

Adsorption Of Methylene Blue from Aqueous Solution with Sulfuric Acid Activated Corn Cobs: Equilibrium, Kinetics, and Thermodynamics Assessment

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ABSTRACT

Three adsorbents with different characteristics were produced in this study by activation of sulfuric acid with different concentrations, from corn (*Zea mays* L.) cobs, which is an agricultural waste by-product resulting from harvesting. After characterization by the parameters such as Boehm titration, determination of pH-pHpzc, and methylene blue – iodine number, and IR analysis, their methylene blue adsorption potentials from aqueous medium were investigated based on equilibrium, kinetics, and thermodynamics evaluations. This study aims to examine the effects of relatively dilute and concentrated acids on the activation process and to gain an economic value to waste materials through the production of a new adsorbent. It was observed that the initial solution pH did not have a significant effect on the adsorption efficiency. The adsorption process reached the equilibrium at the end of the first 120 minutes, and the kinetic data fit the pseudo-second-order kinetic model. Langmuir adsorption capacity (295.5 mg/g) of the adsorbent produced by activating with 50% sulfuric acid was found higher than those produced with 75% and 98% acids. An increase in ambient temperature effected the adsorption positively. As a result, in this study, very low-cost adsorbents were produced from the waste by-product corn cobs, and a new approach was proposed for cleaning wastewater containing dyestuffs.

Keywords:

Adsorption; Corn cobs; Methylene blue; Removal; Sulfuric acid activation

INTRODUCTION

Natural waters are getting more and more polluted due to the activities of many industry organizations such as juice, coffee, and cereal processing plants. The contamination of the water used for drinking and other purposes by partially treated or untreated discharges from chemical industries, petrochemical industries, oil refineries, oil spills, rolling steel mills, unrefined domestic sludge, and pesticide runoff threaten both human health and environmental health [1]. Dyestuffs, one of many different types of contaminants, are among the chemicals that pose this threat. Synthetic dyestuffs are widely used worldwide in textile staining processes. Synthetic dyestuff classes are the azo type, including reactive, disperse, and acid dyes. Azo dyes account for 65% of the total dye production in the world [2]. Today, biological treatment is the most widely used method to decompose dye waste. However, this process is not very successful in removing dyes effectively. For this reason, dyes

are often found chemically unchanged in the waters of wastewater treatment plants; and they can both contaminate drinking water and cause potential aquatic toxicity by condensation in sludge.

In the textile industry, about 1 m³ (1000 mL) of water is required for every 1 ton (1000 kg) of clothes to be stained. The discharge of wastes of these processes into rivers and lakes can have toxic effects on aquatic life. Color impedes the penetration of light into the water and thus impedes the growth of biota by retarding photosynthetic activity. It also chelates metal ions in the water, causing micro-toxicity for aquatic life [3]. It should be borne in mind that even 1.0 mg/L concentration of any dye in drinking water can impart a significant amount of color making it highly unsuitable for human consumption. Most of the dyes used in industrial applications are very stable against photo-degradation, biodegradation and oxidizing agents. Today, several physi-

Article History:

Received: 2020/09/02

Accepted: 2020/09/17

Online: 2020/09/30

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cal and chemical processes are used to treat wastewater. However, many of these processes are expensive and cannot be used effectively to treat a wide variety of dye effluents [4,5].

Activated carbon-based industrial processes are the most widely used methodologies as they have excellent removal efficiency for dyes and of course many other types of contaminants, but the use of these processes is often limited due to the high cost of commercial activated carbons and high energy-process [6]. Therefore, it is inevitable to develop new adsorption-based technologies that can be a powerful alternative to activated carbon-based ones. Number of alternative methods are increasing day by day to reduce costs and also increase efficiency, or at least to compete with other methodologies. For this purpose, studies on lignocellulosic agricultural wastes or by-products are available in the literature. These agricultural wastes can be used inexpensively as a direct adsorbent or by converting into activated carbons or by activating with various agents to improve their adsorption capabilities. This type of agricultural waste by-products can be easily obtained from many industrial establishments, or farming peasants at very low costs.

Hundreds of agricultural-based waste by-products such as corn cob, barley straw [7], carrot waste [8], alder sawdust [9], rice husks, olive pomace, orange waste [10], Kiwicumcumber-potato peel [11], sago waste [12], coffee husk [13], peanut shells [14], rice husk waste, coconut shell [15], hazelnut husk [16], and tea-industry waste [17] are used either directly or by converting into activated carbons to remove various pollutants from aqueous medium. In this way, very low cost and high-performance adsorbents can be obtained from these by-products with no economic value.

In this study, three different adsorbents were produced from corn cobs (CCs) by chemical activation using the different concentrations of sulfuric acid. CCs is a waste by-product after processing of the maize plant (*Zea Mays* L.) cultivated in almost every region of Turkey as well as all over the world. In the 2018/2019 period, approximately 5.7 million tons of corn were produced in Turkey [18]. Significant amounts of waste CCs are released from these products. There is no document that these wastes are used in any area.

The potential of these adsorbents to remove methylene blue (MB), a basic cationic dyestuff, from aqueous solution was investigated in this study. MB is one of the most used dyestuffs in the medical field, but also in dyeing wool, wood, paper, silk and leather, painting, and ink dyes. However, MB may cause some harmful effects on human health. A person exposed to MB may experience heart palpitations, vomiting, shock, cyanosis, known as blue disease, jaundice, arm, and leg paralysis, and tissue gangrene [19–21]. MB is very sensitive to heat. When left at 110 °C for 2 hours, it emits a bad odor

and loses about 14% mass. Anhydrous MB is 94.5% pure and creates foam in aqueous solution [22]. Besides, MB, which has a maximum absorption wavelength of 668 nm, is widely used as a model adsorbate to test the adsorption capacity of the relevant adsorbent or the degradation potential of any TiO₂ film [23,24]. Also, one of the characterization steps of a newly produced adsorbent is of course determination of MB number as well as I₂ number.

In a study in the literature, although it was reported that a new adsorbent was obtained from CCs by activating with concentrated sulfuric acid [25], three different adsorbents were obtained by using different concentrations of sulfuric acid in this study. Relatively dilute acids dissociate more than concentrated acids. Therefore, the adsorbent obtained by activating with relatively dilute acid is expected to have richer surface functional groups. The primary aim of this study is to prove that the adsorbents produced by changing the concentration of sulfuric acid used for activation of CCs have different adsorption capabilities and that dilute acids perform better than concentrated ones. In other words, this study aims to monitor the development and reorganization of adsorption sites on the adsorbent surface containing functional groups and to reveal the adsorption capabilities of the adsorbents produced by changing the concentration of the activation agent. Since we do not find such a study in the literature, we think that this work is original, and the novelty is high. New adsorbents have been produced from CCs, which are an agricultural waste by-product, at almost zero cost, thereby gaining an economic value for such a worthless material. Besides, we believe that this study is very valuable as it is expected that these adsorbents will contribute to the prevention of environmental water pollution.

MATERIAL AND METHOD

Chemicals, Solutions and Matter-Materials Used

All chemicals used in the experimental stages were of analytical purity and were purchased from Merck (Darmstadt, Germany). Ultra-pure water was used in all experiments. Methylene blue (MB) used as an adsorbate in adsorption tests is a basic cationic dye. Other known names of MB, whose empirical Eq. and molar mass are C₁₆H₁₈ClN₃S and 319.85 g/mol, respectively, are methylothioninium chloride, CI 52015, and basic blue 9 [26]. Its molecular structure is shown in Fig. 1.

The appropriate amount of MB was weighed and dissolved in water, and its stock solution of 2500 mg/L was prepared. The six consecutive solutions of 50, 100, 250, 500, 750 and 1000 mg/L were prepared from this stock solution by diluting. Capped PP Falcon tubes of 15- and 50-mL volumes were used in the adsorption tests.

A vacuum filtration system (Isolab, GmbH) was used to separate the adsorbate molecules (MB) and adsorbent particles (CCs-SA) from each other. In this setup, the nitrocellulose membrane (Sartorius Stedim Biotech, France) with a pore size of 0.45 μm was used as a filter paper.

Devices Used

In this study, MB concentrations were determined in a Unicam UV-2 model Spectrophotometer device. Adsorption tests were made with a mechanical shaker (Edmund Bühler GmbH), pH adjustments were made with a Hanna pH-211 model benchtop pH meter (Hanna Inst., USA) and substance weighing was done with a BP1106 model analytical balance (Sartorius Stedim Biotech, France). The IR spectra of the adsorbents were obtained from a Perkin Elmer 1600 FT-IR spectrophotometer (4000–400 cm^{-1}) device.

Preparation of the Adsorbents:

The corn cobs (CCs) were obtained from Akçaabat district of Trabzon province-Turkey. After separating the grains, the remaining CCs were dried in an oven at 105 $^{\circ}\text{C}$ for 24 hours and stored in a desiccator. The dried CCs wastes were used after being milled and sieved to a size of approximately 4 mm.

20 g of CCs were taken and 20 g of H_2SO_4 solutions of three different concentrations (98%, 75% and 50% by weight) were added separately (mixing ratio 1:1). After mixing the mixtures thoroughly, they were kept in the oven at 200 $^{\circ}\text{C}$ for 24 hours. The activated adsorbents were first washed thoroughly with boiling distilled water to remove acid residues and then neutralized by treatment with a 1% NaHCO_3 solution for 24 hours. After the adsorbents were filtered, they were washed again with ultrapure water and finally they were used after drying in the oven at 105 $^{\circ}\text{C}$ for 24 hours [27]. The three different adsorbents obtained were coded as CCs-SA₅₀, CCs-SA₇₅, and CCs-SA₉₈.

Characterization of the Adsorbents:

Analysis of The Surface Acidic Functional Groups (SAFG) of The Adsorbents

The surface acidic functional groups of the adsorbents are mainly examined in three groups as carboxylic, lactic and phenolic. The amounts of these groups in mmol can be determined by Boehm Titration. With 0.05 g adsorbent, 0.1 N 50 mL NaOH, NaHCO_3 and Na_2CO_3 solutions were treated separately for 24 hours. At the end of the process, after the samples were filtered through the cellulose nitrate membrane with pores 0.45 μm in size, the filtrates were titrated with 0.1 N HCl [28].

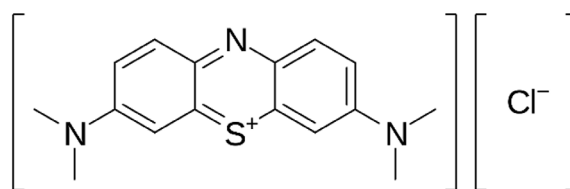


Figure 1. Molecular structure of methylene blue.

Total surface acidic groups (lactic, phenolic and carboxylic) are all determined by NaOH-neutralization. Lactic and carboxylic groups are determined by Na_2CO_3 -neutralization, and only carboxylic groups by NaHCO_3 -neutralization [29].

The amount of surface acidic functional groups in mmol is calculated by the following Eq. 1:

$$SAFG = \frac{[N \times (T_b - T) \times 2.5]}{m} \quad (1)$$

where SAFG means surface acidic functional groups (mmol/g). N is the normality of the titrant solution (HCl). T_b is the titrant consumption (mL) for blank experiments. T represents the titrant consumption (mL) for the different solutions, and m is the amount of adsorbent (g).

pH and pH_{pzc} Values of The Adsorbents

The pH values of the adsorbents were determined by measuring the filtrate with a pH meter after treating the 0.05 g adsorbent with 10 mL ultrapure water heated to boiling point for 24 hours [30].

The pH of an adsorbent at the neutral charge point (pH_{pzc} , pH of point of zero charge) or at the isoelectric point means the pH value at the point where the net charge on the surface of adsorbent is zero. If $\text{pH} > \text{pH}_{\text{pzc}}$, adsorption of cationic species on the adsorbent is more suitable. In the case of $\text{pH} < \text{pH}_{\text{pzc}}$, on the contrary, adsorption of anionic species is more suitable. Knowing the pH_{pzc} value, an appropriate value of the solution pH can be estimated for the adsorption of cationic or anionic species without the need for a wide pH scan. Below pH_{pzc} , the net charge on the surface of an adsorbent is positive and above it is negative.

For the determination of pH_{pzc} values of the adsorbents, a series of 0.1 M NaCl solutions in which their initial pH values were adjusted between 2.0 and 10.0 with 0.1 M NaOH or 0.1 M HNO_3 were treated with 0.1 g of the adsorbent for 24 hours. At the end of the process, after the adsorbent and solution were separated by filtration, the equilibrium pH values of the filtrates were measured with a pH meter. A graph was drawn by subtracting the equilibrium pH values from the initial pH values and placing them on the y-axis (ΔpH) and the initial pH values on the x-axis. The point where the graph cuts the x-axis from the value where y is zero was recorded as pH_{pzc} [31,32].

Methylene blue and Iodine Numbers of The Adsorbents

The methylene blue number (MBn) is a measure of the ability of an adsorbent to adsorb large molecules. This test is one of the most important tests that characterize activated carbons. To find MBn in this study, 10 mL of 1000 mg/L MB solution and 0.02 g of each adsorbent were treated for 12 hours. After the mixture was filtered through a 0.45 μm nitrocellulose membrane, the MB concentration remaining without adsorbed in the filtrate was determined by UV-Vis spectrophotometer. Then, the quantity of MB adsorbed per gram adsorbent (mg/g) was calculated with the help of Eq. 2 below [22].

$$MB_n = \frac{(C_o - C_e)}{m} x V \quad (2)$$

where MBn, it means methylene blue number. C_o and C_e are the initial and equilibrium methylene blue concentrations (mg/L), respectively. V is the solution volume (mL) and m is the adsorbent mass (g).

Iodine (I_2) is a much smaller molecule compared to MB. The high number of I_2 gives important information about the adsorbents' ability to adsorb small atoms or molecules such as metal ions [33]. The increase in surface area, porosity and active groups is a factor that increases I_2 adsorption. The following procedure was used to determine the I_2 number of the adsorbents:

0.2 g of the adsorbent was weighed into a 50 mL pp Falcon tube. 40 mL 0.1 N standard iodine solution (12.7 g I_2 and 19.1 g KI dissolved in 1 L water in total) was added and carefully shaken for 30 \pm 1 h. After the mixture was filtered, the amount of unadsorbed iodine in the solution was titrated with a 0.1 N standard sodium thiosulfate solution. A new 40 mL iodine solution was taken, and the consumption was recorded as a blank by titrating with 0.1 N standard sodium thiosulfate solution without adding the adsorbent and shaking [34]. The I_2 numbers of the adsorbents were calculated by the following equations (Eq.s 3, 4 and 5):

$$I_2 \text{ number (mg / g)} = FxC \quad (3)$$

$$F = \frac{126.93xN_{I_2}xV_f}{mxV_k} \quad (4)$$

$$C = V_k - V_t \quad (5)$$

where N_{I_2} refers to the normality of the standard iodine solution. V_f and V_k mean the filtrate volume (mL) and the standard thiosulfate consumption (mL) for the samples, respectively. m is the adsorbent mass (g).

IR analysis of the adsorbents

Infrared spectrometry (IR) is a frequently used method to illuminate the chemical structures and surface groups

of various adsorbents. In this study, IR spectra were taken by FT-IR (Fourier Transform–Infra-Red) spectrometry for CCs, CCs-SA₅₀, MB loaded CCs-SA₅₀ and MB, and the changes occurring before and after adsorption were examined.

Approximately 10 mg of the well-dried adsorbents were taken into the chamber of the device and IR spectra were taken directly.

Adsorption Tests

In this study, three different adsorbents were obtained by activating the corn cob with sulfuric acid at different concentrations. The adsorption performance of a total of four adsorbents from aqueous solution together with the original corn cob was tested. As the adsorbate, methylene blue (MB), a basic cationic dye, was used to represent the total dyes in the adsorption studies.

0.050 g of the adsorbents were weighed and mixed with 10 mL of 6 different MB solutions between 50-1000 mg/L and treated separately until equilibrium was reached. Then, adsorbent particles and adsorbate molecules were separated from each other with the help of a vacuum filtration device. The concentrations of MB remaining in the filtrate were determined at 668 nm in a UV-Vis spectrophotometer in the mg/L concentration unit. The results were then converted to mg/g by Eq. 6 and % by Eq. 7.

$$Q_e \text{ (mg / g)} = \frac{C_o - C_e}{m} x V \quad (6)$$

$$Q_e \text{ (%) } = \frac{C_o - C_e}{C_o} x 100 \quad (7)$$

where Q_e (mg/g) and Q_e (%) mean the amount of MB molecules adsorbed on the adsorbent at equilibrium. C_o and C_e represent the initial and equilibrium MB concentrations (mg/L), respectively. m is the adsorbent mass (g).

RESULTS AND DISCUSSION

Characterization Results

The results obtained by Boehm titration applied to determine the surface functional groups of the adsorbents are given in Table 1. The table contains quantitative values of the carboxylic, phenolic and lactonic groups of the adsorbents in mmol, and as can be seen, the adsorbents have very rich surface groups. When the surface acidic groups of all adsorbents are compared with each other, CCs-SA₅₀ is the richest adsorbent in total acidic groups. That is, as the concentration of H_2SO_4 used in production increases, the total amount of surface functional groups decreases (Table 1). Due to the greater dissociation of acids in dilu-

te solutions, an increase in the number of active groups bonded on the adsorbents may occur.

When acidic groups are evaluated separately, the richest adsorbent in terms of carboxylic groups is the original CCs. It can be said that some of the carboxyl groups may be degraded during the activation of MK with sulfuric acid at high temperature. On the other hand, CCs are the poorest adsorbent in terms of phenolic and lactonic groups. During the activation with sulfuric acid at high temperature, phenolic and lactonic based new structures are formed on the adsorbents. Besides, depending on the degree of dissociation, large amounts of phenolic and lactonic groups are formed on the CCs-SA₅₀ surface. As a result, it is understood that during the activation of the original CCs with sulfuric acid, the new adsorbents in which their surface groups are highly variable and rich are formed.

Another remarkable result in this study is that although the starting material (CCs) and activating agent (H₂SO₄) are the same, only by changing the percentage concentration of the activating agent, adsorbents with quite different surface characteristics can be produced. Therefore, it is possible to produce adsorbents with very different characteristics according to the purpose.

The results found by calculating the pH and pH_{pzc} values of the adsorbents are given in Table 2 and the relevant graphics in Fig. 2. From the table, an increase is observed in the pH values of the adsorbents obtained with increasing sulfuric acid concentration. This result supports the SAFG analysis results (Table 2). Since the adsorbent with richer surface acidic groups (CCs-SA₅₀) will release more protons in its extraction with water, the pH value of the relevant adsorbent will be lower. The opposite of this situation is generally observed at pH_{pzc} values. Since more base will be required to neutralize the surface of the adsorbent with richer surface acidic groups, the corresponding adsorbent will generally have a higher pH_{pzc} value.

Table 1. Quantitative levels of surface acidic functional groups of adsorbents determined by Boehm titration

Adsorbent	Surface acidic groups (mmol/g)			
	Total	Carboxylic	Phenolic	Lactonic
CCs	2.43	1.75	0.35	0.32
CCs-SA ₅₀	6.18	1.60	3.20	1.38
CCs-SA ₇₅	5.23	1.63	2.75	0.85
CCs-SA ₉₈	4.15	1.05	1.75	1.35

CCs: Original Corn Cobs
 CCs-SA50: The adsorbent obtained by activation of 50% H2SO4
 CCs-SA75: The adsorbent obtained by activation of 75% H2SO4
 CCs-SA98: The adsorbent obtained by activation of 98% H2SO4

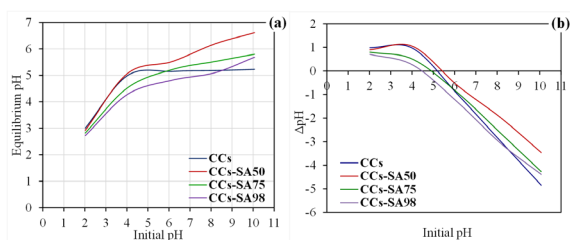


Figure 2. Determination of pH_{pzc} values: (a) Equilibrium pH vs initial pH graph, (b) Initial pH vs ΔpH graph

Comparing the differences between the initial and equilibrium pH values from the graph (Fig. 2(a)), positive differences were observed at low pH values, while negative differences were generally observed at high pH values. Since no buffer is used when adjusting the initial pH of NaCl solutions, the surface groups of the adsorbents can easily interact with the H⁺ and OH⁻ ions in the solution. While H⁺ ions pass from solution to adsorbent at low pH values, OH⁻ transitions occur at high pH values.

Table 3 shows the I₂ and MB numbers of the adsorbents. Looking at the table, it is seen that CCs-SA₅₀ has the highest number of I₂ and MB. Not only porosity but also rich functional groups contribute to the adsorption of large molecule structures. Also, the adsorption of large organic molecules on various adsorbents does not only occur with electrostatic interactions as with small metal ions, besides, but there are also relatively stronger bonds via π-π interactions. I₂ is a small molecule, and the high number of I₂ indicates the affinity of the adsorbent for small ion or molecules such as metal ions. As seen in this study, I₂ numbers are higher than MB numbers. That is, the surface and pore structures of the respective adsorbents may be more favorable for the adsorption of small molecules or ions. However, additional experiments are required to support this result.

The IR spectra taken to determine the types of surface functional groups of adsorbents are shown in Figs. 3 and 4. A comparison is made by taking spectra both before and after adsorption.

Fig. 3(a) shows the IR spectrum for CCs, the starting material used to produce the adsorbents. A slightly flat peak that appears at 3329 cm⁻¹ is caused by both moisture and hydroxyl (-OH) groups present in the sample. Hydroxyl

Table 2. pH and pH_{pzc} values of the adsorbents

Adsorbent	pH	pH _{pzc}
CCs	5.30	5.20
CCs-SA ₅₀	5.58	5.42
CCs-SA ₇₅	5.72	4.90
CCs-SA ₉₈	6.26	4.46

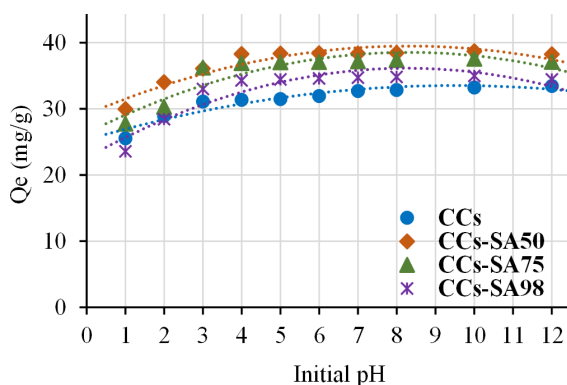


Figure 5. The effect of the initial pH on removal of MB from aqueous solution by CCs and CCs-SA (Co: 250 mg/L, adsorbent amount: 5.0 g/L, agitation time: 4.0 hours, temperature: 25 °C)

When the performances of the adsorbents are compared with each other, it is seen that the CCs-SA₅₀ coded adsorbent obtained with 50% sulfuric acid has a slightly higher performance. This difference will become more pronounced as the concentration of MB increases.

The MB adsorption performance of CCs used directly after being milled without activating with any agent is lower than the other adsorbents. The most important point to be evaluated here is that adsorbent produced with the lowest concentration of sulfuric acid has shown the highest performance. As it is known, strong acids such as sulfuric acid need an aqueous medium to bring out their acidity strength. If there is enough water (or any solvent in which acid can easily release its protons), acids can easily dissociate by donating protons. Since there is relatively more solvent in 50% sulfuric acid, sulfuric acid will certainly dissociate more easily. Concentrated acids are therefore considered to be difficult to dissociate.

In the light of the results obtained, it is seen that pH does not affect much the adsorption efficiency and the optimum pH range is approximately in the range of 4–10. pH is the main factor that controls the electrostatic interactions between the adsorbate and the adsorbent. When the solution pH reaches pH_{pzc} , the net surface charge of the adsorbent will be zero. The pH_{pzc} values of the adsorbents from Table 2 range from 4.46 to 5.42. Although the MB solution is acidic at these pH values, the surface of the adsorbents is neutral. The net charge of the adsorbent surface just above the pH_{pzc} value is negative, but the MB solution is still acidic. Therefore, at these pH values, strong electrostatic interactions will occur between MB, a cationic dye, and the adsorbent surface.

Not only electrostatic interactions occur between large organic molecules such as MB and the respective adsorbent surface, but also strong π - π interactions between the aromatic rings in the organic molecules and the C skeleton of the adsorbent. Besides, non-electrostatic partial H bonds

contribute the adsorption. These interactions are much stronger than electrostatic ones and are almost independent of pH.

Since the original pH values of MB solutions are between about 4.0–6.0, no pH adjustment was required in this study.

There are studies in the literature reporting that pH has little effect on MB adsorption on various adsorbents.

Effect of Contact Time on MB Adsorption Efficiency and Adsorption Kinetics

At this stage, the time to reach equilibrium for the adsorption of MB molecules on the adsorbents was investigated. For this, 5.0 g/L adsorbent suspension and 250 mg/L MB solutions were treated for 0–12 hours. After the solutions taken in different periods were determined by UV-Vis spectrophotometer, the adsorbed amounts (Q_t) per gram adsorbent were calculated. To examine how the adsorption performance has changed during a certain time interval, firstly the t - Q_e graph was plotted as seen in Fig. 6 (a). As can be seen from the graph, the adsorption process was completed after 120 minutes for all adsorbents, so equilibrium was almost reached. However, to be guaranteed, the equilibrium time was optimized as 4.0 hours at this stage, and the contact time was applied as 4.0 hours in further applications.

Various kinetic models have been derived to examine how adsorbate molecules/ions behave on adsorbents in terms of the time dependence of adsorption. The three most famous of these models are: (i) pseudo-first-order kinetic model, (ii) pseudo-second-order kinetic model, and (iii) intraparticle diffusion kinetic model [35–37].

The pseudo first-order kinetic model is a model proposed by Lagergren in 1898 [38]. This model is generally applicable for the first minutes of the adsorption event, not for the total adsorption time. That is, it can be applied from the beginning of the adsorption to the period when equilibrium has not yet been reached. This adsorption rate equation is expressed in Eq. (8) below [39]:

$$\frac{dQ}{dt} = k_1(Q_e - Q_t) \quad (8)$$

The linear shape of this equation is given in Eq. 9 below:

$$\ln(Q_e - Q_t) = \ln Q_e - k_1 t \quad (9)$$

where Q_e (mg/g) and Q_t (mg/g) indicate the amounts of adsorbate adsorbed on the adsorbent at equilibrium and at time t , respectively. k_1 (1/min) is the pseudo-first-order rate constant. If the data fit this model, the $\ln(Q_e - Q_t)$ versus t graph (Fig. 6 (b)) is expected to be linear and this

gives information about whether the kinetic model is suitable for the adsorption data. Q_e and k_1 can be found from the intercept and the slope of the graph, respectively. The pseudo-first order kinetic model can be applied more successfully in the case of a relatively high concentration of adsorbate in the solution [40].

Another model used in the analysis of adsorption kinetic data, the pseudo-second-order kinetic model, unlike the pseudo-first-order kinetic model, works in harmony with the rate control step mechanism throughout the entire adsorption period. Moreover, the kinetic results obtained from adsorption studies with relatively low concentrated adsorbate solutions are better fitted to this model. This model is given by the following Eq. (10) [40]:

$$\frac{dQ_t}{dt} = k_2(Q_e - Q_t)^2 \quad (10)$$

When this equation is transformed into its linear form, Eq. 11 below is obtained:

$$\frac{t}{Q_t} = \frac{1}{k_2 Q_e^2} - \frac{t}{Q_e} \quad (11)$$

where k_2 (g/mg.min) is the second-order rate constant. If a graph to be plotted between t/Q_t and t (Fig. 6(c)) is linear and the value of R^2 is greater than 0.95, it can be said that the second-order kinetic model is compatible with the experimental data. Q_e and k_2 can be determined from the slope of the linear graph and the intercept, respectively.

The kinetic data show that the adsorption rate is not compatible with the pseudo-first-order kinetic model but is quite compatible with the pseudo-second-order model. When the experimental Q_e values are compared with the theoretical Q_e values, it is seen that the experimental data are quite compatible with the second-order rate expression. Additionally, R^2 values support this result (Table 4).

The third kinetic model is different from the first two kinetic models. If the diffusion mechanism in porous structures cannot be clearly explained by pseudo-first- and second-order equations, the intraparticle diffusion kinetics can be used. This kinetic model is expressed by the following Eq. (12):

$$Q_t = k_{id}t^{1/2} + C \quad (12)$$

where Q_t is a constant that characterizes the adsorbed quantity (mg/g) at any time t , k_{id} (mg/g.min^{1/2}) intraparticle diffusion rate constant, and C (mg/g) the boundary layer thickness. k_{id} and C can be determined from the slope and intercept of the graph to be plotted between Q_t and $t^{1/2}$, respectively [41].

The intraparticle diffusion model assumes that the adsorption mechanism generally consists of three steps, and that the adsorption rate is controlled by at least one of these steps: (i) mass transfer from aqueous solution to the external boundary layer of the adsorbent particles as a thin film, (ii) adsorption at sites on the internal or external surface of the adsorbent. Energy at this stage depends on whether the adsorption mechanism is physical or chemical, and this stage is thought to occur quite rapidly, (iii) diffusion towards adsorption sites within the pores of the adsorbent particles [42].

More than one linear correlation can be observed in the graph to be plotted between Q_t and $t^{1/2}$. The first sharp line observed indicates film diffusion (or boundary layer diffusion) or film adsorption. The second straight line is the section in which the excess adsorbate molecules are adsorbed towards the interior of the pore due to the saturation of the boundary layer, in other words, where intraparticle diffusion is the rate control step. The third part represents the equilibrium state, and in this part, intraparticle diffusion begins to slow down due to the very little adsorbate concentration remaining in the solution. If the second line, the intercept (C) of the line representing intraparticle diffusion, passes through the origin, it is concluded that only intraparticle diffusion is the step controlling the adsorption rate. If it does not pass through the origin, it can be said that the adsorption rate is controlled by more than one mechanism [43].

When looking at the graph for the intraparticle diffusion model in Fig. 6(d), it is seen that two different linear lines are formed. Here, the first line represents intraparticle diffusion. As seen in Fig. 6(d), the first line almost passes through zero. Therefore, it can be said that the rate control step in the adsorption of MB on the adsorbents is generally controlled by the intraparticle diffusion mechanism. It is also seen from Table 4 that C values are very close to zero.

Concentration Effect on MB Adsorption and Adsorption Isotherms

In this section, the effect of increasing concentrations of MB solutions on the adsorption mechanism was investigated by using the fixed mass of four different adsorbents. The relationship between the increasing adsorbate molecule/ion in the solution and the amount of adsorbate adsorbed on per unit quantity of the relevant adsorbent is called "adsorption isotherm". Adsorption isotherms are useful for selecting the most suitable adsorbent in an adsorption process, and also they are very useful in assessing the performance of systems in which adsorption occurs [44].

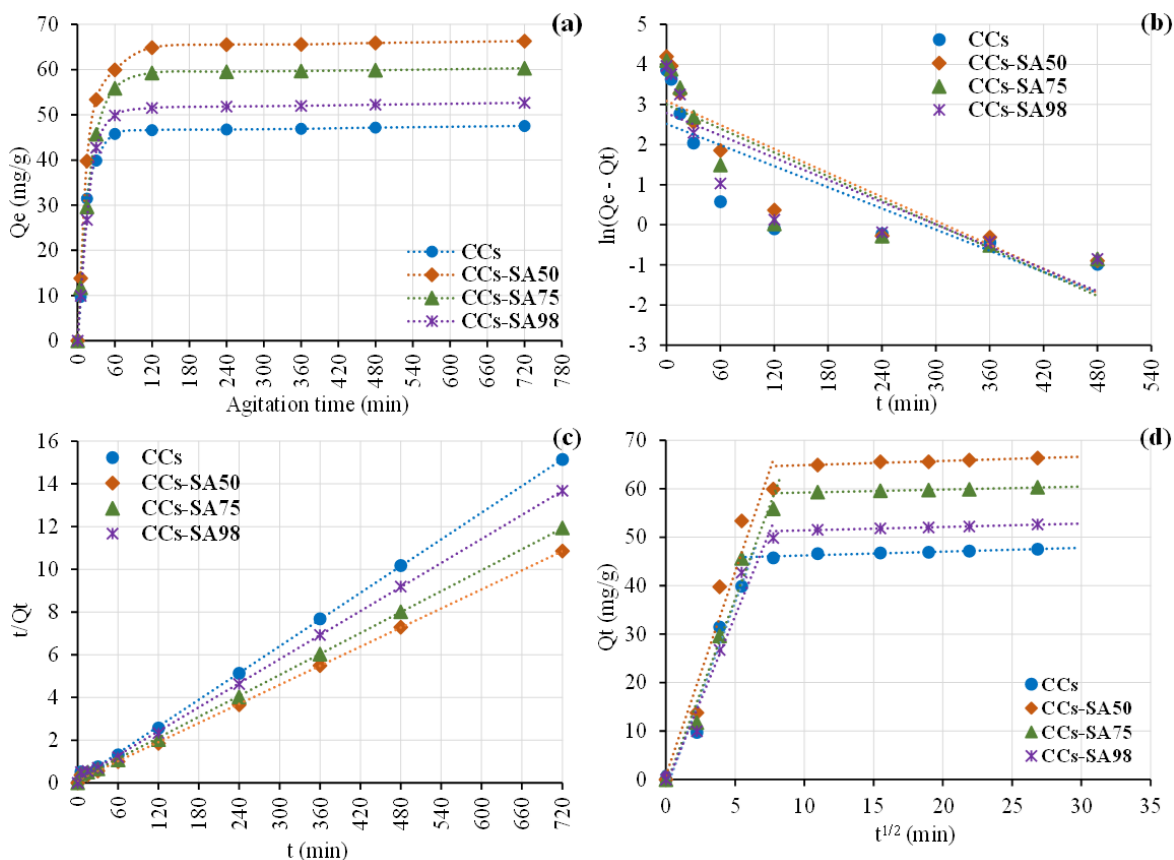


Figure 6. Effect of equilibrium time on the removal of MB from aqueous solution by CCs-SA, and the kinetic models: (a) Effect of time to reach equilibrium, (b) Linear plot of $\ln(Q_e - Q_t)$ vs t for pseudo-first-order kinetic model, (c) linear plot of t/Q_t vs t for pseudo-second-order kinetic model, (d) plot of $t^{1/2}$ vs Q_t for intraparticle diffusion kinetic model (pH: 6.0, C_0 : 500 mg/L, adsorbent amount: 5.0 g/L, agitation time: 0–12 hours, temperature: 25 °C)

5.0 g/L adsorbent suspensions and six different MB solutions with increasing concentrations between 50 and 1000 mg/L were treated for 4.0 hours. Adsorbent particles and adsorbate molecules were separated from each other by filtration, and unadsorbed MB molecules in the solution were determined by UV-Vis spectrophotometer. The quantities of MB adsorbed per gram of the adsorbent were calculated from the relevant equations.

As can be seen from the C_0 vs Q_e plot in Fig. 7 (a), the quantity of MB adsorbed against increasing MB concentration increases. However, this increase is not linear. The

presence of adsorbate molecules increasing against the fixed amount of adsorbent will cause the adsorbent to become saturated after a while and thus the adsorption rate to slow down. Even if the quantity of adsorbate increases after a while, the adsorbent will not be able to adsorb more adsorbate molecules.

It is very useful the adsorption equilibrium isotherms to determine the adsorption capacity of an adsorbent for an adsorbate. In the equilibrium state, there is no concentration change either on the surface of the adsorbent or in the solution. The adsorption capacity of an adsorbent for an ad-

Table 4. Kinetic model constants for MB adsorption from aqueous solution

Adsorbent	$Q_e(\text{exp.})$ (mg/g)	Pseudo-first-order kinetic			Pseudo-second-order kinetic			Intraparticle diffusion		
		$Q_e(\text{theo.})$ (mg/g)	k_1 (min^{-1})	R^2	$Q_e(\text{theo.})$ (mg/g)	k_2 (g/mg.min)	R^2	k_{id} ($\text{mg/g.min}^{1/2}$)	C (mg/g)	R^2
CCs	47.53	12.38	8.79×10^{-3}	0.6848	47.96	3.02×10^{-2}	0.9995	7.74	-2.15	0.9538
CCs-SA ₅₀	66.31	21.92	9.96×10^{-3}	0.7876	67.11	1.85×10^{-2}	0.9996	8.40	0.88	0.9420
CCs-SA ₇₅	60.31	20.07	9.95×10^{-3}	0.7508	61.20	1.75×10^{-2}	0.9994	7.70	-1.18	0.9770
CCs-SA ₉₈	52.65	16.26	9.26×10^{-3}	0.7277	53.33	2.12×10^{-2}	0.9994	6.98	-1.14	0.9644

$Q_e(\text{exp.})$: Experimental Q_e value

$Q_e(\text{theo.})$: Theoretical Q_e value

sorbate generally includes the relationship of three properties; (i) the concentration of the adsorbate in the fluid phase (C_e), (ii) the concentration of the adsorbate on the adsorbent (Q_e), and (iii) the temperature of the system (T). If the temperature of the system is kept constant, C_e and Q_e can be used to create a graph expressing the equilibrium state. This graph is the adsorption isotherm [45].

The graph plotted between the adsorbate concentration (C_e , mg/L) remaining in the solution after the adsorption process and the quantity of MB (Q_e , mg/g) adsorbed on 1 g of the adsorbent is shown in Fig. 7(b).

Two well-known isotherm models, which provide important information about the adsorption process and the surfaces of adsorbents by establishing a relationship between C_e and Q_e , stand out today: Langmuir and Freundlich isotherm models.

In the Langmuir adsorption isotherm developed by Irving Langmuir in 1932, the following assumptions were mainly proposed [46]:

- Adsorption of the adsorbate ion or molecules occurs at specific binding sites localized on the surface of the adsorbent.
- All adsorption sites on the surface of the adsorbent have very similar properties to each other.
- At the end of the adsorption process, the surface of the adsorbent is covered with the only monolayer of adsorbed molecules.
- There is no interaction between the adsorbate ion or molecules adsorbed on the adsorbent surface, that is, it is assumed that there is no adsorbate-adsorbate interaction.

The mathematical equation for the curvilinear form of the Langmuir isotherm is as in Eq. 13 below:

$$Q_e = \frac{bC_e}{1 + bC_e} \quad (13)$$

In Eq. 14, the linearized form of Eq. 13 is given:

$$\frac{C_e}{Q_e} = \frac{C_e}{Q_{\max}} + \frac{1}{bQ_{\max}} \quad (14)$$

where Q_e is the quantity of adsorbate adsorbed by 1 g adsorbent (mg/g), Q_{\max} is the maximum monolayer adsorption capacity (mg/g), C_e is the concentration of the adsorbate solution after reaching equilibrium (mg/L), and b represents the Langmuir constant associated with free energy or adsorption enthalpy (L/mg). The plot of C_e/Q_e vs C_e is a straight line indicating the suitability of

the adsorption to the Langmuir model. Q_{\max} and b can be determined from the slope and intercept, respectively.

Another model Freundlich isotherm model, which allows examining the adsorption equilibrium conditions on heterogeneous surfaces with a multi-layer adsorption mechanism, and which was first proposed by German Physical Chemist Herbert Max Finley Freundlich [47].

The curvilinear and linear forms for the Freundlich isotherm model are as Eq.s 15 and 16 below:

$$Q_e = K_f \times C_e^{1/n} \quad (15)$$

$$\ln Q_e = \ln K_f + \frac{1}{n} \ln C_e \quad (16)$$

where K_f (mg/g) is an empirical parameter associated with the adsorption capacity and n is the adsorption intensity and indicates the strength of the relationship between adsorbate and adsorbent. High values of K_f are an indication of how close the affinity of adsorbent and adsorbate to each other. The value of n varies with the heterogeneity of adsorption sites on the adsorbent surface. Also, the value of n is expected to be between 1 and 10 in terms of suitability of the adsorption process for an adsorbent-adsorbate couple to be selected. The value $1/n$ is the heterogeneity factor and generally takes values in the range 0–1. The more heterogeneous the adsorbent surface is, the closer the $1/n$ value becomes zero. The accuracy of this isotherm in heterogeneous adsorption systems is, of course, better than the Langmuir isotherm.

The plot of $\ln C_e$ versus $\ln Q_e$ is linear, and K_f and $1/n$ can be easily found from the intercept and slope of the line.

Figs 7(c) and 7(d) show linear Langmuir and Freundlich isotherm plots for adsorption of MB on four adsorbents. When the R^2 values of the lines are examined first (in Table 5), it is seen that the data fit both models with a high correlation. However, when looking at Table 5, R^2 values for the Langmuir isotherm of other adsorbents except CCs are greater than those for the Freundlich isotherm. In other words, while MB adsorption on CCs is more compatible with the Freundlich model, the Langmuir isotherm model for the other three adsorbents seems more compatible. This result arises from the R^2 values obtained from the linear graphs. From the Langmuir linear isotherm, the Q_{\max} values can be calculated. Q_{\max} and other constants are given in Table 5. However, an important point here is that these constants change as the quantity of adsorbent changes. As the quantity of adsorbent decreases, the Q_{\max} values will also increase. The reason for this is discussed in the next parameter (Table 5). Therefore, the quantity of adsorbent used should be considered when comparing the obtained Q_{\max} values with the literature.

Looking at the Q_{\max} values in Table 5, the adsorbent with the code CCs-SA₅₀ has the highest value as expected. The Q_{\max} value of 1.0 g/L adsorbent amount is 295.5 mg/g and this value is higher than many values obtained from other studies in the literature. A comparison with some studies in the literature on maximum adsorption capacities (Q_{\max}) is given in Table 7. (See Conclusion section)

It will be more useful to evaluate the curvilinear isotherm forms to determine which isotherm model is compatible with the adsorption data. New theoretical Q_e values are derived by replacing the constants obtained from linear graphs in curvilinear Eqs (Eq.s 13 and 15) and these values are compared with experimental Q_e values on a curvilinear graph. In this respect, when looking at the curvilinear graphs drawn in Fig. 8, it can be interpreted which curve better represents the experimental Q_e values (round symbols in black). The first curvilinear graph is for CCs and the experimental points here represent the Freundlich isotherm model best. Because the Freundlich curve follows the experimental points relatively better than the Langmuir curve. Anyway, the R^2 value of the related linear graph is slightly higher for the Freundlich isotherm. This height has been proven better here. However, for the other three adsorbents obtained by activation with sulfuric acid, the experimental points represent the best Langmuir isotherm. Both results are understandable. Because, since the original CCs is a natural structure, there are extremely heteroge-

neous formations on its surface. The structure has highly amorphous properties and on its surface, there are functional groups and chemical structures of quite different types and strengths.

Effect of Adsorbent Quantity on MB Adsorption

In the previous parameter, the changes in the adsorption with increasing MB concentrations in the fixed adsorbent mass were examined and discussed. Here, the adsorption behavior was observed by increasing the adsorbent mass while the MB concentration was constant, and the data obtained were interpreted. Here, two different MB concentrations and different adsorbent mass were treated separately, and the maximum capacities were calculated. 10 mL of 250 mg/L and 500 mg/L MB solutions were treated separately with three different adsorbent quantities of 10, 50 and 100 mg (1.0, 5.0 and 10.0 g/L adsorbent suspensions). At the end of the agitation process, after determining the concentrations of unadsorbed MB in the solution by UV-Vis spectrophotometer, the quantity of MB adsorbed on the adsorbents with the relevant equations were calculated as both % and mg/g, and the graphs were plotted (Fig. 9).

From the Fig. 9, while MB% adsorption increased with increasing the adsorbent mass, the quantity of adsorbed MB per gram adsorbent decreased. Because, as can be seen from

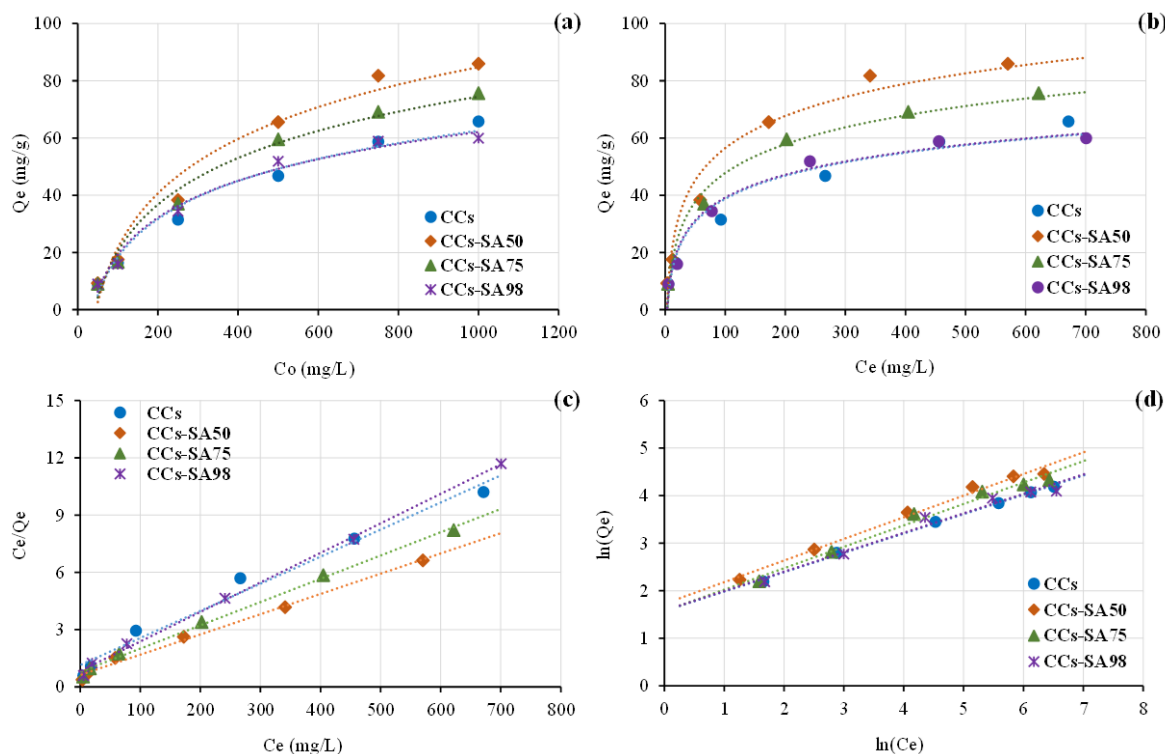


Figure 7. Concentration effect and adsorption isotherms on removal of MB from aqueous solution by CCs-SA: (a) C_0 vs Q_e plot, (b) C_e vs Q_e plot, (c) Linear Langmuir isotherm plot (C_e vs C_0/Q_e plot), (d) Linear Freundlich isotherm plot ($\ln(C_0)$ vs $\ln(Q_e)$ graph) (pH: 6.0, C_0 : 50–1000 mg/L, adsorbent quantity: 5.0 g/L, agitation time: 4.0 hours, temperature: 25 °C)

Table 5. Constants from Langmuir and Freundlich isotherms

Adsorbent quantity (g/L)	Adsorbent	LANGMUIR			FREUNDLICH		
		Q_{max} (mg/g)	b (L/mg)	R^2	K_f (mg/g)	n	R^2
1.0	CCs	202.5	6.46×10^{-3}	0.9698	9.63	2.291	0.9930
	CCs-SA50	295.5	8.31×10^{-3}	0.9953	11.25	2.028	0.9745
	CCs-SA75	215.9	1.10×10^{-2}	0.9980	12.78	2.339	0.9596
	CCs-SA98	175.7	1.39×10^{-2}	0.9995	14.09	2.605	0.9410
5.0	CCs	70.4	1.24×10^{-2}	0.9787	4.83	1.574	0.9973
	CCs-SA50	94.3	1.69×10^{-2}	0.9931	5.61	1.724	0.9882
	CCs-SA75	82.0	1.56×10^{-2}	0.9959	4.84	1.576	0.9811
	CCs-SA98	64.7	1.86×10^{-2}	0.9979	4.87	1.583	0.9736
10.0	CCs	55.2	1.14×10^{-2}	0.9714	2.37	0.863	0.9984
	CCs-SA50	61.5	2.00×10^{-2}	0.9955	3.19	1.159	0.9586
	CCs-SA75	56.2	1.96×10^{-2}	0.9963	2.96	1.086	0.9533
	CCs-SA98	51.4	2.07×10^{-2}	0.9971	2.83	1.039	0.9422

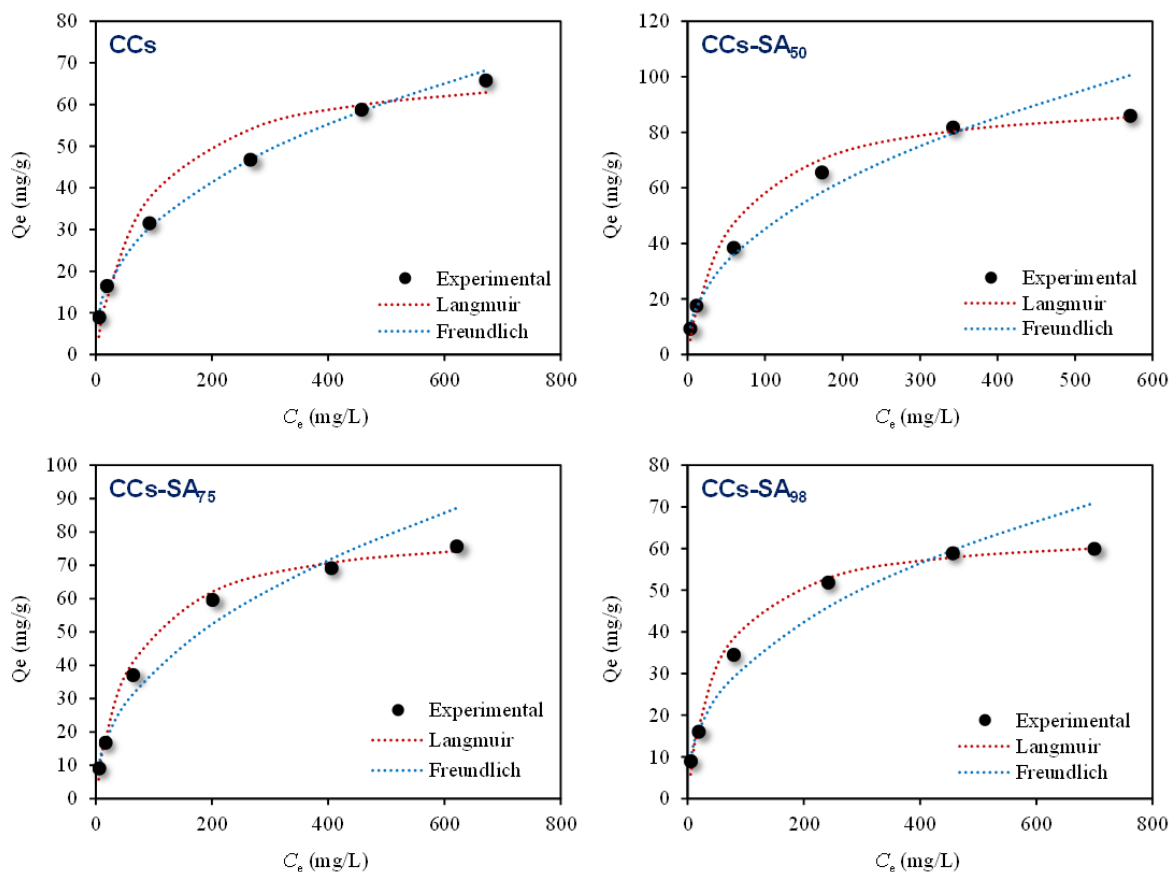


Figure 8. Curvilinear Langmuir and Freundlich isotherms derived for MB adsorption

the figure, the % increase quantity is not linear. Therefore, when all results obtained are converted into adsorbed quantities per unit adsorbent (mg/g), the adsorption efficiency will decrease as expected.

This result can be proved mathematically. If Eq.s (5) and (6) are combined, the following new Eq. (17) is derived. As seen in the equation, the adsorbent mass (m) and Ads.% are inversely proportional.

$$Q_e = \frac{Ads.\% \times C_o \times V}{100m} \quad (17)$$

This may be mainly due to two reasons: (i) Increasing the quantity of adsorbent at constant MB concentration leads to the formation of unsaturated sites on the adsorbent surface. (ii) The adsorption capacity of the adsorbent becomes smaller as the agglomeration of large quantities of adsorbent particles will lead to a decrease in the total surface area. Considering Table 5 given in the previous parameter, as can be seen, the highest capacity value is reached with the lowest adsorbent quantity.

Desorption of MB Molecules Adsorbed on CCs-SA

Re-use of adsorbents used to remove various types of contaminants from water and wastewater after regeneration is very important for the economics of the process. Therefore, in this parameter, various desorption solutions (1:1 diluted acetone and alcohol solutions, and 0.1 M HCl, NaCl and NaOH solutions) were prepared for the regeneration of loaded adsorbents and their performance was tested.

First, 10 mL of 100 mg/L MB solution was added into a serial tube containing 0.05 g of adsorbent. After 4.0 hours of agitation under optimum conditions, the adsorbent and adsorbate were separated by filtration. After the loaded adsorbents were thoroughly washed and dried in the air, the desorption solutions shown in Fig 10 were added to them. These desorption solutions were selected based on those used in similar studies in the literature. It can be considered that acetone and alcoholic solvents will perform higher. As can be seen from the column charts in Fig 10, the performance of organic solvents is higher. However, the loaded MB molecules could not be desorbed quantitatively with any desorption solution. There could be several reasons for this. First, MB molecules may be linked by chemical bonds on respective adsorbents. Second, adhesion can be through many mechanisms, not necessarily chemical bonds, but strong and weak. The adsorption mechanisms of dyestuffs can be not only through electrostatic interactions as in metal ions, but also through strong π - π dispersion interactions between the aromatic rings of the dye molecules and the graphene layers of the adsorbent, and non-electrostatic partial H-bonds [48].

Interactions between the adsorbent and the adsorbate basically occur in two ways; electrostatic and non-electrostatic. Electrostatic interactions occur where the adsorbate is an electrolyte, that is, it can ionize in the aqueous solution by accepting or donating electrons. These interactions can be attractive or repulsive depending on the solution pH. Non-electrostatic interactions are attractive in all conditions, and mainly include van der Waals forces,

hydrophobic interactions, and H-bonding. The factors affecting the adsorption process are the properties of the adsorbent and adsorbate, the solution chemistry, and the adsorption temperature. Compounds containing aromatic groups such as MB are adsorbed on carbon materials mostly with π -electrons in the aromatic ring [49].

In the next parameter, the physical and chemical mechanism of the adsorption process taking place on the relevant adsorbent is discussed from the thermodynamic data.

Temperature Effect on MB Adsorption and Adsorption Thermodynamics

The effect of temperature on the adsorption yield is important for the applicability of the process in all seasons. Also, the effect of temperature can give important information about the adsorption mechanism. Thermodynamic evaluations can be made with temperature change. In this regard, 250 mg/L MB solutions and 5.0 g/L of each adsorbent were treated for 4.0 hours. Then, the MB amount (mg/g) retained by 1 g adsorbent was calculated, and temperature change graphs were plotted.

As seen in Fig. 11(a), an increase in temperature reflected positively on the adsorption efficiency. When the temperature increased from 5 °C to 50 °C, MB adsorption increased from 26.4 mg/g to 39.0 mg/g (from 52.9% to 78.0%) on CCs, 30.1 mg/g to 41.5 mg/g (from 60.2% to 83.0%) on CCs-SA₅₀, 28.9 mg/g to 39.2 mg/g (57.7% to 78.3%) on CCs-SA₇₅ and 28.0 mg/g to 38.3 mg/g (55.9% to 76%) on CCs-SA₉₈.

The results show that the adsorption behavior of MB on the relevant adsorbents is endothermic, that is, a process that takes place with higher efficiency by accepting the temperature of the environment. The positive effect of temperature increase on the efficiency of adsorption can be attributed to reasons such as the increase in the interaction between the adsorbent and the adsorbate more, the passive sites becoming more active, and the expansion of the pore structures of the adsorbent, and the more effective role of intra-particle diffusion.

Adsorption thermodynamics were also examined from the temperature change data obtained at this stage. Thermodynamics determines the internal energy, enthalpy, entropy, and free energy values of the system during a physical or chemical transformation and examines their dependence on the reaction conditions [50]. The thermodynamic parameters ΔG , ΔS and ΔH can be found from the following equations:

$$\Delta G = \Delta H - T\Delta S \quad (18)$$

$$K_d = C_a / C_e \quad (19)$$

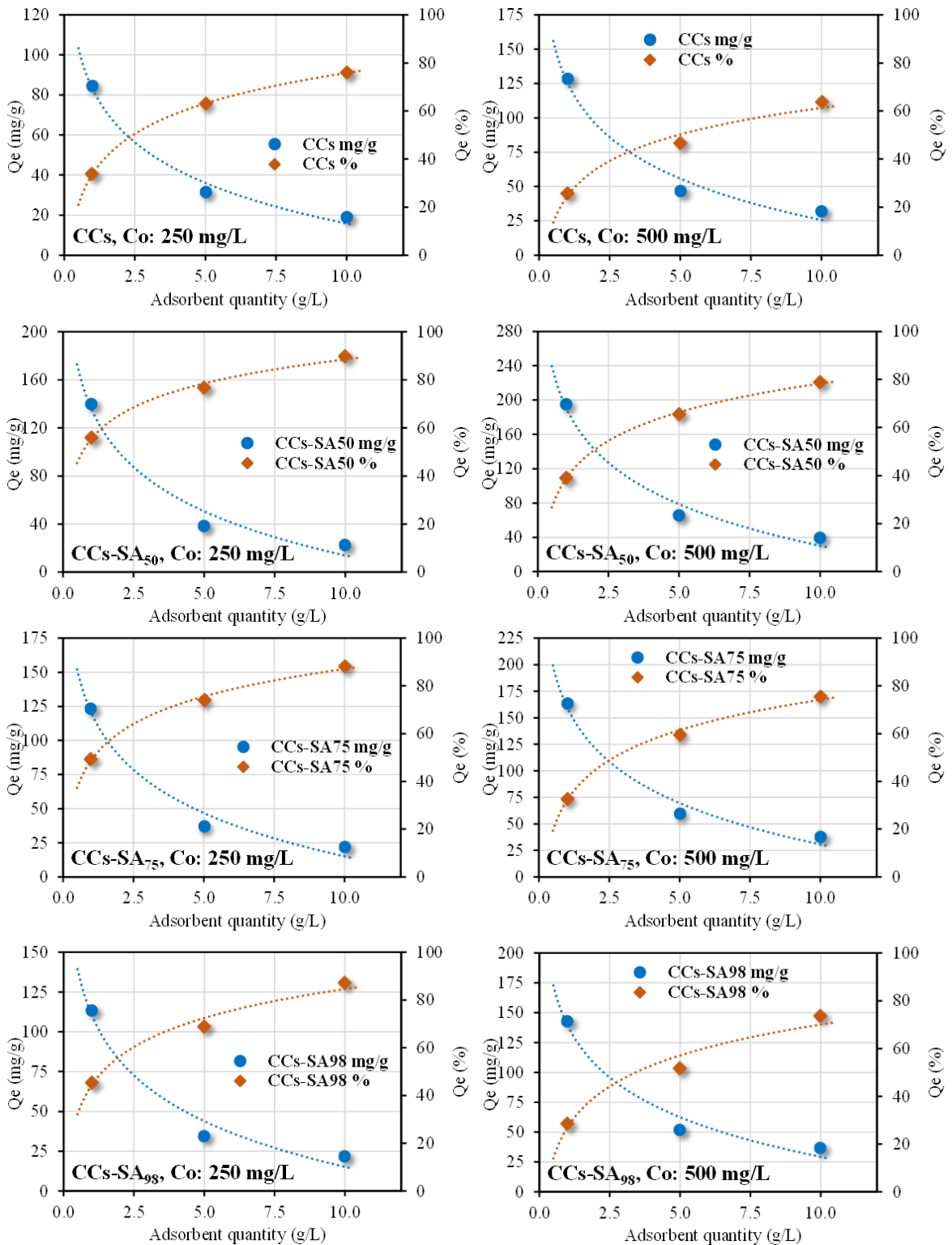


Figure 9. The effect of the adsorbent quantity on the removal of MB from the aqueous solution by CCs-SA (pH: 6.0, C_i : 250 and 500 mg/L, adsorbent quantity: 1.0, 5.0 and 10.0 g/L, agitation time: 4.0 hours, temperature: 25 °C)

$$\Delta G = -RT \ln K_d \quad (20)$$

$$\ln K_d = \frac{\Delta S}{R} - \frac{\Delta H}{R} \quad (21)$$

ΔG : Gibbs free energy change (kJ/mol)

ΔH : Enthalpy change (kJ/mol)

ΔS : Entropy change (kJ/mol.K)

T : Absolute temperature (K)

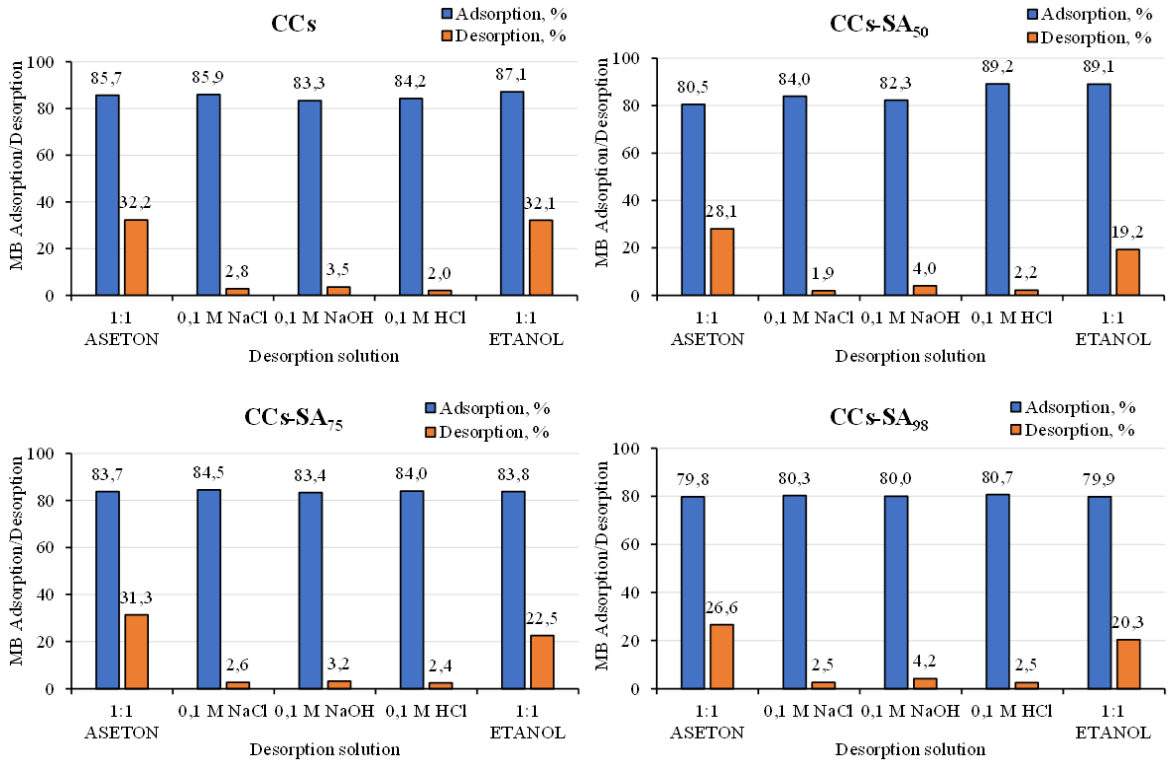


Figure 10. Desorption of MB molecules adsorbed on the adsorbents (C_e : 100 mg / L)

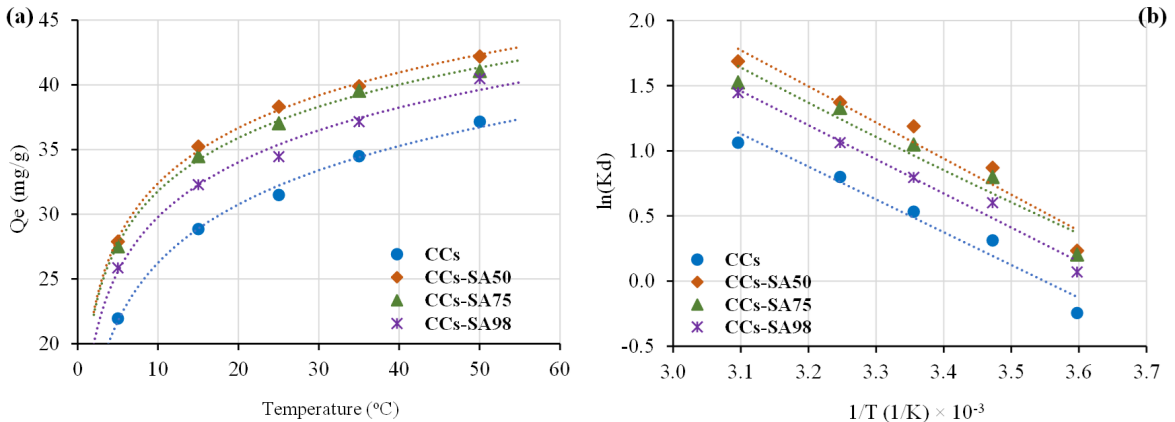


Figure 11. (a) Effect of medium temperature on removal of MB from aqueous solution by CCs-SA, (b) $1/T - \ln(K_d)$ graph for thermodynamic data (pH: 6.0, C_e : 250 mg/L, adsorbent quantity: 5.0 g/L, agitation time: 4.0 hours, temperature: 5 – 50 °C)

R: Universal gas constant (J/mol.K)
 K_d : Adsorption equilibrium constant
 C_a : The concentration of adsorbate retained in the unit mass of the adsorbent (mg/L)
 C_e : The concentration of adsorbate left in the solution after adsorption (mg/L)

First, the equilibrium constant K_d is calculated from Eq. 19. A graph to be plotted between $\ln(K_d)$ and $1/T$ in Eq. 21 is expected to be linear as in Fig. 11(b). While the slope of this graph gives ΔH , ΔS can be found from the intercept.

The data obtained from thermodynamic calculations are given in Table 6. With increasing temperature, ΔG values

become increasingly negative. A negative value of ΔG indicates that adsorption occurs spontaneously. The enthalpy value of physical adsorption is generally not greater than 4 kJ/mol, but not less than 20 kJ/mol for chemical adsorption [51]. Therefore, when looking at the ΔH values obtained from this study in Table 6, it is seen that all of them are slightly higher than 20 kJ/mol. In other words, it can be said that the adsorption process proceeds by chemical means. In the previous parameter, it was discussed that MB molecules retained on the adsorbents could not be quantitatively desorbed. The results obtained from the thermodynamic data also confirm this result due to the possibility of the process being chemical.

Table 6. The effect of ambient temperature on the removal of MB from aqueous solution by CCs-SA: Thermodynamic data

Adsorbent	T (°C)	K _a	ΔG (kJ/mol)	ΔS (J/mol.K)	ΔH (kJ/mol)
CCs	5	0.78	0.57		
	15	1.37	-0.75		
	25	1.70	-1.32	74.26	20.92
	35	2.22	-2.05		
	50	2.89	-2.85		
CCs-SA ₅₀	5	1.31	-0.62		
	15	2.36	-2.06		
	25	3.28	-2.94	82.64	22.00
	35	3.90	-3.49		
	50	5.20	-4.43		
CCs-SA ₇₅	5	1.23	-0.47		
	15	2.22	-1.91		
	25	2.85	-2.60	79.76	21.35
	35	3.78	-3.40		
	50	4.60	-4.10		
CCs-SA ₉₈	5	1.07	-0.16		
	15	1.82	-1.44		
	25	2.21	-1.97	79.64	21.78
	35	2.89	-2.72		
	50	4.24	-3.88		

Positive ΔS values increase the probability of random formation of the adsorption equilibrium occurring at the solid-liquid interface during adsorption. In other words, it indicates an increase in the amount of energy that cannot be used, that is, an increase in the disorder of the system.

CONCLUSION

In this study, three new adsorbents were produced by chemical activation using different concentrations of sul-

furic acid from corn cobs (CCs). Based on the results obtained from the characterization and adsorption studies, the following results were obtained:

- The adsorbent with the richest surface acidic functional groups is CCs-SA₅₀ (Table 1), which was obtained by activating with the lowest concentration of sulfuric acid (50%).
- When the I₂ and MB numbers of the adsorbents were evaluated, it was found that the adsorbent with the code CCs-SA₅₀ had the highest values.
- It has been observed that MB molecules are adsorbed on all adsorbents with high efficiency over a wide initial pH range, and it has been observed that a precise pH adjustment is not required before adsorption tests. Since the original pH values of the MB solutions are around 6, there is no need to make any pH adjustment before the operations.
- When Langmuir adsorption capacities of adsorbents are compared, the MB capacity of the adsorbent with the code CCs-SA₅₀ is the highest. This result proves that the adsorbent produced by dilute sulfuric acid activation has a higher capacity.
- Table 7 presents a comparison of the capacity value obtained from this study with the literature. As can be seen from the table, the capacity value obtained from this study is higher than many studies in the literature. Therefore, it has been proven that especially the adsorbent with the CCs-SA₅₀ code can be used effectively in removing dyes from contaminated water.
- It has been determined that the increase of the medium temperature has a positive effect on MB adsorption, ad-

Table 7. Comparison of the MB adsorption capacities with the literature

Q_{max} (mg/g)	Q_{max} (mg/g)	Adsorbent mass (g/L)	Solution pH	Ads. Temp. (°C)	Ref.
Sunflower oil cake	16.43	2.0	6.0	25	[52]
<i>Posidonia oceanica</i> (L.) dead leaves	270.3	5.0	6.5	30	[53]
CuO loaded coconut shell AC*	331.5	3.0	9.0	45	[54]
Surfactant-modified AC	232.5	0.15	5.0	25	[55]
Corn cob activated carbon	37.45	0.5	6.0	35	[56]
Jute fiber carbon	225.64	1.5	4.0	28	[57]
Graphene	153.85	0.5	3.0 – 10.0	20	[58]
Garlic peel	82.64	3.0	6.0 – 10.0	30	[59]
Cedar sawdust	111.97	5.0	7.0	20	[60]
Activated corn cobs	295.5	1.0	6.0	25	This study

*AC: Activated carbon

sorption is a spontaneous process, and since ΔH values are greater than 20 kJ/mol, MB adsorption on the adsorbents mainly proceeds chemically.

In conclusion, thanks to this study, both the waste materials have been regained an economic value and the possible damages of these wastes to the environment have been prevented. Besides, it will be possible to eliminate other pollution with the adsorbents produced from these wastes.

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