

NATIONAL & INTERNATIONAL SCIENTIFIC EVENTS

International Conference on Ubiquitous Information Management and Communication

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Location: Kuala Lumpur, Malaysia

Begins: January 03 2024
Ends: January 05, 2024

IEEE Consumer Communications & Networking Conference

Venue: Flamingo Hotel
Location: Las Vegas, USA

Begins: January 06 2024
Ends: January 09, 2024

The 37th International Conference on Micro Electro Mechanical Systems

Venue: AT&T Hotel and Conference Center
Location: Texas, USA

Begins: January 21 2024
Ends: January 25, 2024

The 14th International Conference on Key Engineering Materials

Venue: N/A
Location: Dubai, United Arab Emirates

Begins: March 06 2024
Ends: March 09, 2024

10th International Conference on Computer Technology Applications

Venue: Hotel Ibis Wien Mariahilf
Location: Vienna, Austria

Begins: May 15 2024
Ends: May 17, 2024

12nd World Biomaterials Congress

Venue: EXCO
Location: Daegu, Korea

Begins: May 26 2024
Ends: May 31, 2024

22nd Triennial Congress of The International Ergonomics Association

Venue: Jeju International Convention Center
Location: Jeju Island, Korea

Begins: August 25 2024
Ends: August 29, 2024

18th European Conference on Soil Mechanics and Geotechnical Engineering

Venue: Altice Arena
Location: Lisbon, Portugal

Begins: August 26 2024
Ends: August 30, 2024

13th European Symposium on Martensitic Transformations

Venue: Lecco Campus
Location: Lecco, Italy

Begins: August 26 2024
Ends: August 30, 2024

49th International Conference on Infrared, Millimeter, and Terahertz Waves

Venue: Perth Convention and Exhibition Centre
Location: Perth, Australia

Begins: September 01 2024
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38th International Conference on Coastal Engineering

Venue: The Pontifical Gregorian University
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Begins: September 08 2024
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69th IEEE Holm Conference on Electrical Contacts

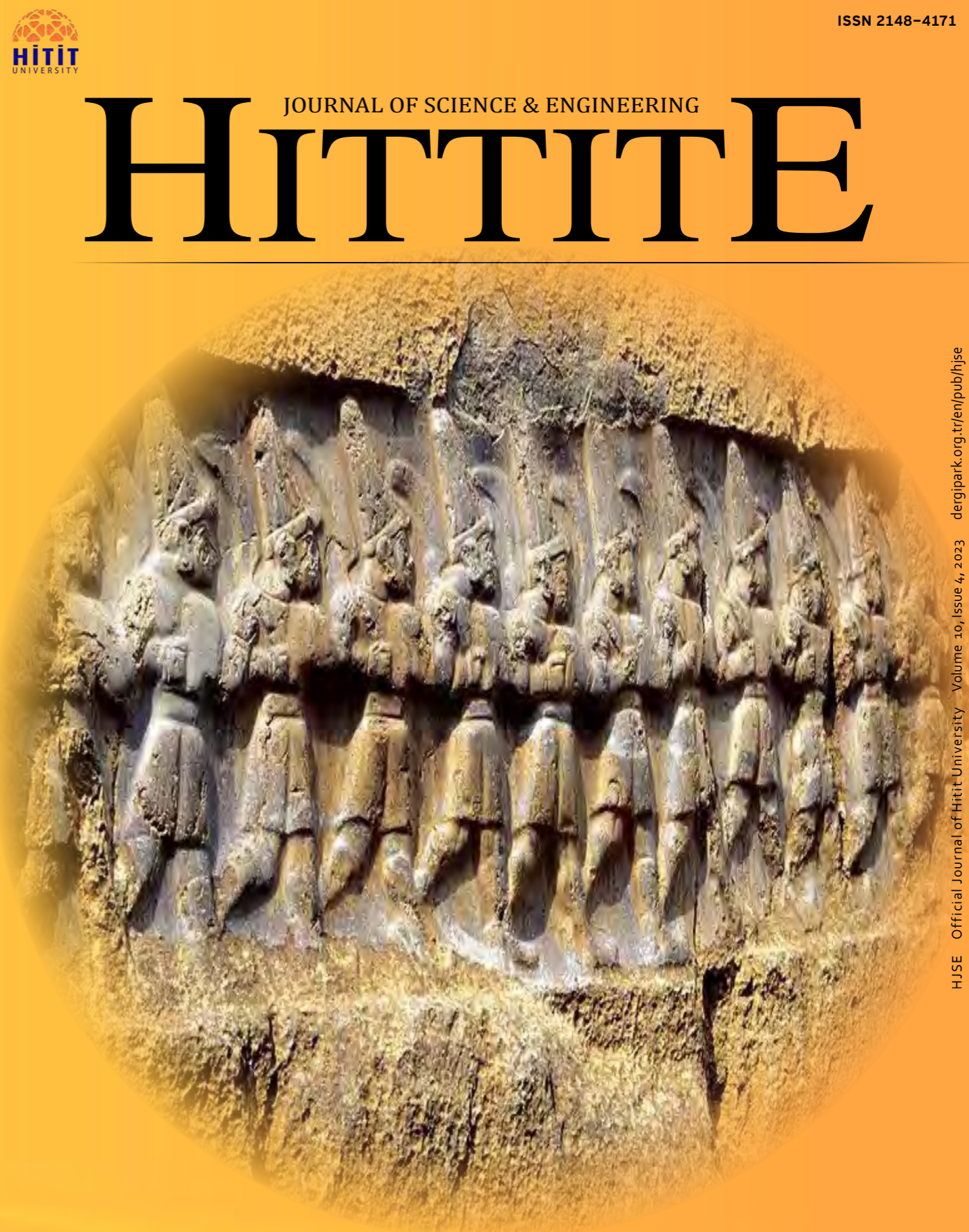
Venue: Graduate Hotel
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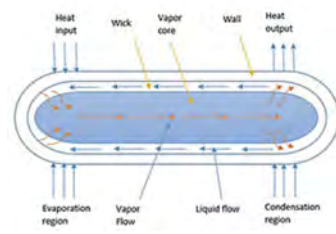
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The Effect of Wick Permeability and Porous Radius on Capillary and Entrainment Limit in A Heat Pipe Reactor 279-285

Gizem Bakir

This study aims to determine the optimum effective porous radius and wick permeability for this reactor and investigate the effect of effective porous radius and wick permeability on the heat pipe limitations.



Strontium Isotopic, Ostracod fauna, and Paleoenvironmental Features of the Late Miocene Sequence in Mut/Dağpazarı Region (Southern Turkey) 287-299

Umit Safak, Hande Sonsun and Nusret Nurlu

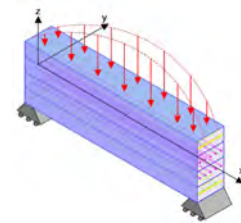
The study conducted a comprehensive examination of the Middle-Late Miocene period in the Dağpazarı, Ballı, and Mut Formations by analyzing the ostracod fauna and utilizing strontium isotope chemostratigraphic dating.



Bending of a Cross-Ply Laminated Composite Beam Under a Sinusoidal Transverse Loading 301-307

Fatih Karaçam

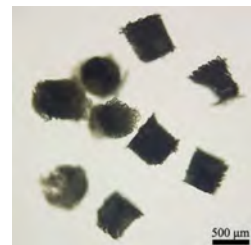
Bending of a laminated composite beam under to a sinusoidal loading is carried out for simply support boundary condition for a specific cross-ply stacking sequence. To demonstrate the accuracy of the analytical results, a computer-aided engineering (CAE) approach is used.



Nucleobase-Modified Microgels Synthesized via Microfabrication Technology for DNA Adsorption 309-315

Kemal Cetin

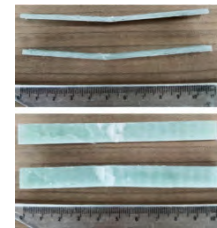
The objective of this study is to fabricate micron-sized hydrogels as adsorbents for DNA.



Mechanical and Tribological Properties of Carbon Fiber/Glass Fiber-Reinforced Epoxy Hybrid Composites Filled with Al2O3 Particles 317-322

Cantekin Kaykilarli, Aymurat Haydarov, Duygu Kose and Hasibe Aygul Yeprem

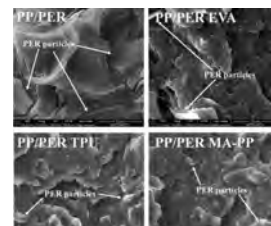
In this study, we produced Aluminum oxide (Al₂O₃) reinforced carbon fiber and glass fiber reinforced polymer (CFRP, GFRP) composites and investigated mechanical and tribological properties.



Optimizing Perlite-Polymer Interface Interactions in Composites based on Polypropylene via the Utilization of Several Compatibilizers 323-329

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Performance Comparison of Waste Cooking Oil on Coal Slime Flotation with Sunflower Oil and Gas Oil 337-337

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This study explores the potential use of waste cooking sunflower oil (WSO) as an eco-friendly collector for coal slime flotation.



Thermodynamic Analysis of the Integrated System that Produces Energy by Gradual Expansion from the Waste Heat of the Solid Waste Facility 339-348

Ahmet Elbir

Especially when considering the amount of power used in waste plants and the corresponding waste heat generated, an approach to recover waste heat from these facilities has been proposed.



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As the team of Hittite Journal of Science and Engineering, we have published the new issue (2023-Volume 10, Issue 4). As a Editor in Chief, I am grateful to all our authors and contributing reviewers of this issue. I also would like to thank to the President of Hitit University, Prof. Dr. Ali Osman Öztürk, for his support and interest in HJSE and also to the Associate Editors of HJSE, namely Prof. Dr. Dursun Ali Kose and Assoc. Prof. Dr. Oncu Akyildiz, as well as our Production Editors, Asst. Prof. Dr. Mustafa Reşit Haboğlu, Asst. Prof. Dr. Erhan Çetin, Harun Emre Kıran and Ömer Faruk Tozlu for their invaluable efforts in making of the journal.

I would like to share a good news with the researchers, scientists and reviewers participating with HJSE Team. HJSE has been recently accepted to the DOAJ index, one of the internationally important indexes. DOAJ (Directory of Open Access Journals); It is an independent index containing approximately 20 thousand peer-reviewed open access journals, covering all fields of science, technology, medicine, social sciences, arts and humanities. DOAJ is supported internationally by libraries, publishers and research institutions.

As Editor in Chief, I would like to thank to the authors submitting their papers to HJSE. In this issue, the articles from the eight branches of engineering including "Manufacturing", "Jeological", "Mechanical", "Biomedical", "Metallurgical and Materials", "Textile", "Mining" and "Energy" Engineering were published.

The new team members of HJSE have joined us as "Section Editors". I am grateful to them for accepting this important task. It is an honour for me to announce them. Prof. Dr. Murat Hoşöz from the Department of Automotive Engineering, Kocaeli University, Prof. Dr. Kazim Savaş Bahçeci from the Department of Food Engineering, Hitit University, Prof. Dr. Cengiz Baykasoğlu from the Department of Mechanical Engineering, Hitit University and Prof. Dr. Akif Akgül from the Department of Computer Engineering, Hitit University.


It's my pleasure to invite the researchers and scientists from all branches of engineering to join us by sending their best papers for publication in Hittite Journal of Science and Engineering

Dr. Ali Kiliçarslan

Editor-in-Chief

The Effect of Wick Permeability and Porous Radius on Capillary and Entrainment Limit in A Heat Pipe Reactor

Gizem Bakır 

 Sivas Cumhuriyet University, Department of Manufacturing Engineering, Sivas, Türkiye

ABSTRACT

For heat extraction in nuclear systems, interest in the design of nuclear reactors with heat pipes has increased. The determination of heat limitations is one of the remarkable factors for safety when heat pipes are used for nuclear systems. In this study, capillary and entrainment limit values for the heat pipe were calculated in a heat pipe reactor with potassium working fluid operating at 650 K. Five different effective porous radii (10.1×10^{-6} , 10.225×10^{-6} , 10.35×10^{-6} , 10.425×10^{-6} and 10.6×10^{-6} m) and five different wick permeability (4.75×10^{-12} , 5×10^{-12} , 5.25×10^{-11} , 5.5×10^{-12} and 5.75×10^{-12} m²) is considered for sintered copper wick heat pipe. While the effects of effective porosity radius, wick permeability, and wick radius on the capillary barrier were studied, only the effects of effective porosity radius were studied. While the effects of effective porosity radius, wick permeability, and wick radius on the capillary barrier are studied, only the effects of effective porosity radius are studied. The highest values of the capillary and entrainment limits are obtained when the porosity radius is 10.1×10^{-6} m. Besides, maximum capillary limits are achieved when the wick permeability is 5.75×10^{-12} m² and the effective porosity radius is 10.1×10^{-6} . This study aims to determine the optimum effective porous radius and wick permeability for this reactor and investigate the effect of effective porous radius and wick permeability on the heat pipe limitations.

Keywords:

Heat pipe; Nuclear reactor; Porous radius; Wick permeability; Wick radius; Capillary limit; Entrainment limit

INTRODUCTION

The heat-pipe-cooled reactor stands out with its high-power density, ease of handling, long-term life (>5 years), and reliability. Recently, the investigation of heat pipes for heat transfer in nuclear cores has been a research topic for researchers [1-4]. The heat pipe is a highly efficient and passive heat transfer mechanism that uses latent heat from evaporation without pump power. It is used in many fields, including nuclear reactors, due to its high efficiency. There are some limitations to the heat transfer of heat pipes. Incorrect determination of heat transfer limits may result in calculating the heat extraction values of the heat pipes incorrectly, in this case, thus causing accidents. The capillary limit is one of the most significant limits for determining these limitations.

Heat pipe reactors have become a popular topic due to the efficiency of heat pipes and their increasing area of applications. Sun et al [5] designed a 120 kW lithium heat pipe reactor power supply that can be used for multiple applications. In their design, 70% enriched uranium nitride fuel and lithium heat pipes were used.

For their study, an MCORE code combining MCNP and ORIGEN was used. In general, it was found that the designed basic parameters met the safety requirements, and the reactor was safe in terms of neutronics. Zhang et al. [6], designed a fast reactor that transfers heat to potassium-filled high-temperature pipes and thermoelectric generators. Both finite element and thermal resistance network methods were used to simulate the potassium heat pipe system. The normal operating conditions and two accident scenarios were calculated to prove the reliability of the new system model. Liu et al. [7], proposed the design of a new passive heat removal system using heat pipe technology to develop the passive safety feature of the molten salt reactor. An experimental system was developed to validate the design of the passive heat removal system of the reactor. An eutectic salt mixture was chosen as the working fluid, and different ranges of it were considered for the heat pipes. They reached lower temperatures when they had a greater distance between the heat pipe spacings. The distance between heat pipe spacings was an important factor affecting the temperature difference. Wang et al.

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[8], analyzed a molten salt reactor using high-temperature heat pipe technology. In their study, they set up an experimental system to verify the feasibility of the passive heat extraction system in the reactor. The experimental results showed that although some of the heat pipes did not work normally, the heat pipe system removed a significant amount of heat from the drain tank. Wang et al. [9], investigated the design of a 25 kWe heat pipe cooled reactor for multiple uses. Based upon the heat pipe cooled reactor design, a thermohydraulic computer code was developed to analyze the time-dependent and time-independent performance of the reactor. For this reactor, 65% enriched UN and potassium are used as fuel and heat pipe working fluid, respectively. In their results, the selected parameters met the safety requirements. Guillen and Turner [10] used axially grooved heat pipes and investigated the applicability of these heat pipes for heat extraction in microreactors. The HTPIPE code is used for the analysis. The performance limits of a sodium heat pipe with a threaded square wick structure were compared to those of an equivalent heat pipe with a circular wick. It was reported that, at operating temperatures below 777 °C the annular wick outperforms the corrugated wick, while at temperatures above 777 °C the corrugated wick outperforms the annular wick.

Some researchers have studied the capillary limit in the heat pipe. Subedi et al. [11] studied the thermal properties of a flat micro heat pipe. They calculated the capillary and maximum temperature limits to determine the maximum heat transfer. For the theoretical results of the optimized wick design, the maximum heat transfer rate and the surface temperature distribution were compared for the capillary limit and maximum temperature limit cases. Yu et al. [12] analyzed the effect of the wick geometry of a heat pipe on the heat transfer capacities. A special analytical computer model was designed using the Newton-Raphson method and applied this model to analyze the capillary, viscous, entrainment, sonic, and boiling heat transfer limits of the heat pipe. It was found that the capillary limit leads to the determination of the maximum heat transfer limit. Xin et al. [13] aimed to design the optimum mini grooved flat heat pipe. A mathematical model of axial fluid flow and heat transfer in a mini grooved flat heat pipe has been created. They emphasized that capillary radius values are an important parameter for calculating capillary limit values. Zhou et al. [14] investigated experimentally the effects of ultra-thin heat pipe, wick width, and fill rate parameters on thermal performance. It was found that when the wick width is 4 mm, the maximum heat carrying capacity of the ultra-thin heat pipe can reach 8.5 W. Zhang et al. [15] characterized the porous structures and capillary performances of the wicks and measured the thermal efficiency of the heat pipes to calculate the capillary limit of the heat pipe. Copper powder sintered heat pipes in various shapes, dendritic and irregular powder

heat pipes provided superior heat transfer capabilities. Some researchers work on entrainment limit. Sandeep and Prakash [16] conducted a study on copper heat pipe filling with acetone. The capillary and entrainment limits were investigated. Python code was used for calculating capillary and entrainment limits. The highest values of capillary and entrainment limits were found as 52.6 W and 98.65 W, respectively. Mansour [17] researched the heat convection limits and heat transfer coefficient for a heat pipe using copper-acetone at various vapor temperatures. A new correlation for the heat transfer coefficient was developed. Latent heat evaporation, pipe diameter, and Reynolds number were effective on all heat transfer limits presented. It was observed that while an increment in the capillary, entrainment and capillary limits occurs with the increase in vapor temperature, the boiling limit is reduced.

THE CONCEPT OF HEAT PIPE

A heat pipe is a mechanism that makes it possible to transport thermal energy efficiently. It consists of a structure whose inner surface is covered with a thin layer of porous material, usually called grooved. The container can be made in a cylindrical shape or in any other suitable shape. The pores of the wick are filled with a working liquid suitable for the application, and the liquid vapor covers the remaining internal volume. Since the vapor and its liquid are in equilibrium, the pressure value in the vessel is same to the vapor pressure value, which conforms with saturation conditions [18].

Heat pipes have a simple configuration and a simple heat transfer mechanism. The heat pipe structure is presented in Fig. 1. Heat pipes allow very efficient heat transfer from one end to the other. When heat is applied on the evaporator part, while the working liquid vaporizes from the wick, it causes the condensation of the vapor on the wick in the condensation part and removes heat by releasing the latent heat of the vapor [18].

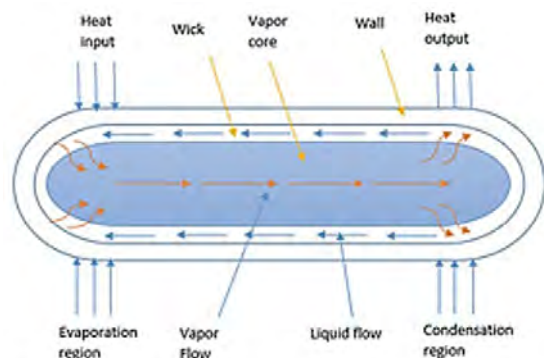


Figure 1. Structure of heat pipe

Heat Pipe Nuclear Reactors

Reactors require a circulating pump or transport fission or decomposition heat with liquid or gas based on a natural circulation, so the use of heat pipes for primary heat transfer is a new approach. The usage of heat pipes technology for nuclear reactors is new for the nuclear industry. However, heat pipe technology has been researched for decades and numerous tests have been conducted in both radiation and non-radiation test environments.

A heat pipe reactor simplifies system integration. Namely eliminating the components required for a pumped loop. This simplifies the system. Other advantages of using heat pipes in a nuclear reactor include modularity, testability, simplified system integration, passivity, and elimination of single point failures. It has also been suggested that the reactor design can operate for more than 10 years without adding fuel and is best suited to serve as a nuclear battery rather than a central power source [19,20].

In this study, the effects of important parameters affecting the capillary limit, such as porosity radius, wick permeability, and wick radius were investigated in a heat pipe reactor with potassium liquid as working fluid. Besides, the effect of the porous radius was studied for entrainment limit.

MATERIALS AND METHODS

The dimensions and materials of the potassium liquid heat pipes used in this study were taken from the literature [21] and the sizes of the heat pipes are presented in Table 1.

Table 1. Heat Pipe Dimension [21].

Evaporation length	450 mm
Adiabatic length	600 mm
Condenser length	1200 mm
Vapor core radius	18 mm
Wall thickness	30 mm
Wick thickness	26.4 mm

The operating temperature of the heat pipe nuclear reactor which is a hypothetical nuclear power plant was assumed to be 650 K and calculations were made based on 650 K. The potassium working fluid was used following the work of [22, 23] and at the above assumed temperature. Neutron absorption values are also one of the important factors in selecting a material for a nuclear reactor. Potassium is a suitable material for use in nuclear reactors because it has a low neutron absorption cross section.

The most appropriate correlations for the capillary limit were taken from the literature to correctly calculate the heat extraction value in a heat pipe nuclear reactor. The

necessary parameters for the heat pipe calculations were taken from the values given in Table 1. In addition, the thermophysical properties of potassium were calculated using Ref [24-27].

The porosity radius and wick permeability of the sintered copper tube heat pipe were selected and evaluated following the literature [28-31]. Some important parameters affect the capillary limit, such as porosity radius, wick permeability, wick radius, thermophysical properties of the fluid, and contact angle. Five different porosity radius (10.1×10^{-6} , 10.225×10^{-6} , 10.35×10^{-6} , 10.425×10^{-6} , and 10.6×10^{-6} m) and five different wick permeabilities (4.75×10^{-12} , 5×10^{-12} , 5.25×10^{-12} , 5.5×10^{-12} , and 5.75×10^{-12} m²) were considered and the effects of these parameters on the capillary limit were investigated. In these calculations, the capillary limit was calculated using Eq. (1) and it is given as follow,

$$Q_c = \frac{\sigma L_v \rho_l}{12 \mu_l} \cdot \frac{KA_w}{l_{eff}} \cdot \left(\frac{2}{r_{eff}} - \frac{\rho_l \cdot g \cdot \cos \psi \cdot l_t}{\sigma} \right) \quad (1)$$

In Eq. (1), l_v is latent heat (J/kg), σ is surface tension (N/m), A_w is cross-sectional area of wick (m²), ρ_l is density of liquid (kg/m³), K is wick permeability (m²), μ_l is viscosity of fluid (N-s/m²), r_{eff} effective porosity radius of wick (m), g is gravitational force (9.8 m/s²) and l_t is total length of heat pipe (m). where ψ is the contact angle between the liquid and the wick. Here this angle is assumed to be 90°. r_{eff} is the effective radius of the surface pore (m) and K (wick permeability) values were taken from ref [28-31] in accordance with the literature. l_{eff} is the effective length of the heat pipe (m) and is expressed as follows;

$$l_{eff} = \frac{L_{evaporator}}{2} + L_{adiabatic} + \frac{L_{condenser}}{2} \quad (2)$$

where $L_{evaporator}$ is the evaporation zone length (m), the $L_{adiabatic}$ is adiabatic zone length (m) and the $L_{condenser}$ is the condensation zone length (m).

Five different porosity radii (10.1×10^{-6} , 10.225×10^{-6} , 10.35×10^{-6} , 10.425×10^{-6} , and 10.6×10^{-6} m) were considered and the effects of these parameters on the entrainment limit were investigated. The entrainment limit was calculated by using Eq. (3) The equation is given as follow [28];

$$Q_{sr} = A_v \cdot L_v \cdot \sqrt{\frac{\rho_v \cdot \sigma}{2 \cdot r_c}} \quad (3)$$

Here, r_c is the hydraulic radius of the surface pore (m), A_v is vapor core cross-sectional area (m²) and ρ_v is vapor

density (kg/m^3). It is assumed that the wick hydraulic radius is equal to the effective of porosity radius for entrainment limit.

All calculations are done by using calculator.

RESULTS AND DISCUSSION

Capillary Limit

The capillary limit is related to the fundamental conditions that enable heat pipe operation and is formed due to capillary pressure differentiation at the vapour-liquid interfaces in the section of the evaporator and condenser. The driving potential for liquid circulation is the capillary pressure differentiation, the maximum capillary pressure has to be higher than the sum of all pressure drops in the heat pipe.

The maximum heat transfer rate can be specified because of capillary limitation for most of the heat pipes, [28,32].

Effect of Porosity Radius on Capillary Limit

The pore radius directly affects the capillary pumping potential, as a smaller pore radius results in higher capillary pressure. Pore size and wick properties affect the operating limits of heat pipes. It has become a popular topic to work on the fabrication of new wicks with improved properties that can hinder the development of vapor in the porous structure or release it easily. Many studies have been conducted on the effects of the properties of the porous structure on heat limitation [32-34].

Fig. 2 demonstrates the variation of the capillary limit with temperature for all effective porosity radii. Eq. (1) is used to calculate the capillary limit. As can be seen from the figure, the capillary limit does not change significantly with

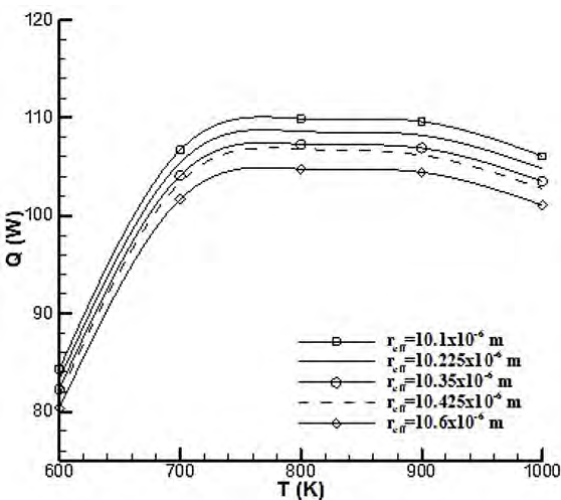


Figure 2. The variation of capillary limit with temperature for all effective porosity radius

increasing temperature. The values of capillary limit were calculated when the effective porosity radius was 10.1×10^{-6} , 10.225×10^{-6} , 10.35×10^{-6} , 10.425×10^{-6} and 10.6×10^{-6} m ($K=4.75 \times 10^{-12} \text{ m}^2$). The capillary limit changes inversely with the effective porosity radius. For this reason, the capillary limit values decrease as the effective porosity radius increases. The highest capillary limit values were found the effective porosity radius was 10.1×10^{-6} m, while the lowest capillary limit values were found when the porosity was 10.6×10^{-6} m.

The graph of capillary limits for five different effective porosity radii at a temperature of 650 K is presented in Fig. 3. It can be seen from the Fig. 3, the value of the capillary limit value decreases as the effective porosity radius increases. When the values of effective porosity radius are 10.1×10^{-6} , 10.225×10^{-6} , 10.35×10^{-6} , 10.425×10^{-6} and 10.6×10^{-6} m at a temperature of 650 K, the capillary limit values are 95.5, 94.3, 93.2, 92.5 and 90.8 W, respectively. The highest capillary limits occurred when the effective porosity radius was 10.1×10^{-6} m. Since the effective porosity radius inversely proportional with the capillary limits, the highest capillary limit is obtained when the lowest effective porosity radius is used.

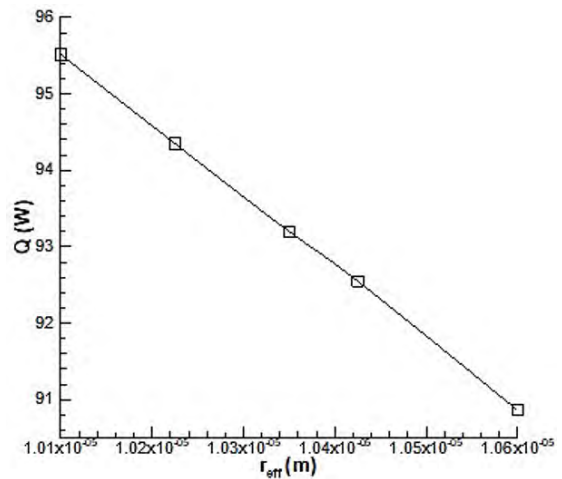


Figure 3. Variation of capillary limit values for all porosity radius at a temperature of 650 K.

Effect of Wick Permeability on Capillary Limit

The increment in the permeability can cause a decrement in flow resistance and increment of the capillary limit. The wick permeability is one of the most significant parameters effecting the capillary limit. The effect of wick permeability on capillary limit is an interesting topic for researchers [35,36].

Fig. 4 shows the change in the effect of wick permeability on the capillary limit with temperature. As can be seen, the capillary limit does not change significantly with incre-

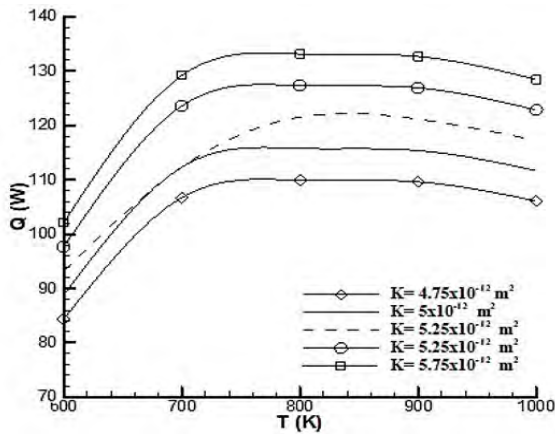


Figure 4. Variation of the effect of wick permeability on the capillary limit with temperature

asing temperature. The capillary limit increases with increasing wick permeability. The reason for this is that the wick permeability and the capillary limit are directly proportional. The capillary limits were calculated for wick permeability 4.75×10^{-12} , 5×10^{-12} , 5.25×10^{-11} , 5.5×10^{-12} and $5.75 \times 10^{-12} \text{ m}^2$ (the porosity radius was assumed to be $10.1 \times 10^{-6} \text{ m}$). The results show that the highest capillary limit is obtained when the wick permeability is $5.75 \times 10^{-12} \text{ m}^2$, while the lowest capillary limit is obtained when it is $4.75 \times 10^{-12} \text{ m}^2$.

The graph of capillary limits for five different effective wick permeability values at a temperature of 650 K is shown in Fig. 5. The wick permeability is plotted such that the capillary limit value increases with increasing permeability. From Fig. 5, it can be seen that as the permeability increases, the capillary limit value also increases. At 650 K, when the permeability of the wicks is 4.75×10^{-12} , 5×10^{-12} , 5.25×10^{-11} , 5.5×10^{-12} and $5.75 \times 10^{-12} \text{ m}^2$, the capillary limit values are 95.5, 100.5, 102.7, 110.6 and 115.6 W, respectively. The case where the capillary limit is the highest is the one where the wick permeability value is $5.75 \times 10^{-12} \text{ m}^2$.

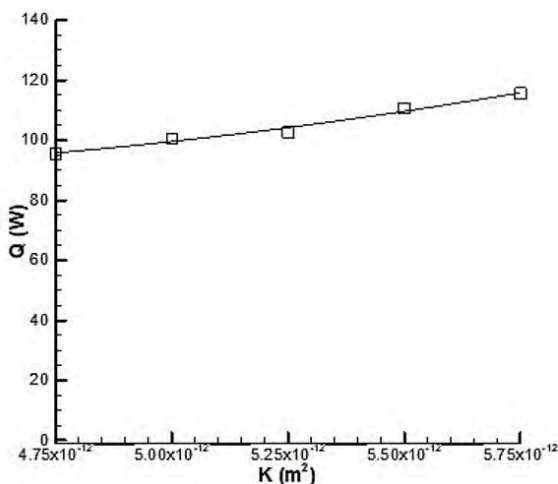


Figure 5. Variation of capillary limit values for all wick permeability values at a temperature of 650 K

Entrainment Limit

Since vapor and liquid move in converse directions, a shear force occurs at the interface between liquid vapor interfaces. At high relative speeds, liquid droplets can break off from the wick surface and enter the vapor flowing into the condensation region. If the entrainment is too much, the evaporation zone dries out. The entrainment limit is the heat transfer rate at which this phenomenon occurs. Entrainment is determined by the sound of droplets hitting the condenser region end of the heat pipe. The entrainment limit is generally associated with either low or medium temperature small diameter heat pipes or heat pipes has high temperature when heat input is high in the evaporator zone. Eq. (3) is used to calculate the entrainment limit.

Effect of Porosity Radius on Entrainment Limit

Fig. 6 shows the variation of entrainment limit with temperature for all effective porosity radii. Eq. (1) is used in the capillary limit calculations. It can be seen from Fig. 5 that entrainment increases with increasing temperature. The entrainment limits were calculated once the effective porosity radius was 10.1×10^{-6} , 10.225×10^{-6} , 10.35×10^{-6} , 10.425×10^{-6} , and $10.6 \times 10^{-6} \text{ m}$. The entrainment limit and the effective porosity radius are inversely proportional. Therefore, the entrainment limits reduce as the effective porosity radius increases. When the effective porosity radius was $10.1 \times 10^{-6} \text{ m}$, the highest entrainment limit was achieved.

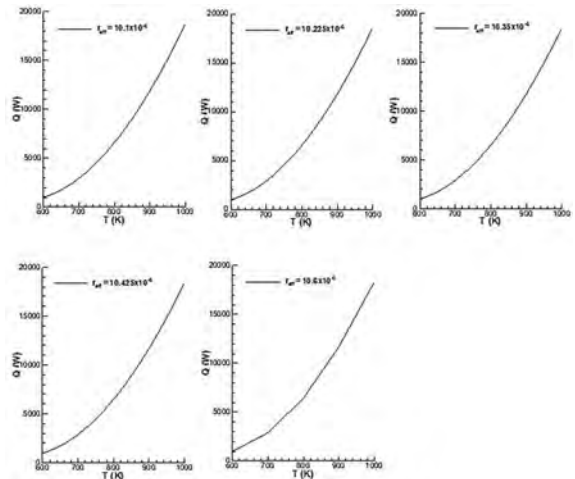


Figure 6. Variation of entrainment limit with temperature for all effective porosity radius.

In Fig. 7 entrainment limits for five values of the effective porosity radius at a temperature of 650 K is presented. Increasing the effective porosity radius resulted in decreasing the entrainment limits. At 650 K, when the effective porosity radius is 10.1×10^{-6} , 10.225×10^{-6} , 10.35×10^{-6} , 10.425×10^{-6} , and $10.6 \times 10^{-6} \text{ m}$, the entrainment limits are 2310, 1968, 1956,

1949, and 1945 W, respectively. The highest entrainment limit was reached when the effective porosity radius is 10.1×10^{-6} m.

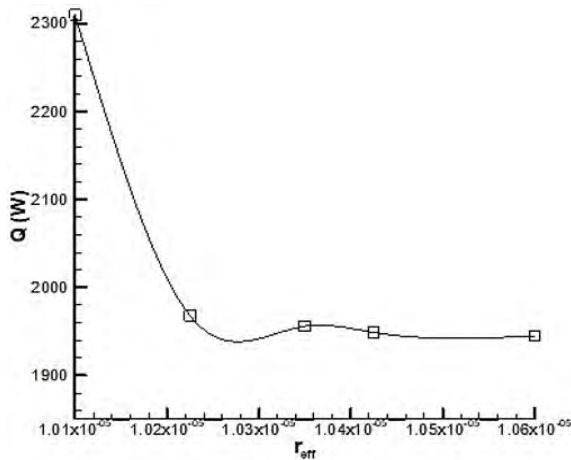


Figure 7. Variation of entrainment limit values for all values for all porosity radius at a temperature of 650 K

CONCLUSION

In this study, the effects of effective porosity radius and wick permeability on capillarity and entrainment limit in a heat pipe nuclear reactor were investigated. Based on the results of this study, the following conclusions are made:

- The highest capillary limit was reached when the effective porosity was 10.1×10^{-6} m.
- A decrease in effective porosity results in an increase in capillary limit
- The case where the capillary limit is obtained highest is when the wick permeability value is 5.75×10^{-12} m².
- An increase in wick permeability results in an increase in capillary limit.
- When the effective porosity radius was 10.1×10^{-6} m, the highest entrainment limit was achieved.
- An decrease in effective porosity results in an increase in entrainment limit.
- It has been found that the capillary limit is more effective than the entrainment limit in determining the heat pipe limitation. This is because the capillary limit has lower temperature values.
- For this heat pipe reactor, the best effective porosity radius and permeability are determined as 10.1×10^{-6} m and 5.75×10^{-12} m², respectively.

CONFLICT OF INTEREST

The author deny any conflict of interest.

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Strontium Isotopes, Ostracod Fauna, and Paleoenvironmental Characteristics in the Late Miocene Sequence of the Mut/Dağpazarı Region, Southern Turkey

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ABSTRACT

The primary focus of this study was the Dağpazarı village in the Mut region of Mersin, southern Turkey. In this research area, two stratigraphic sections were meticulously measured. The study conducted a comprehensive examination of the Middle-Late Miocene period in the Dağpazarı, Ballı, and Mut Formations by analyzing the ostracod fauna and utilizing strontium isotope chemostratigraphic dating. This research determined that the upper levels of the Mut/Köselerli formations, specifically from the Burdigalian to Serravallian, signify the commencement of the Miocene succession in the study area. The Dağpazarı Formation, characterized by abundant silty-clay, *Ostrea* fossils, and lignite layers, is deposited unconformably just above these levels. This formation contains the following ostracod taxa; *Bairdia subdeltoidea*, *C. glypta*, *Cytheridea acuminata acuminata*, *Acanthocythereis hystrix*, *Krithe monosteracensis*, *Neomonoceratina mouliana*, *Hemicyprideis sp.*, *Cistacythereis caelatura*, *Cyherella terguemi*, *T. prava*, *K. langhiana*, *A. ulicznyi*, *Pokornyella deformis minor*, *Loxoconcha alata*, *Tenedocythere salebrosa*. Furthermore, the planktonic foraminifera species are; *O. universa*, *Globigerinoides trilobus*, *Glb. ruber*, *Orbulina bilobata*, *Glb. sacculifer*, *O. suturalis*, and the formation includes abundant bryozoa, echinoid spines, gastropods such as *Terebralia* at distinct levels, and fish otolith. The formation, dating from the late Serravallian to the early Tortonian, exhibits the shallow reef characteristics that continued to develop in the late Miocene. The formation consists of dark green, bulbous weathered claystone, *Bairdia subdeltoidea* and *Ostrea* which are reduced in size at the levels that pass into hard clayey sandstone, abundant benthic foraminifera with abundant echinoid spines. The formation consists of benthic foraminifera, hard clayey sandstone, and weathered dark green claystone, which contains numerous echinoid spines. *Ostrea* and *Bairdia subdeltoidea* are also present. The upper section of the analyzed succession concludes with silty, compact, clayey limestone layers and light-colored limestone bands. The Tirtar Ballı Formation, which conformably overlays the Dağpazarı Formation, signifies the culmination of a relatively recent reef formation during the Tortonian period. Ostracod species such as *Aurila pigadiana*, *Thalmannea hodgii*, *Buntonia sublatissima dertonensis*, *Bairdia subdeltoidea*, *Aurila sp.* *Bassiouni* have been defined. The limestones also contain abundant benthic foraminifera and echinoid spines. The $^{87}\text{Sr}/^{86}\text{Sr}$ ratio analyzed from the carbonate sample obtained from the Dağpazarı formation is 0.708920. Based on these isotope data, the age of the Dağpazarı formation was calculated to be 8.7 million years (Ma).

Keywords:

Mut; Dağpazarı; Planktonic foraminifera; Strontium isotope; Ostracod

INTRODUCTION

The study area is situated in the northern part of the town center of Mut, within the Central Taurus Mountains (Fig. 1). In the initial geological investigations conducted in the research area and its vicinity, particular emphasis was placed on studying

the structural evolution of the region since the Paleozoic, mapping the rock formations, and analyzing tectono-stratigraphic developments. Following this, numerous researchers conducted comprehensive studies in the fields of general geology, paleontology,

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and stratigraphy [1-23]; [24-33]. Economic geology studies have predominantly focused on oil and coal [34-35]. Furthermore, there has been a significant increase in studies related to carbonate precipitation in Neogene rocks. This research was conducted to provide a comprehensive analysis of the Neogene sediments exposed in the Dağpazarı area, with a primary focus on ostracod fauna. In the Mut Basin, situated in the Middle Taurus Belt, calcareous nannofossil biochronology has been documented in the Mut-Ermenek section, specifically in the Dağpazarı reef. This reef developed as a result of the Miocene marine transgression and is primarily found in the upper sections of the reef, known as the Dağpazarı Formation. Coral biofacies were identified by Gürlü [22], and Ilgar et al. [137] documented the late Serravallian to early Tortonian dug valley fill sediments, known as the Dağpazarı Formation [33-23]. The main objective of this study was to conduct a comprehensive analysis, including stratigraphic, chemostratigraphic (Sr isotopic), and micropaleontological examinations, with a specific focus on ostracod fauna. The research highlights the relatively recent reef sediments found in the Dağpazarı Formation, which is the primary subject of this study, as well as the overlying Tirtar/Ballı Formation.

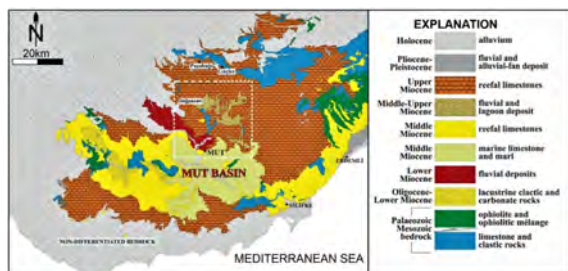


Figure 1. Geological map of the Dağpazarı research area and its vicinity [23].

The ostracod assemblages from the Late Miocene (Tortonian) in this research were examined and compared with ostracod faunas from Late Miocene (Tortonian) studies conducted in other regions of the Eastern Mediterranean in Turkey. Additionally, isotope data reported from nearby areas were analyzed in conjunction with the data obtained in this study. Ostracod assemblages from the Tortonian period in these Eastern Mediterranean-origin basins, namely Antalya/Serik, Mut, Mut/Dağpazarı, Karaman, Silifke-Erdeмли/Mersin, Adana, and Antakya basins, were compared with the ostracod assemblage in this study. It was observed that they shared similar species. This study elucidates the formation of a young reef during the Tortonian period in the Adana Basin (Kuzgun Formation) [36], as well as in Silifke-Erdeмли (Sarıaydın Formation) [37]. Similar depositional conditions and young reef characteristics were also identified in the Antakya Basin (Nurzeytin Formation) [38-39] (Fig. 8).

MATERIAL AND METHODS

Paleontological Analysis

The research was carried out on the 1/25000 scaled Mersin O30b3 map sheet. Measured sections were taken from two different areas in Dağpazarı Village and 50 washing samples were collected for micropaleontological analyses. The laboratory washing method was performed to obtain the ostracod fauna. 150 grams of each of the hard and moderately soft samples obtained from the sections were taken and divided into small pieces by placing them between thick paper and hitting them with a hammer. Crumbled samples were placed in 1-liter glass beakers and hot water and 15% diluted hydrogen peroxide (H_2O_2) were added to disintegrate and left for 24 hours to dissolve. The samples have been washed under pressurized water with a set of 60, 120, 230 mesh sieves and then dried in an oven and put into separate bags according to their sieve numbers. After the separation of the microfossils contained in the samples from the grains, the genus and species of the samples collected in the collection slides were determined. 28 ostracod genera and 44 taxa have been defined in the research.

Identified species and genera have been counted, lateral and vertical distribution of ostracods have been enumerated and their numerical abundances have been defined. Symbols describing the semiquantitative frequency of ostracods are used in this distribution table. Very rare (1-2 cover) ve rare (3-5 cover) frequencies are denoted by symbols such as r + and o, common (6-15 cover), frequent (16- 25 cover) and very frequent (>25 cover) and frequencies ●, □, ■. Paleoenvironmental interpretation of the research area was conducted based on the statistical and relative data. This interpretation was carried out in accordance with previous works by Morkhoven [110], Doruk [111], Bassiouni [112], and Freels [40-43]. Plate 1-2 was created by choosing scanning electron microscope (SEM) images of specific ostracod species and genera that were identified in these studies.

Petrographical and Isotopical Analyses

Thin sections of the samples were analyzed using binocular microscopes under polarized light (Leica DMEP). Subsequently, these thin sections were further examined using an optical microscope that utilized both transmitted and reflected light. Two of the most commonly utilized classifications are those developed by Folk and Dunham [44-45,46]. The thin sections of the limestones from the Dıvlek and Maz Formations were prepared by the Department of Geological Engineering at Çukurova University. The petrographic examination was conducted using the Leica DMEP microscope at Çukurova University. Strontium isotope geochemistry experiments were carried out at the Radiogenic Isotope Laboratory, R & D Training, and Mea-

surement Center of METU (Sr Isotope Ratio Analysis Experimental Instruction), following the detailed procedures and conditions outlined by Köksal et al. [47]. The isotope analyses were conducted by METU and involved using ultrapure water and chemicals. Weighing, chemical dissolution, and chromatographic operations were performed in a clean laboratory setting that met class 100 cleanroom standards. Specifically, certain sedimentary (limestone) samples underwent $^{87}\text{Sr}/^{86}\text{Sr}$ isotopic analyses at the METU Central Laboratory's Radiogenic Isotope Laboratory in Ankara, following the analytical techniques outlined by Köksal and Göncüoğlu [48].

RESULTS

Stratigraphy

The Miocene units in the research region can be listed from bottom to top as follows: Langhian-Serravalian Mut Formation, late Serravalian-early Tortonian Dağpazarı Formation, and Tortonian Tirtar/Balı Formation (Fig. 2).

Lithostratigraphy

Mut Formation

The Mut Formation was initially named by Sezer [119], and later Gedik et al. [34] also used this name [49, 34]. The reefal Mut Formation can be correlated with the fol-

lowing formations: Silifke Formation [27], Göktepe Reef Limestone Member defined around Ermenek-Karaman [11], Mut Formation around Ermenek [50], and Karaisalı Formation in the Adana Basin [51]. The Mut Formation is characterized by reefal limestone and is found at the base of the succession in a relatively low thickness in this study. The age of the formation has been defined by different researchers as late Burdigalian-Langhian [23], Langhian-Serravalian [28-30,17], Middle Miocene [19-21], and late Serravalian-Tortonian [22]. When analyzing the age of the Mut Formation based on the age given by the overlying unit in this study, it is reported as Burdigalian-Serravalian (Fig. 3).

Dağpazarı Formation

The Dağpazarı Formation was initially defined by Atabey et al. [87], while Gedik et al. [34] referred to it as the Köseleli Formation [17,34]. This formation begins with silt, clay, and clayey limestone, and includes oostreal silty and sandy layers, greenish claystone with vegetation, and lignite. Towards the upper part of the succession, there is a lithological transition to fossiliferous sandstones and hard clayey sandstones (Fig. 2).

The age of the Dağpazarı Formation has been previously reported as Serravalian [17] and late Serravalian-Tortonian [23]. In this study, the age of the formation was determined as late Serravalian-early Tortonian, primarily based on the ostracod content and supported by strontium isotope data.

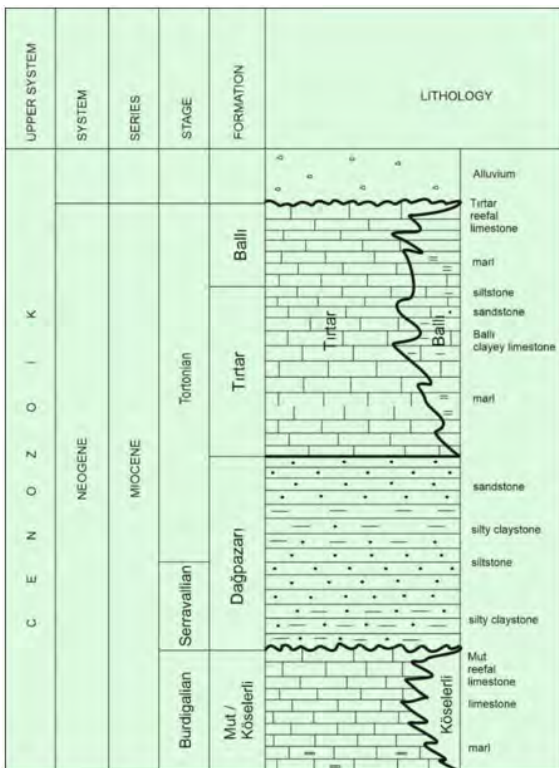


Figure 2. Generalized stratigraphic section of the research region of Dağpazarı [47].



Figure 3. a. General view of the outcrops of Mut formation (view to north) b-c. General outcrop of Dağpazarı formation and clayey limestone.

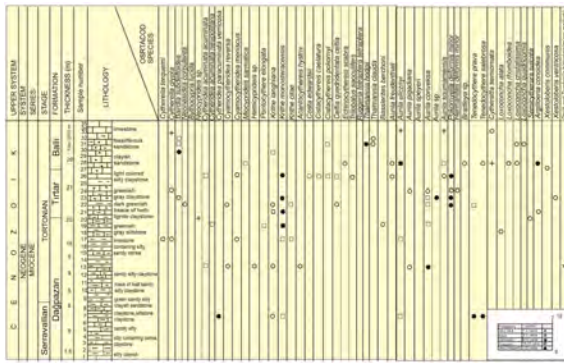


Figure 4. The distribution of the ostracod species in the Dağpazarı I measured stratigraphic section.

Tirtar Formation

The Tirtar Formation was initially named by Atabey et al. [87]. This unit is characterized by limestone as the predominant lithology and contains algae, corals, benthic foraminifers, and mollusks [17]. Atabey et al. [87] and Ilgar et al. [93] proposed the age of the formation as Tortonian (Fig. 2) [17,34]. In this study, a predominant consideration of ostracod content and strontium isotope data led to the determination of the formation's age as Tortonian.

Ballı Formation

Atabey et al. [87] the unit was named for the first time and this name was given because the type section location is in the village of Ballı [17]. Planktonic foraminifera and nannoplanktons have been defined in the formation where claystone, marl and clayey limestone form the dominant lithology (Fig.2). Atabey et al. [87] found *Globigerinoides obliquus extremus* in the unit [17]. In addition, Ilgar et al. [93] suggested the age of the formation as Tortonian [23]. In this study, when the ostracod content and strontium isotope data are evaluated predominantly, the age of the formation is considered as Tortonian.

Measured Stratigraphic Sections

Stratigraphic sections were measured from two distinct ridges by selecting strategic locations within the research area. These locations offered the best exposure of successions providing Late Miocene age information in the Dağpazarı region.

Dağpazarı I Measured Stratigraphy Section

The section was measured between coordinates X1: 36.829371, Y1: 33.464047, Z1: 1287 m, and X2: 36.828976, Y2: 33.464154, Z2: 1492 m, with a total thickness of 205 meters. The section begins at the base with ostreid-rich, clayey, and silty layers belonging to the Dağpazarı Formation. As we move upwards, it transitions into weathered, greenish-gray claystone, silty clay, and fossiliferous clay-siltstone layers. Above this, the Tirtar/Ballı Formation is found, showing a smooth transition. The upper part of the succession is characterized by clayey sandstone, fossi-

liferous clayey sandstone, which remains relatively intact. This formation characterizes a reef in unweathered silty, clayey limestone (Tirtar) and upwardly unweathered limestone (Ballı) lithology. The following ostracod taxa were reported at the base levels of the Dağpazarı Formation in the section: *Cytherella terguemi*, *Cytheridea acuminata acuminata*, *Cytheridea acuminata verrucosa*, *Krithe monosteracensis*, *Krithe langhiana*, *Aurila ulicznyi*, *Cytherella glypta*, *Cytheridea acuminata neapolitana*, *Miocyprideis sarmatica*, *Hemicyprideis sp.*, *Krithe monosteracensis*, *Krithe citae*, *Aurila convexa*, *Ruggieria tetraptera tetraptera*, *Aurila soummamensis*, *Tenedocythere salebrosa*, *Pokornyyella deformis minor*, *Tenedocythere prava*, *Echinocythereis scabra*. In the upper levels, *Bairdia subdeltoidea*, *Thalmanzia hodgii*, *Thalmanzia clauda*, *Aurila soummamensis*, and *Aurila ulicznyi* were identified in the middle level of the formation. At the bottom levels, gastropods like *Terebralia* and fish otoliths were found. It's also notable that there is an increase in shallowing, and lagoonal conditions seem to dominate the environment. The ostracod genera identified in this formation generally suggest an epineritic environment, including *Ruggieria*, *Tenedocythere*, *Cytheretta*, *Aurila*, and *Pokornyyella*. Additionally, ostracod species that typically indicate infraneritic environments, like *Krithe*, *Echinocythereis*, and *Buntonia*, have also been reported. The presence of ostracod species characterizing lagoon-littoral environments suggests a transitional feature from very shallow marine conditions to partially deep-sea conditions, including species like *Hemicyprideis*, *Loxocorncha*, and *Loxocorniculum*. Hence, it can be concluded that there is data indicating the presence of reef front and back textures in the Late Miocene (Tortonian) sequence. Shallow-water (epineritic depth) ostracod species like *Bairdia subdeltoidea*, *Aurila ulicznyi*, and *Aurila soummamensis* symbolize the reef's back and roof within the clay layers between the limestone beds of the Tirtar/Ballı Formation.

In the stratigraphic section, the Tirtar/Ballı Formation contains a wealth of bryozoa, echinoid spines, and gastropods, including *Terebralia*, which is also observed at various levels within the section.

Dağpazarı II Measured Stratigraphy Section

The section was measured between coordinates X1: 36.826641, Y1:33.460034, Z1:1315 m., and X2: 36.826871, Y2:33.461080, Z2:1420 m. The section has a total thickness of 135 m and consists of cream-colored clayey limestone, clayey limestone-sandstone alternation, and sandstone belonging to the Dağpazarı Formation, which are observed at the lower, middle, and upper levels of the succession. The Dağpazarı Formation is succeeded by the reefal Tirtar/Ballı Formation, which consists of claystone, hard clayey limestone, and hard limestone, conformably overlaying it (Fig.5).

The ostracod species observed at the base levels of the Dağpazarı Formation in the section include *Cytherella glypta*, *Neonesidea corpulenta*, *Bairdoppilata supradentata*, *Neomonoceratina mouliana*, *Ruggieria tetraptera tetraptera*, *Aurila convexa*, *Aurila albicans*, *Aurila soummamensis*, *Aurila woodwardii*. Planktonic foraminifera species reported at the base of the section comprise *Trilobatus sacculifers*, *Orbulina suturalis*, *Morozovella angulosa*. Planktonic foraminifera species identified in the middle and upper levels include *Cytherella terquemi*, *Aurila sp.* Additionally, ostracoda species such as *Globigerinoides ruber*, *Orbulina bilobata*, *Orbulina suturalis*, *Orbulina universa* have been reported. The ostracod species identified in the claystone and clayey limestone levels of the Tirtar/Ballı Formation include *Aurila convexa*, *Krithe langhiana*, *Pokorniyella deformis minor*, *Ruggieria tetraptera tetraptera*, *Acanthocythereis hystrix*, *Aurila speyeri*, *Aurila soummamensis*, *Aurila ducasseae*, *Tenedocythere mediterranea*, *Loxoconcha tumida*, *Argilloecia conoidea* (Fig.5). This assemblage characterizes the reef lagoon and the core of a young reef, indicating that the section is influenced by lagoon-littoral conditions as well as the neritic marine environment.

Strontium Isotope Chemostratigraphy

Strontium isotope chemostratigraphy plays a crucial role in deciphering the Earth's geological history. The $^{87}\text{Sr}/^{86}\text{Sr}$ pattern in seawater can be employed for robust correlations when other chemostratigraphic, lithostratigraphic, or biostratigraphic indicators prove to be inadequate. The accuracy of reconstructing seawater strontium isotopes depends significantly on two factors: the quality and reliability of chronological control in the reference data and the preservation of the samples, both of which can vary with the age of the period under examination.

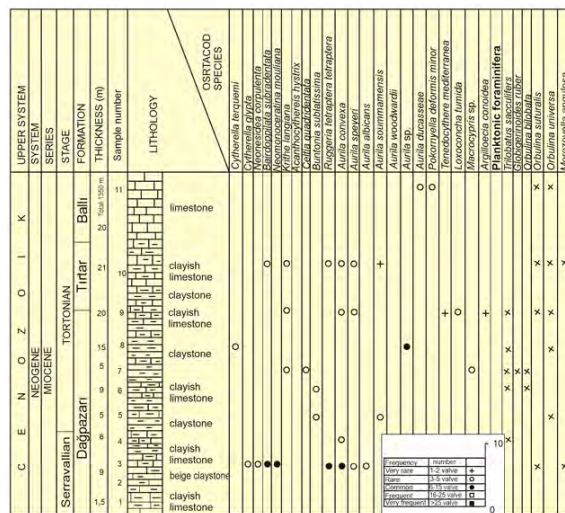


Figure 5. The distribution of the ostracod species in the Dağpazarı 2 measured section

Marine strontium ratios ($^{87}\text{Sr}/^{86}\text{Sr}$) have evolved over the Earth's history, primarily driven by the interplay between unradiogenic strontium sourced from the Earth's mantle and radiogenic strontium from terrestrial input (continental crust) [54-55], as illustrated in Fig. 6 [52-53].

Three samples (Dp-1; 0,708920±15, Dp-2; 0,709644±8, Dp-3; 0,709733±7) were gathered from the studied area in order to analyze strontium and two of these samples did not yield results due to effects such as contamination and diagenesis. The ratio of $^{87}\text{Sr}/^{86}\text{Sr}$ analyzed from the limestone sample collected from the Dağpazarı formation is 0.708920. The age of the Dağpazarı formation was estimated as 8.7 Ma based on these isotope data.

DISCUSSION

Ostracod fauna-based correlation of Late Miocene (Tortonian) lithostratigraphic units of the study area with other Late Miocene (Tortonian) lithostratigraphic units in the Eastern Mediterranean region of Turkey is depicted in Fig. 7.

Antalya (Serik), Karpuzçay Formation

Karpuzçay formation was first named and reported by Akay et al. [57]. The type locality of the formation is Karpuzçay Village in the Antalya Miocene Basin. This formation comprises siltstone, thin-bedded sandstone, and sandy limestone alternations. The ostracod assemblage identified in the formation includes *Bairdia subdeltoidea*, *Miocyprideis sarmatica*, and *Aurila soummamensis* [57-58] (Fig.8).

Dağpazarı/Mut, Dağpazarı and Tirtar/Ballı Formations

The Dağpazarı/Mut, Dağpazarı, and Tirtar/Ballı formations were initially named by Atabey et al. [17]. The Dağpazarı Formation is characterized by clayey, weathered, greenish-gray siltstone at its base, which transitions into oostreal-bearing clayey siltstone, and further up

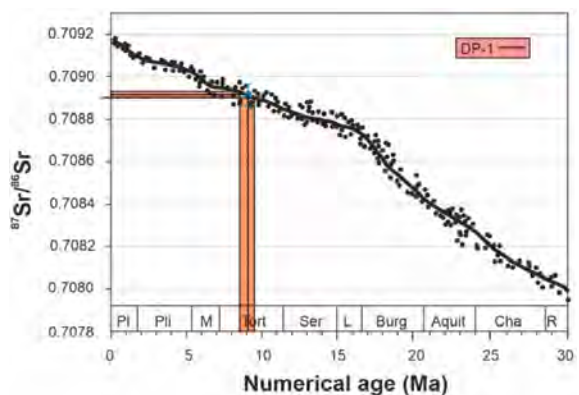


Figure 6. Strontium isotope variation curve for the Miocene interval [56].

within this formation includes the following genera and species: *Cytherella vandenboldi*, *C. creutzburgi*, *C. sordida*, *C. seminulum*, *Neomonoceratina acupicta*, *N. interiecta*, *Miocyprideis sarmatica*, *Parakrithe robusta*, *Cyprideis anatolica*, *Krithe monosteracensis*, *C. pannonica*, *Cytheridea acuminata acuminata*, *Cistacythereis pokornyii*, *C. caelatura*, *Loxoconcha tumida*, and *Paracypris polita*. The age of the Sarıaydın Formation was given as Tortonian? [27] (Gökten, [97]) and Late Serravallian-Tortonian [37], (Fig.8).

Kuzgun (Adana) Formation

The Formation (Adana) Formation was originally defined by Schmidt [51], and its type locality is situated in Kuzgun Village along the Adana-Karaisalı road. This formation is characterized by a transition from meandering river sediments at the base to shallow marine conditions in the upper levels. During the Tortonian, the region experienced sea level fluctuations, with alternating rises and falls [61]. Within this formation, you can find substantial fossiliferous greenish claystone, light-colored clayey limestone, and well-sorted yellowish-cream colored sandstones with a reefal character, particularly at the İncirlik locality, situated to the southeast of Adana [36]. The ostracod community in this formation is exceptionally diverse, including the following species: *Cytherella vulgata*, *C. glypta*, *Neomonoceratina mouliana*, *Schneidrella dromas*, *Cyamocytheridea meniscus*, *Carinocythereis antiquata antiquata*, *Aurila soummamensis*, *Loxoconcha rhomboidea*, *Paracypris polita*. The formation is attributed to the Tortonian age [36,61-62].

Nurzeytin (Antakya Basin) Formation

The Nurzeytin Formation in the Antakya Basin was initially designated by Selçuk in [63]. The type locality is situated in the vicinity of Nurzeytin, Yazır, Sivrikavak, and Babatorun. This formation is characterized by reef-like lithologies including sandstone, clayey limestone, marl, and claystone. The ostracod assemblage in this formation is highly diverse, and the following taxa have been identified: *Cytherella glypta*, *Cyprideis torosa*, *Acaocythereis hystrix*, *Aurila convexa*, *A. speyeri*, *Hermanites haidingeri minor*, *Ruggieria tetraptera tetraptera*, *Tenedocythere prava*, *T. mediterranea*, *Xestoleberis ventricosa*, *X. communis*. The formation has been suggested to span the Late Serravallian-Tortonian and Tortonian ages [38-39,63]. From these descriptions, it's clear that the Tortonian development in these six significant locations in the Eastern Mediterranean Region of Anatolia is remarkably similar in terms of lithology, environmental conditions, and ostracod fauna. The ostracod fauna of the Dağpazarı Formation in this new study closely resembles the ostracod species identified from these six locations, with the exception of *Cyprideis* species, which were not encoun-

tered in this study. The environment exhibits distinct back-reef facies characteristics with lagoon-like *Neocyprideis* and lagoon-litoral ostracod species like *Hemicyprideis* and *Loxoconcha*. It also displays distinct shallow reef front and core characteristics with ostracod genera adapted to epineritic depths, such as *Acanthocythereis*, *Aurila*, *Pokornyella*, *Tenedocythere*, *Neomonoceratina*, *Pontocythere*, and *Ruggieria*. Furthermore, ostracod genera indicative of infraneritic depths and bathyal environments, such as *Macrocypris*, *Argilloecia*, *Bythocypris*, *Krithe*, and *Bradleya*, are typical of deep reef front facies (Fig. 7). The Mut Basin is situated in the Eastern Mediterranean region of the Alpine-Himalayan Mountain Belt (AHMB) and in the Central Taurus sector of the Taurus Mountains in southern Turkey.

The late Burdigalian marine transgression led to the submersion of the Antalya, Mut, and Adana basins, initiating the deposition of the first marine sediments in these basins during the Neogene. Consequently, the Burdigalian-Serravallian period witnessed the formation of the reefal limestones of the Mut Formation and the marl-clay limestones of the Köselirli Formation in the Mut Basin. As a result of the decrease in sea level in the Late Serravallian, the basin started to become shallow and a young reef deposition took place on the Mut formation reef limestones in the Late Serravallian-early Tortonian. This unit is the Dağpazarı Formation, and the reef limestones of the Tirtar Formation and the layered limestones of the Ballı Formation were deposited on the unit in the north of the Mut Basin. In the vicinity of Dağpazarı Village, the sedimentary layers consisting of mudstone, silty claystone, and sandstone that overlay the Mut Formation were initially considered part of the Köselirli Formation and examined. However, due to variations in lithology, deposition environment, and age, these layers were later designated as the Sertavul Formation. The formation typically represents a lagoon environment situated behind the reef. It is occasionally associated with fluvial deposits, coastal sand, coal seams, and limestone deposits. This rock unit has been identified as the Dağpazarı Formation, indicating its characteristics of a back-reef lagoon and alluvial fan environment. [17]. It was also stated by these authors that the Dağpazarı formation is transitional with the Köselirli and Mut formations deposited in the completely regressive phase of the sea. Early-middle Miocene sea level changes in the Mut Basin have also been studied, but clear data are not available [20, 22].

It is detailed that an incised valley, formed as a result of the late Serravallian eustatic sea-level decline, is observed, where the Dağpazarı Formation overlies the Mut reefal limestones with erosive unconformity [23]. It is mentioned that the sedimentary facies identified in the formation were deposited within this valley, following a subsequent relative

sea-level rise that occurred in the early Tortonian. A comprehensive study of planktonic foraminifera was conducted using mudstone and marl samples obtained from the Dağpazarı and Ballı Formations.

The study employed Mediterranean planktonic foraminiferal biostratigraphy and the ATNT52004 magnetic chronostratigraphy table to determine the Serravallian and Tortonian ages. It was also noted that due to the isostatic uplift of the Taurus Mountains in the late Tortonian, marine sedimentation in the Mut Basin ceased, leading to the exposure of the basin [65-67]. In this research, the fossil content of the unconformable Dağpazarı Formation overlying the Mut limestones at the base and the Tirtar/Ballı Formations, based on the ostracod fauna, was documented. These three lithological units (Dağpazarı, Tirtar/Ballı Formations) have developed with a young reef character and contain ostracod genera and species that accurately represent the back-reef-lagoon, core, and fore-reef facies.

In this new study, the Dağpazarı Formation exhibits a lagoon character with ostracod species like *Neocyprideis*, while the back reef is characterized by ostracod species such as *Hemicyprideis* and *Loxoconcha*, displaying lagoon-littoral characteristics. Additionally, the shallow reef fore-core is marked by ostracod genera with epineritic depth, including *Acanthocythereis*, *Aurila*, *Pokorniyella*, *Tenedocythere*, *Neomonoceratina*, *Pontocythere*, and *Ruggieria*. The deep reef front is identified by ostracod genera with infraneritic depth, including *Macrocypris*, *Argilloecia*, *Bythocypris*, *Krithe*, and *Bradleya*. Additionally, this study identified significant genera indicative of lagoon sediments and marine input. [23].

The study notably provided a comprehensive presentation of the ostracod genera and species specific to the fore-reef facies, marking the first such detailed account in this research. Additionally, banded levels of *Ostrea* were identified in the littoral sections of the middle levels of the Dağpazarı Formation. The presence of the genus *Ostrea* is recognized as an indicator of shallowing in the environment [68-69]. This study was conducted in a succession characterized by the deposition of a young reef, which culminated in the Tortonian age in the northern part of the Mut Basin.

CONCLUSIONS

This study was conducted in and around Dağpazarı Village, located to the north of the Mut Basin. The research area includes sandy, clayey, silty, fossiliferous, and relatively younger sequences that overlay the Mut limestones (Mut Formation). The fossil content of the Dağpazarı, Tirtar/Ballı formations, which are very thin and unconformably emplaced on the Mut formation, has been revealed by predominantly using the ostracod assemblage and

strontium isotopic data. Within this assemblage, ostracod genera indicative of a deepening neritic environment with a shallow neritic core, along with a littoral reef next to a lagoon, have been identified. This reefal succession, which originated during the Tortonian, has been investigated from lithological, chronostratigraphic, and chemostratigraphic perspectives. Furthermore, the ostracod assemblages from late Miocene (Tortonian) studies within the Eastern Mediterranean bioprovince of Turkey were also compared. In the lithostratigraphic and chronostratigraphic correlation from west to east, it was observed that the ostracod assemblages in the Tortonian of the Antalya, Mut, Karaman, Silifke-Erdemli, Adana, and Antakya basins closely resemble the ostracod assemblages found in the Tortonian of the Dağpazarı region.

Late Miocene reef-like sedimentary deposits with young reef characteristics were identified in the Late Tortonian (Miocene) successions within the Antalya, Dağpazarı/Mut, Karaman, Silifke-Erdemli, and Adana Basins, which are part of the Turkey-Eastern Mediterranean Province.

The ostracod assemblage has confirmed that the late Miocene (Tortonian) sediments in the Antakya Basin exhibit a shallow reefal character, characterized by creamy-white clayey units and marls. The $^{87}\text{Sr}/^{86}\text{Sr}$ ratio obtained from the carbonate sample within the Dağpazarı Formation is 0.708920. Based on this isotope data, the age of the Dağpazarı Formation has been calculated as 8.7 million years (Ma).

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CONFLICT OF INTEREST

Authors approve that to the best of their knowledge, there is not any conflict of interest or common interest with an institution/organization or a person that may affect the review process of the paper.

AUTHOR CONTRIBUTION

The authors shared all the roles and contributed equally to the paper.

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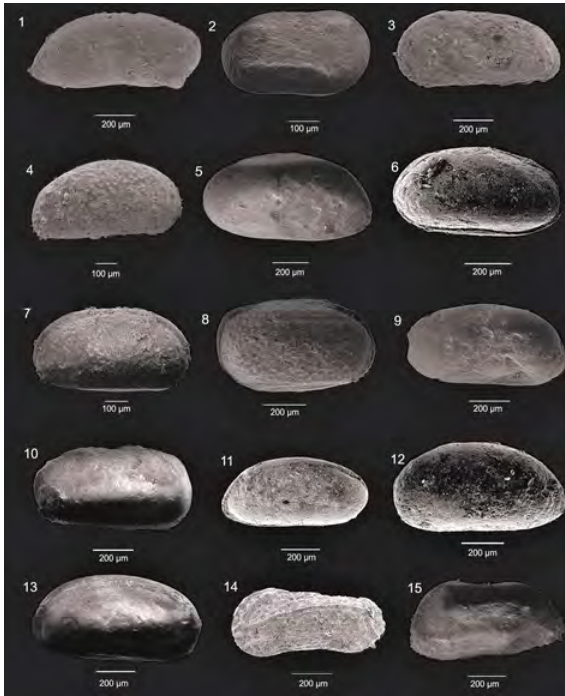
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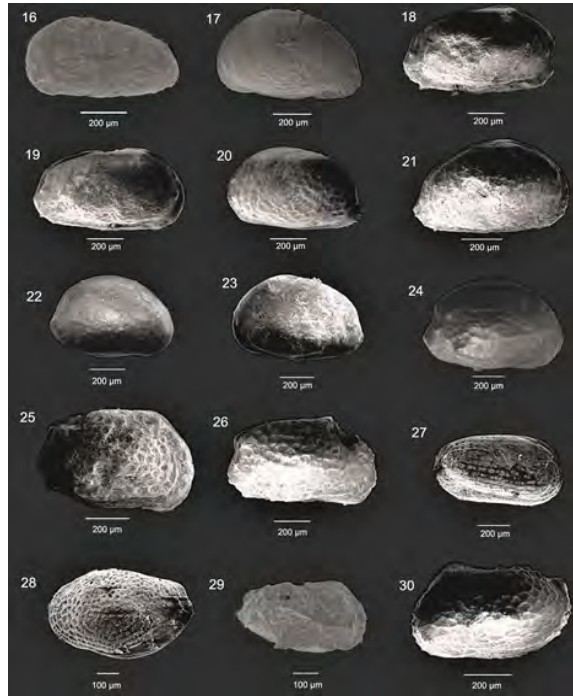
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Plate I



- Figure 1. *Bythocypris lucida* (Sequenza)
1. Left cover, side view, Dağpazarı 1 Measured Stratigraphy Section, Sample 21
- Figure 2. *Cytherella glypta* Doruk
2. Shell, left exterior view, Dağpazarı 2 Measured Stratigraphy Section, Sample 3
- Figure 3. *Cytheridea acuminata neapolitana* Kollmann
3. Left cover, side view, Dağpazarı 1 Measured Stratigraphy Section, Sample 7
- Figure 4. *Cytheridea acuminata acuminata* Bosquet
4. Right cover, side view, Dağpazarı 1 Measured Stratigraphy Section, Sample 26
- Figure 5-6. *Cyamocytheridea reversa* (Egger)
5. Carapace, right external view, Dağpazarı 1 Measured Stratigraphy Section, Sample 22
6. Shell, right external view, Dağpazarı 1 Measured Stratigraphy Section, Sample 13
- Figure 7-8. *Cyamocytheridea meniscus* Doruk
7. Shell, left exterior view, Dağpazarı 1 Measured Stratigraphy Section, Sample 26
8. Carapace, right side view, Dağpazarı 1 Measured Stratigraphy Section, Sample 17
- Figure 9-10. *Pontocythere elongata* (Brady)
9. Shell, right external view, Dağpazarı 1 Measured Stratigraphy Section, Sample 21
10. Carapace, right side view, Dağpazarı 1 Measured Stratigraphy Section, Sample No. 21
- Figure 11-12. *Krithe citae* Oertli
11. Shell, right external view, Dağpazarı 1 Measured Stratigraphy Section, Sample 23
12. Right cover, side view, Dağpazarı 1 Measured Stratigraphy Section, Sample 13
- Figure 13. *Krithe monostercensis* (Sequenza)
13. Shell, right external view, Dağpazarı 1 Measured Stratigraphy Section, Sample 26
- Figure 14. *Cistacythereis pokornyi* (Ruggieri)
14. Shell, left exterior view, Dağpazarı 1 Measured Stratigraphy Section, Sample 31
- Figure 15. *Ruggieria tetraptera tetraptera* (Sequenza)
15. Shell, left exterior view, Dağpazarı 2 Measured Stratigraphy Section, Sample 10

Plate II



- Figure 16. *Thalmannia clauda* (Doruk)
16. Shell, left exterior view, Dağpazarı 1 Measured Stratigraphy Section, Sample 32
- Figure 17. *Aurila convexa* (Baird)
17. Shell, left exterior view, Dağpazarı 2 Measured Stratigraphy Section, Sample 10
- Figure 18-19. *Aurila freudenthali* Sissingh
18. Shell, right external view, Dağpazarı 1 Measured Stratigraphy Section, Sample 26
19. Shell, right external view, Dağpazarı 1 Measured Stratigraphy Section, Sample 26
- Figure 20-21. *Aurila ulicznyi* Sissingh
20. Shell, left exterior view, Dağpazarı 1 Measured Stratigraphy Section, Sample 28
21. Shell, right external view, Dağpazarı 1 Measured Stratigraphy Section, Sample 17
- Figure 22. *Aurila speyeri* (Brady)
22. Shell, right external view, Dağpazarı 2 Measured Stratigraphy Section, Sample 9
- Figure 23. *Aurila soummamensis* Coutelle and Yassini
23. Shell, left exterior view, Dağpazarı 1 Measured Stratigraphy Section, Sample 28
- Figure 24. *Pokorniyella deformis minor* Moyes
24. Shell, right external view, Dağpazarı 2 Measured Stratigraphy Section, Sample 11
- Figure 25. *Tenedocythere prava* (Baird)
25. Shell, right external view, Dağpazarı 1 Measured Stratigraphy Section, Sample 22
- Figure 26. *Tenedocythere salebrosa* Uliczny,
26. Shell, right external view, Dağpazarı 1 Measured Stratigraphy Section, Sample 28
- Figure 27. *Cytheretta semiornata* (Egger)
27. Shell, right external view, Dağpazarı 1 Measured Stratigraphy Section, Sample 34
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Bending of a Cross-Ply Laminated Composite Beam Under a Sinusoidal Transverse Loading

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ABSTRACT

Bending of a laminated composite beam under to a sinusoidal loading is carried out for simply support boundary condition for a specific cross-ply stacking sequence. To demonstrate the accuracy of the analytical results, a computer-aided engineering (CAE) approach is used. In the analytical solution, a unified shear deformation theory with a parabolic shape function is used. The longitudinal and vertical displacements, normal and shear stresses, namely, the bending stresses of analytical and CAE solutions are obtained and compared with the literature. Although two different methods are used in the study, the analysis results converge to the reference values. The variation of the displacements, normal and shear stresses are illustrated in the graphics with respect to the beam length and thickness respectively.

Keywords:

Bending; Static analysis; Laminated composite beam; Shear deformation beam theory; Computer-aided engineering

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INTRODUCTION

Since the composite materials can be designed in different ways with the desired mechanical properties for various stacking sequences, matrix and fiber materials, they have been widely used in many structural elements. These elements are generally constructed of laminated composite materials, and too many design parameters are taken into consideration in the design and analysis process. Sankar (2001) obtained an elasticity solution for laminated beams under sinusoidal loading. The stresses and displacements were obtained by use of a non-dimensionalized design parameter that varies exponentially for constant mechanical properties [1]. Sayyad et al (2014) performed a static flexural analysis of a simply supported single-layer composite beam under various loadings and obtained the results by a precise elasticity solution [2]. Sayyad et al (2015) investigated the bending of composite beams by use of a trigonometric beam theory due to transverse shear deformation, and compared the results with those of the other trigonometric theories [3]. Pimenta et al (2015) investigated the sinusoidal-web beams under the effects of lateral and torsional buckling. In this manner, firstly, an experimental investigation was performed, and then a finite-element model was created and tested using the data from the experiments. In the prediction of the beam resistance, a theoretical model was proposed, and a computational program was established. Finally, using the first order reliability

approach, reliability analyses were performed, and the results were compared with the literature [4]. Pagani et al (2017) developed the static analyses of sandwich, and laminated beams under a transverse sinusoidal loading by applying the Lagrange expansion-based refined beam model for a simple supported boundary condition. The 3-D FEM (Finite Element Method) results were computed and compared with the previous studies [5]. Jiaoa et al (2017) investigated the effect of geometry of composite I-beams for the buckling capacity theoretically, and in order to validate the theoretical approach, number of experiments and simulations were carried out [6]. Liu et al (2018) searched the non-linear bending behavior of anisotropic composite beams for different distributed loadings and compared the results with FEM solution [7]. Dorduncu (2019) investigated the bending stresses of composite beams by use of a refined zigzag theory. The method's capabilities and robustness were presented for various sets of aspect ratios and boundary conditions [8]. Karakoti and Kar (2019) examined the sinusoidally-corrugated laminated composite panels by use of a customized computational code to obtain the bending responses of panels for various boundary conditions. The model's accuracy was confirmed with the comparison and validation of the analytical results [9]. Pandey and Gadade (2019) used FEM in the static analysis of a composite beam. As a present model, the nine-noded, 12-degree-of-

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freedom isoparametric Lagrange interpolation function was developed. To compare the FEM results with the literature, the maximum non-dimensional deflection values for symmetric and unsymmetric laminates under concentrated loads were calculated for various boundary conditions [10]. By taking into account four different carbon nanotube distributions, Sobhy (2019) introduced a novel analytical method for the bending of functionally graded plates reinforced with single-walled carbon nanotube in different temperature conditions. For simply supported boundary condition, the present plate was subjected to various distributed loadings, and non-dimensionalized stress and displacement values were obtained [11]. In the bending and vibrational analysis of reinforced beams, Wang et al. (2019) suggested a 2-D (Two-Dimensional) elasticity model for a sinusoidal distributed load and various boundary conditions, non-dimensionalized displacement, stress, and natural frequency parameters were derived [12]. Pathirana and Qiao (2019) investigated the critical buckling load of sinusoidal panels under simply support boundary condition by use of Rayleigh-Ritz method. To predict the critical load, a semi-analytical solution was used, and due to the finite element analysis, the results were obtained with better correlation. Considering the twisting capacities and different material properties, the study was conducted to assess the effects of the buckling amplitude, thickness, and aspect ratio [13]. Pathirana and Qiao (2020) studied the buckling behaviour sinusoidal panels under in-plane loading by Rayleigh-Ritz approach. The local buckling load is predicted accurately by a precise solution method. The local buckling behavior were captured at any aspect ratios, thickness, and amplitudes [14]. Zaboony and Jassim (2022) used the classical lamination theory to obtain the analytical solutions for laminated composite beams. In the analytical bending solution, several boundary conditions and loadings were taken into consideration. The boundary conditions were chosen as simple-simple, clamped-free and clamped-clamped, and the loading types were chosen at the center point with uniform distributed load [15]. Zhu et al (2022) investigated the properties of engineered cementitious composites due to the ductility, strength, fatigue and cracking behavior. To examine the impacts of various fiber contents, three different types of hybrid designed cementitious composites with various volume fractions of steel and polyethylene fiber were evaluated [16].

In the present work, the bending analysis of a cross-ply laminated composite beam under a uniform sinusoidal transverse loading for simple support boundary condition is performed both analytically and by use of a CAE software. For the comparison purposes, initially, the longitudinal and vertical displacements, normal and shear stresses are

obtained analytically for a specific material, at different points where the maximum displacements and stresses may occur. The computer aided engineering approach is developed for given parameters, and the results are compared with the ones obtained by use of finite element method and analytically by use of a shear deformation beam theory in the literature [20-21].

ANALYTICAL MODEL

The beam is assumed to have a rectangular cross-section and constructed of linear elastic layers. It has a length of “L”, total thickness of “h”, unit width, and the coordinate axes are located at the mid-plane where $0 \leq x \leq L$ and $-h/2 \leq z \leq h/2$, respectively. A laminated composite beam under a uniform sinusoidal transverse loading is presented in Fig.1.

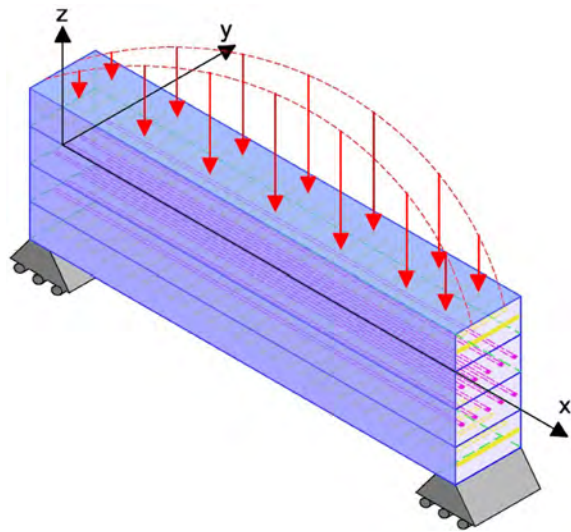


Figure 1. A laminated composite beam under a uniform sinusoidal transverse loading

In the analytical solution, a unified shear deformation beam theory is used which is firstly applied to the composite shells developed by Soldatos and Timarcı (1993). The shear deformation effects are taken into consideration by use of a general shape function “ $\phi(z)$ ” depending on the beam thickness. In addition, with the appropriate selection of the shape functions, the previous beam theories can also be obtained. The displacement fields for the unified shear deformation beam theory are given as follows:

$$\begin{aligned}
 U(x, y, z; t) &= u(x, y; t) - z w(x; t)_{,x} + \phi(z) u_1(x; t) \\
 V(x, y, z; t) &= v(x, y; t) - z w(x; t)_{,y} + \phi(z) v_1(x; t) \\
 W(x, y, z; t) &= w(x, y; t)
 \end{aligned}
 \tag{1}$$

Since the displacement component along y-axis is zero for the beam, the following displacement fields “U” and “W” are obtained as follows, where “u”, “w” and “u₁” are the displacement functions of the mid-plane.

$$U(x, z; t) = u(x; t) - z w(x; t)_{,x} + \mathcal{O}(z) u_{I,x}(x; t) \quad (2)$$

$$W(x, y, z; t) = w(x, y; t)$$

In order to satisfy the stress-free conditions at the top and bottom surfaces and continuity of interlaminar stresses through the thickness of the beam, a parabolic shape function is chosen in the study as follows [17]:

$$\mathcal{O}(z) = z \left(1 - \frac{4z^2}{3h^2} \right) \quad (3)$$

The displacement fields given in Eq. 2 yield to the kinematic relations where the subscript “,” corresponds to the differentiation with the relevant axis.

$$\varepsilon_x = u_{,x} - z w_{,xx} + \mathcal{O}(z) u_{I,x} \quad (4)$$

$$\gamma_{xz} = \mathcal{O}'(z) u_I$$

Using the generalized Hooke's law, the stress-strain relations in each layer of the beam can be expressed as follows:

$$\begin{bmatrix} \sigma_x \\ \tau_{xz} \end{bmatrix} = \begin{bmatrix} \bar{Q}_{11} & 0 \\ 0 & \bar{Q}_{55} \end{bmatrix} \begin{bmatrix} \varepsilon_x \\ \gamma_{xz} \end{bmatrix} \quad (5)$$

The transformed reduced stiffness “ \bar{Q}_{ij} ” depend on the reduced stiffness “ Q_{ij} ” and fiber orientation angles “ θ ” of the relevant layers (Jones, 1975). The rigidities with two subscripts, and more than two subscripts correspond to the classical and shear deformation beam theories, respectively [18].

$$\bar{Q}_{11} = Q_{11} \cos^4 \theta + 2(Q_{12} + 2Q_{06}) \sin^2 \theta \cos^2 \theta + Q_{22} \sin^4 \theta \quad (6)$$

$$\bar{Q}_{55} = Q_{44} \sin^4 \theta + Q_{55} \cos^4 \theta$$

The reduced stiffness parameters depend on the mechanical properties such as elasticity modulus “E”, shear modulus “G” and Poisson's ratio “ ν ”, and are given as follows:

$$Q_{11} = \frac{E_1}{1 - \nu_{12}\nu_{21}}, \quad Q_{12} = Q_{21} = \frac{E_2\nu_{21}}{1 - \nu_{12}\nu_{21}}, \quad Q_{22} = \frac{E_2}{1 - \nu_{12}\nu_{21}} \quad (7)$$

$$Q_{44} = G_{23}, \quad Q_{55} = G_{13}, \quad Q_{66} = G_{12}$$

$$\frac{E_1}{E_2} = \frac{\nu_{12}}{\nu_{21}} \quad (8)$$

By the appropriate use of stress-strain relations in the force and moment equations,

$$N_x = \int_{-h/2}^{h/2} \sigma_x dz, \quad Q_x^a = \int_{-h/2}^{h/2} \tau_{xz} \Phi^a(z) dz \quad (9)$$

$$M_x = \int_{-h/2}^{h/2} \sigma_x z dz, \quad M_x^a = \int_{-h/2}^{h/2} \sigma_x \Phi^a(z) dz$$

the following constitutive equations are obtained. “a” corresponds to the shear deformation effects, “A”, “B”, “D” denote the extensional, coupling and bending rigidities respectively, and “ Q_x^a ” “ Q_x ” is the shear force. Rigidities

with two subscripts correspond to the classical theory, whereas the ones with more than two subscripts correspond to shear deformation theory.

$$\begin{bmatrix} N_x \\ M_x \\ M_x^a \end{bmatrix} = \begin{bmatrix} A_{11} & B_{11} & B_{111} \\ B_{11} & D_{11} & D_{111} \\ B_{111} & D_{111} & D_{1111} \end{bmatrix} \begin{bmatrix} u_{,x} \\ -w_{,xx} \\ u_{I,x} \end{bmatrix}, \quad Q_x^a = A_{55} u_I \quad (10)$$

The extensional, coupling and bending rigidities are defined as follows:

$$A_{11} = \int_{-h/2}^{h/2} \bar{Q}_{11}^{(k)} dz, \quad A_{55} = \int_{-h/2}^{h/2} \bar{Q}_{55}^{(k)} (\mathcal{O}'(z))^2 dz$$

$$B_{11} = \int_{-h/2}^{h/2} \bar{Q}_{11}^{(k)} z dz, \quad B_{111} = \int_{-h/2}^{h/2} \bar{Q}_{55}^{(k)} \mathcal{O}(z) dz \quad (11)$$

$$D_{11} = \int_{-h/2}^{h/2} \bar{Q}_{11}^{(k)} z^2 dz, \quad D_{111} = \int_{-h/2}^{h/2} \bar{Q}_{11}^{(k)} \mathcal{O}(z) z dz,$$

$$D_{1111} = \int_{-h/2}^{h/2} \bar{Q}_{11}^{(k)} (\mathcal{O}(z))^2 dz$$

For a laminated beam under a uniform transverse loading of $q(x)$, the governing equations can be considered as follows:

$$N_{x,x} = 0$$

$$M_{x,xx} = q(x) \quad (12)$$

$$M_{x,x}^a - Q_x^a = 0$$

The beam is considered to be under a uniform sinusoidal loading where “m” is the wave number, and given as follows:

$$q(x) = q_0 \sin(\alpha x), \quad \alpha = \frac{m\pi}{L} \quad (m = 1, 2, \dots) \quad (13)$$

The boundary conditions prescribed at both ends where $x=0$ and $x=L$, are obtained by application of Hamilton's principle, and given for simply supported, cantilever and free boundary conditions respectively.

$$N_x = w = M_x = M_x^a = 0$$

$$u = w = w_{,x} = u_I = 0 \quad (14)$$

$$N_x = M_{x,x} = M_x = M_x^a = 0$$

In order to satisfy the simple support boundary condition, the following Navier-type displacement functions are used, whereas “ C_1 ”, “ C_2 ” and “ C_3 ” are the amplitudes of the displacement functions.

$$u = C_1 \sin\left(\frac{m\pi x}{L}\right), \quad u_I = C_2 \cos\left(\frac{m\pi x}{L}\right), \quad w = C_3 \sin\left(\frac{m\pi x}{L}\right) \quad (15)$$

Using the constitutive equations in governing equations, the set of three equations with three unknowns are obtained. The unknown parameters can be determined computationally when the boundary condition is applied at both ends.

FINITE ELEMENT MODEL

In recent years, it has been observed that the use of computer-aided design software is insufficient especially in determining the static and dynamic loads, and the thermal effects of the designs under specific operating conditions. Since the performance of the design will largely depend on the actual operating conditions, it is of great importance to predict these conditions correctly. Under the consideration of these parameters, it will be wise to use a different software solution in the analysis of engineering designs. In the design process, a CAE software is generally used to include the real operating conditions and to create a simulation and perform the analysis in a virtual environment. The CAE software is commonly used in many engineering fields such as automotive, aerodynamic, flow and structural analysis. Especially in the engineering applications, the optimum results can be obtained in a shorter time with the minimum cost. While the design process of a product or system is independent of time and operating conditions, the same parameters should also be taken into consideration in the analysis. The reliability of the results will largely depend on the correct use of the solution technique and the limit values. Thus, the theoretical information in the relevant study becomes significant in the determination of these values. Therefore, especially in cases where the theoretical information is incorrect or insufficient, CAE software may not give the correct or sufficient results. Number of different analyses such as static strength, fatigue, vibration, heat transfer and impact can be performed by use of the finite element method (FEM) based engineering software. As a result, the CAE software shortens the time required for the design process considerably and allows to analyze and predict the optimum results for the product or system before the manufacturing process. In this study, Abaqus is utilized for the CAE solution. Since the plane and shell elements are generally effective in modelling and analyzing the laminated composite structures and converge faster, 3-D brick elements are chosen for the solid modelling.

RESULTS AND DISCUSSION

The vertical and longitudinal displacements and the shear and normal stresses, namely, the bending stresses are presented in Table 1 at different points. The vertical and longitudinal displacement values are obtained at $x=L/2$, $z=0$ and $x=0$, $z=h/2$, respectively. The normal stresses are obtained at $x=L/2$, $z=h/4$, whereas the shear stresses are obtained at $x=L/4$, $z=0$ in accordance with Ref. [15].

The beam is simply supported, constructed of four layers, has the stacking sequence of $[90^\circ/0^\circ/0^\circ/90^\circ]$, length of $L=6.35$ m, thickness of $h=2.794$ m and a uniform sinusoidal distributed loading $q_0=1000$ N/m is applied at the top. The beam material is chosen as boron/epoxy with the following mechanical properties [19]:

$$\begin{aligned} E_{11} &= 241.5 \text{ GPa}, & E_{22} &= E_{33} = 18.89 \text{ GPa} \\ G_{23} &= 3.45 \text{ GPa}, & G_{12} &= G_{13} = 5.18 \text{ GPa} \\ \nu_{23} &= 0.25, & \nu_{12} &= \nu_{13} = 0.24 \end{aligned} \quad (16)$$

The results are compared with Karama et al (1998) that were obtained by Abaqus software [20]. The vertical and longitudinal displacements and bending stresses were also obtained by use of a sinusoidal and exponential shape functions in Karama et al (1998, 2003), and a parabolic shape function in Karacam (2005) [21], respectively. In the present study, the numerical results have shown that the proposed model has better results than the others. In the determination of the displacement and stress values, a unified shear deformation beam theory in which the previous beam theories can be obtained by use of an appropriate shape function, is adopted in the numerical model. In the comparison of results, the following equation is used to obtain the error in percentage.

$$Error(\%) = \frac{(Reference\ Value - New\ Value)}{Reference\ Value} \times 100 \quad (17)$$

Table 1. The vertical (W) and longitudinal (U) displacements, shear (τ_{xz}) and normal (σ_{xx}) stresses for simple support boundary condition.

Model	W ($\times 10^{-4}$) [m]	U ($\times 10^{-4}$) [m]	τ_{xz} [Pa]	σ_{xx} [Pa]
Present Study	-6.2155	2.3554	-1031670	7685460
Error (%)	1.88	1.85	2.55	1.91
Karacam (2005)	-6.2317	2.0382	-892316	7527000
Error (%)	2.2	11.8	11.3	3.9
Karama (2003)	-6.3701	2.1196	-940098	8112840
Error (%)	4.4	8.3	6.6	3.5
Karama (1998)	-6.1006	2.3125	-1006000	7835200

In Fig. 2, the variation of vertical displacement is presented along the beam length. In accordance with the simply support boundary condition, the displacement values at the beginning and end of the beam where $x=0$ and $x=L$, are obtained as zero. The maximum displacement value is obtained in the middle of the beam as it is expected. Due to the sinusoidal transverse loading, the negative values in the vertical axis indicate that the displacement values are obtained in the negative z- direction.

In Fig. 3, the vertical displacement distribution is presented. It is obvious from the figure that both sides of the beam which are illustrated in red regions have zero displacement, whereas the regions in dark blue correspond to the maximum displacement values.

In Fig. 4, the variation of longitudinal displacement along the beam thickness is presented. Since the sinusoidal loading acts from the top, the upper surface of the beam is

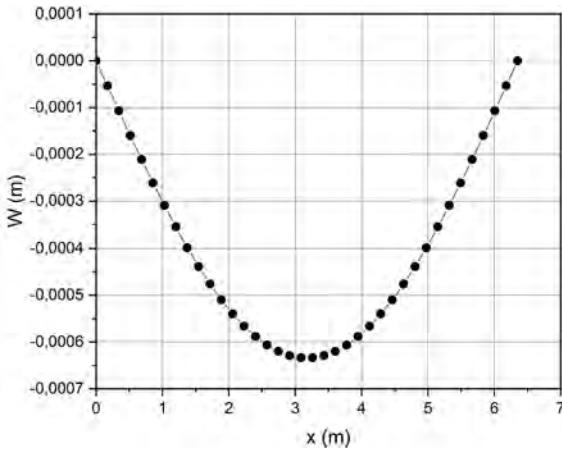


Figure 2. The variation of vertical displacement along the beam length.

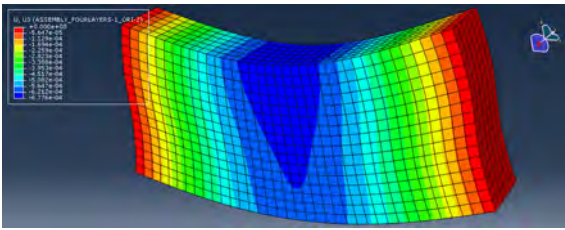


Figure 3. The vertical displacement distribution.

lengthened, whereas the lower surface is shorten. Thus, the maximum values are obtained at the bottom and top surfaces where $z=h/2$ and $z=-h/2$. The longitudinal displacement values presented along x-axis in the figure have a common factor of “ 10^{-4} ”. Since the longitudinal displacement at the mid-plane of the beam when $z=0$ is “ 0.06×10^{-4} ”, it is obvious from the figure that the displacement at this value is very close to zero.

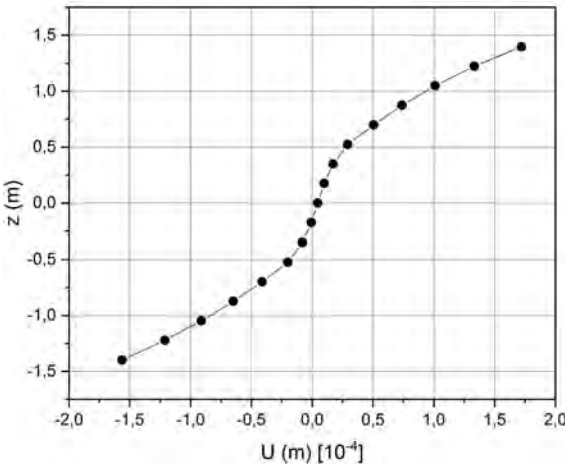


Figure 4. The variation of longitudinal displacement along the beam thickness.

The longitudinal displacement distribution along the beam thickness is presented in Fig. 5. The red and dark blue regions indicate the positive and negative maximum displacement values at the bottom and top surfaces along x-axis.

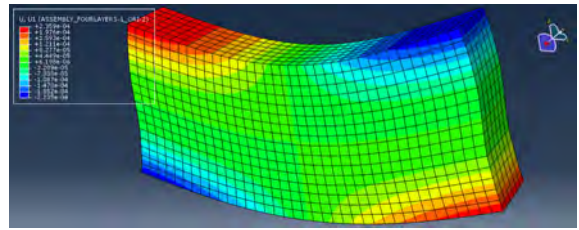


Figure 5. The longitudinal displacement distribution.

In the mid-plane, the longitudinal displacement values are close to zero as in the previous figure.

In Fig. 6, the variation of normal stress along the beam length is presented. The maximum value is obtained in the mid-point, and stress values are obtained as zero at both ends of the beam respectively.

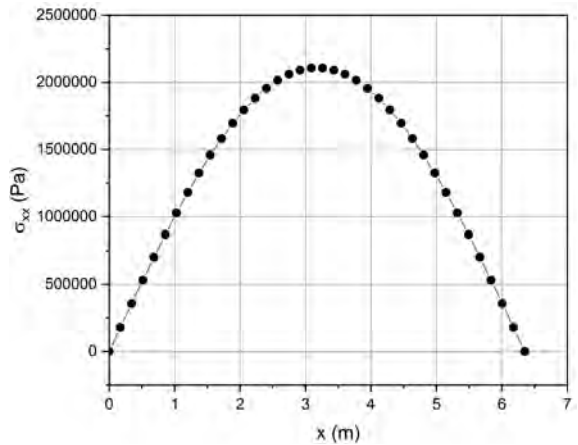


Figure 6. The variation of normal stress along the beam length.

In Fig. 7, the normal stress distribution along the beam length is presented. For the specific point where $x=L/2$ and $z=h/4$, the stress values are close to the analytical solution. The positive and negative stress values correspond to the tensile and compressive stresses.

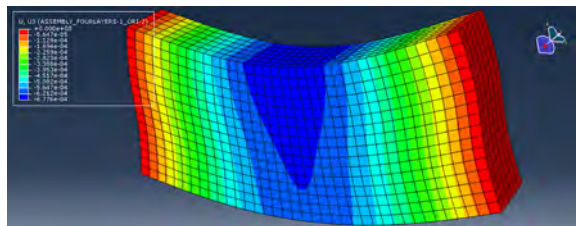


Figure 7. The normal stress distribution.

In Fig. 8, the variation of shear stress along the beam thickness is presented. At the bottom and top surfaces, the shear stresses are obtained as zero in accordance with the shear deformation beam theory, and the maximum stress value is obtained in the mid-plane.

In Fig. 9, the shear stress distribution along the beam thickness is presented. The stress values are close to the refe-

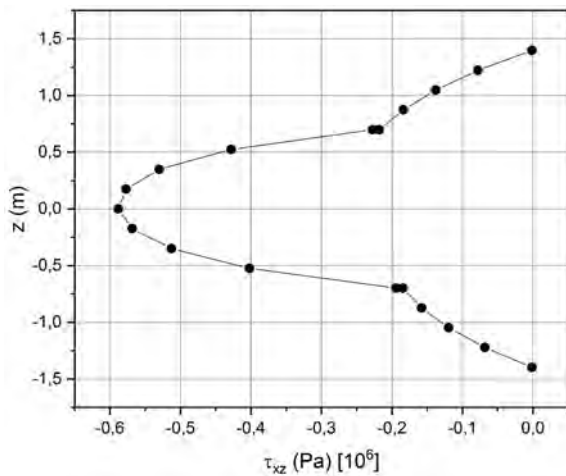


Figure 8. The variation of the shear stress along the beam thickness.

rence values where $x=L/4$, and $z=0$. The colored regions are similar with the curve obtained by the analytical solution in the previous figure.

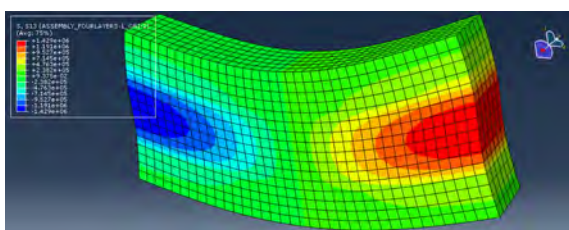


Figure 9. The shear stress distribution.

CONCLUSION

In this study, the bending analysis of a composite beam under a uniform sinusoidal load is performed. By use of the proposed model, the results are compared with the analytical and CAE solutions of the previous studies. When the results are compared with the reference values, the percentage values of errors are obtained as 1.88% and 1.85% for vertical and longitudinal displacements, 2.55% and 1.91% for the shear and normal stresses, respectively. Thus, it is concluded from the results that there is a significant decrease in percentage error values from 11.8% and 11.3% for the longitudinal displacement and shear stress values, whereas there is a minor change from 2.2% and 3.9% for the vertical displacement and normal stress values when compared with the analytical solution of Karacam, 2005. In the future works, the dynamic analysis can be performed in order to obtain the natural frequencies and buckling loads. Additionally, the static and dynamic analyses can be expanded by taking various design parameters into consideration such as loading type, stacking sequence, layer thickness and boundary conditions.

CONFLICT OF INTEREST

The author deny any conflict of interest.

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Nucleobase-Modified Microgels Synthesized via Microfabrication Technology for DNA Adsorption

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ABSTRACT

DNA isolation is a crucial procedure since DNA-based assays have great importance in molecular biology, biochemistry and biomedical applications. The objective of this study is to fabricate micron-sized hydrogels as adsorbents for DNA. Poly(2-hydroxyethyl methacrylate-co-glycidyl methacrylate) microgels were synthesized by free radical polymerization in the presence of N,N'-methylenebisacrylamide as a crosslinker, in the microholes of a microstencil array chip. Then, adenine was immobilized to microgels through the epoxy groups of glycidyl methacrylate. Scanning electron microscopy and Fourier transform infrared spectroscopy were employed to investigate the chemical and morphological characterizations of the microgels. The findings of the experiments demonstrate that the microgels had a cylindrical shape, were of uniform size, and had a height and diameter of around 500 μm . Observation of aromatic C=C peak confirmed the existence of adenine ligand in the microgel structure. Adsorption studies were carried out to determine the optimal conditions for DNA adsorption of nucleobase-immobilized microgels. After initially increasing, the quantity of DNA adsorbed onto the microgels reached a saturation level at a DNA concentration of around 2.0 mg/mL. The maximum adsorption was 38.54 mg/g microgels for an initial DNA concentration of 2.0 mg/mL in the optimum medium pH and temperature. DNA adsorption capabilities are shown to not significantly decline in recurrent adsorption-desorption cycles. As a result of the findings, adenine-immobilized microgels were demonstrated to be a viable option for DNA adsorption. Additionally, as a reference for future research, this study highlights the benefits of microfabrication technology, such as its simplicity of use in fabricating adsorption materials with the desired size, shape, and uniformity.

Keywords:

Adsorption; DNA; Hydrogels; Microfabrication; Microgels; Nucleobase

INTRODUCTION

DNA isolation/extraction from biological samples is a fundamental and significant process in biochemistry, molecular biology, forensics, clinical analysis, and DNA-based biomedical applications [1–3]. DNA isolation has great potential usage in gene therapy, the treatment of autoimmune diseases, DNA vaccination, pathogen detection, biosensor applications and so on [2,4–6]. The importance of DNA and DNA isolation has made it crucial to develop DNA isolation procedures and techniques. The need for innovative methods is demonstrated by the fact that conventional ones need time-consuming steps like centrifugation and precipitation as well as the usage of harmful chemicals for both the environment and human health [7].

Hydrogels are polymeric structures with a high-water retention capacity in their 3D matrices. They are insoluble in water due to their physically or/and chemically cross-linked structure, but instead, exhibit high swelling capacity [8,9]. Because of their promising properties, hydrogels have been used in various applications in biochemistry, biotechnology, and biomedical engineering. For example, they can be used in tissue engineering owing to their tissue-like swelling properties and biocompatibility, in drug delivery systems because of their ability to load the desired amount of drug and injectable formulation, and in affinity chromatography for the separation of biomolecules like proteins due to allowing modifications such as ligand immobilization of the polymer matrix [10–12].

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Microfabrication processes have been widely employed in electronics and bioelectronics in order to fabricate micro-electro-mechanical systems (MEMS) including sensors, cantilevers, microreservoirs, micropumps, rotors, channels, valves, and so on [13]. Besides electronics, micro- and nano-fabrication methods are potentially powerful tools to improve devices in biotechnology and biochemical processing, such as miniaturized chromatography systems, lab-on-a-chip devices, and microreactors [14,15]. Microengineered hydrogels, one of the significant products of microfabrication, have great potential in tissue engineering and drug delivery systems due to their abilities of mimicking the physical, mechanical, and biological features of natural tissues and organs [16–18].

Recently, Wu et al. studied the effect of metal ions such as Na^+ , Mg^{2+} , Ca^{2+} , Mn^{2+} and Zn^{2+} on the adsorption of both single-stranded DNA (ssDNA) and double-stranded DNA (dsDNA) onto microplastics and they reported that the transition metals, i.e., Mn^{2+} and Zn^{2+} , showed a higher adsorption capacity than Mg^{2+} for both dsDNA and ssDNA [19]. For DNA extraction and amplification, Wang et al. immobilized Ti^{4+} on magnetic composite microspheres and reported the extraction ability as $84 \pm 4 \mu\text{g}/\text{mg}$ [20]. By polymerizing HEMA with N-methacryloyl-L-tryptophan which is a hydrophobic ligand, Çorman et al. synthesized two different types of hydrophobic cryogels: the first is poly(2-hydroxyethyl methacrylate-N-methacryloyl-L-tryptophan) [P(HEMA-MATrp)] cryogel, and the second is P(HEMA-MATrp) particles embedded PHEMA cryogel [21]. Maximum adsorption of DNA on p(HEMA-MATrp) cryogel and p(HEMA-MATrp) embedded PHEMA composite cryogel were found to be 15 mg/g and 38 mg/g polymer, respectively. The results showed that embedding hydrophobic micro-particles showed higher adsorption capacity compared to hydrophobic cryogels [21]. Zandieh et al. studied on adsorption of DNA oligonucleotides onto microplastics in the absence and presence of metal ions and reported that polyethylene terephthalate and polystyrene showed the highest DNA adsorption efficiency [22]. Wang et al. prepared self-assembled zinc meso-tetra(4-pyridyl)porphyrin for DNA adsorption and adsorption of single-stranded DNA showed higher efficiency compared to duplex DNA [23]. In another study, Meng et al. developed a biosensor based on adsorption of DNA on polydopamine nanoparticles via different metal ions including Na^+ , K^+ , Mg^{2+} and Ca^{2+} coordination and detection limit in various biological samples including serum was provided as $<1 \text{ nM}$ target DNA [24]. Muñoz et al. investigated the effect of homonuclear boron bonds on the adsorption of DNA nucleobases using quantum-mechanics calculations and concluded that the adsorption is improved by homonuclear bonds in the boron nitride nanosheets [25].

In this study, microfabrication technology was used to

synthesize micro-engineered hydrogels, i.e., microgels with a height and diameter of around 500 μm . Microgels were produced in the microholes of a microstencil array chip (MAC) by free-radical polymerization of 2-hydroxyethyl methacrylate (HEMA) and glycidyl methacrylate (GMA) while N, N'-methylenebisacrylamide (MBA) was employed as a crosslinker. Investigating the effects of medium pH, initial DNA concentration, adsorption time, and ambient temperature on the adsorption capacity of microgels allowed for the identification of the optimal DNA adsorption conditions.

MATERIAL AND METHODS

Materials

HEMA, DNA (D3159, from herring sperm), GMA, ammonium persulfate (APS), MBA, and N,N,N',N'-tetramethyl ethylene diamine were purchased from Sigma Chemical Co. (St. Louis, MO, USA). Direct-Q 3 UV; Merck Millipore, Burlington, MA, USA system provided deionized water (DI Water) throughout the duration of the experimental research.

Fabrication of Microgels

Microgels prepared with the aid of a MAC are described as follows: Firstly, MBA (0.1% w/v) was dissolved in deionized (DI) water. HEMA:GMA ratio was adapted from an earlier study [26]. After adding HEMA (2.25 mL) and GMA (0.50 mL) to the MBA solution, it was magnetically stirred for 15 min. After APS (28.96 mg) was dissolved in the mixture, TEMED (11.4 μL) was added. Following the addition of ethanol (4 mL), the solutions were stirred once more and nitrogen bubbled for 5 min. The mixture was carefully put on a MAC. After 3 hours of polymerization at 60 °C, it was terminated at 4 °C, and microgels were collected.

Immobilization of Adenine onto Microgels

0.1 M of adenine solution was prepared in DI water : dioxane (1:1 v/v) and microgels were added into this mixture then the immobilization reaction was performed at 80 °C by shaking for 24 h [27].

Characterization Studies

Prior to the Attenuated Total Reflection–Fourier Transform Infrared (ATR–FTIR) analysis, microgels were firstly freeze-dried at -110°C for 24 h in a freeze-drying unit (Labogene Coolsafe Touch, Denmark). Using a Thermo Scientific Nicolet iS20 FTIR-ATR spectrophotometer (USA), FTIR spectra of the microgels were obtained in the wavelength range from 4000 to 500 cm^{-1} through 32 repeated scans at a 4 cm^{-1} resolution. Before the sample test, background measurements were made, which were automatically subtracted from the sample re-

sults. The overall shape and dimensions of the freeze-dried microgels were examined using an optical microscope (Olympus SZ6, Japan). To discuss the morphology of the microgels, a ZEISS GeminiSEM 500 field emission scanning electron microscope (FE-SEM) (Germany) was used.

Adsorption Studies

DNA adsorption capability of microgels was investigated in a batch experiment setup. The following conditions were studied to determine the optimal conditions for DNA adsorption of the microgels. The effects of medium pH (4-9) and temperature (4-45 °C), as well as the effects of initial DNA concentration (0.25-4.0 mg/mL) and adsorption time (2.5-60 min) on DNA adsorption capacity of microgels were investigated. DNA concentrations were determined at 260 nm using a UV-visible spectrophotometer and the amount of adsorbed DNA was evaluated via the Equation 1:

$$Q = \frac{(c_0 - c_f)v}{w} \quad (1)$$

where Q (mg/g dry microgel) is the adsorption capacity. The initial and final concentrations of DNA (in mg/mL) are shown by the symbols C_0 and C_f before and after the adsorption process, respectively. W is the dried microgel mass in g, and V is the volume of the DNA solution in mL.

RESULTS AND DISCUSSION

General shape and size of the microgels were evaluated via optical microscopy. As shown in Fig.1, microgels exhibit cylindrical shapes with the highest size of around 400–500 μm. Surface morphology of the microgels were revealed using FE-SEM as shown in Fig. 2. Microgels exhibit, in general, homogenous porous microstructure.

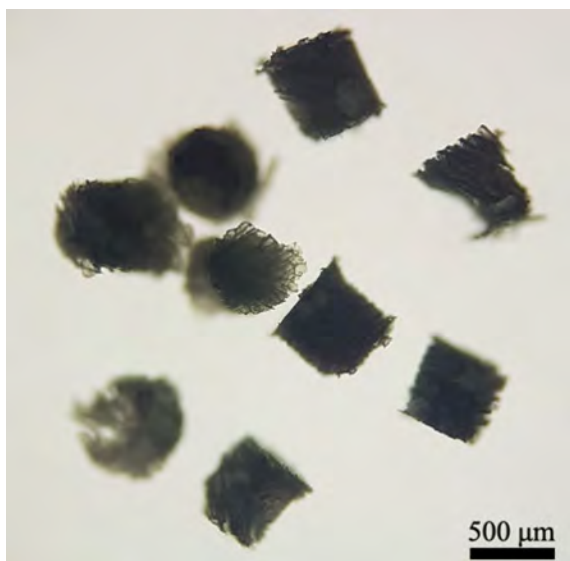


Figure 1. Optical microscopy images of the microgels

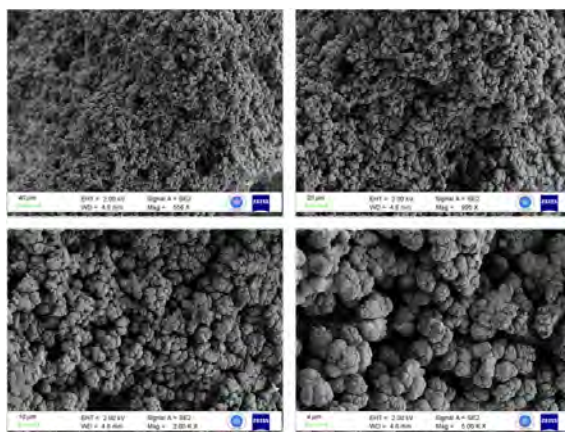


Figure 2. FE-SEM images of the microgels

We employed the Fourier transform infrared (FT-IR) spectroscopy approach to analyze the chemical composition of both plain and immobilized microgels (Fig. 3). The common bands were given at about 3400 cm^{-1} , 1710 cm^{-1} , and 2968 and 2946 cm^{-1} , respectively, for the -OH, C-H (aliphatic) and C=O bonds [26]. The C=C peaks at 1637 cm^{-1} have relatively low intensities, which supports polymerization.

The almost absence of C=C peaks around 1630 cm^{-1} confirms the polymerization [28]. Besides these, aromatic C=C peak indicates the existence of adenine ligand.

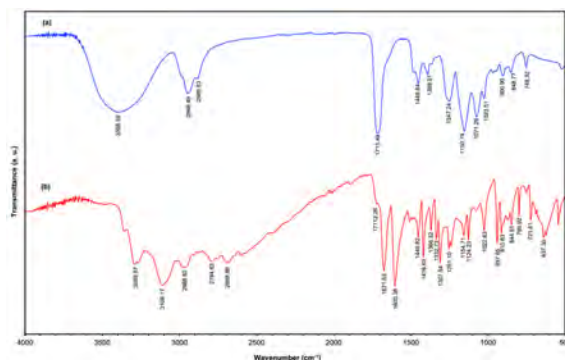


Figure 3. FT-IR spectra of the (a) P(HEMA-GMA) and (b) P(HEMA-GMA)-Adenine microgels

Fig. 4 depicts how medium pH affects the adsorption of DNA by the microgels. At pH 7.0, the adsorption capacity was at its maximum while declined at more alkaline and more acidic pH regions. Decrements in adsorption capacities were observed for pH 4.0 and pH 9.0 by about 18% and 23%, respectively, compared to the one in pH 7.0. This indicates that the interaction between adenine and thymine was weakened in acidic and basic environments by the presence of hydronium or hydroxy ions [29].

Fig. 5 presents the effect of adsorption time on the DNA adsorption by the microgels. Although the rate of DNA ad-

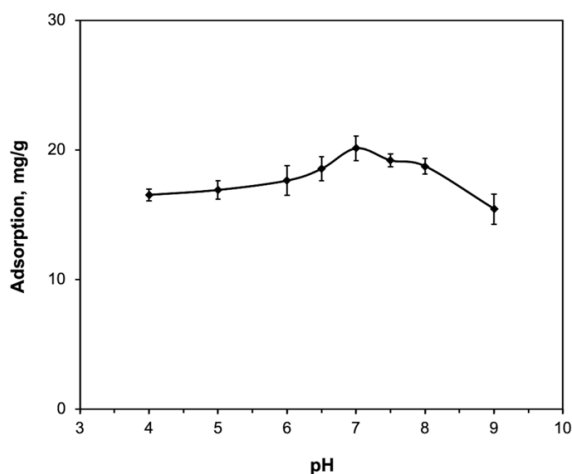


Figure 4. The adsorbed amount of DNA at various pH values (Temperature: 25 °C; initial DNA concentration: 0.5 mg/mL)

sorption was initially high, it started to decline after only 2.5 min, and equilibrium adsorption was attained upto 5 min. As a result, for the optimal adsorption capacity, ligand and analyte molecules need a short interaction time. It is clear that the interaction between DNA molecules and microgels had a high affinity since microgels might reach their maximum adsorption capacity in just 5 min. This is mostly due to the fact that microgels include adenine molecules as ligands, which is consistent with the literature [7]. Additionally, DNA molecules can quickly reach and interact with the active regions of the gel matrix because of the hydrophilic nature of hydrogels [30].

As it is seen in Fig. 6, there was an increment in the adsorption capacity as the initial concentration of DNA increased. At an initial DNA concentration of 0.5 mg/L, the adsorption capacity of microgels was 20.18 mg/g, whereas, at an initial DNA concentration of 1.0 mg/mL, it reached up to 38.54 mg/g. At a DNA concentration of around 2.0 mg/L, the adsorption process approached a plateau level, i.e., 38.54

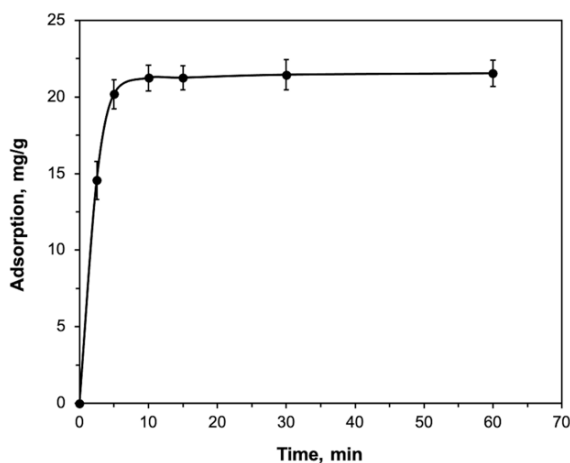


Figure 5. The adsorbed amount of DNA at various adsorption time (Running buffer: pH 7.0 phosphate; temperature: 25 °C; initial DNA concentration: 0.5 mg/mL)

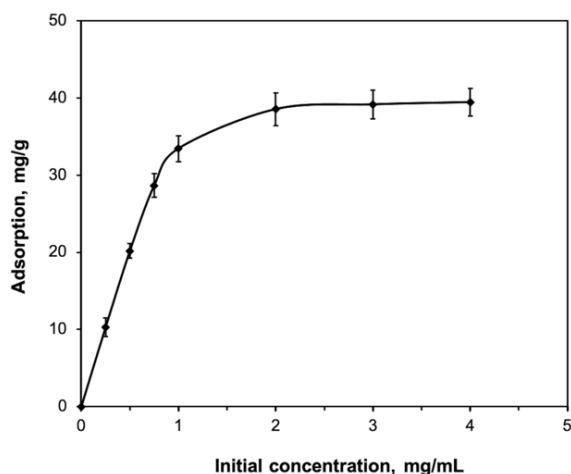


Figure 6. The adsorbed amount of DNA at various DNA concentrations (Running buffer: pH 7.0 phosphate; temperature: 25 °C)

mg/g. Even if the initial concentration value of DNA was exceeded, DNA adsorption has reached a dynamic equilibrium value because all active adenine ligands in the microgels were occupied with analyte molecules, i.e. DNA. Similar results have been observed in previous DNA adsorption studies [24,31,32].

As shown in Fig. 7, it can be observed that the adsorption capacity slightly increased as the temperature raised. One possible explanation is that as the temperature increased, the DNA double helix structure may partially expanded, facilitating easier interaction between the ligand and nucleotides [7].

A comparison of the adsorption capacity and duration of adsorption process of the microfabricated microgels with those of some other adsorbents reported in literature is listed in Table 1. Considering the fast kinetics of the DNA adsorption of the microgels, it is predicted that these newly designed microgels may be a good alternative in DNA adsorption.

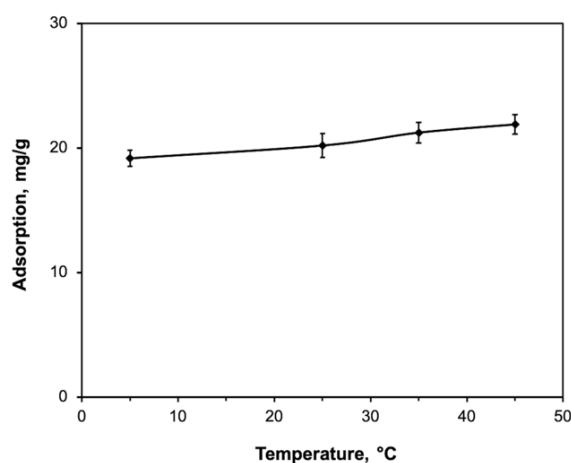


Figure 7. The adsorbed amount of DNA at various temperature values (Running buffer: pH 7.0 phosphate; initial DNA concentration: 0.5 mg/mL)

Table 1. Comparison of the DNA adsorption capacities of numerous adsorbents.

Adsorbent	Adsorption capacity	Adsorption time (min)	Ref.
Hemoglobin modified magnetic nanocomposites (NCs)	27.9 mg/g	15	[1]
Co(II) immobilized poly(GMA-EDMA) cryogels	33.81 mg/g	30	[5]
Aminosilane-modified magnetic nanoparticles (NPs)	4.7 mg/g	40	[33]
Ethylenediamine functionalized poly(glycidyl methacrylate) beads	90.4 µg/g	-	[34]
P(HEMA-(l)-histidine methyl ester)	13.5 mg/g	-	[35]
Silica-magnetite NCs	43.1 mg/g	8	[36]
Triethylamine modified poly(GMA-EDMA) monoliths	21.54 mg/mL	-	[37]
Cibacron Blue F3GA-attached poly(hydroxyethyl methacrylate)	32.5 mg/g	120	[38]
Zirconia magnetic NCs	53.5 mg/g	5	[39]
Magnetic polyaniline/maghemite NCs	75.2 mg/g	10	[40]
P(HEMA-MATrp) cryogels	3.53 mg/g	60	[21]
P(HEMA-MATrp) microbeads in PHEMA cryogels	8.35 mg/g	60	[21]
Composite cryogels of cyanobacterial extracellular polymeric substances and PHEMA	2.4 mg/g	-	[41]
Fe ²⁺ ions attached EPS-PHEMA composite cryogels	39.7 mg/g	-	[41]
Cu ²⁺ -attached magnetite NPs embedded PHEMA cryogels	19.97 mg/g	120	[42]
16mer peptide modified poly(EDMA-GMA)	65.1 µg/g	5	[43]
Indium Tin Oxide NPs	28.5 nM	120	[44]
Magnetic Mesoporous Silica NPs	121.6 mg/g	>20 h	[45]
Microfabricated nucleobase-modified microgels	38.54 mg/g	10	This study

While a material's capacity to be reused has economic benefits, it is also vital to reducing the usage of single-use plastics from polluting the environment [46]. For this objective, the adsorption capabilities of the synthesized microgels were evaluated for their not only single-use but also repeated-use effects on DNA adsorption capability. Figure 8 illustrates how the adsorption capacity of the same microgels decreased after each use in comparison to the prior capacity. During the adsorption-desorption cycle, a decrease in the adsorption capacity of the adsorbent may be observed for various reasons including loss in the active site for the analyte molecules due to tear and/or wear in the adsorbent, precipitation on the adsorbent surface, low desorption ef-

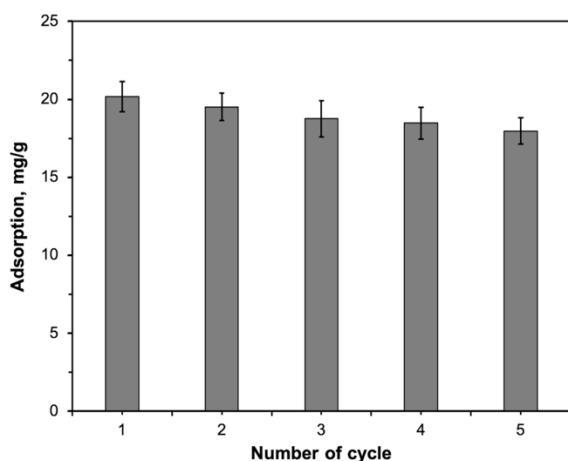


Figure 8. Reusability of the microgels (Running buffer: pH 7.0 phosphate; temperature: 25 °C; initial DNA concentration: 0.5 mg/mL)

iciency and so on [47,48]. After five uses, it was found that the reduction was only 10% of the initial adsorption capacity, resulting a good recycling ability compared with the earlier studies [35,38,49].

CONCLUSION

In the microholes of a microstencil array chip, poly(2-hydroxyethyl methacrylate-co-glycidyl methacrylate) microgels were created by free radical polymerization in the presence of N,N'-methylenebisacrylamide as a crosslinker. Then, adenine was immobilized to microgels using glycidyl methacrylate's epoxy groups. At a DNA concentration of around 2.0 mg/mL, the amount of DNA adsorbed onto the microgels reached a saturation level after initially growing. The amount of adsorbed DNA apparently depends on the initial DNA concentration. At the optimal temperature and pH of the medium, the maximum adsorption was 20.18 mg/g and 38.54 mg/g microgels at initial DNA concentrations of 0.5 and 2.0 mg/mL, respectively. It has been demonstrated that DNA adsorption capacity was not noticeably decreased throughout repeated adsorption-desorption cycles. This study showed that adsorption materials of desired size, shape, and uniform size can be easily produced using the microfabrication technique.

CONFLICT OF INTEREST

Authors approve that to the best of their knowledge, there is not any conflict of interest or common interest with an institution/organization or a person that may affect the review process of the paper.

AUTHOR CONTRIBUTION

Kemal Cetin Methodology, Investigation, Visualization, Writing - original draft.

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Mechanical and Tribological Properties of Carbon Fiber/Glass Fiber-Reinforced Epoxy Hybrid Composites Filled with Al₂O₃ Particles

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ABSTRACT

In this study, we produced Aluminum oxide (Al₂O₃) reinforced carbon fiber and glass fiber reinforced polymer (CFRP, GFRP) composites and investigated mechanical and tribological properties. Al₂O₃ was dispersed in epoxy resin using a mechanical stirrer. The composites are produced via the hand lay-up method and dried at room temperature for 48 hours. The properties of composites were determined via Archimedes' method, flexural, impact, hardness and wear tests. The highest flexural strength and hardness were found at 946.3 MPa and 48.7 HBA for 3 wt.% Al₂O₃ reinforced CFRP, respectively. The highest impact strength was observed at 187.4 kJ/m² for an un-reinforced GFRP composite. The lowest Coefficient of Friction (COF) and wear depth was found 3 wt.% Al₂O₃ reinforced GFRP composites.

Keywords:

Aluminium oxide; CFRP; Epoxy; GFRP; Hardness; Impact strength

INTRODUCTION

Polymers and their composites are used in many common and advanced engineering applications. They are becoming a good alternative to products made out of metal due to several attractive properties, including lightweight, high strength, ease of processing, low waste of material during manufacturing, and cost-effectiveness. As a result, major efforts have been made to use polymers in diverse industrial applications, using a variety of reinforcements, including fibers, to boost the physical and mechanical properties of the polymers. As a result, fiber-reinforced polymer matrix composites are extremely appealing due to their low friction coefficient, biodegradability, high strength, high stiffness, good corrosion resistance, and low weight. These materials are currently used in almost all aspects of daily life, from homes to aerospace applications(1-3).

Fiber-reinforced polymeric composites have become widely accepted for application in various sectors, including infrastructure, automotive, aerospace, and, most recently, oil and gas. Due to their high strengths and low densities, and ease of manufacture, polymers and their composites are being used more frequently. When compared to traditional metallic systems, these

materials are appealing due to two key properties. They can be customized to have stacking sequences that offer high strength and stiffness in directions of heavy loading, despite having a relatively low density. Composite materials are made of resin and reinforcement that is chosen for the application and the desired mechanical qualities (4-7).

The reinforcement of fiber-reinforced materials is chosen from carbon, glass, basalt, wood, paper or aramid, while the matrix is selected from various resins (epoxy, polyester, phenolic, vinyl ester, etc.) While the matrix encloses and protects the fibers, the fibers generally act as the primary load-bearing element. Matrices serve as load-transfer components between the fibers, shielding the structure from adverse environmental situations like high temperatures and humidity(8, 9).

Carbon fiber and glass fiber-reinforced polymer (CFRP/GFRP) composites have been frequently used in the aviation and space industry. As a result of their outstanding qualities, including their high strength, flexibility and stiffness, low weight, and excellent fatigue resistance. Glass fibers (GFs) work well under high tensile stress but aren't strong enough for compression

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because of their fragile character. Conversely, plastic materials can handle compression loading very well but cannot resist high tension. The GFRP created by combining these two materials creates a composite material that can withstand compressive and tensile loads. The use of GFRP composites in thermal, electrical and sound insulation, sporting equipment, boat and ship construction, aerospace applications, automotive, and sheet molding compounds is growing as a result of these features. Carbon fibers (CFs) are carbon-based fibers with typical properties such as high tensile strength and stiffness, low weight, high-temperature tolerance, low thermal expansion and great chemical resistance. CFRP composite materials are being used in a growing variety of aircraft components. In comparison to other types of fibers, CFs have a higher success rate and are light in nature(8-11).

High toughness and strength, adhesion, durability at low and high temperatures, low moisture absorption, thermal stability, high chemical, electrical and corrosion resistance, low shrinkage, good adherence to a variety of substrates, and simplicity of production are only a few of the advantages of epoxy. Epoxy is widely used in various products, including adhesives, construction, petrochemicals, automotive, aeronautics, semiconductor encapsulation, biocompatible implants, protective coatings, laminates and electric and electronic systems. Epoxy has excellent properties but a fragile structure, poor tribological performance, limited flame resistance, and low crack strength. The two main methods used to solve the problem are chemical treatment and the addition of second-phase particles (12-18).

Three main ways are often used to evolve the features of polymer matrix composites: the kind of polymer, the types of particles and fibers, and the interface between fibers. By incorporating fillers (such as Aluminum Oxide (Al_2O_3), Titanium Oxide (TiO_2), WC, SiC, and Graphite) into epoxy, the mechanical characteristics of epoxy are improved without changing the glass transition temperature. Al_2O_3 is widely used in the electronics, chemistry, chemical engineering, and aerospace industries due to its exceptional mechanical properties, chemical stability, excellent thermal properties, cost-effectiveness, good corrosion resistance, and enormous electrical properties. However, this material's fracture durability precludes its use in critical structural applications. (13, 14, 19-21).

Some recent works have studied GFRP/CFRP composites reinforced with Al_2O_3 . Asi et al.(22) prepared Al_2O_3 (0, 2.5, 7.5, 10, 12.5 and 15 wt.%) reinforced GFRP composites and investigated the mechanical properties. They observed that the tensile strength decreased with the increasing wt.% Al_2O_3 . Al_2O_3 -reinforced GFRPs' tensile strengths are lower than the unreinforced GFRP composite. However,

the highest bending strength was found in a 10 wt.% Al_2O_3 reinforced GFRP composite, and an increase of approximately 33% occurred compared to the unreinforced specimen. Mohanty et al.(23) fabricated nano- Al_2O_3 (0, 1, 2, 3, 4 and 5 wt.%) reinforced Glass/Carbon fiber epoxy composites and investigated composites' mechanical behaviour. They determined that composites' tensile strength decreases with the reinforcement of Al_2O_3 . Raju et al.(24) produced GFRP reinforced with Al_2O_3 (0, 5, 7.5 and 10 wt.%) composites and analyzed mechanical and tribological behaviour. They observed that Al_2O_3 reinforced enhanced composites' tensile strength (254 to 352 MPa), hardness (63 to 72 Shore-D) and wear resistance. Nayak et al.(25) prepared $\text{Al}_2\text{O}_3/\text{SiO}_2/\text{TiO}_2$ (10 wt.%) reinforced GFRP composites and investigated mechanical properties. The highest hardness and impact energy were found for Al_2O_3 -reinforced GFRP composites. Patel et al.(26) prepared Al_2O_3 and SiC (5 wt.%) nanoparticles reinforced GFRP and studied tribological features of the composites. As a result of the wear tests, the lowest wear loss was found in Al_2O_3 -reinforced GFRP composites at all applied normal loads and sliding speeds. Zhang et al.(27) focused on the tribological properties of the nano- Al_2O_3 (2, 4, 6, 8 and 10 wt.%) reinforced CFRP composites it produces. Based on their research, they found that reinforcing 4 wt.% Al_2O_3 decreased the rate of wear and the Coefficient of Friction (COF) by 74.7 % and 65.5 %, respectively when compared to the unreinforced CFRP. Kaybal et al.(28) researched mechanical strength of the nano- Al_2O_3 (1, 2, 3, 4 and 5 wt.%) reinforced CFRP. According to this study, the tensile strength and flexural strength reach the highest values with 2 wt.% Al_2O_3 reinforcement.

In the present investigation, we were produced hybrid (Al_2O_3 -GFs/CFs) reinforced epoxy matrix composites via the hand lay-up method. This study aims to obtain the optimum reinforcement amount to achieve the produced composites' highest mechanical and tribological properties.

MATERIALS AND METHOD

The epoxy resin (Epikote Resin 828 Lvel) is used with the hardener (Epikure Curing Agent 866) to produce composites. The mixing ratio for epoxy resin and curing agent is 3:1, respectively. Twill CFs (200 gr/m², fiber diameter: 7 μ m, laminate thickness: 0.327 mm) and twill GFs (200 gr/m², laminate thickness: 0.15 mm) were used. Al_2O_3 powders (Eti Aluminum, +98.5%, particle size:-100 mesh, Bulk Angle:32-36°, Cas:1344-28-1) are used as reinforcement.

In this study, we used the same production route to fabricate varying composites. Firstly, Al_2O_3 was dispersed in epoxy resin for 4 min using a mechanical stirrer. CFs and GFs were cut to the size of 250 mm length and 250 mm

width. The epoxy curing agent is added to the Al_2O_3 -epoxy mixture. The mixture was applied to CFs and GFs with a brush and after that, the composite was cured at room temperature for 48 hours. In this procedure, 4-layer hybrid composites were produced; the GFs-reinforced samples' thickness is approximately 2.2 mm and the thickness of the CFs-reinforced samples is about 1.1 mm. The composition of composites with reinforcement and sample codes are given in Table 1. While generating the sample code (XY), X represents the type of fiber (C: CFs and G: GFs) in the composite and Y represents the amount of Al_2O_3 (wt.%) in the composite.

Table 1. Sample codes and composition of composites

Sample Code	Epoxy:Fiber (wt. % ratio)	Fiber Type	Al_2O_3 (wt.%)
C0			-
C3		CFs	3
C5			5
C7			7
G0	1:1		-
G3		GFs	3
G5			5
G7			7

The epoxy matrix composites' densities were determined according to Archimedes' method in an ethanol medium and mean values were calculated based on three measurements. The fabricated samples were machined to Charpy impact test (l:80 mm x w:10 mm x t:4 mm), flexural strength (l:80 mm x w:10 mm x t:4 mm) and Barcol hardness test by the respective ISO 179-2, ISO 178-3 and ISO 59, respectively. We used a Devotrans Charpy Impact Tester for the impact test, AVK MH1/AS-102 for the 3-point bend test (The maximum load cell capacity: 500 kp) and Barcol Impressor for the Barcol hardness test. Images were taken from the fracture surfaces of the specimens after the impact tes-

ting with the Leica M-125 stereomicroscope. Reciprocating dry sliding wear tests were performed in a Bruker™ UMT2 Tribometer under 3 N force with 5 mm/s speed for 20 m of total distance by using 5 mm diameter chrome steel balls (ASTM E52100). Wear depths were obtained by examining the change in Z-axis values on the device. The processing and characterization of epoxy matrix composites are given schematically in Fig.1.

RESULTS AND DISCUSSION

Table 2 illustrates the density values of the composites. Relative density values for the produced specimens are between 94.05% and 80.27%. The relative densities of GFRP composites are always lower than CFRP composites. The highest relative density was observed in the C0 specimen. The relative density of CFRP composite specimens decreased with the reinforcement of Al_2O_3 . Nayak et al.(29) prepared nano- Al_2O_3 (0.1, 0.3 and 0.7 wt.%) reinforced GFRP composites, and observed that an increasing Al_2O_3 amount increased the void content. Because of their higher viscosity, highly reinforced materials are more difficult to mix and are more likely to produce voids(30). Also, this could be because the entrapped gas could not get out of the epoxy matrix throughout the production and curing processes(29).

Table 2. Relative density of CFRP and GFRP composites.

Sample Code	Theoretical Density (g/cm ³)	Relative Density (%)
C0	1.46	94.05
C3	1.5	90.95
C5	1.528	87.16
C7	1.551	85.01
G0	1.909	84.83
G3	1.946	80.27
G5	1.984	83.43
G7	1.850	84.06

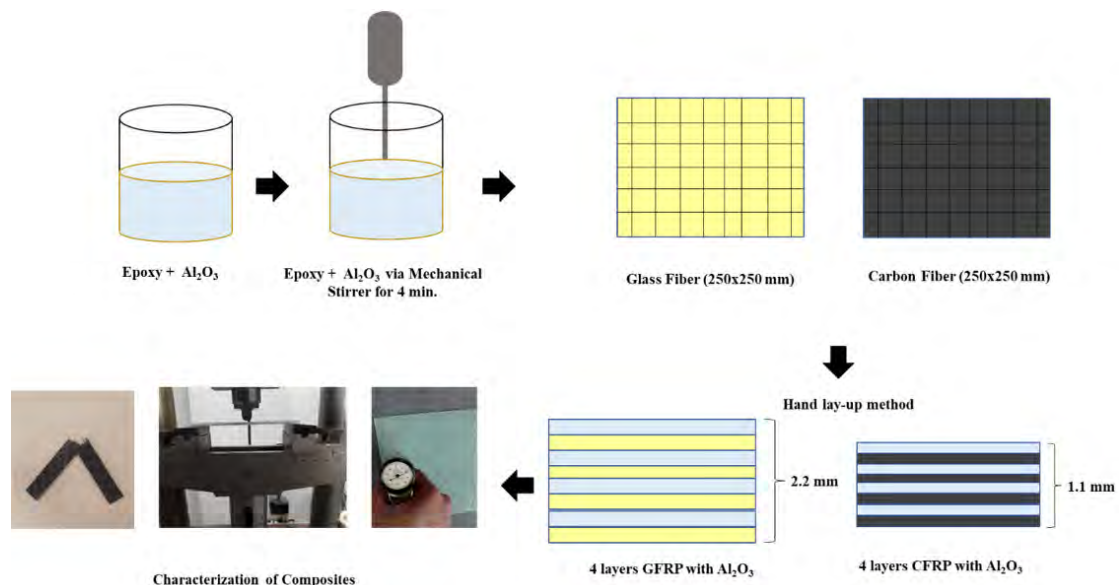


Figure 1. Processing and characterization of epoxy matrix composites

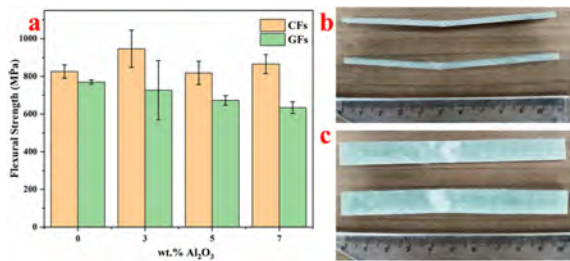


Figure 2. Flexural strength performance of epoxy matrix composites (a) flexural strength of the composites (b,c) image of specimens after testing

The 3-point bending test results of the composites are given in Fig. 2. The data shown are the average of three tests for each sample type. Flexural strength is determined between 946.3 and 634.1 MPa. The highest flexural strength values are obtained for 3 wt.% Al₂O₃ reinforced CFRP composites. With the addition of 3 wt.% Al₂O₃, the flexural strength increased by 15% compared to the unreinforced CFRP sample. However, Al₂O₃ reinforcement above these amounts affected the flexural strength adversely for CFRP composites. Unlike the CFRP, Al₂O₃ reinforcement decreased the flexural strength of GFRP composites and this decrease increased with increasing Al₂O₃ content. This is because as the Al₂O₃ content increases, the void content and Al₂O₃ particle agglomeration also increase, which can cause matrix swelling and the development of microcracks at the interface(29, 31). Moreover, the lower flexural properties may have been brought on by the filler's and epoxy resin matrix's poor interface bonding(22). Similar results are also available in the literature. Wang et al. prepared Al₂O₃ reinforced CFRP and analyzed flexural strength and they determined that the maximum flexural strength was 760 MPa with 15 g/m² (areal densities of Al₂O₃) Al₂O₃ reinforced

composites(32). Asi et al. produced GFRP-filled Al₂O₃ particles and investigated flexural strength. They determined that the optimum wt.% Al₂O₃ amounts was 10%(22). These studies found that above the optimum amounts, flexural strength was deteriorating.

The results from the varying amounts of Al₂O₃ reinforcement on the composite from the Charpy impact test are illustrated in Fig. 3. The data shown are the average of three tests for each sample type. The impact strength is determined between 42.2 and 187.4 kJ/m². The highest impact strength was found in unreinforced GFRP, and there was a decrease in impact strength with Al₂O₃ reinforcement (Approximately 28% decrease with the reinforcement of 7 wt.% Al₂O₃). Compared to GFRP, CFRP showed much lower impact strength overall. On the other hand, there was a remarkable 80.22% increase in the impact strength of the CFRP with the addition of 3 wt.% Al₂O₃. Increasing the Al₂O₃ amount also had a negative effect on CFRP. The stereomicroscope images (Fig. 3 (d-g)) were shown the presence of fiber breaks (1), delamination (2), voids (3) and matrix breakage (4) in the fracture surfaces. Wang et al. prepared Al₂O₃-reinforced CFRP and investigated impact strength. They found that the optimum Al₂O₃ was 15 g/m² and with the increase of the reinforcement ratio to 20%, the impact strength decreased by approximately 16%(32).

Fig. 4 demonstrates the effect of Al₂O₃ for CFRP/GFRP composites on hardness behaviour. Hardness is obtained between 33.5 and 48.7 HBA. The maximum hardness value in both composite types was obtained in the samples reinforced with 3 wt.% Al₂O₃. Compared to the unreinforced samples, there was a 12.99% and 7% increase in hardness for CFRP and GFRP, respectively. Increasing the Al₂O₃ amount above 3 wt.% also had a negative effect on the hardness of both composite types. It's a general rule that the hardness of a material goes up as the filler increases. Fillers give epoxy resins their hardness, and as the amount of filler increases, so does the hardness of the epoxy(33). It was observed that agglomeration in CFRP composites decreased the impact and flexural strength with above 3 wt.% Al₂O₃; hence, a decrease in hardness is also observed. Similar results are also available in previous studies(33-35).

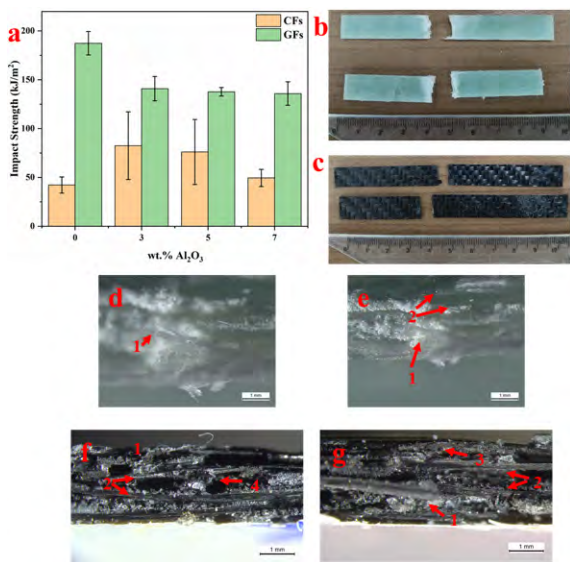


Figure 3. Impact performance of epoxy matrix composites (a) impact strength of GFRP/CFRP composites with varying wt.% Al₂O₃ (b,c) image of specimens after testing and stereomicroscope image of specimens after impact test (d) G0, (e) G5, (f) C0 and (g) C7

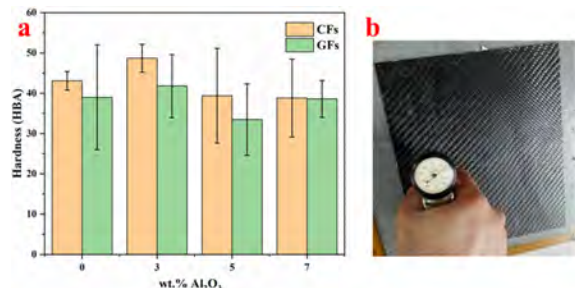


Figure 4. Hardness results of the composites (a) the hardness of composites with varying wt.% Al₂O₃ and (b) Barcoll hardness test view

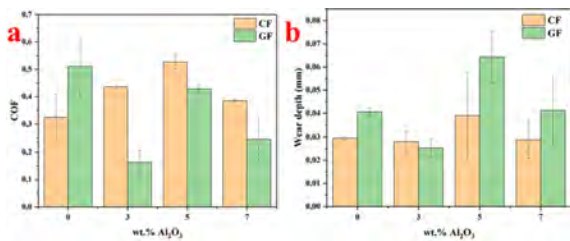


Figure 5. Wear test results of the composites (a) COF and (b) wear depth

The COF and wear depth of composites that originated from varying Al₂O₃ wt.% amounts are illustrated in Fig. 5. The average COF and wear depth values refer to at least three tests. The COF and wear depth values are between 0.1625-0.5264 and 0.0252-0.0642 mm, respectively. The composites' lowest COF and wear depth values were determined for the G3 samples. Studies in the literature show that the materials with the lowest COF and wear depth have the highest wear resistance (36-38). The highest COF was obtained for the C5 samples, and the maximum wear depth was observed G5 samples. In CFRP composites, adding Al₂O₃ increased the COF value compared to the unreinforced sample. In contrast, in GFRP composites, adding Al₂O₃ increased the COF value compared to the unreinforced sample. The lowest wear depth for both composite types was obtained in the samples reinforced with 3 wt.% Al₂O₃. Zhang et al. found the lowest COF and wear rate results for 4 wt.% nano-Al₂O₃ reinforced CFRP composites(27).

CONCLUSIONS

The GFRP and CFRP reinforced with Al₂O₃ composites are produced via the hand lay-up method and investigated the mechanical and tribological properties. The conclusions are as follows:

- The relative density of the composites generally decreased with Al₂O₃ reinforcement. Also, the relative densities of CFRP composites are higher compared to GFRP.
- The highest flexural strength values are obtained for 3 wt.% Al₂O₃ reinforced CFRP composites. Al₂O₃ reinforcement decreased the flexural strength of GFRP composites and this decrease increased with increasing Al₂O₃ amount.
- The highest impact strength was found in unreinforced GFRP, and there was a decrease in impact strength with Al₂O₃ reinforcement. On the other hand, there was an outstanding increase in the impact strength of the CFRP with the addition of 3 wt.% Al₂O₃.
- The maximum hardness value in both composite types were obtained in the samples reinforced with 3 wt.% Al₂O₃.

- The lowest COF and wear depth was found 3 wt.% Al₂O₃ reinforced GFRP composites.

As a result of the studies, it has been determined that the optimum Al₂O₃ ratio is 3 wt.%. Future research will focus on ensuring a more homogenous distribution of reinforcements in the epoxy as well as improved surface adherence between the reinforcement and the matrix.

CONFLICT OF INTEREST

Authors approve that to the best of their knowledge, there is not any conflict of interest or common interest with an institution/organization or a person that may affect the review process of the paper.

AUTHOR CONTRIBUTION

Cantekin Kaykilarli: Investigation, Characterization, Writing-Review&Editing

Aymurat Haydarov: Production, Characterization, Writing.

Duygu Kose: Production, Characterization, Writing.

Hasibe Aygul Yeprem: Investigation, Supervision, Writing-Review&Editing

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Examination Of Perlite-Polymer Interface Interactions in Polypropylene-Based Composites via Several Compatibilizers

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ABSTRACT

The surface interaction between the polymer and the mineral additive is one of the most significant aspects influencing the efficiency of mineral-filled polymeric composites. In this work, three distinct compatibilizers were introduced to composites based on polypropylene (PP) and perlite to improve interactions between the constituents. On composites comprising 10% expanded perlite content, three different ratios of ethylene vinyl acetate copolymer (EVA), thermoplastic polyurethane elastomer (TPU), and maleic anhydride grafted polypropylene (MA-PP) compatibilizers were employed. The composite was produced using an approach designated melt blending followed by injection molding. The composites containing MA-PP compatibilizer possessed the most outstanding performance, according to the results of mechanical, physical, and dynamic mechanical evaluations and morphological characterizations. The investigated aspects indicated a rise in the composites containing 10 percent compatibilizer with the lowest adding amount, whereas performances declined at high compatibilizer contents. Along with these results, it was determined that the compatibilizers included in the PP/perlite composite system assisted in the fabrication of the composites by promoting the force values and melt flow rates identified during melt mixing. Following the test outcomes, MA-PP performed better than TPU and EVA in terms of compatibilizer efficiency. In general, it has been revealed that the selection of MA-PP compatibilizer in the manufacturing stages would offer benefits in terms of both simplicity of processing and mechanical strength where expanded perlite will be adopted as a natural filler for PP-based composites.

Keywords:

Mineral additive; Polymer composites; Expanded perlite; Compatibilizer; Polypropylene; Polymer processing

INTRODUCTION

Because they are inexpensive and straightforward to handle, minerals are frequently used as reinforcement for polymer-based substances. Due to the low degree of incompatibility between the natural mineral surface and the polymer phase, the incorporation of mineral additives in polymeric composites has several limitations despite benefits like low weight, low cost, and recyclability (1-5). As a practical option to address the compatibility difficulties, tuning the chemical nature of the matrix-filler interface via integration of compatibilizer leads to improved mechanical resistance of composite materials (6-10).

The amorphous volcanic silica glass known as perlite is a naturally formed mineral with a high level of

water. This aluminosilicate may expand by thirty times its original volume after heating. The majority of the world's perlite reserves, or more than 50%, are in Türkiye. Similar to volcanic particulate minerals, expanded perlite powder was used as an additive for various polymeric matrices (6, 11, 12). Polymers compounded with perlite mineral include polyolefins, polyesters, elastomers, and copolymers based on various forms such as films, foams, resins, fabrics, and 3D parts. Table 1 summarizes the polymers and investigated properties by citing these research studies (13-51).

As indicated in Table 1, research works dealing with PP/perlite composites were performed in four studies which reported that incompatibility between inor-

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Table 1. PER reinforced polymer composites in the literature.

Polymer matrix	Examined behavior	Reference number
Polyethylene (PE)	Thermal and mechanical	(13-19)
Polypropylene (PP)	Mechanical and processing	(20-23)
Polystyrene (PS)	Mechanical	(24, 25)
Polyvinylalcohol (PVA)	Thermal and mechanical	(26)
Acrylonitrile-butadiene-styrene (ABS)	Flame retardancy and mechanical	(27-29)
Poly(lactic acid) (PLA)	Crystallinity and thermal stability	(30, 31)
Polyethyleneglycol (PEG)	Heat storage	(32)
Hydroxyapatite (HA)	Tissue engineering	(33, 34)
Polyaniline (PAn)	Electrical conductivity	(35)
Natural rubber	Odour-adsorbing	(36, 37)
Polyester fabrics	Acoustical	(38)
Polyphenylene sulphide (PPS)	Tribological	(39)
Polyurethane (PU)	Thermal insulation	(40-42)
Paraffin	Heat storage	(43, 44)
Epoxy resin	Ablative	(45-48)
Novalac resin	Tribological	(49)
Chitosan	Thermal stability	(50)
Polymethacrylic acid (PMAA)	Drug delivery	(51)
Butadiene rubber	Industrial goods	(52)

ganic perlite filler and organic PP phase influenced the mechanical behavior of composites negatively (20-23). Since the efficiency of maleic anhydride grafting is stated as the favored option for polymer composites (53-55), maleic anhydride grafted PP (PP-MA) was preferred as a compatibilizer. In addition to PP-MA, thermoplastic polyurethane (TPU) and ethyle-vinyl-acetate (EVA) were utilized to increase surface interactions in perlite-loaded PP composites attributed to their miscibility in the PP phase (56-59).

The interphase between additive and polymer phases plays a key role in the properties of composite materials attributed to physical and chemical aspects. The formation of interfacial interactions on the polymer-additive interface by integration of compatibilizers that can interact with both perlite and PP. For this reason, PP-MA, TPU, and EVA were compounded to enhance the interface adhesion of the inorganic perlite phase with organic PP matrix. Based on the findings of this study, performances of PP/perlite composites in terms of mechanical, morphological, processing, and melt-flow properties were compared to PP/EVA, PP/TPU, and PP/PP-MA composites involving perlite. Additionally, adding amount of perlite powder was investigated based on examined behaviors.

MATERIAL AND METHODS

Materials

PP with the trade name of Petoplen EH-251 was obtained from Petkim, İzmir, Türkiye. MA grafted PP was used as a compatibilizer with a commercial name Exxelor™ PO 1020 supplied by ExxonMobil, Texas, USA. The degree of grafting for PP-MA was indicated as a high graft level by the producer. Ester-based TPU (R130A85) was purchased from Ravago Petrochemicals, İzmir, Türkiye. The commercial name of EVA was Alcludia PA-461 supplied by Repsol S.A., Madrid, Spain. The vinyl acetate content of this EVA grade was 33%. According to their datasheets provided by producers, melting temperatures of EVA, TPU, and PP-MA polymers were 59 °C, 190 °C, and 162 °C, respectively.

Expanded perlite with a bulk density of 300–1000 g/cm³ was supplied by Eti Maden, İzmir, Türkiye. The average particle size of PER was found to be 18 µm thanks to the particle size distribution curve shown in Fig. 1.

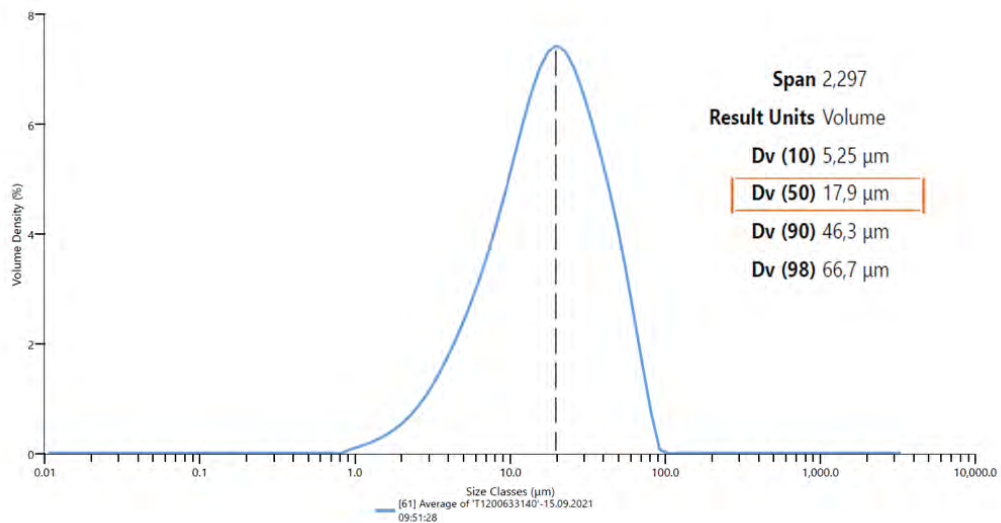


Figure 1. Particle size distribution curve of PER.

Composite Production

PP, TPU, PP-MA pellets, and PER powder were dried under vacuum at 80 °C for 2 h to remove moisture content before the compounding process. Composite samples were fabricated via Xplore MC15HT micro-extruder. Adding amount of PER in composites was kept constant at 10% by weight. Three different concentrations for compatibilizers 10%, 20%, and 30% by weight were used. Processing temperature of 185°C, screw speed of 100 rpm, and mixing time of 4 min were applied during the melt-mixing process. After the compounding step, dog-bone shaped test specimens with a dimension of 7.6 × 2.0 × 80 mm³ for the tensile test and the dimension of 45 × 20 × 6.5 mm³ for the D-type Shore hardness test was shaped using Daca injection molding instrument.

Characterization Techniques

Malvern Panalytical Mastersizer 3000 was used to evaluate the particle size of PER powder. Xplore Instruments program was employed to quantify force values throughout the extrusion process. The screw force values in the melt were determined using the micro-compounder's rheological software as a function of mixing time. Lloyd LR 30 K universal tensile testing machine was used for tensile properties of composites. Shore hardness values were determined using the Zwick R5LB041 digital hardness device. MFI measurements were performed via Coesfield Meltfixer LT using a 2.16 kg standard load at 185°C. The JSM-6400 Electron Microscope, a field emission scanning electron microscope, was used for observing the morphological characteristics of composite materials. A small coating of gold was applied to the surfaces of the cracked samples from the tensile test to establish conductive surfaces.

RESULTS AND DISCUSSION

Force Measurements

According to Fig. 2, force vs. time graphs demonstrate that PER additions elevated mixing force values due to powder incorporation boosted shear force as a result of increased melt viscosity throughout the extrusion operation. Compatibilizer inclusions with 10% content yielded lower force values compared to the PP/PER composite. The inclusion of EVA yielded a remarkable reduction in force values of PP/PER, whereas higher force values were obtained by TPU and PP-MA additions compared to the PP/PER EVA sample. Before high-scale production stages, this metric offers experimental data for planning manufacturing on the cost of fabricating the resultant composite materials. Since lower force data were recorded in compatibilizer-included composites relative to the force values of the PP/PER sample, the production of PER-filled PP composites can be carried out more economically in the presence of EVA, PP-MA, and TPU.

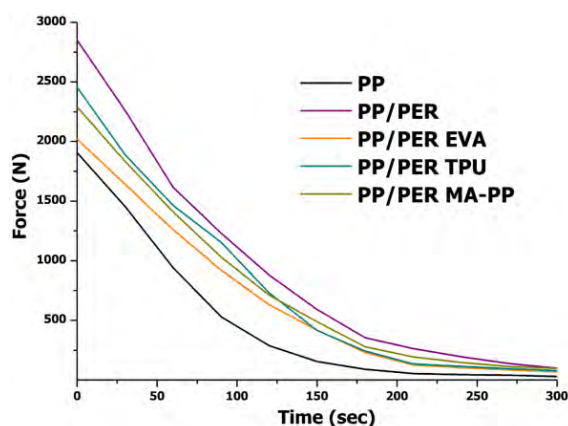


Figure 2. Force vs. time curves of PP and composites.

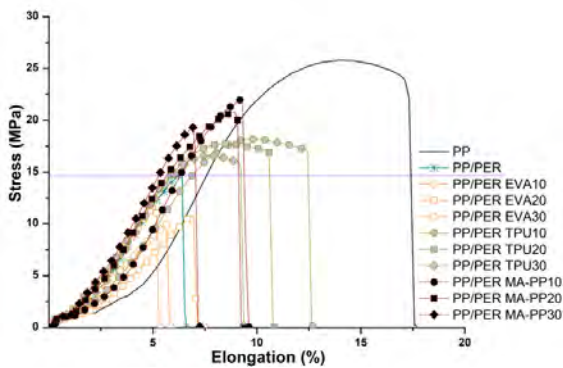


Figure 3. Stress vs. strain curves of composites.

Tensile Properties

Fig. 3 depicts tensile stress vs. percent strain curves. Tensile test data for PP and its composites, which include tensile strength, strain at break, and tensile modulus parameters are illustrated in Fig. 4.

The unfilled PP displayed ductile behavior according to its stress vs. strain curve in Fig. 3 in which necking behavior was observed. Since there was no necking property at the ultimate strength value. On the contrary, brittle characteristic was obtained after the incorporation of PER. Additionally, tensile stress and strain exhibited dramatic decline by PER addition. Using TPU as a compatibilizer caused to increase

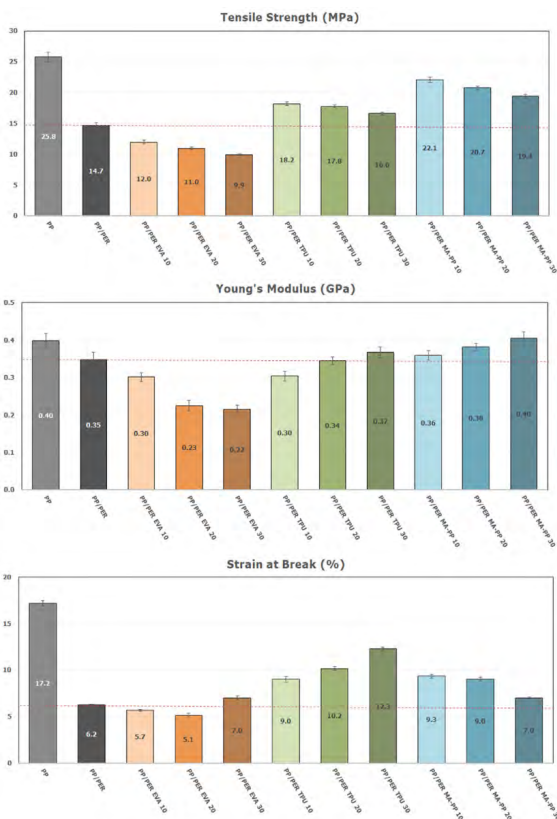


Figure 4. Tensile test data of samples.

in the ductile behavior of composites stem from its high-strain elastomeric property whereas integration of PP-MA showed no effect on the brittle form of PP/PER.

Fig. 4 implied that EVA addition to the PP/PER system reduced tensile strength and Young's modulus parameters as well as strain values. As a common result, an increase in compatibilizer concentration resulted in a decline in the tensile strength of composites. TPU and MA-PP exhibited higher strength values compared to the PP/PER sample. The greatest tensile strength performance was achieved as PER-containing composites compounded with PP-MA compatibilizer since MA graft on PP structure enhanced compatibility between PER and polymer interface (55, 60).

Based on Young's modulus data, EVA displayed the worst performance among compatibilizers since remarkable reductions in modulus were observed. Conversely, TPU and PP-MA additions showed a positive effect on the modulus parameter of PP/PER. Young's modulus of composites enhanced as the added amount of compatibilizer increased

TPU-incorporated composites displayed a remarkable increase in percentage strain parameters attributed to the well-known high elongation behavior of TPU elastomer. PP/PER EVA composites gave the lowest results in terms of tensile strain.

Hardness Results

D-type Shore hardness data of unfilled PP and PER-filled PP composites are listed in Table 2. There were no significant differences in hardness measurement results compared to the reference material (PP). The shore hardness of PP displayed a slight increase with the addition of PER powder. Since EVA has an elastomeric nature, its

Table 2. Shore hardness results of composites.

Sample code	Hardness (Shore D)
PP	77.0 ± 0.1
PP/PER	77.5 ± 0.1
PP/PER EVA 10	76.5 ± 0.1
PP/PER EVA 20	76.0 ± 0.1
PP/PER EVA 30	75.0 ± 0.1
PP/PER TPU 10	78.0 ± 0.1
PP/PER TPU 20	78.5 ± 0.1
PP/PER TPU 30	79.5 ± 0.1
PP/PER MA-PP 10	77.5 ± 0.1
PP/PER MA-PP 20	77.5 ± 0.1
PP/PER MA-PP 30	78.0 ± 0.1

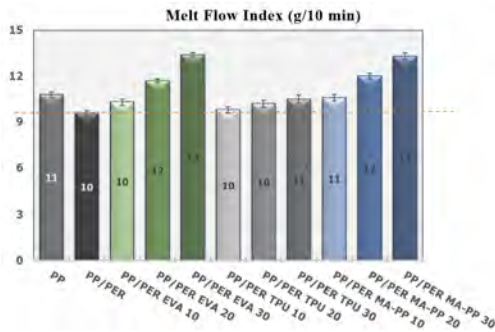


Figure 5. MFI data of samples.

integration into the PP/PER composite system resulted in reductions in the Shore D hardness of composites. On the contrary, TPU inclusions yielded improvement in hardness results despite it has elastomeric characteristics. The main reason for this observation might be the higher Shore D value of TPU with respect to PP. Similarly, PP-MA addition led to an increase in the Shore D parameter of the PP/PER composite.

Melt-flow Behaviors

Melt-flow index analysis is widely employed in thermoplastics for assessing the viscosity of molten polymers. Fig. 5 depicts the MFI characteristics of PP and related composites. When compared to unfilled PP, PER-incorporated composite possessed a lower MFI value. The rising quantity of MFI was found to be notable for composite samples containing a higher percentage of compatibilizers. TPU-loaded composites gave lower MFI values that were very similar to that of PP/PER. MFI specifications for composites were found to be in a limited spectrum while compared to unfilled PP as an overall finding regarding the melt-flow behavior of PER-loaded PP composites.

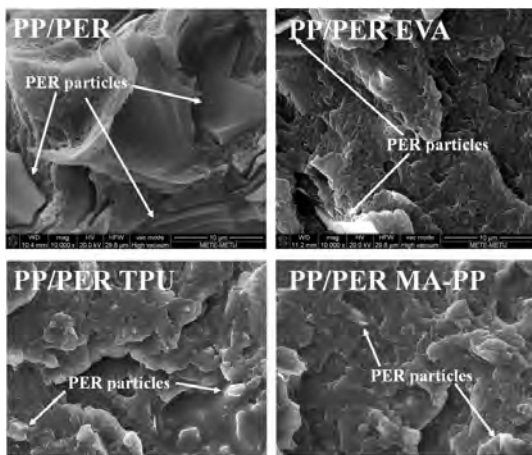


Figure 6. SEM micro-images of composites.

Morphological Analysis

The morphological study of composite samples was accomplished using SEM micro-images, which are illustrated in Fig. 6. Large gaps between PER particles and the PP matrix were detected in the SEM micrograph of PP/PER. The presence of compatibilizers donated strong adhesion and dispersion homogeneity in composite morphology. The formation of large gaps between phases was found to disappear after the inclusion of EVA as well as TPU. Similar to other compatibilizers, introducing PP-MA caused enhanced surface adhesion and distribution quality of PER according to the SEM image in Fig. 6. The result offered visible confirmation for improvements in associated composite performances pointed out in previous chapters.

CONCLUSION

One of the most crucial factors affecting the performance of mineral-filled polymeric composites is the surface interaction between the polymer and the mineral additive. In this research study, three different compatibilizers were used to enrich the interactions between phases in perlite-containing polypropylene (PP) composites. For this purpose, three different ratios of ethylene vinyl acetate copolymer (EVA), thermoplastic polyurethane elastomer (TPU), and maleic anhydride grafted polypropylene (MA-PP) compatibilizers were used on composites containing 10 percent expanded perlite mineral. Melt mixing followed by injection molding processes were used as the composite production process. In light of the findings obtained after mechanical, physical, and dynamic mechanical analysis and morphological characterizations, composites containing MA-PP compatibilizer showed the best performance. In the composites containing 10 percent compatibilizer with the lowest adding amount, an improvement was observed in the investigated properties, and a decrease in performances was detected at high compatibilizer concentrations. In addition to these findings, it was observed that the force values and melt flow rates measured during melt mixing, compatibilizers-introduced into the PP/perlite composite system facilitated the processing of the composites. According to the test results, the performance ranking among compatibilizers was found to be MA-PP > TPU > EVA. As a general conclusion, it has been evaluated that the preference of MA-PP compatibilizer in the production stages where expanded perlite will be used as a natural filler in PP-based composites will provide advantages in terms of both ease of processing and mechanical strength.

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CONFLICT OF INTEREST

Authors approve that to the best of their knowledge, there is not any conflict of interest or common interest with an institution/organization or a person that may affect the review process of the paper.

AUTHOR CONTRIBUTION

Çağrıalp Arslan: Methodology, Software, Validation, Writing- original draft. Ümit Tayfun: Data curation, Visualization, Investigation, Writing- review and editing. Mehmet Doğan: Supervision, Conceptualization.

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Performance Comparison of Waste Cooking Oil on Coal Slime Flotation with Sunflower Oil and Kerosene

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ABSTRACT

This study explores the potential use of waste cooking sunflower oil (WSO) as an eco-friendly collector for coal slime flotation. WSO and coal slime are both waste materials and can be hazardous to human health and the environment, if not disposed of properly. In this study, co-disposal of the two wastes was investigated; a kerosene (petroleum derived oil) and crude sunflower oil (CSO) were used for collector efficiency comparisons. This study also presents a green, low-cost and environmentally friendly alternative. Kinetic flotation tests were carried out to study the flotation selectivity, flammability and combustible recovery. Contact angle measurements were performed with 3 different oils (CSO, WSO and kerosene) by sessile drop method to determine the hydrophobicity and surface properties of coal. Fourier-transform infrared (FTIR) spectroscopy was utilized to analyze for the chemical composition of both WSO and slime coal samples.

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Keywords:

Sunflower oil; Waste cooking oil; Kerosene; Coal slime; Flotation

INTRODUCTION

Waste cooking oil, a liquid waste from kitchens and food sectors, can be hazardous to the environment and human health [1, 2]. The challenges of the treatment of WCOs are primarily involve: the disposal-collection strategy and waste reconversion [3]. In terms of WCO reconversion, they can be employed as primary raw materials in a variety of industrial processes, for instance for the production of biofuel or bio-lubricants, animal feed, and asphalt additives. Other WCO applications are only those that are directly related to their chemical composition.

The mining and washing of coal produces coal slime as a by-product. It is a semi-solid material comprised of water and crushed coal. It is mostly composed of flotation waste from coking coal preparation plants, slurry created after hydraulic coal transportation as well as washing slurry from power plant coal washing facilities [4-6].

Kerosene is a common collector in coal flotation, although it has a high collector consumption (approximately 10 kg/t) and a high cost [7, 8]. Turkey produces 5 million tons of bituminous run of mine coal annually.

About 5-7% of these coals are taken under the thickener as "coal slime" or "coal fines wastes" after being washed in dense medium plants. After being dewatered using filter presses, these coals are either disposed of in waste pools or used as fuel for thermal power plants. Concentration of these coal slimes with very fine size ($d_{50} \sim 35 \mu\text{m}$) by flotation method is a very costly process. Because it contains high amounts of clay minerals and these clays adsorb large amounts of collectors. Prices per liter of petroleum product in Turkey are higher than in other countries of the world many times over. Therefore, to optimize the coal flotation process in Turkey, an economic collector must be found. In the present case, Turkey does not have any flotation plant for the recovery of coal slime. The biggest reason for this is the collector cost. Kerosene is a petroleum product collector, which is particularly preferred in coal flotation due to its high yield and selectivity. As petroleum products are non-renewable and have extremely flammable properties, there is a need for new research on alternative collectors. In this context, the use of vegetable oils as an alternative collector to petroleum products for coal flotation has been reported by researchers [9-19]. Vegetable oils (VOs) have low concentrations of nitrogen, sulfur,

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and heavy metals, it is also a non-polluting raw material that is renewable and readily available. VOs are being actively researched for alternative applications, such as biodiesel production and utilization as raw materials in the chemical and industrial sectors. These oils contain long-chain fatty acids that possess dual functions as frothers and collectors, thanks to their ester groups that contribute to their frothing abilities [10, 20, 21]. Thus, it was assumed that WSO would improve coal particle flotation recovery [9, 12, 22]. Moreover, crude soybean and olive oils, each vegetable oils, were mentioned within the literature as collectors for fine coal recovery. For example, Colza oil turned into used as a collector to get high-calorific and low-ash coal. Additionally, Polanga and Mahua oils were utilized as collectors to increase the floatability of high ash Indian non-coking coal [23]. Numerous researchers have indicated the potential use of vegetable oils or waste cooking oils (WSOs) as collectors in coal flotation and agglomeration processes [11, 21]. The use of WSOs as a collector can be caused by two main problems that can occur in flotation plants. The first of these is the clogging of the liquid carrier pipes and sluices with oil. This problem can be solved by using various surfactants. The other problem is the oily wastewater that will come out after the process. There are many methods that can be applied to remove oils from oily wastewater. For example, gravimetric separators remove free oil from wastewater [24, 25]. According to the US Department of Agriculture (USDA) data for the years of 2021-2022 world vegetable oil production is 214.8 million tons. This oil is used for cooking more than half of it, and on average ~ 100 million tons of WSO is produced every year [26, 27]. In this study, WSO was used as a collector in the coal flotation and the results were compared with the kerosene and sunflower oil as a collector.

MATERIAL AND METHODS

Materials

The coal slime utilized in the flotation studies was sourced from the thickener underflow stream of a coal washing plant in Turkey, where Zonguldak bituminous coal was processed (Fig. 1).

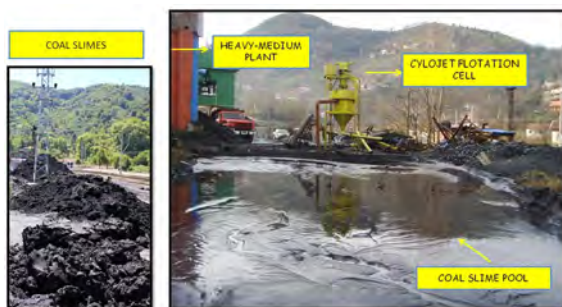


Figure 1. Image of coal slimes and clean coal production from the slime pool by flotation.



Figure 2. Flowsheet of collector prepared from kitchen waste oil.

The plant operates with a capacity of 150 t/h. Coal with a size of $-100 + 1$ mm is washed by a heavy-medium cyclone with three products; raw coal with a size of -1 mm is deslimed by a hydrocyclone ($\varnothing 400$ mm) and the coarser fraction is routed through coal spirals. The hydrocyclone overflow material (coal slime) is sent to a thickener ($\varnothing 12$ m) and then pumped into the coal sludge pool.

WSO was obtained from the kitchen waste cooking oil. The waste oil was collected in a 500 ml beaker with mixture of oil, waste water and food residue. Due to waste oil contains food residue, firstly the raw materials were sieved for the removal of solid waste and then WSO collector was prepared via filtration and heating processes. For contact angle measurements, we obtained the coal sample as a lump size from the entrance of a washery plant located in Zonguldak, Turkey.

Characterization of Coal Fine Wastes

Proximate analysis was performed to determine the characteristics of the waste coal sample. Proximate analysis was performed on a dry basis and the ash content was 33.75% the total sulfur content was 0.68%. The calculated volatile matter and fixed carbon contents are 29.10% and 37.45%, respectively. According to these results, it can be said that coal has high ash content and low sulfur content. It is in the category of medium volatile coal in terms of volatile matter content.

As a result of the size analysis of the waste coal sample with the Mastersizer 3000 laser diffraction particle size analyzer, the average particle size (d_{50}) of the material was found to be 45 micrometers, and the d_{80} size was 190 micrometers.

Table 1. Properties of the WSO.

Physical Properties	Value
Viscosity	73 mPa/s
Density	0.91 g/cm ³
Oil-water interfacial tension	22.02 mN/m

Collector Types; CSO, WSO and Kerosene

CSO (2000 g/t) was obtained from Kristal company in Izmir, Turkey and used as received in the experiments. WSO (2000 g/t) was used multiple times to cook meat, vegetables, and fish. Properties of the WSO are presented in Table 1.

Kerosene (from Tupras Company in Izmir, Turkey) as a traditional collector was used to compare with the proposed collectors in coal flotation process. Eucalyptus oil is used as a frother.

METHODS

Kinetic Flotation Tests and Release Tests

Flotation tests were carried out in a Denver machine with a 1.5-liter cell capacity. The impeller speed was set to 1100 revolutions per minute. In all experiments, the solid ratio was set at 10%. The sample was mixed well with tap water in the cell for 10 minutes before each flotation test to ensure that the surface was wet. Kinetic flotation tests were performed to determine WSO, CSO and kerosene collection potential (for 30, 60, and 240 seconds of froth scraping).

The obtained concentrates underwent filtration, followed by washing with acetone and drying in an oven. Prior to initiating the kinetic flotation tests, a "release test" procedure, developed by Dell, was employed to determine the final washability limit of the coal sample [28]. The optimal washability result was achieved by varying stirring speeds in a Denver cell and employing high reagent dosages (10 kg/t WSO, 0.4 kg/t eucalyptus oil). Fig. 3 illustrates a schematic representation of the particle-oil adsorption process during coal flotation, using kerosene, CSO, and WSO.

To assess the flotation performance, various metrics including yield, assay, efficiency index, recovery, and selectivity index were examined. In this study, the comparison of flotation performance was based on the combustible recovery-concentrate ash curve. Additionally, the effectiveness of coal flotation was evaluated using an efficiency index (EI), which was calculated using Eq. 1 [29, 30].

$$EI = CR \times \left(\frac{At}{Ac} \right) \quad (1)$$

where CR: combustible recovery, Ac:concentrate ash content, and At: tailing ash content [31].

Contact Angle Measurements

Contact angle is a common technique for determining a material's wettability. As mentioned earlier, wettability is determined by measuring the contact angle formed between the solid and the liquid surface when they come into contact [32].

The contact angle of kerosene, CSO and WSO was measured using the Sessile Drop method on a flat coal surface with an Attention theta contact angle goniometer (Fig. 4).

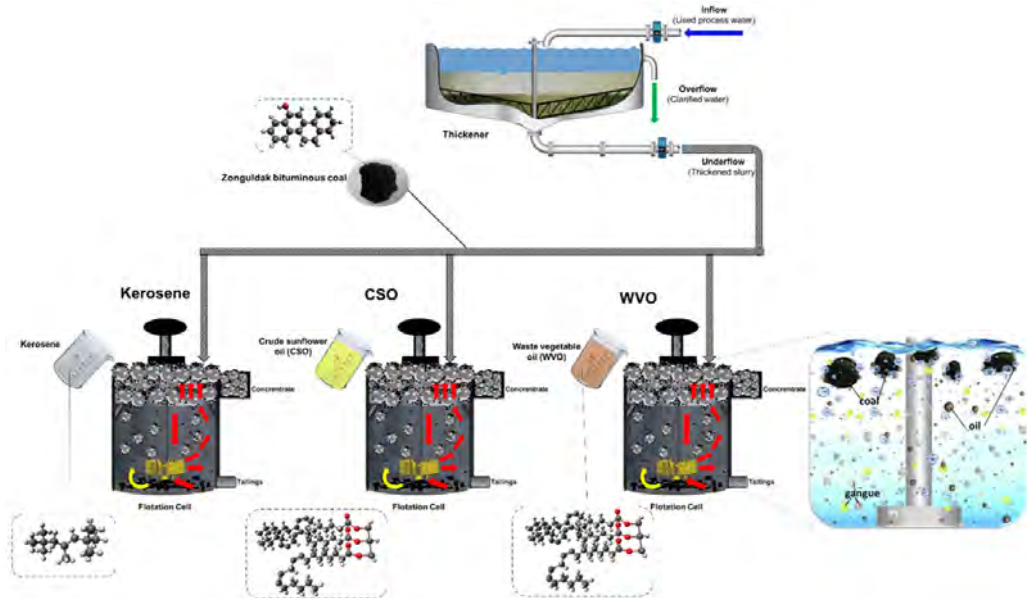


Figure 3. Schematic illustration of coal flotation with Kerosene, CSO and WSO.

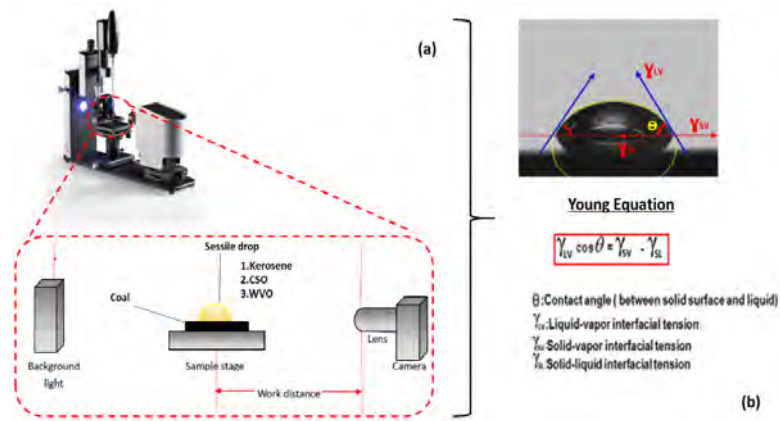


Figure 4. (a) The illustration of the contact angle goniometer (b) schematic representation of wetting statics in Young's equation for solid-liquid-vapor system.

Contact angle measurements were taken after a 15-20 second interval once the water drop size had increased. This approach was utilized to determine the contact angle values. All measurements were conducted at a temperature range of approximately 20-22°C.

The contact angle represents the angle created by a liquid droplet on a solid surface, as determined by the Young equation [33]. In Fig. 4 (b), the contact angle of an oil droplet on coal is depicted, influenced by three interfacial tensions: liquid-vapor, solid-vapor, and solid-liquid. This relationship is described by Young's equation, as shown in Eq. 2.

$$\gamma_{LV} \cos \theta = \gamma_{SV} - \gamma_{SL} \quad (2)$$

where θ is the contact angle, γ_{LV} : liquid-vapor, γ_{SV} : solid-vapor, and γ_{SL} : solid-liquid are the interfacial tensions.

RESULTS AND DISCUSSION

FTIR spectra can be used to evaluate the chemical characteristics of coal, WSO and coal floated with WSO samples, which were recorded with Thermo Scientific Nicolet 6700 FT-IR Spectrometer, over range of 400–4000 cm^{-1} . The FTIR spectrum of coal is presented in Fig. 5.

The band at 1437 cm^{-1} is attributed to vibration of CH_2 group and hydrophobic functional [34, 35]. The peaks at 2853 cm^{-1} , 2922 cm^{-1} are related to C-H stretching. [36]. The peak at 722 cm^{-1} may be the O-H stretching [37]. The peaks at 3522 cm^{-1} and at 1593 cm^{-1} are for OH and COOH group, respectively. The peaks around 1000 cm^{-1} may be attributable to C-O-C. According to literature [30, 35, 38, 39] the bands at 3452 cm^{-1} were assigned to OH vibrations. The peaks observed at 2920 cm^{-1} is due to the aliphatic hydrocarbon groups vibration in coal [40].

Releasing test results for WSO, CSO, and kerosene is important for assessing their suitability for different applications, ensuring compliance with standards, and ensuring optimal performance and efficiency. As seen in Fig. 6, kerosene has a higher collection capacity than WSO. In the experiments using kerosene, 8.97% ash clean coal was recovered with 64.58% combustible recovery value, while in the experiments using WSO, 9.88% ash clean coal was

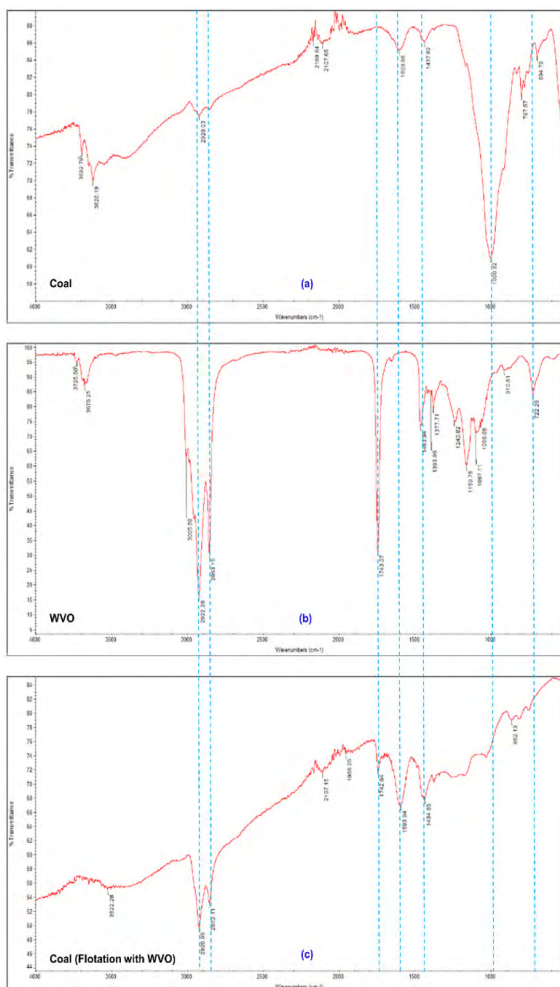


Figure 5. FT-IR spectra of samples: a) coal, b) WSO, and c) coal floated with WSO.

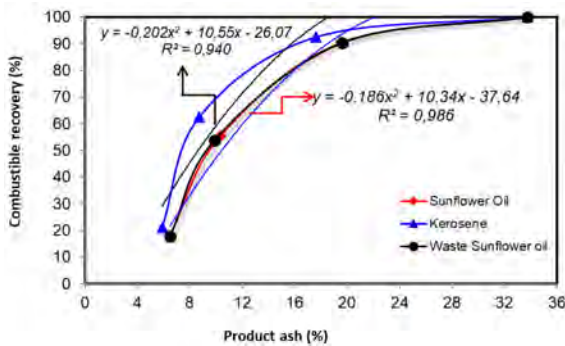


Figure 6. Release test results with WSO, CSO and kerosene.

recovered with 53.73% combustible recovery value. If clean coal product with 10% ash is desired to be sold, the kerosene collector has a combustible recovery rate of approximately 69%, while the WSO has a rate of around 54%. The lower combustible recovery of WSO has been hypothesized to be due to the hydrophilic oxygen bonds present in its structure, which limits its ability to collect. Kerosene is an effective collector due to its absence of oxygen groups and its purely hydrocarbon structure. Recent research suggests that oxygen-containing functional groups, particularly the carboxyl group, play a crucial role in enhancing coal surface wettability [41].

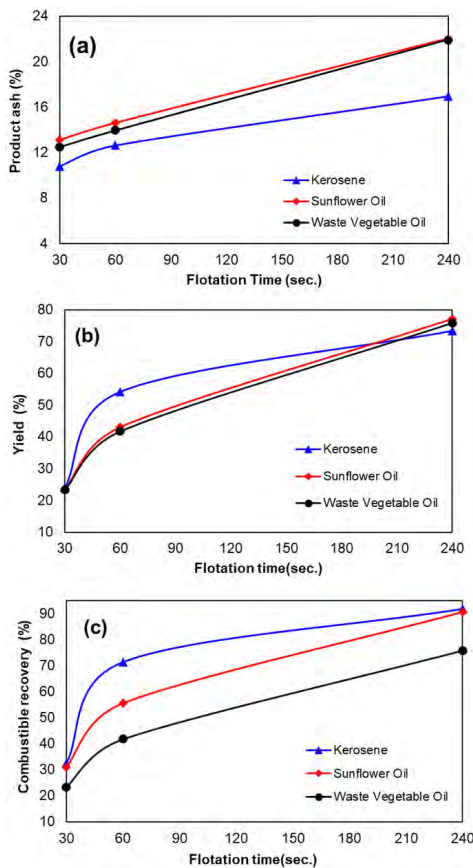


Figure 7. (a) Product ash, (b) yield and combustible recovery values obtained in kinetic tests depending on flotation time with WSO, CSO and kerosene used as collectors.

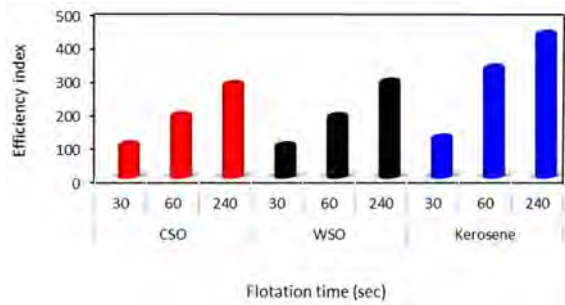


Figure 8. Flotation efficiency index (EI) at various collecting times with WSO, CSO, and kerosene.

Zhou et al. (2015) have reported that carboxyl and hydroxyl groups are the most effective promoters of surface wettability based on XPS peak-split data. Fig. 7 illustrates the results of kinetic flotation tests conducted using CSO, WSO, and kerosene.

Fig. 7 indicates that the combustible recovery of kerosene at the end of 240 seconds flotation time is 94.17%, while the combustible recovery value obtained with WSO is 88.98%. The results indicate that the kerosene collector exhibits higher selectivity compared to CSO and WSO. For instance, after 240 seconds of flotation, the product ash obtained was 17.94% with kerosene, whereas it was 21.73% with the WSO collector.

The efficiency index of CSO, WSO, and kerosene collectors increased as flotation time increased for the three types of collectors, as shown in Fig. 8. At all-time intervals, the efficiency index of kerosene was higher than that of CSO and WSO. For instance, after 240 seconds of flotation time, the efficiency index for kerosene is 471.65, whereas for WSO it is 284.80.

As depicted in Fig. 9, the contact angles measured for kerosene, WSO, and CSO oils on the coal surface were 100°, 91°, and 88°, respectively. The results from Fig. 7 show that kerosene exhibits superior collecting properties on the coal surface compared to CSO and WSO. Hence, these findings support the flotation experiments.

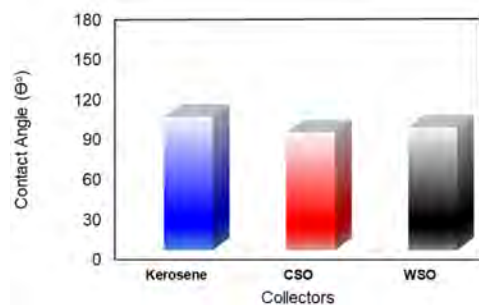


Figure 9. A representation of the contact angles formed by sessile liquid drops (kerosene, CSO and WSO) on the smooth surface of coal.

CONCLUSION

This study shows that using WSO oil in coal slime flotation is applicable, green, efficient, low-cost, and environmentally friendly. The results were evaluated with kerosene and WSO, which have a significant difference between them. Based on the study's findings, WSO effectively lowered the ash content of fine bituminous coal from 33.75% to 6.50%. While WSO can result in clean coal with low ash content, its combustible recovery is lower than that of kerosene. It is most likely due to the WSO's lower surface coating ability than kerosene. In the release test, WSO achieved a clean coal with 10% ash and a combustible recovery of 54%, while kerosene had a higher recovery of 69%. Kerosene also showed greater selectivity, with a product ash of 17.94% compared to 21.73% for WSO after 240 seconds of flotation. The selectivity index for kerosene was 471.65, while WSO had a lower value of 284.80. Overall, WSO's performance was approximately 15% lower than kerosene in all aspects, and it had a 40% lower efficiency index compared to kerosene. This is an expected result, but in the near future, oil reserves will be depleted and mankind will turn to renewable resources.

CONFLICT OF INTEREST

Authors approve that to the best of their knowledge, there is not any conflict of interest or common interest with an institution/organization or a person that may affect the review process of the paper.

AUTHOR CONTRIBUTION

All authors contributed to the study conception and design. Material preparation, data collection and analysis. Dilek Şenol-Arslan: Conceptualization, Methodology, Writing - original draft, Visualization. Hasan Hacifazlıoğlu: Data curation, Investigation, Supervision, Writing - review and editing.

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Thermodynamic Analysis of the Integrated System that Produces Energy by Gradual Expansion from the Waste Heat of the Solid Waste Facility

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ABSTRACT

The rapid increase in consumer societies leads to a rise in waste facilities. Especially when considering the amount of power used in waste plants and the corresponding waste heat generated, an approach to recover waste heat from these facilities has been proposed. Initially, the waste heat from the solid waste facility was assessed using the Rankine cycle. Subsequently, an Organic Rankine Cycle (ORC) system was integrated into the lower cycle of the steam Rankine cycle. The integrated system was completed by harnessing waste heat from the Rankine steam cycle in the carbon dioxide cycle. These power generation systems are designed with two turbines, each with gradual expansion. Using sub-cycles, 1 kg/s of air at 873.2 K was obtained by evaluating the waste heat. In terms of energy efficiency, it can be observed that the R744 gradual expansion cycle exhibits the highest energy and exergy efficiency. Cooling with water in heat exchangers reduces exhaust efficiency. The highest mass flow requirement is found in the ORC system when the R123 fluid is used. The energy efficiency for the entire system was calculated as 22.4%, and the exergy efficiency for the entire system was calculated as 60.7%. When Exergo Environment Analysis was made, exergy stability factor was found to be %60.7, exergetic sustainability index was found to be 2.66. There is also 370K waste heat available, which is recommended for use in drying units. These calculations were performed using the Engineering Equation Solver (EES) program.

Keywords:

Energy; Exergy; Gradual expansion; Waste heat; Exergo environment analysis

INTRODUCTION

Gas turbines are thermal machines commonly used in applications such as power generation or aircraft propulsion. The principle of gradual expansion (stepwise expansion) is a design feature employed to increase efficiency and optimize the performance of gas turbines. In this context, waste gases at high temperatures and pressures, resulting from the operational principles of gas turbines in industrial processes, energy production facilities, and other similar applications, can be repurposed and converted into energy without harming the environment. Thermal energy obtained by recycling waste heat can be used in various ways, such as hot water production, steam generation, or electricity production, thereby enhancing energy efficiency and striving for more effective resource utilization. This article will explore methods for utilizing waste heat from gas turbines, discussing the advantages, challenges, and applica-

tion areas of these methods. Thus, the significance of this innovative approach, which contributes to sustainable energy production, will be emphasized. Published studies in the literature, They realized an integrated Organic Rankine Cycle (ORC) to recover the waste heat of exhaust gases in the Afyon Biogas Power Plant, which produces biogas from chicken manure. They stated that waste heat recovery to the power plant greatly increases the performance parameters and economic cost savings values of the system. They calculated the maximum power capacity of the facility supported by the Organic Rankine Cycle as 4828.8 kW. They calculated the energy and exergy efficiencies as 37.4% and 32.1%, respectively, when the power plant operates under optimum operating conditions [1]. In this article, thermodynamic and thermoeconomic analyzes as well as optimization of the organic Rankine cycle (ORC) were carried

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out. The system was applied to an existing solid waste power plant with an installed power of 5.66 MW in order to generate additional power from exhaust gas. The originality of this article is that they made calculations based on the analysis of the possibility of converting the exhaust gas at 566 °C into electricity using the ORC system in the waste-to-energy concept [2]. They calculated the energetic and exergetic analysis of a multiple generation system consisting of a micro gas turbine, an organic Rankine cycle (ORC), an absorption cooler and a water heater [3]. He aimed to increase the efficiency of systems by using thermodynamic cycles from waste heat sources. The thermodynamic results of increasing the efficiency of the system by adding subcycles of the waste heat of a gas turbine to the designed system were examined [4]. Provides the design, analysis and optimization of a new municipal solid waste fueled combined cycle power plant to meet the grid electricity needs of an urban municipality [5]. They implemented a gas turbine cycle model adopting the organic Rankine cycle (ORC) in which supercritical CO₂ (S-CO₂) was used as the working fluid. Thermodynamic analysis of the system used Aspen Plus and EES programs. As a result of thermodynamic analyses, the electricity production capacity, energy and exergy efficiencies of the proposed system were found

to be 1530.88 kW, 23.30% and 59.60%, respectively [6]. Thermodynamic and thermoeconomic analyzes as well as optimization of the organic Rankine cycle (ORC) were carried out. The system was adapted to an existing solid waste power plant with an installed power of 5.66 MW in order to generate additional power from exhaust gas [7]. They integrated the organic Rankine cycle (ORC) into a 2 MW natural gas engine to generate electricity by recovering the engine's exhaust heat [8]. In their study, they proposed a thermoeconomic optimization study of a vehicle-mounted ORC unit to recover waste heat from various exhaust gas conditions of a vehicle [9]. They have made a detailed comparison of the potential of ORC and S-CO₂ as bottoms of industrial gas turbines in Combined Heat and Power (CHP) system. They stated that the S-CO₂ dip cycle gives better results than ORC in both electrical and thermal efficiency, since the cycle pressure ratio is not affected by the thermal user temperature in the s-CO₂ solution examined [10]. Thermodynamic analysis of the single-stage, single-expansion S-CO₂/ORC system, which operates at the same lower and upper temperatures as the single-stage, double-expansion S-CO₂/ORC system, was examined [11]. They designed an organic Rankine cycle (ORC) waste heat recovery system with an internal heat exchanger (IHE) to recover waste heat from

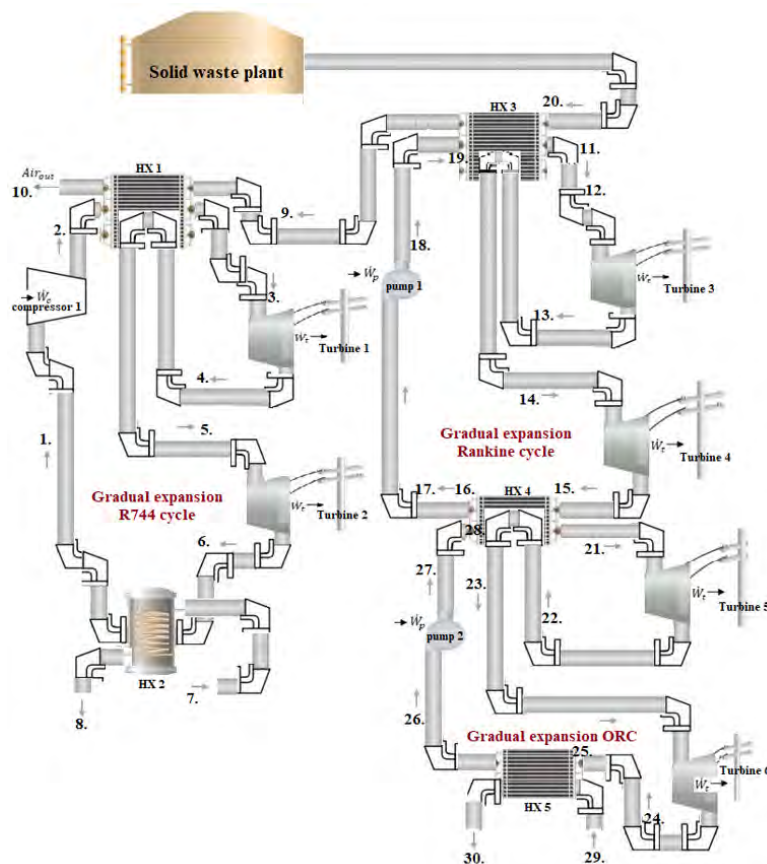


Figure 1. Integrated power generation plant with thermodynamic analysis.

diesel engine exhaust [12]. The main difference between stepwise expansion with reheat (Regenerative Rankine Cycle) and Non-Regenerative Rankine cycle energy cycles is energy recovery. Gradual expansion with reheat improves efficiency by recovering the energy of the steam after expansion and contributes to more electricity production. Stepless expansion, on the other hand, expands without this recovery process and is therefore less energy efficient. Which cycle is preferred depends on the specific requirements and cost factors of the application.

In the design of gradual expansion, the strategy of reheating and raising the fluid's temperature during pressure drops between the blades in gas turbines is employed to enhance thermal efficiency and performance. This process is often referred to as reheat or interstage heating. Consequently, reheating and increasing the fluid's temperature through reheat or intermediate stage heating in gas turbines offer several benefits, including improved thermal efficiency, enhanced performance, a broad operating range, and optimized control. This strategy represents a crucial design method used by engineers to ensure that gas turbines operate with greater effectiveness and efficiency.

MATERIAL AND METHODS

System Description

Fig. 1 shows the schematic view of the integrated power generation facility for which thermodynamic analysis was performed.

In Fig. 1, the waste heat from the solid waste facility was first evaluated in the Rankine cycle. An ORC system has been added to the lower cycle of the steam Rankine cycle. The integrated system was completed by adding the waste heat from the Rankin steam cycle to the carbon dioxide cycle. These power generating systems are designed with two turbines each with gradual expansion.

1. 2→3: Heat transfer from adiabatic and counterflow Heat Exchanger, waste heat transfer to carbon dioxide cycle 9→10 HX-1

2. 3→4: Expanding the adiabatic Turbine-1 to generate work

3. 4→5: Heat transfer from adiabatic and counterflow Heat Exchanger, waste heat to carbon dioxide cycle HX-1

4. 5→6: Reheating the working fluid to Turbine-2 inlet temperature,

5. 6→1: Heat removal by Heat Exchanger as isobar. HX-2

6. 1→2: Increasing the pressure of the with the adiabatic compressor.

7. 18→12: Heat transfer from adiabatic and counterflow Heat Exchanger, waste heat transfer to Rankine cycle 20→9 HX-3

8. 12→13: Expanding the adiabatic Turbine-3 to generate work

9. 13→14: Heat transfer from adiabatic and counterflow Heat Exchanger, waste heat to Rankine cycle HX-4

10. 14→15: Reheating the working fluid to Turbine-4 inlet temperature,

11. 15→17: Heat removal by Heat Exchanger as isobar. HX-4

12. 17→18: Increasing the pressure of the saturated liquid with the adiabatic pump.

13. 27→21: Heat transfer from adiabatic and counterflow Heat Exchanger, waste heat transfer to ORC 24→20 HX-4

14. 12→13: Expanding the adiabatic Turbine-5 to generate work

15. 13→14: Heat transfer from adiabatic and counterflow Heat Exchanger, waste heat to ORC HX-4

16. 14→15: Reheating the working fluid to Turbine-6 inlet temperature,

17. 15→17: Heat removal by Heat Exchanger as isobar. HX-5

18. 17→18: Increasing the pressure of the saturated liquid with the adiabatic pump.

Assumptions for thermodynamic analysis:

Pure substance is used in the system.

All compression processes in the system are adiabatic.

Pressure drops in system components and pipeline as well as heat transfer over the pipeline were also neglected.

All heat exchangers are counter flow. Heat exchanges are identical.

System operates in steady state.

Gravitational potential energy and kinetic energy are not taken into account.

The isentropic efficiency of compressors, pumps and turbines is 90%

The ambient temperature was taken as 293.2 K.

The exhaust exit temperature of the furnace or heating system used in the solid waste facility was taken as 873.2 K [13].

Energy and exergy analyzes

For steady state in thermodynamic analysis, the basic mass balance equation can be given as follows [14-15,16];

$$\sum \dot{m}_{in} = \sum \dot{m}_{ex} \tag{1}$$

where \dot{m} is the mass flow rate, the in and ex indices represent the inlet and outlet states, respectively. The energy balance is given as:

$$\begin{aligned} \dot{Q}_{in} + \dot{W}_{in} + \sum_{in} \dot{m}(h + \frac{v^2}{2} + gz) \\ = \dot{Q}_{ex} + \dot{W}_{ex} + \sum_{ex} \dot{m}(h + \frac{v^2}{2} + gz) \end{aligned} \tag{2}$$

Here, \dot{Q} is the heat transfer rate, \dot{W} is the power, h is the specific enthalpy, v is the velocity, z is the height, and g is the gravitational acceleration. The entropy balance equation for steady-state conditions is written as:

$$\sum_{in} \dot{m}_{in} s_{in} + \sum_k \frac{\dot{Q}_k}{T_k} + \dot{S}_{gen} = \sum_{ex} \dot{m}_{ex} s_{ex} \tag{3}$$

where s is the specific entropy and \dot{S}_{gen} is the entropy generation rate. The exergy balance equation can be written as:

$$\begin{aligned} \sum \dot{m}_{in} ex_{in} + \sum \dot{E}x_{Q,in} + \sum \dot{E}x_{W,in} \\ = \sum \dot{m}_{ex} ex_{ex} + \sum \dot{E}x_{Q,ex} + \sum \dot{E}x_{W,ex} + \dot{E}x_D \end{aligned} \tag{4}$$

The specific flow exergy can be written as:

$$ex = x_{ph} + ex_{ch} + ex_{pt} + ex_{kn} \tag{5}$$

The kinetic and potential parts of the exergy are assumed to be negligible. Also, the chemical exergy is assumed to be negligible. The physical or flow exergy (ex_{ph}) is defined as:

$$ex_{ph} = (h - h_o) - T_o(s - s_o) \tag{6}$$

where h and s represent specific enthalpy and entropy, respectively, in the real case. h_o and s_o are enthalpy and entropy at reference medium states, respectively.

Exergy destruction is equal to specific exergy times mass;

$$E_{xd} = ex * m \tag{8}$$

$\dot{E}x_D$, are work-related exergy ratios and are given as:

$$Ex_D = T_0 \dot{S}_{gen} \tag{9}$$

$\dot{E}x_W$, are work-related exergy ratios and are given as:

$$Ex_W = \dot{W} \tag{10}$$

$\dot{E}x_Q$, are the exergy rates related to heat transfer and are given as below.

$$\dot{E}x_Q = (1 - \frac{T_o}{T}) \dot{Q} \tag{11}$$

$\dot{E}x_{D,syst}$. Exergy destruction in the system;

$$\dot{E}x_{D,syst} = \dot{E}x_{in} + \dot{E}x_{out} \tag{12}$$

What work comes out of the system;

$$\dot{W}_{net\ out} = \dot{Q}_{in} - \dot{Q}_{out} \tag{13}$$

system thermal efficiency (η);

$$\eta = \frac{\text{energy in exit outputs}}{\text{total energy inlets}} \tag{14}$$

The exergy efficiency (ψ) can be defined as follows;

$$\psi = \frac{\text{exergy in exit outputs}}{\text{total exergy inlets}} \tag{15}$$

Exergoenvironmental Analysis

fei shows exergoenvironmental impact factor, $\dot{E}x_{D,tot}$. is total exergy destruction rate, $\dot{E}x_{D,in}$. is input exergy rate [17],

$$fei = \frac{\dot{E}x_{D,tot}}{\dot{E}x_{in}} \tag{16}$$

Cei is exergoenvironmental impact coefficient, ψ_{ex} represents exergy efficiency of the system,

$$Cei = \frac{1}{\psi_{ex} / 100} \tag{17}$$

Φei is exergoenvironmental impact index,

$$\Phi ei = fei \times Cei \tag{18}$$

Φeii represents exergoenvironmental impact improvement,

$$\Phi eii = \frac{1}{\Phi ei} \tag{19}$$

fes is the exergy stability factor,

$$fes = \frac{\dot{E}x_{D,out}}{\dot{E}x_{D,out} + \dot{E}x_{D,tot}} \tag{20}$$

Φest represents exergetic sustainability index.

$$\Phi est = fes \times \Phi eii \tag{21}$$

Table 1. Thermodynamic properties of the positions of the carbon dioxide cycle.

Location	T [K]	s [kJ/kg.K]	P [bar]	h [kJ/kg]	ex[kj/kg]
1.R744	313.2	-1.08	80	-103.6	214.1
2.R744	374.9	-1.072	190	-70.52	244.7
3.R744	460	-0.7164	190	75.99	287
4.R744	428.2	-0.7108	135	54.51	263.9
5.R744	460	-0.6163	135	96.41	278.8
6.R744	412.7	-0.6072	80	62.73	241.8
7.Water inlet	293.2	0.2965	1	84.01	0
8.Water outlet	303.2	0.4374	1	126	0.7042
9.Air inlet	492.2	7.371	1	495.3	47.97
10.Air outlet	370	7.08	1	370.8	8.675
To. R744	293.2	-0.01403	1	-5.168	0

RESULTS AND DISCUSSION

In one study, modeling ORC as a second stage waste heat recovery system after the primary steam cycle, the system efficiency of the steam cycle was found to be 7.63%. With the addition of ORC, this efficiency increased to 7.81% [18]. R123 has a low boiling point temperature (27.82 °C), making it a preferable fluid for aluminum cycles. They calculated the efficiency of the Basic ORC system as 6.15% and the Regenerative ORC system as 7.98% [19]. In a study optimized for reheated S-CO₂ Brayton cycle, thermal efficiency was found to be 15.2–36.3% and 14.8–35.6% [20]. In examining the Exergo Environmental Analysis, they found the exergy stability factor to be 60% and the exergetic sustainability index to be 2.62.

Thermodynamic properties of the positions of the carbon dioxide cycle are presented in Table 1.

Comparison between regenerative reheat cycle and non-regenerative non-reheat cycle is provided in Fig. 3.

Table 2 compares the thermodynamic results of the system operating with reheating and gradual expansion in the case of stepless and non-reheating operation.

Considering the carbon dioxide cycle, in case of switching from the reheated gradual expansion cycle to the conventional cycle, there will be a 71.4% decrease in exergy efficiency and a 32.5% decrease in energy efficiency. Additionally, the mass flow rate of carbon dioxide will increase by 3.7%, while the mass flow rate of water required for cooling will also increase by 4.3%.

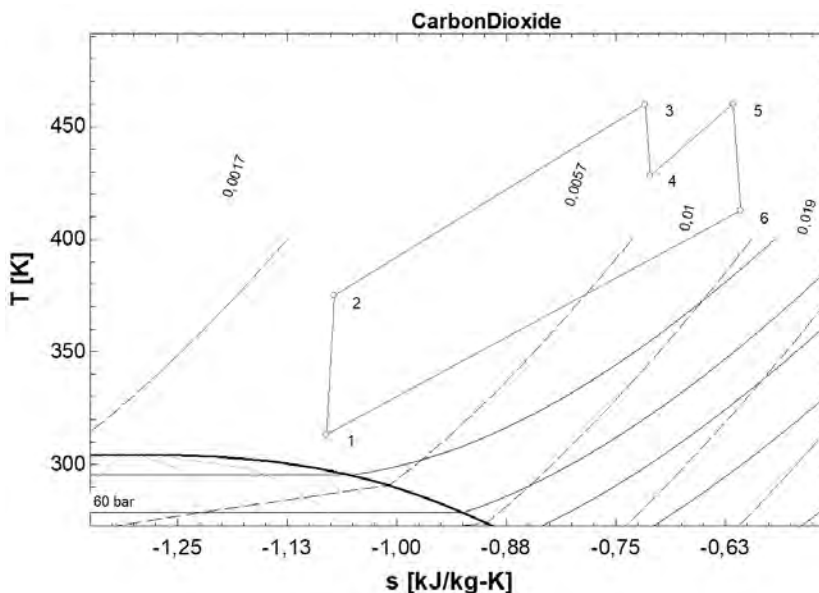


Figure 2. The temperature entropy diagram for the R744 gradual expansion.

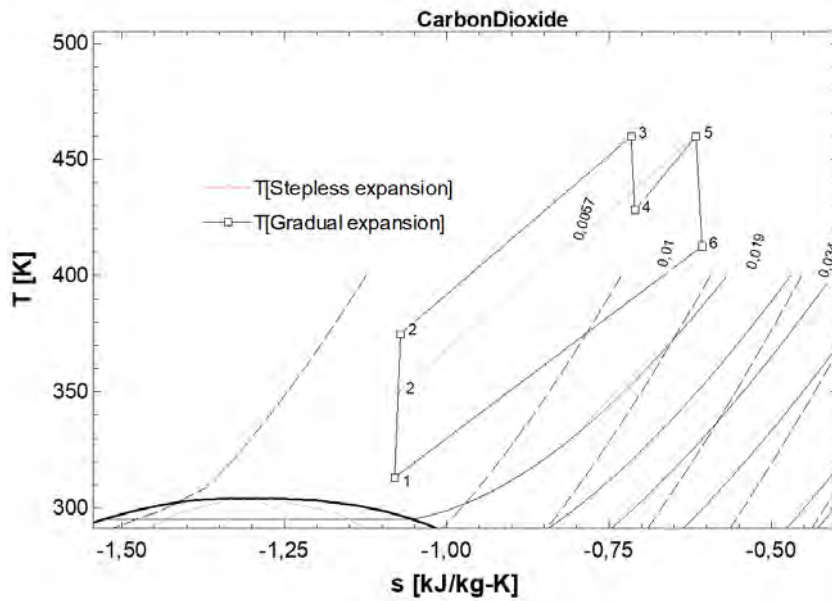


Figure 3. Comparison of regenerative and non-regenerative cycles for carbon dioxide as the working fluid.

Table 2. Thermodynamic consequences of gradual and stepless expansion.

location	R744 Cycle gradual expansion	location	R744 Cycle stepless expansion
Q in [9-10]	124,5 kW	Q in [9-10]	124,5 kW
R744exergy	78,96 %	R744exergy	22,6 %
R744energy	24,9 %	R744energy	16,8 %
Ex comp1	1,71 kW	Ex comp1	1,062 kW
Ex Turb.1	1,08 kW	Ex Turb.1	1,83 kW
Ex Turb.2	1,76 kW	Ex Turb.2	-----
Ex HX1	1,889 kW	Ex HX1	7,036 kW
Ex HX2	20,12 kW	Ex HX2	20,86 kW
HX1	95,19 %	HX1	82,1 %
HX2	10,08 %	HX2	10,03 %
comp1 [1-2]	92,17 %	comp1 [1-2]	91,62 %
Turb.1 [3-4]	92,92 %	Turb.1 [3-4]	92,6 %
Turb.2 [5-6]	92,66 %	Turb.2 [5-6]	-----
m R744	0,6608 kg/s	m R744	0,6857 kg/s
Wcomp.1 [1-2]	21,88 kW	Wcomp.1 [1-2]	1,68 kW
WTurb.1 [3-4]	14,19 kW	WTurb.1 [3-4]	23,09 kW
WTurb.2 [5-6]	22,25 kW	WTurb.2 [5-6]	-----
Q out [1-6]	109,9 kW	Q out [1-4]	114,1 kW
m su	2,616 kg/s	m su [2,728 kg/s

Table 3. Thermodynamic properties of the positions of the Rankine cycle.

Location	T [K]	s [kJ/kg.K]	P [bar]	h [kJ/kg]	ex[kj/kg]
11. water	443.5	6.662	7.989	2768	817.8
12. water	505.5	6.966	7.989	2912	872.6
13. water	452.3	6.991	4.738	2812	765.4
14. water	505.5	7.227	4.738	2925	809.1
15. water	395.5	7.287	1.487	2716	582.9
16. water	384.2	7.226	1.487	2693	577
17. water	384.2	1.431	1.487	466	49.42
18. water	384.3	1.431	7.989	466.8	50.13
19. water	443.5	2.045	7.989	720.6	123.9
To.water	293.2	6.846	1	293.4	0
20. Air inlet	873.2	7.982	1	903.4	276.7
9. Air outlet	492.2	7.371	1	495.3	47.94

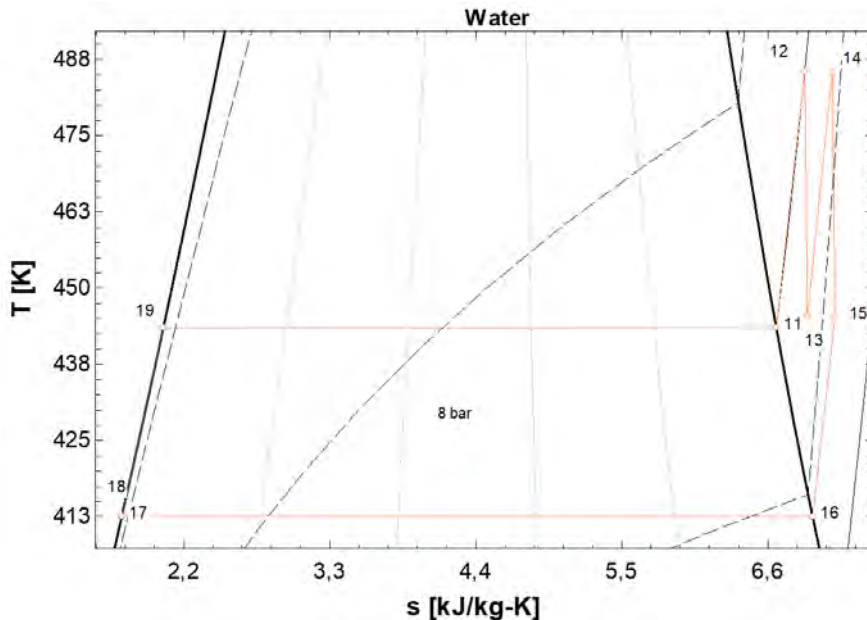


Figure 4. The temperature entropy diagram for the Rankine gradual expansion.

Table 3 gives the thermodynamic values of the positions in the Rankine cycle for Figure 4.

Table 4 gives the thermodynamic properties of the ORC positions.

The temperature entropy diagram for the ORC gradual expansion is given in Fig. 5.

In Table 5, the thermodynamic results of all subcomponents are shown for both the R744 gradual expansion transcritical cycle, the steam gradual expansion Rankine cycle, and the ORC gradual expansion for R123 refrigerant; Heat

exchange, energy and exergy analysis of system components, amount of fluid used in the system, power produced in the cycles and power consumed are calculated and presented separately.

The results were obtained by evaluating 1 kg/s air waste heat at 873.2 K with sub-cycles. In terms of energy efficiency, it is seen that the R744 gradual expansion has the highest energy and exergy efficiency. Cooling with water in heat exchangers reduces the exhaust efficiency. The mass flow requirement is highest in ORC, where R123 fluid is used. The energy efficiency for the entire system was calculated as 22.4% and the exergy efficiency for the entire system was

Table 4. Thermodynamic properties of ORC positions.

Location	T [K]	s [kJ/kg.K]	P [bar]	h [kJ/kg]	ex[kj/kg]
21. R123	363.2	1.689	6.259	436.9	35.53
22. R123	348.9	1.691	3.904	429.7	27.61
23. R123	363.2	1.724	3.904	441.4	29.75
24. R123	338.9	1.729	1.549	426.5	13.38
25. R123	313.2	1.67	1.549	407.2	11.34
26. R123	313.2	1.143	1.549	241.9	0.7897
27. R123	313.4	1.143	6.259	242.3	1.123
28. R123	363.2	1.304	6.259	297	8.599
To. R123	293.2	1.074	1	221.1	0
29. Water inlet	293.2	0.2972	1	84.22	0
30. Water outlet	303.2	1.074	1	221.1	0.7042

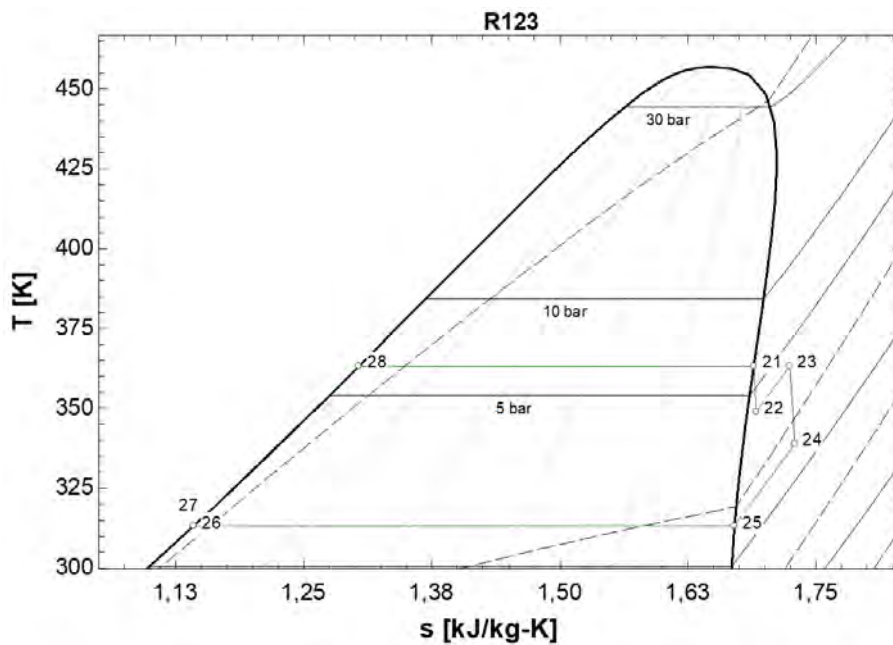


Figure 5. Temperature entropy diagram for ORC.

calculated as 60.7%. ϕ_{ei} shows exergoenvironmental impact factor (0.138) is total exergy destruction rate, (37.049 kW) is input exergy rate (268.02 kW), C_{ei} is exergoenvironmental impact coefficient (1.64), ψ_{ex} represents exergy efficiency of the system (60.7), Φ_{ei} is exergoenvironmental impact index (0.227), Φ_{eii} represents exergoenvironmental impact improvement (4.39), ϕ_{es} is the exergy stability factor (60.7), Φ_{est} represents exergetic sustainability index (2.66). When Exergo Environment Analysis was made, exergy stability factor was found to be %60.7, exergetic sustainability index was found to be 2.66. There is also 370 K waste heat. It is recommended to use a temperature of 370 K for drying units. Since carbon dioxide has a higher heat conduction coefficient than water, it accelerates heat transfer. At the same time,

carbon dioxide has a lower viscosity than water, which allows the fluid to move more easily within the heat exchanger and reduces energy losses. The study results reveal compatible results when compared to other literature studies. The focus of this study will make a significant contribution towards increasing the usability of gradual expansion.

CONCLUSION

The rapid increase in consumer societies means an increase in waste facilities. Processing these waste products in facilities brings with it high energy costs. The gas turbines used in these facilities have serious waste heat. In this study, a thermodynamic proposal has been

Table 5. Thermodynamic results of all subcomponents.

location	H ₂ O Cycle	location	R123 Cycle	location	R744 Cycle
Q_{in}^{heat} [9-20]	408.1 kW	Q_{in}^{heat} [15-17]	358.9 kW	Q_{in}^{heat} [9-10]	124.5 kW
ψ H ₂ Oexergy	4.3 %	ψ R123exergy	7.3 %	ψ R744exergy	78.96 %
η H ₂ Oenergy	12 %	η R123energy	10.73 %	η R744energy	24.9 %
Ex pump.1	0.01 kW	Ex pump.2	0.06 kW	Ex comp1	1.71 kW
Ex Turb.3	1.15 kW	Ex Turb.5	1.17 kW	Ex Turb.1	1.08 kW
Ex Turb.4	2.78 kW	Ex Turb.6	2.49 kW	Ex Turb.2	1.76 kW
Ex HX3	90.6 kW	Ex HX4	21.52 kW	Ex HX1	1.889 kW
Ex HX4	21.52 kW	Ex HX5	26.67 kW	Ex HX2	20.12 kW
ϕ HX3	60.39 %	ϕ HX4	74.7 %	ϕ HX1	95.19 %
ϕ HX4	74.7 %	ϕ HX5	25.1 %	ϕ HX2	10.08 %
ϕ pump.1 [17-18]	92.37 %	ϕ pump.2 [26-27]	90.68 %	ϕ comp1 [1-2]	92.17 %
ϕ Turbine.3 [12-13]	93.25 %	ϕ Turbine.5 [21-22]	91.5 %	ϕ Turbine.1 [3-4]	92.92 %
ϕ Turbine.4 [14-15]	92.29 %	ϕ Turbine.6 [23-24]	91.26 %	ϕ Turbine.2 [5-6]	92.66 %
m water	0.1595 kg/s	m R123	1.739 kg/s	m R744	0.6608 kg/s
Wpump.1 [17-18]	0.1213 kW	Wpump.2 [26-27]	0.6402 kW	Wcompressor.1 [1-2]	21.88 kW
WTurb.3 [12-13]	15.93 kW	WTurb.5 [21-22]	12.61 kW	WTurb.1 [3-4]	14.19 kW
WTurb.4 [14-15]	33.31 kW	WTurb.6 [23-24]	25.98 kW	WTurb.2 [5-6]	22.25 kW
Q_{in}^{heat} [15-17]	358.9 kW	Q_{in}^{heat} [24-26]	321 kW	Q_{in}^{heat} [1-6]	109.9 kW
m air [20-10]	1 kg/s	m water [29-30]	7.676 kg/s	m water [7-8]	2.616 kg/s

put forward on how to reduce this waste heat into useful energy. Carbon dioxide's higher heat conduction coefficient accelerates heat transfer, while its lower viscosity allows for easier fluid movement within the heat exchanger, reducing energy losses. In terms of energy efficiency, it is seen that the R744 transcritical gradual expansion has the highest energy and exergy efficiency. Water cooling in heat exchangers reduces exergy efficiency. Since the cooling water has a low temperature, the temperature difference is high. This can increase heat transfer efficiency and improve exergy efficiency. The mass flow requirement is highest in ORC, where R123 fluid is used. The energy efficiency for the entire system was calculated as 22.4% and the exergy efficiency for the entire system was calculated as 60.7%. When Exergo Environment Analysis was made, exergy stability factor was found to be %60.7, exergetic sustainability index was found to be 2.66. It is recommended to use a temperature of 370 K for drying units. The study results reveal compatible results when compared to other literature studies.

As a result, reheating and increasing the temperature of the fluid using reheat or intermediate stage heating in gas turbines will provide a number of benefits such as increasing thermal efficiency, improving performance, having a wide operating range and optimizing control. This strategy

will be an important design method used by engineers to ensure efficient operation of the facility with systems integrated into waste facilities.

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CONFLICT OF INTEREST

Authors approve that to the best of their knowledge, there is not any conflict of interest or common interest with an institution/organization or a person that may affect the review process of the paper.

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