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Ankara University, Faculty of Sciences,
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IRON-CATALYZED ARYL SELECTIVE ACYLATION OF MIXED DIORGANOZINCS

ÖZGEN ÖMÜR PEKEL AND N. DİDEM KAHYA

ABSTRACT. Iron-catalyzed acylation of mixed alkylarylzincs with aromatic acyl halides in THF provides a new route for aryl-aryl coupling. This procedure is an atom-economic supplement to transition metal-catalyzed acylation of diorganozincs.

1. INTRODUCTION

Aromatic ketones are important building blocks in several natural and active pharmaceutical products. For the synthesis of ketones, the coupling of acyl chlorides with organometallic reagents provides a direct and convenient methodology [1,2] and overcomes some drawbacks of Friedel-Crafts acylation [3]. So far, useful synthetic protocols have been developed for the acylation of mostly Grignard [4-14], organocopper [15,16] and -zinc [17,18] compounds. Acylation of Grignard reagents, RMgX has some restrictions such as the formation of side products including tert-alcohols. In the case of using diorganocuprate reagents, R_2CuM ($\text{M}=\text{Li}, \text{MgX}$), the problem of the functional group arises. However, diorganozinc, R_2Zn , and monoorganozinc, RZnX reagents are good reaction partners for acylation, not only due to their high tolerance to functional groups but also not the formation of tert-alcohols. The initial reports about the acylation of RZnX and R_2Zn focused on Cu [19] or Pd [20-22] catalysis. In the recent years, steady advances have been made in the acylation of organozinc reagents and due to the high cost-Pd catalysts, inexpensive Co [23-25], Fe [23,26], and Ni [27-30] catalysts also received attention.

Diorganozincs, R_2Zn , are more reactive than organozinc halides, RZnX . However, in the reaction of diorganozincs, only one organic group is transferred to an electrophile, essentially wasting the other R groups. This circumstance is unattractive when the starting organyl halide or organolithium or Grignard reagent

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to be transmetallated is expensive or difficult to prepare and when a large excess of diorganozinc is required to obtain high yield and/or selectivity in their reactions. Mixed diorganozincs, R^1R^2Zn , in which one of the R groups has a lower transfer rate than the other have been developed. Recently, mixed diorganozincs R_RR_TZn which have one transferable R_T together with the residual group R_R have been successfully used in organic synthesis [31-51].

Our group carried out a series of synthetic and mechanistic work [52-57] on the selectivity of organyl groups of mixed diorganozincs, R^1R^2Zn in their C-acyl coupling reactions. We observed that group transferability in the acylation of alkylarylzinc could be controlled using cosolvent, transition metal catalyst, and organic catalyst. We have already reported a transition metal-free protocol for alkyl-aryl coupling using mixed (alkyl)(aryl)zinc reagents in THF in the presence of *n*-Bu₃P [53]. We found that group selectivity depends on the donor solvent [52] and aryl group transfer takes place in THF:TMEDA (2:1) [54]. Recently, we also reported a new route in the presence of nano-NiO catalysis for aryl-aryl coupling of (alkyl)(aryl)zincs [57].

However, the percentages of these metals in the earth's crust are extremely small, and their prices are rather expensive. Also, phosphines are unstable in air. So, it is required to handle them in a glove box. As an improvement of these disadvantages, we have focused on using iron compounds as a catalyst, because iron is abundant and less expensive.

Herein we report that inexpensive and non-toxic Fe-catalyzed acylation of (*n*-alkyl)(phenyl)zincs with aromatic benzoyl chlorides provides an alternative atom economic route for the synthesis of diarylketones by acylation of diarylzincs in the presence of transition metal catalysis.

2. EXPERIMENTAL

All reactions were carried out in oven-dried glassware under a positive pressure of nitrogen using standard syringe-septum cap techniques [58]. GC analyses were

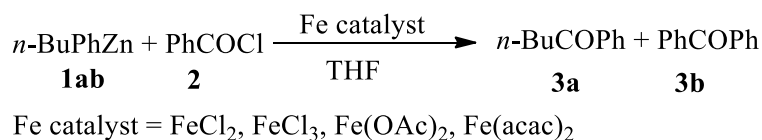
performed on a Thermo Finnigan gas chromatograph equipped with a ZB-5 capillary column packed with phenylpolysiloxane using the internal standard technique.

For the preparation of *n*-butylphenylzinc reagents, phenylzinc chlorides were reacted with *n*-butylmagnesium chloride. Phenylzinc chloride was prepared by the addition of phenylmagnesium bromide (2 mmol) to ZnCl₂ (2 mmol) in THF (2 ml) at -20 °C and stirring at that temperature for 15 min. To freshly prepared arylzinc chloride (2 mmol), *n*-butylmagnesium chloride (2 mmol) was added and the mixture was stirred at -20 °C for another 15 min.

To the freshly prepared mixed (*n*-butyl)(phenyl)zinc reagent (2 mmol), Fe catalyst (20 mol % 1 mmol) was added at -20 °C and the mixture was stirred at that temperature for 15 min. If used, cosolvent (or additive) was added. Benzoyl chloride (1 mmol, 0.12ml) was added dropwise at -20 °C. The reaction mixture was stirred at room temperature for 2 h. After the addition of the internal standard, the mixture was hydrolyzed with the NH₃/NH₄Cl solution. The organic phase was analyzed by GC.

3. RESULTS AND DISCUSSION

For the investigation of group selectivity in the iron-catalyzed acylation of (*n*-alkyl)(aryl)zinc reagents (Scheme 1), we chose reaction of (*n*-butyl)(phenyl)zinc with benzoyl chloride in THF as a model reaction based on our previous studies [52-57]. *n*-BuPhZn **1ab** was prepared using Grignard reagents and *n*-butylmagnesium bromide was added to phenylzinc chloride prepared by transmetalation of phenylmagnesium bromide with ZnCl₂/THF at -15 °C. We determined the relative transferability of the organyl groups by calculating the GC yields of ketones using authentic samples.



Scheme 1. Group selective coupling of (*n*-butyl)(phenyl)zinc **1ab** with benzoyl chloride **2** in the presence of iron catalysis.

Firstly, we investigated the effect of reaction conditions on the group selectivity of (*n*-Bu)(Ph)Zn **1ab** in iron-catalyzed acylation with benzoyl chloride **2**. As iron catalysts, FeCl₂, FeCl₃, Fe(OAc)₂ and Fe(acac)₂ were used (Table 1). The yield of the uncatalyzed reaction did not exceed 20% with a **3a:3b** ratio of 50:50.

TABLE 1. Screening iron catalysts in the reaction of (*n*-butyl)(phenyl)zinc **1ab** with benzoyl chloride **2**. Optimization of the reaction parameters ^a.

$$n\text{-BuPhZn} + \text{PhCOCl} \xrightarrow[\text{THF, r.t., 2h}]{\text{Fe catalyst}} n\text{-BuCOPh} + \text{PhCOPh}$$

1ab **2** **3a** **3b**

Entry	Fe catalyst / Additive	Solvent	Total yield, % ^{b,c}	roup selectivity ^d 3a:3b
1	-	THF	20	50:50
2	FeCl ₂ (20 mol %)	THF	56	41:59
3	FeCl ₂ (20 mol %) / LiCl(1 equiv.)	THF	64	56:44
4	FeCl ₃ (20 mol %)	THF	85	15:85
5	FeCl ₃ (20 mol %)	THF:NMP(3:1) ^e	62	65:35
6	FeCl ₃ (20 mol %)	THF:Diglyme(3:1) ^e	15	40:60
7	FeCl ₃ (20 mol %)	THF:TMEDA(2:1) ^e	18	28:72
8	FeCl ₃ (20 mol %) / MgCl ₂ (20 %)	THF	70	21:79
9	FeCl ₃ (20 mol %/LiCl(20 %)	THF	87	17:83
10	Fe(OAc) ₂ (20 mol %)	THF	87	15:85
11	Fe(OAc) ₂ (20 mol %) / LiCl(1equiv.)	THF	74	14:82
12	Fe(acac) ₂ (20 mol %)	THF	57	15:85
13	Fe(acac) ₂ (20 mol %)/LiCl(1equiv.)	THF	52	27:78

^aThe reactions were carried out using 1 mmol of benzoyl chloride **2** and 2 mmol of (*n*-butyl)(phenyl)zinc **1ab**. Mol % amount of catalysts **3** were indicated.

^b The sum of GC yields of *n*-Bu coupling product **3a** and Ph coupling product **3b**.

^cAll the data are the average of at least two experiments.

^dThe ratio of GC yields of **3a** and **3b**.

^eNMP=N-methylpyrrolidine, Diglyme=Diethylene glycol dimethyl ether, TMEDA= Tetramethylenediamine.

As can be seen from Table 1, all iron catalysts are not successful in group selective coupling of **1ab** with **2** in THF. The catalysis reaction of 20 mol% FeCl₂ at room temperature resulted in a medium yield (56%) with a poor group selectivity (Table 1, entry 2) (*n*-Bu transfer:Ph transfer ratio=41:59). Using LiCl as an additive led to a somewhat higher yield (Table 1, entry 3); however, the reaction did not occur in the presence of *n*-Bu₃P-FeCl₂. Catalysis of 20 mol% FeCl₃ in a two-hour reaction at

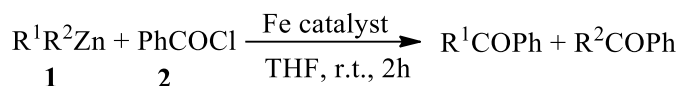
room temperature increased the coupling yield (85%) and Ph selectivity (*n*-Bu transfer:Ph transfer ratio=15:85) (Table 1, entry 4). Increasing the reaction time changing the catalyst amount to 10-25% decreased the yield to 78-80% but did not change the Ph selectivity. Varying the temperature (0 °C or 60 °C) led to a significant decrease in the yield. The effect of cosolvent was also investigated, however the use of NMP (N-methylpyrrolidine) and especially diglyme (diethylene glycol dimethyl ether) or TMEDA (tetramethylenediamine) gave quite low yields (Table 1, entries 5-7). Interestingly, the *n*-butyl group:phenyl group transfer ratio decreased in THF:TMEDA compared to that found in THF:NMP. The addition of MgCl₂ resulted in lower yield (70%) and lower Ph selectivity although the reaction medium is not Mg-free (Table 1, entry 8). However, the addition of LiCl did not make a change in the yield and Ph selectivity (Table 1, entry 9). Under optimized conditions, Fe(OAc)₂-catalysis (20 mol % catalyst, room temperature, and two-hour reaction) gave a quite high yield (87%) and Ph selectivity (*n*-Bu transfer: Ph transfer rate=15:85) (Table 1, entry 10) and these results are the same as those obtained in the presence of FeCl₃ catalysis (Table 1, entry 4).

Using LiCl as an additive lowered the yield to 74%, however, it did not change the Ph selectivity (Table 1, entry 11). Coupling in the presence of Fe(acac)₂ did not provide higher yield and Ph selectivity in the absence and presence of LiCl additive (Table 1, entries 12 and 13).

Our experimental results show that the best iron catalysts for Ph selective coupling of (*n*-Bu)(Ph)Zn **1ab** with benzoyl chloride **2** seemed to be FeCl₃ and Fe(OAc)₂. Before deciding between FeCl₃ and Fe(OAc)₂, as the most active catalyst(s) in the benzoyl coupling of (*n*-butyl)(phenyl)zinc **1ab**, we compared the atom economic utility of **1ab** in the presence of these catalysts (Table 2). For this purpose, we found the background yields of **1ab**, i.e. acylation yields of homo diorganozinc reagents, *n*-Bu₂Zn, **1a₂** and Ph₂Zn, **1b₂**. We also evaluated the methyl group as a residual group instead of the *n*-butyl group in the (*n*-alkyl)(phenyl)zinc **1ab** to find a higher yield and the phenyl selectivity of acylation. The background yields for uncatalyzed benzoylation of mixed diorganozincs **1ab** were found to be 90% for *n*-Bu₂Zn **1a₂** (Table 2, entry 1) and 66% for Ph₂Zn **1b₂** (Table 2, entry 2). We observed that the acylation yield of the Ph group in (*n*-Bu)(Ph)Zn **1ab** is about the same with the acylation yield of Ph₂Zn **1b₂** in the presence of FeCl₃ catalysis (Table 2, entries 4

and 5). In the presence of Fe(OAc)₂ catalysis, the acylation yield of Ph group in (*n*-Bu)(Ph)Zn **1ab** was found pretty higher than that in Ph₂Zn. These results confirmed the atom-economic character of (*n*-Bu)(Ph)Zn **1ab** in the iron-catalyzed acylation with **2**. The use of (Me)(Ph)Zn **1bc** as the mixed organozinc in the acylation resulted in much lower yield than that of (*n*-Bu)(Ph)Zn **1ab** in the presence of FeCl₃ catalysis (Table 3, entries 4 and 6) and Fe(OAc)₂ catalysis (Table 2, entries 7 and 9).

TABLE 2. Coupling of *n*-Bu₂Zn **1a₂**, Ph₂Zn **1b₂** and (Me)(Ph)Zn **1bc** with benzoyl chloride **2** in THF in the presence of FeCl₃ and Fe(OAc)₂catalysts.^a



Entry	R ¹ , R ² , catalyst	Total yield, % _{b,c}	Group selectivity ^d R ¹ COPh:R ² COPh
1	<i>n</i> -Bu, <i>n</i> -Bu	90	-
2	Ph, Ph	66	-
3	<i>n</i> -Bu, Ph	20	50:50
4	<i>n</i> -Bu, Ph, FeCl ₃ (20 mol %) ^c	85	15:85
5	Ph, Ph, FeCl ₃ (20 mol %)	82	-
6	Me, Ph, FeCl ₃ (20 mol %)	64	0:100
7	<i>n</i> -Bu, Ph, Fe(OAc) ₂ (20 mol %) ^c	87	15:85
8	Ph, Ph, Fe(OAc) ₂ (20 mol %)	48	-
9	Me, Ph, Fe(OAc) ₂ (20 mol %)	62	0:100

^a The reactions were carried out using 1 mmol of benzoyl chloride **2** and 2 mmol of **1a₂**, **1b₂** or **1bc**. A mol % amount of catalyst was indicated.

^b The sum of GC yields of R¹COPh and R²COPh.

^c All the data are the average of at least two experiments.

^d The ratio of GC yields of R¹COPh and R²COPh.

^e Taken from Table 1.

4. CONCLUSION

In conclusion, we have shown that selective acylation of aryl groups in FeCl₃ or Fe(OAc)₂ catalyzed reactions of mixed *n*-alkyl phenylzincs reagents with aromatic acyl halides in THF is an efficient method for the synthesis of diarylketones.

We have demonstrated that

- (i) This route provides a new simple and atom economic alternative to transition metal-catalyzed acylation of diarylzinc reagents.
- (ii) Fe catalysts are inexpensive and non-toxic, so this procedure is a supplement to Ni catalyzed acylation of mixed n-alkyl phenylzincs.
- (iii) These findings provide another support for Erdik's hypothesis of the dependence of group selectivity of mixed diorganozincs on the reaction parameters [52-57].

ÖZET

Karışık alkilarylçinkoların THF'deki aromatik açıl halojenürlerle demir katalizli açılması, aril-aroil eşleşmesi için yeni bir yöntemdir. Bu yöntem, diorganoçinkoların geçiş metali katalizli açılmasına atom-ekonomik bir alternatiftir.

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Current Address: ÖZGEN ÖMÜR PEKEL: Department of Chemistry, Ankara University, 06100 Ankara, TURKEY

E-mail Address: oomur@science.ankara.edu.tr

ORCID: <https://orcid.org/0000-0003-3833-4447>

Current Address: N. DİDEM KAHYA (Corresponding author): Department of Chemistry, Ankara University, 06100 Ankara, TURKEY

E-mail Address: kahya@ankara.edu.tr

ORCID: <https://orcid.org/0000-0001-9255-0867>



THE INHIBITOR EFFECTS OF *CANNABIS SATIVA* L. EXTRACTS ON THE CORROSION OF ALUMINIUM in H₂SO₄ SOLUTIONS

TURAN YANARDAĞ, NİLGÜN BAYRAKTAR, YAĞMUR KAHRAMAN
YANARDAĞ, YASİN ÖZGEN, AND ALİ ABBAS AKSÜT

ABSTRACT. The aim of study was to investigate the effect of terpenoids in cannabis (*Cannabis sativa* L.) obtained from Diyarbakır line as corrosion agent on the corrosion of aluminum. Corrosion protection of aluminum (99.9% purity) with *cannabis* plant has been investigated using electrochemical methods. The methods with electrochemical impedance spectroscopy (EIS) and current potential showed that the plant has a potential to prevent corrosion of aluminum at 298 K in 0.5 M H₂SO₄ solution around 98%. The experimental results indicated that the cannabis plant can be used as an environmentally friendly inhibitor for aluminum.

1. INTRODUCTION

The standard electrode potential of aluminum is very negative (-2.35 V) compared to the Standard Hydrogen Electrode (SHE). Aluminum is known as the most widely used anode material with high energy capacity (8.1 kW h/kg) in all atmospheric environments [1-7]. Aluminum and its alloys offer a wide range of properties in different industrial fields such as the automotive industry, the aeronautical and aerospace area, construction industry, the electrical and electronic. Aluminum can easily form a thin and compact oxide film in the atmospheric environment. This film can be soluble in acidic solution. For this reason, we need to make an extra coating for preventing corrosion of aluminum in acidic solution with an inhibitor. Generally, inhibitor also should be cheap, useful, non-hazardous to health and accessible. Accordingly, *Cannabis sativa* L. plant used as an inhibitor in this study. It can be grown economically at almost any location of Turkey, where plenty of sunlight, temperature and sufficient humid climates are available. The plants from Diyarbakır

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line are suitable for seed production and show numerous branches and abundant flower formation preferred for the experiment. In addition, the plants contain several cannabinoids (terpenophenolic compounds) having medical benefits [8].

The use of inhibitors is one of the most practical methods to prevent corrosion of metals. Various inhibitors of aluminum in aqueous solutions have been reported [9-14]. However, many of them are hazardous, costly and not safe for the environment and human health. Therefore, it is desired if safer corrosion inhibitors for aluminum against surrounding environments are available. Environmentally friendly plant extracts can be considered as lower cost inhibitors. Phytochemicals including alkaloids, and flavonoids, heteroatoms such as N, S, O, π -electrons on the aromatic ring and π -electrons in the plant extracts are adsorbed on the metal surface to prevent corrosion.

Cannabis sativa L. preparations are derived from the female plant of *Cannabis* (Family Cannabidaceae). The use of *Cannabis sativa* L. in medicinal treatments has become widespread in recent years. Substances such as nabilone, dronabinol and its some derivatives are used in the treatment of glaucoma, multiple sclerosis and chemotherapy [15].

Presently *Cannabis sativa* L. plant is being assessed as an industrial crop in Turkey. Therefore, its cultivation is supported and promoted at the state level. The plant extract has been used to prevent corrosion of aluminum. After the treatment with the extract obtained from this plant, industrial waste is not observed. Because of these features, this plant has been found suitable for industrial use and it is recommended to carry out the necessary procedures to spread it.

2. MATERIALS AND METHODS

2.1. Experimental material

Cannabis sativa L. was obtained from Department of Field Crops, Faculty of Agriculture, Ankara University, Turkey. The cannabis seeds were collected from the wild flora of Diyarbakır province. The seeds were sown in 4 m long 3 rows manually by hand followed by covering them properly with loose soil. The seeds were placed at 1 cm depth in 3 replicated rows that were separated by 30 cm on 06.05.2019. Aluminum metal (99.9% purity, 5 mm diameter of cylindrical surface area, 0.19625 cm² geometric area) fixed on the Teflon tube with adhesive was taken from ETİ Aluminum A.Ş, Seydişehir, Konya.

2.2. *Harvesting and drying*

Upper leaves and flowers of the female *Cannabis sativa* L. were harvested on 04.09.2019 in the morning at 06:00 and dried under cool and shady conditions [16].

2.3. *Processing*

The dried sample was ground to powder. This dry sample of 10 g was dissolved in 200 mL of 0.5 M sulfuric acid and stirred for 1 day with a heating without boiling. The homogenized mixture was heat filtered to give 30 mL solution for each of 2, 6 and 24 h.

2.4. *Extraction*

Cannabis sativa L. extract was used to prevent corrosion of pure aluminum. The extraction was carried out following modified method of Turner and Mahlberg [17].

2.5. *Electrochemical Impedance Spectroscopy (EIS)*

The electrochemical impedance method provides information about the mechanisms occurring on the surface with applying sinusoidal potential perturbation to the electrode surface, and measuring both the current flow and the shift in the phase of the resulting current [18]. Electrochemical impedance was carried out using 5 mV amplitude sinusoidal signal at the low frequency 0.1 Hz. Electrochemical impedance measurement results of the aluminum in extract solution are shown in Fig.1.

2.6. *Electrochemical analysis and measurement of corrosion inhibition*

Corrosion of aluminum in *Cannabis sativa* L. extract were carried out by electrochemical system. This system consist of CHI 660 B instrument potentiostat, polyscience thermostat, glass cell and a computer for obtaining corrosion parameters. Glass cell consists three electrodes; aluminum metal, reference electrode (3 M solution with chloride (Cl⁻) concentration, Ag/AgCl) and platinum (platin wire) electrode. Potentials were obtained by this reference electrode. Aluminum metal surface polished with alumina and washed with double distilled water before experiments. After washing aluminum were immersed in *Cannabis sativa* L. extract solution, the impedance measurements were carried out at the open circuit potential

(-0.688 V) and samples in a steady state during 20 min, when impedance was measured. The current potential measurements were performed (scan rate 1mV/s).

$$E (C - P)(\%) = \frac{i_{corr}(\text{blank}) - i_{corr}(\text{C. sativa L.})}{i_{corr}(\text{blank})} \times 100 \quad \text{Eq. 1}$$

$$E (R_p)(\%) = \frac{[R(\text{C. sativa L.}) - R(\text{blank})]}{R(\text{C. sativa L.})} \times 100 \quad \text{Eq. 2}$$

$$i_{corr} (\text{Stern - Geary}) = \left[\frac{\beta_a \cdot \beta_c}{2,303(\beta_a + \beta_c)} \right] \times \frac{1}{R_{ct}} \quad \text{Eq. 3}$$

Corrosion rates (i_{corr}) were obtained from current potential curves with extrapolation anodic and cathodic Tafel slope to the corrosion potential (Fig.2) from CHI660B instrument. Corrosion inhibition efficiencies E (C-P, %) and E (S-G, %) were calculated using i_{corr} and from polarization and charge transfer resistances (Rct), using Eq.1 and Eq.2 [18], respectively. i_{corr} calculated from M. Stern and A. L. Geary equation (Eq.3) [19-21] using R_p resistance from current potential curves. In this equation, the β_a is the anodic slope, the β_c is the cathodic slope, the R_p resistance from the current potential curves (Table 2).

3. RESULTS AND DISCUSSION

3.1. Meteorological observations

Comparing the meteorological data for long term with the data of year 2019, it was obvious that the temperature and relative humidity values for 2019 and long term were very close to each other (Table 1). However, precipitation showed a significant increase during May and remarkable reduction during June to August 2019 period when compared to the long term averages. Furthermore, the average of climatic data for 2019 showed average temperature, precipitation and relative humidity of 20.65°C, 28.28 mm and 49.35% during 2019 in the same order. Total precipitation remained 113.10 mm.

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TABLE 1. Averages of meteorological data for long term and 2019*.

Months	Temperature (C°)		Precipitation (mm)		Relative Humidity (%)	
	Long Term	2019	Long Term	2019	Long Term	2019
May	18.1	16.0	35.9	51.8	48.9	57.3
June	22.4	19.9	42.6	34.7	52.2	52.0
July	23.0	23.4	33.9	14.1	42.1	44.5
August	24.3	23.3	28.7	12.5	40.5	43.6
Average	21.95	20.65	35.28	28.28	45.93	49.35

Total 141.10 113.10

* The Directorate general of Meteorology Ankara.

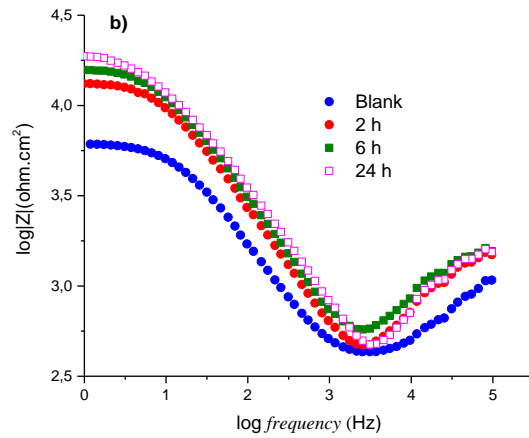
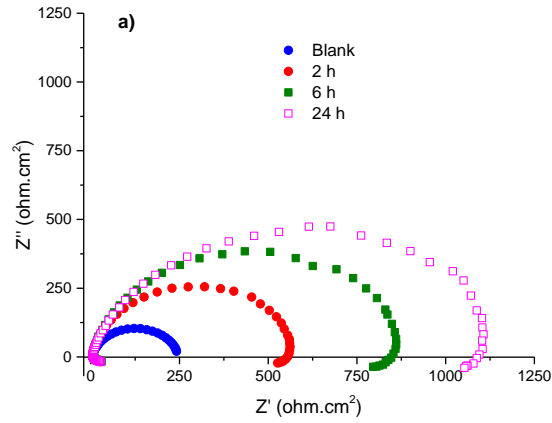
3.2. Inhibition efficiency

The inhibition efficiency of the extract was evaluated using polarization resistance obtained from electrochemical impedance curves (Fig.1). In the impedance method, the resistance increases at the metal/solution interface that occurs on the metal surface without the current passing through the same mechanism in real (Z') and imaginary (Z'') axes. The Nyquist plots obtained during the immersion time for 2 h, 6 h and 24 h exhibit a depressed semicircle from high frequency(100 kHz) region to low frequency region (0.1 Hz). Semicircular curves showed that this mechanism has charge transfer controlled [18,22-24]. Moreover, the radius of the semicircles observed for the aluminum resistance increases with increasing immersion time (Fig.1(a)), demonstrating an increase in the corrosion resistance. The corresponding Bode and Bode-phase plots were shown in Fig.1(b) and (c), respectively. Both the resistance value and the phase angle (θ) increase with increasing duration of the immersion.

$$C_{dl} = \left[\frac{1}{2\pi f (Z''_{max})} \right] \times \frac{1}{R_{ct}} \quad \text{Eq. 4}$$

Double layer capacitance (C_{dl}) was also calculated in this study. Charge transfer resistance (R_{ct}) was found benefit from Fig.1(a). In this equation, R_{ct} shows the charge transfer resistance and f is the frequency corresponding to the maximum value of Z'' . This is given in Eq.4. The C_{dl} value in the table decreases gradually for

2 h, 6 h and 24 h respectively. The reason for this is that aluminum is well coated with *Cannabis sativa* L. and the ability of capacitance decreases on aluminum surface. In other words, the reduction of the surface slows down as the surface coated. Consequently, the corrosion rate slows down as C_{dl} decreases. As the coating time increases, the passage of electrons on the aluminum surface slows down (Table 2).



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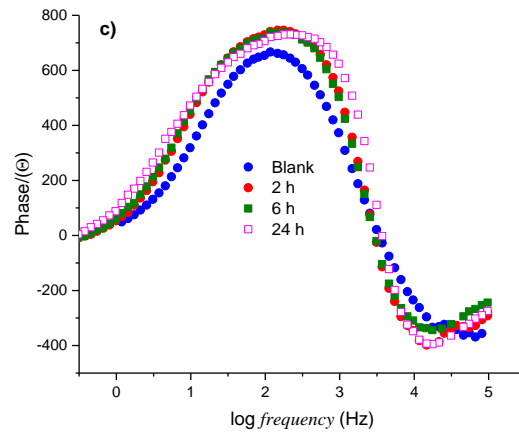


FIGURE 1. Electrochemical impedance curves of aluminum **a)** Nyquist **b)** Bode- $|Z|$ **c)** Bode-phase plots in the presence of *Cannabis sativa* L. extract in 0.5 M H₂SO₄ with during 2 h, 6 h and 24 h.

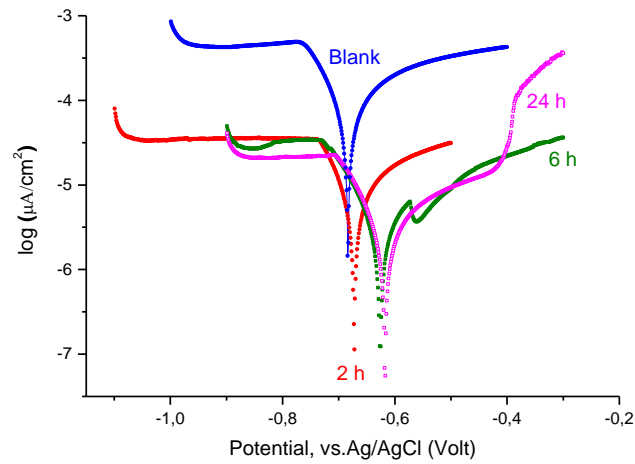


FIGURE 2. Potentiodynamic current potential curves of aluminum in 0.5 M H₂SO₄ in the presence of *Cannabis sativa* L. extract with during 2 h, 6 h and 24 h.

There are many organic compounds in *Cannabis sativa* L. These compounds are most commonly phenolic mono or poly terpene compounds [16,17]. These compounds interact with aluminum deposited on the metal surface without passing into the study solution. The resistance at the metal/solution interface increase from nearly 225 $\Omega \cdot \text{cm}^2$ to 1200 $\Omega \cdot \text{cm}^2$. As the resistance increased, aluminum showed the ability to cover the metal surface in acidic solution by means of activated carbon centered carbanions of these compounds. Thus, the average corrosion inhibition increased to 98% and the corrosion of aluminum was significantly reduced. A reduction potential was observed at -0.55 V (Fig.2). It is shown that more than one compound in the *Cannabis sativa* L. extract can give together less soluble compounds on the aluminum metal surface. Corrosion rate and other parameters were obtained from electrochemical current potential curves in the presence of *Cannabis sativa* L. at 298 K shown in Table 2.

TABLE 2. Corrosion parameters obtained from current potential curves for pure aluminum in 0.5 M H_2SO_4 solution in the presence of *Cannabis sativa* L. extract during 2 h, 6 h and 24 h at 298 K.

Media	E_{corr} (Volt)	β_a (mV/dec)	β_c (mV/dec)	R_p ($\Omega \cdot \text{cm}^2$)	C_{dl} ($\mu\text{F}/\text{cm}^2$)	R_{ct} ($\Omega \cdot \text{cm}^2$)	Corrosion Rate (i_{corr} , $\mu\text{A}/\text{cm}^2$)		E (%)				
							C-P	(S-G) $_{sp}$	(S-G) $_{act}$	C-P	(S-G) $_{sp}$	Avrg	
Blank	-0.686	196	359	295	2131	225	470	187	-	-	-	-	-
+ <i>C. sativa</i> L.													
2 h	-0.668	325	239	3721	473	690	16	16	67	96	91	85	
6 h	-0.610	318	38	4592	448	880	3.25	3.2	74	99	98	90	
24 h	-0.607	293	31	4926	70	1200	2.50	2.4	81	99	99	93	

Avrg: Average, C-P: Current Potential, S-G: Stern-Geary.

4. CONCLUSIONS

Electrochemical methods showed that the compounds in *Cannabis sativa* L. exhibit better inhibitive effect on the corrosion of pure (purity 99.9%) aluminium. It was noticed that the *Cannabis sativa* L. extract significantly reduced the corrosion rate and increased the resistance of surface aluminum (98%). The extract shifts the potential of aluminum in a positive direction from -0.686 to -0.607 V. It acted as a anodic inhibitor. Corrosion resistances were measured by the current potential and impedance methods for 2 h, 6 h and 24 h, respectively. According to the impedance curves, the reaction between *Cannabis sativa* and aluminum occur by the same mechanism. This mechanism is charge transfer controlled. The impedance measurements showed that a protective layer is formed on the aluminum during the

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period. Moreover, double layer capacitance (C_{dl}) decreases as resistance increases, which shows that molecular coating ability decreases on aluminum surface. Impedance and current potential methods are compatible with each other in this study. The experimental results showed that the *Cannabis sativa* L. plant can be used as an environmentally friendly inhibitor for aluminum.

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ÖZET

Bu çalışmanın amacı, Diyarbakır hattına ait kenevir (*Cannabis sativa* L.) içindeki terpenik bileşiklerin alüminyumun korozyonuna etkisini araştırmaktır. Alüminyumun (%99.9 saflıkta) kenevir bitkisi ile korozyona karşı korunması elektrokimyasal yöntemler kullanılarak araştırıldı. Elektrokimyasal empedans spektroskopisi (EIS) ve akım potansiyel yöntemler, bitkinin 298 K de 0.5 M H₂SO₄ ortamında %98 civarında alüminyumun korozyonunu önleme potansiyeline sahip olduğunu gösterdi. Deneysel sonuçlar, kenevir bitkisinin alüminyum için çevre dostu bir inhibitör olarak kullanılabileceğini belirtti.

Anahtar Kelimeler: Korozyon önleyici, Aromatik bitki, Kurutma koşulları, Kannabinoid (terpenik) bileşikler.

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Current Address: TURAN YANARDAĞ: Department of Chemistry, Ankara University, 06100 Ankara, TURKEY

E-mail: tyanardag@ankara.edu.tr

ORCID: <https://orcid.org/0000-0001-7292-0891>

Current Address: NİLGÜN BAYRAKTAR: Department of Field Crops, Ankara University, 06110 Ankara, TURKEY

E-mail: nbayrak@agri.ankara.edu.tr

ORCID: <https://orcid.org/0000-0003-0425-6305>

Current Address: YAĞMUR KAHRAMAN YANARDAĞ: Department of Field Crops, Ankara University, 06110 Ankara, TURKEY

E-mail: ykahraman@ankara.edu.tr

ORCID: <https://orcid.org/0000-0002-4235-5366>

Current Address: YASİN ÖZGEN: Department of Field Crops, Ankara University, 06110 Ankara, TURKEY

E-mail: yozgen@ankara.edu.tr

ORCID: <https://orcid.org/0000-0002-1317-1031>

Current Address: ALİ ABBAS AKSÜT: Department of Chemistry, Ankara University, 06100 Ankara, TURKEY

E-mail: aksut@science.ankara.edu.tr

ORCID: <https://orcid.org/0000-0003-3076-4282>

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- [2] Kelley, J. L., General Topology, Van Nostrand, 1970.
- [3] G. Huve, K. Takahashi and M. Hashimoto, Brain activity recognition with a wearable fNIRS using neural networks, Mechatronics and Automation, (2017), 1573-1578.

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