \theta_0}{d\eta^2} \quad (29)$$

$$P^1 : \frac{d^2 \theta_1}{d\eta^2} + N_t \left(\frac{d\theta_0}{d\eta} \right)^2 - N_b \frac{d\theta_0}{d\eta} \frac{d\phi_0}{d\eta} + Pr Rf_0 \frac{d\theta_0}{d\eta} \quad (30)$$

$$P^2 : \frac{d^2 \theta_2}{d\eta^2} + 2N_t \frac{d\theta_0}{d\eta} \frac{d\theta_1}{d\eta} + N_b \frac{d\theta_0}{d\eta} \frac{d\phi_1}{d\eta} + N_b \frac{d\theta_1}{d\eta} \frac{d\phi_0}{d\eta} + Pr R \frac{d\theta_0}{d\eta} f_1 + Pr R \frac{d\theta_1}{d\eta} f_0 \quad (31)$$

Substituting Eq. (25) into (22) and selecting at the various order yields:

$$P^0 : \frac{d^2 \phi_0}{d\eta^2} + \left(\frac{N_t}{N_b} \frac{d^2 \theta_0}{d\eta^2} \right) \quad (32)$$

$$P^1 : \frac{d^2 \phi_1}{d\eta^2} + \left(\frac{N_t}{N_b} \frac{d^2 \theta_1}{d\eta^2} \right) - RSc \frac{d\phi_0}{d\eta} f_0 \quad (33)$$

$$P^2 : \frac{d^2 \phi_2}{d\eta^2} + \frac{N_t}{N_b} \frac{d^2 \theta_2}{d\eta^2} + RSc \frac{d\phi_0}{d\eta} f_1 + RSc \frac{d\phi_1}{d\eta} f_0 \quad (34)$$

Taking leading order boundary condition as:

$$f_0 = 0, \frac{df_0}{d\eta} = 1, \theta_0 = 1, \phi_0 = 1 \text{ at } \eta=0 \quad (35a)$$

$$f_0 = 0, \frac{df_0}{d\eta} = 0, \theta_0 = 0, \phi_0 = 0 \text{ at } \eta=1 \quad (35b)$$

Simplifying Eq. (26) applying the boundary condition Eq. (35) yields:

$$f_0 = \eta^3 - 2\eta^2 + \eta \quad (36)$$

Simplifying Eq. (29) applying the boundary condition Eq. (35) yields:

$$\theta_0 = 1 - \eta \quad (37)$$

Simplifying Eq. (32) applying the boundary condition Eq. (35) yields:

$$\phi_0 = 1 - \eta \quad (38)$$

Taking the first order boundary condition as:

$$f_1 = 0, \frac{df_1}{d\eta} = 1, \theta_1 = 1, \phi_1 = 1 \text{ at } \eta=0 \quad (39a)$$

$$f_1 = 0, \frac{df_1}{d\eta} = 0, \theta_1 = 0, \phi_1 = 0 \text{ at } \eta=1 \quad (39b)$$

Simplifying Eq. (27) and applying the first order boundary condition Eq. (39) yields:

$$f_1 = \frac{17R\eta^7}{420} - \frac{5R\eta^6}{36} - \frac{R\eta^8}{280} - \eta^4 \left(\frac{M}{6} + \frac{R}{6} \right) + \eta^5 \left(\frac{M}{20} + \frac{13R}{60} \right) - \frac{\eta^2}{2} \left(\frac{2M}{15} + \frac{R}{84} \right) + \frac{\eta^3}{6} \left(\frac{11M}{10} + \frac{23R}{210} \right) \quad (40)$$

Simplifying Eq. (30) applying the first order boundary condition Eq. (39) yields:

$$\theta_1 = \frac{\text{Pr } R\eta^5}{20} - \frac{\text{Pr } R\eta^4}{6} + \frac{\text{Pr } R\eta^3}{6} + \left(-\frac{N_b}{2} - \frac{N_t}{2} \right) \eta^2 + \left(\frac{N_b}{2} + \frac{N_t}{2} - \frac{\text{Pr } R}{20} \right) \eta \quad (41)$$

Simplifying Eq. (33) applying the first order boundary condition Eq. (39) yields:

$$\phi_1 = \left(\frac{RSc}{6} - \frac{N_t \text{Pr } R}{20N_b} \right) \eta^5 + \left(\frac{N_t \text{Pr } R}{6N_b} - \frac{RSc}{6} \right) \eta^4 + \left(\frac{RSc}{6} - \frac{N_t \text{Pr } R}{6N_b} \right) \eta^3 + \left(\frac{N_t}{2} + \frac{N_t^2}{2N_b} \right) \eta^2 + \left(\frac{N_t \text{Pr } R}{20N_b} - \frac{RSc}{20} - \frac{N_t}{2} - \frac{N_t^2}{2N_b} \right) \eta \quad (42)$$

The coefficient p^2 for $f(\eta), \theta(\eta)$ and $\phi(\eta)$ in Eqs. (28), (31) and (34) were too long to be mentioned here but it is expressed graphically in all the results and in the result validation, Table 1. Therefore substituting eq. (36) and (40) into the power series Eq. (23) yields:

$$f = \eta^3 - 2\eta^2 + \eta + \frac{17R\eta^7}{420} - \frac{5R\eta^6}{36} - \frac{R\eta^8}{280} - \eta^4 \left(\frac{M}{6} + \frac{R}{6} \right) + \eta^5 \left(\frac{M}{20} + \frac{13R}{60} \right) - \frac{\eta^2}{2} \left(\frac{2M}{15} + \frac{R}{84} \right) + \frac{\eta^3}{6} \left(\frac{11M}{10} + \frac{23R}{210} \right) + \dots \quad (43)$$

Similarly substituting the Eqs. (37) and (41) into the power series Eq. (24) can be expressed as:

$$\theta = 1 - \eta + \frac{\text{Pr} R \eta^5}{20} - \frac{\text{Pr} R \eta^4}{6} + \frac{\text{Pr} R \eta^3}{6} + \left(-\frac{N_b}{2} - \frac{N_t}{2} \right) \eta^2 + \left(\frac{N_b}{2} + \frac{N_t}{2} - \frac{\text{Pr} R}{20} \right) \eta + \dots \quad (44)$$

Also the Eqs. (38) and (42) upon substituting into the power series (25) is expressed as:

$$\phi = 1 - \eta + \left(\frac{RSc}{6} - \frac{N_t Pr R}{20 N_b} \right) \eta^5 + \left(\frac{N_t Pr R}{6 N_b} - \frac{RSc}{6} \right) \eta^4 + \left(\frac{RSc}{6} - \frac{N_t Pr R}{6 N_b} \right) \eta^3 + \left(\frac{N_t}{2} + \frac{N_t^2}{2 N_b} \right) \eta^2 + \left(\frac{N_t Pr R}{20 N_b} - \frac{RSc}{20} - \frac{N_t}{2} - \frac{N_t^2}{2 N_b} \right) \eta + \dots \quad (45)$$

Table 1. Comparison of values for temperature and concentration when M=R=1, Ec=Pr=Sc=N_t=N_b=0.1, Pr=10

η	θ(η)			φ(η)		
	Sheikholeslami et al. [37]	Present work	Error %	Sheikholeslami et al. [37]	Present work	Error %
0	1.0000	1.0000	0.0000	1.0000	1.0000	0.0000
0.1	0.8562	0.8566	0.0004	0.9426	0.9429	0.0003
0.2	0.7209	0.7213	0.0004	0.8776	0.8779	0.0003
0.3	0.5590	0.5993	0.0003	0.7994	0.7996	0.0002
0.4	0.4912	0.4916	0.0004	0.7069	0.7072	0.0003
0.5	0.3954	0.3960	0.0004	0.6024	0.6027	0.0003
0.6	0.3094	0.3097	0.0003	0.4888	0.4891	0.0003
0.7	0.2293	0.2296	0.0003	0.3691	0.3695	0.0004
0.8	0.1524	0.1527	0.0003	0.2462	0.2467	0.0003
0.9	0.0763	0.0767	0.0004	0.1225	0.1229	0.0004
1.0	-0.000	-0.000	0.0000	-0.000	-0.000	0.0000

RESULTS AND DISCUSSION

The result obtained from the analytical solutions using the HPM is discussed in this section. As observed the validity of results when compared with solutions obtained in literature forms satisfactory agreement as depicted in Table 1.0. Effect of parameters on flow, heat transfer and concentration are reported graphically. With thermal fluidic parameters at various values on the velocity, temperature and concentration profile are presented. The Figure 2 shows the effect of viscosity parameter (R) on the velocity distribution, as depicted as R increases the velocity distribution increases slightly due to increase in fluid activation energy causing an increase in fluid motion with maximum effect near the lower plate. While it is shown from Figure 3 that velocity distribution decreases at increasing numerical values of Lorentz force or magnetic parameter (M) which can be physically explained by the decrease in momentum boundary layer thickness caused by magnetic force field whose effect is maximum towards the lower plate and falls rapidly towards the upper plate.

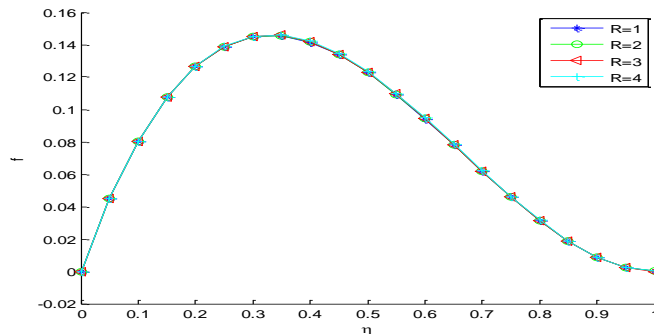


Figure 2. Effect of viscosity parameter (R) on velocity profile when Pr=10, Sc=N_t=N_b=0.1 and M=1

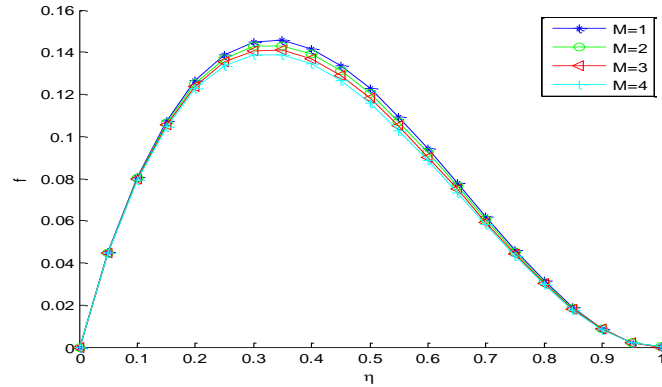


Figure 3. Effect of Magnetic parameter (M) on velocity profile when $Pr=10, Sc=N_t=N_b =0.1$ and $R=1$

The effect of increasing values of viscosity parameter (R) is demonstrated in Figure 4. It is observed that temperature distribution decreases at increasing R as a result of enhanced fluid motion causing rapid heat dissipation with the temperature profile maximum at the lower and minimum at the upper plate respectively. Magnetic parameter (M) effect on temperature distribution is clearly illustrated in Figure 5 which shows quantitative increase in M result in increasing thermal boundary layer thickness represented by slight increase in temperature. Increasing effect of thermophoretic parameter (N_t) on temperature distribution is seen in Figure 6 which depicts an increase in temperature profile while Brownian parameter (N_b) effect on temperature distribution is seen in Figure 7 where it is illustrated that increasing N_b gives a corresponding increase in temperature distribution.

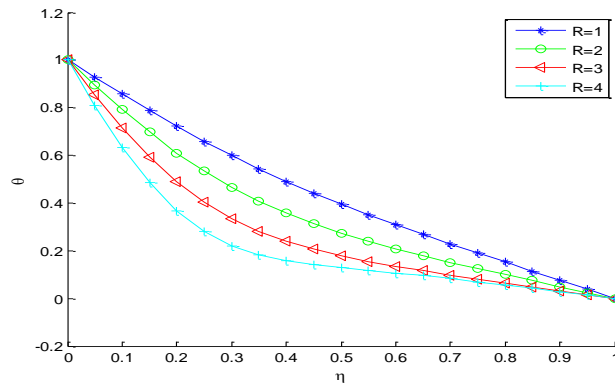


Figure 4. Effect of viscosity parameter (R) on Temperature profile when $Pr=10, Sc=N_t=N_b =0.1$ and $M=1$

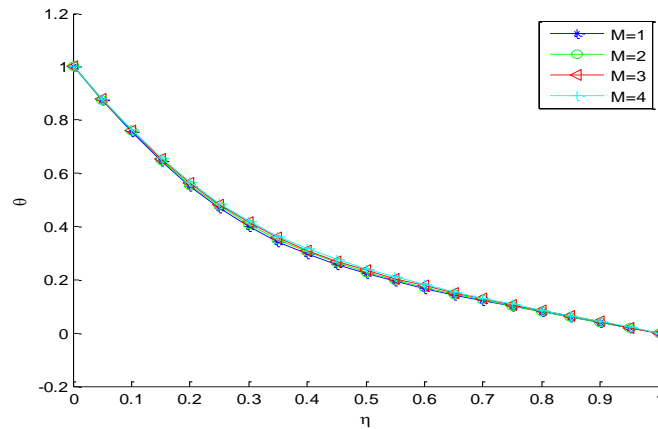


Figure 5. Effect of Magnetic parameter (M) on Temperature profile when $Pr=10$, $Sc=N_t=N_b=0.1$ and $R=1$

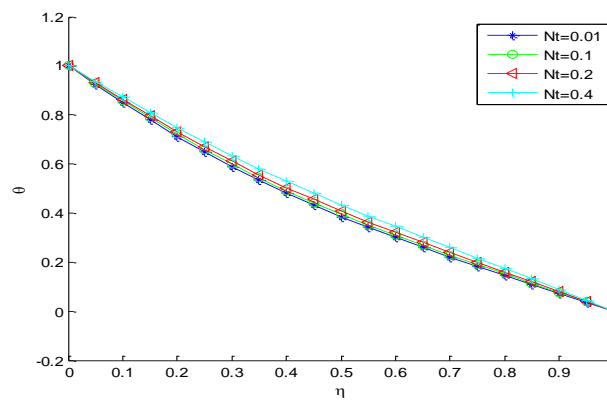


Figure 6. Effect of thermophoretic parameter (N_t) on Temperature profile when $Pr=20$, $Sc=N_b=0.1$ and $M=R=1$

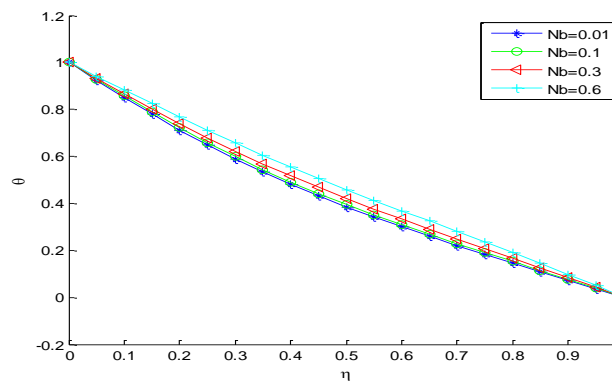


Figure 7. Effect of Brownian motion parameter (N_b) on Temperature profile when $Pr=10$, $Sc=N_t=0.1$ and $M=R=1$

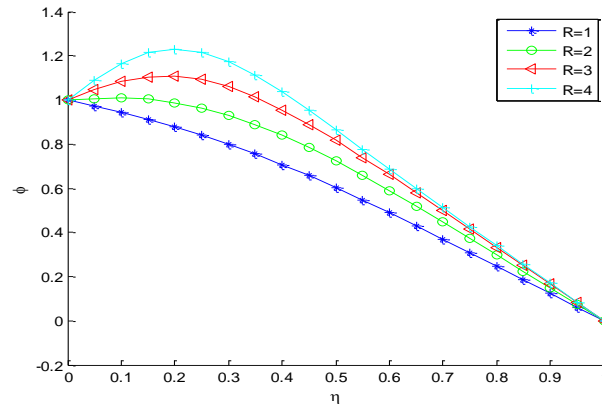


Figure 8. Effect of viscosity parameter (R) on concentration profile when $Pr=10, Sc=N_t = N_b =0.1$ and $M=1$

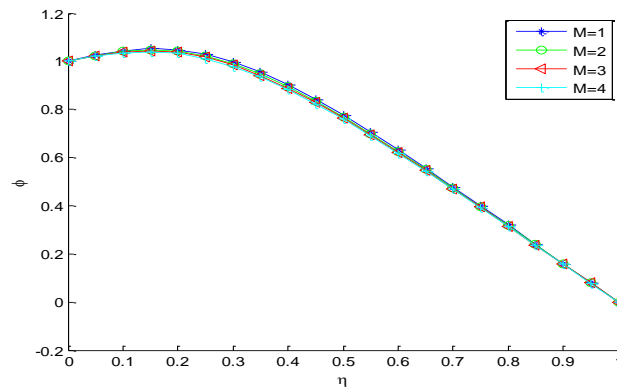


Figure 9. Effect of magnetic parameter (M) on concentration profile when $Pr=10, Sc=N_t = N_b =0.1$ and $R=1$

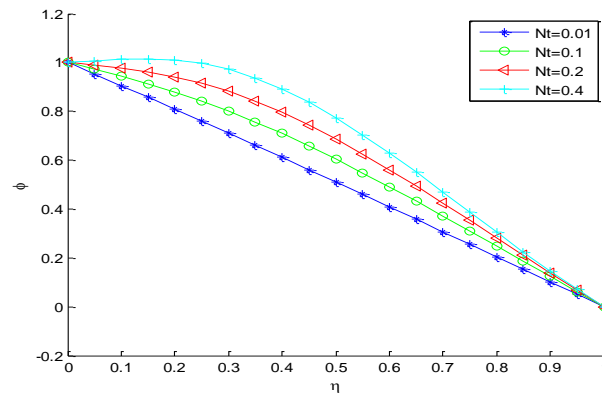


Figure 10. Effect of thermophoretic parameter (N_t) on concentration profile when $Pr=10, Sc= N_b =0.1$ and $M= R=1$

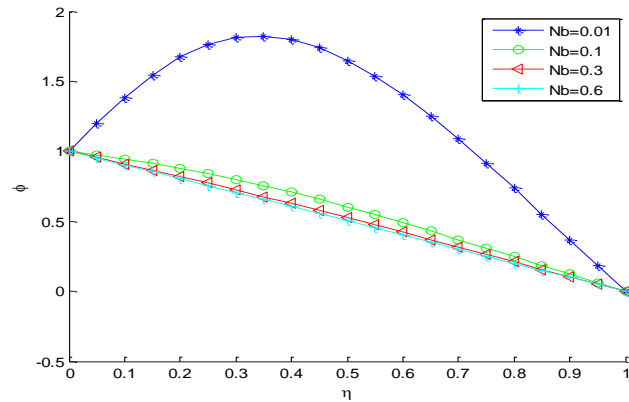


Figure 11. Effect of Brownian motion parameter (N_b) on concentration profile when $Pr=10$, $Sc= N_t =0.1$ and $M=R=1$

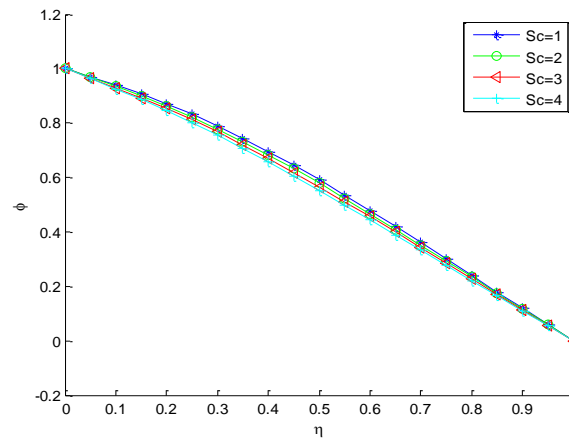


Figure 12. Effect of Schmidt number (Sc) on concentration profile when $Pr=10$, $N_b= N_t =0.1$ and $M= R=1$

Viscosity parameter (R) effect on Nano concentration is observed in Figure 8. It is shown that increasing R , concentration effect is maximum towards the lower plate due to increasing overall transport energy capacity. Magnetic parameter (M) effect on nanoparticle concentration is demonstrated in Figure 9 which depicts decreasing Nano concentration caused by increased magneto hydrodynamic boundary layer owing to higher thermal conductivity. It can be observed in Figure 10 that thermophoretic parameter (N_t) causes an increase in concentration profile as N_t increases quantitatively due to increasing fluid thermal diffusivity. Figure 11 depicts the effect of increasing values of Brownian motion parameter (N_b) on Nano concentration. As observed increasing values of N_b causes significant decrease in nano particle concentration owing to increased diffusion rate of reacting species. The effect of Schmit number (Sc) on concentration is observed in Figure 12. It is seen that increasing values of Sc leads to increased fluid viscosity causing a corresponding decrease in Nano concentration.

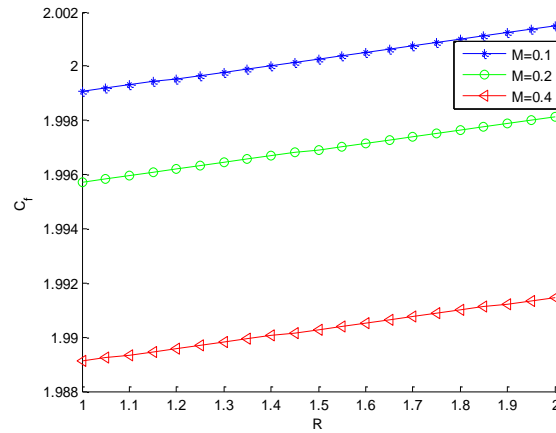


Figure 13. Effect of Magnetic parameter (M) on skin friction when $Pr=10$, $N_b=N_t=0.1$

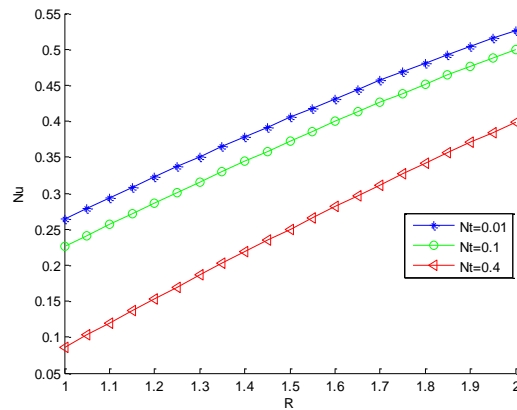


Figure 14. Effect of thermophoretic parameter (N_t) on Nusselt number when $Pr=10$, $N_b=0.1$ and $M=1$

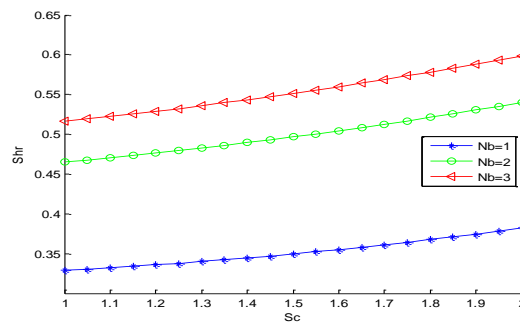


Figure 15. Effect of Brownian motion parameter (N_b) on Sherwood number when $Pr=10$, $N_t=0.1$ and $M=R=1$

The effect of magnetic parameter (M) is illustrated on the skin friction in Figure 13, it is demonstrated that increasing M causes decrease in skin fluid friction which is higher at the upper plate wall whereas increasing values of thermophoretic parameter (N_t) as observed in Figure 14 causes a similar decrease on the Nusselt number i.e. the fluid heat transfer. Also the effect of Sherwood number on flow is observed in Figure 15. It is illustrated that increasing values of Brownian parameter (N_b) causes an increase on mass flow rate of fluid.

CONCLUSION

This present study analyses nanofluid flow through parallel plates arranged horizontally against each other, under the influence of uniform magnetic flux. The nanofluid flow described by nonlinear ordinary differential equations arising from the mechanics of the fluid are analyzed adopting the homotopy perturbation method (HPM). Various thermal-fluidic parameters such as viscosity parameter, Magnetic parameter, Schmidt number are investigated on flow, heat transfer and concentration. Result reveals skin friction and Nusselt number decreases while Sherwood number increases near walls during heat and mass transfer of Nano mix. This study proves useful in the advancement of transport and heat transfer processes in micro mixing, fuel cells, energy conservation, and pharmaceutical processes amongst other applications.

NOMENCLATURE

C	Concentration
c_p	Specific heat capacity of nanofluid
D_B	Diffusion coefficient of diffusing species
k	Thermal conductivity
$M = \frac{\sigma B_0^2 h^2}{\rho \nu}$	Magnetic parameter
$N_b = (\rho c)_p D_B (C_h) / (\rho c)_f \alpha$	Brownian motion parameter
$N_t = (\rho c)_p D_T (T_H) / [(\rho c)_f \alpha T_c]$	Thermophoretic parameter
p^*	Nanofluid fluid pressure
$Pr = \frac{\mu}{\rho_f \alpha}$	Prandtl's number
$R = \frac{ah^2}{\nu}$	viscosity variational parameter
$Sc = \frac{\mu}{\rho_f D}$	Schmidt number
T	Temperature
$u = axf'(\eta)$	x component velocity
$v = -ahf(\eta)$	y component velocity
μ	Dynamic viscosity
ρ_f	Base fluid density
$\eta = \frac{y}{h}$	Similarity variable
$\theta(\eta) = \frac{T - T_h}{T_0 - T_h}$	Dimensionless Temperature
$\phi(\eta) = \frac{C - C_h}{C_0 - C_h}$	Dimensionless Concentration

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