

## Experimental Investigation of the Thermal Performance of Iron Oxide-Water Nanofluid Subjected To a Magnetic Field in a Horizontal Tube

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### Keywords

Nanofluid,  
Magnetic field,  
Heat transfer,  
Iron oxide

**Abstract:** In this study, an experimental analysis was performed to evaluate the thermal behavior of iron oxide-water nanofluid as it traverses a straight copper tube, under the influence of a constant heat capacity and the application of a magnetic field. Four types of fluids were used in the experiment. These are pure water, 0.5% concentration of Fe<sub>3</sub>O<sub>4</sub>-water nanofluid, 1% concentration of Fe<sub>3</sub>O<sub>4</sub>-water nanofluid and 1.5% concentration of Fe<sub>3</sub>O<sub>4</sub>-water nanofluid. Experiments were conducted at two distinct flow rates as  $10 \times 10^{-5} \text{ m}^3 \text{ s}^{-1}$  and  $13 \times 10^{-5} \text{ m}^3 \text{ s}^{-1}$ . The inlet temperatures of the fluids and the surface temperature of the copper tube were maintained at the same level throughout all experiments. The Nusselt number was determined at Reynolds numbers of 4200 and 5400 in experiments conducted under turbulent flow conditions. The thermal performances of the fluids were compared by comparing the obtained Nusselt numbers. The experiments demonstrated that as the Reynolds number increased, the Nusselt number also increased, with the most notable enhancement of 20.7% observed in the iron oxide-water nanofluid at a 1.5% concentration and a Reynolds number of 5400 under a magnetic field. Additionally, both the heat transfer coefficient and the Nusselt number improved with the use of nanofluids.

## Yatay Bir Boruda Manyetik Alan Uygulanan Demir Oksit-Su Nanoakışkanının Isıl Performansının Deneysel Olarak İncelenmesi

### Anahtar Kelimeler

Nanoakışkan,  
Manyetik alan,  
Isı transferi,  
Demir oksit

**Öz:** Bu çalışmada sabit ısı sığası ve manyetik alan etkisi altındaki düz bir bakır borudan akan demir oksit-su nanoakışkanının ısı performansını deneysel olarak incelenmiştir. Deneyde dört tip akışkan kullanılmıştır. Bunlar; saf su, %0,5 konsantrasyonunda Fe<sub>3</sub>O<sub>4</sub>-Su nanoakışkanı, %1,0 konsantrasyonunda Fe<sub>3</sub>O<sub>4</sub>-Su nanoakışkanı ve %1,5 konsantrasyonunda Fe<sub>3</sub>O<sub>4</sub>-Su nanoakışkanıdır. Deneyler  $10 \times 10^{-5} \text{ m}^3 \text{ s}^{-1}$  ve  $13 \times 10^{-5} \text{ m}^3 \text{ s}^{-1}$  olmak üzere iki farklı debide gerçekleştirilmiştir. Akışkanların giriş sıcaklıkları ve bakır borunun yüzey sıcaklığı tüm deneylerde eşit tutulmuştur. Türbülanslı akış şartlarında gerçekleşen deneylerde iki farklı Reynolds (Re=4200 ve Re=5400) sayısındaki Nusselt sayısı hesaplanmıştır. Elde edilen Nusselt sayıları karşılaştırılarak akışkanların ısı performansları karşılaştırılmıştır. Yapılan deneyler sonucunda Reynolds sayısının artması ile Nusselt sayısının da artış gösterdiği, nanoakışkanların kullanımı ile toplam ısı transfer katsayısının ve Nusselt sayısının artış gösterdiği gözlemlenmiştir. Nusselt sayısındaki en büyük artış, manyetik alan etkisi altında, Re=5400 değerinde %1,5 konsantrasyonunda demir oksit-su nanoakışkanda gerçekleşmiştir ve saf suya göre %20,7 oranında artış tespit edilmiştir.

### 1. INTRODUCTION

The movement of heat from an object at a higher temperature to one at a lower temperature occurs due to

the existence of a temperature gradient. The process of heat energy transitioning between systems or objects is referred to as heat transfer. Naturally, heat transfer always occurs from high to low temperatures; however, modern

systems equipped with advanced equipment also enable heat transfer from low to high temperatures.

With energy resources quickly running out, humanity is striving to utilize what we have in the most effective manner possible. In many energy systems, heat transfer occurs. Therefore, scientists want to increase heat transfer efficiency. The application of nanofluids in thermal systems represents a significant advancement in heat transfer technology. Nanofluids are produced by incorporating solid particles with dimensions ranging from 1 to 100 nanometers into a base fluid. The primary objective of this procedure is to enhance heat transfer due to the interaction of the solid particles within the fluid. The term nanofluid was first used by Maxwell in 1881. Maxwell [1] conducted studies by adding solid particles to liquids. Various studies in this area have been reviewed.

Tekir et al. [2] investigated the thermal properties of a nanofluid made from different proportions of iron oxide, copper, and water ( $\text{Fe}_3\text{O}_4 - \text{Cu} - \text{H}_2\text{O}$ ) under the influence of a magnetic field. In their study, they conducted experiments between the values of  $994 < \text{Re} < 2337$ . The researchers noted that the Nusselt (Nu) number rose as the fluid velocity increased. At the same time, they observed that water  $\text{Fe}_3\text{O}_4$  and Cu nanoparticles increased the heat transfer. The study found that applying a magnetic field to the nanofluids improved heat transfer by 14% compared to when no magnetic field was present. They determined that the hybrid nanofluids used; %1  $\text{Fe}_3\text{O}_4$  - %1 Cu - %98 water type showed the best performance under magnetic field. Demirpolat and Uyar [3], determined the thermal conductivities of the nanoparticles produced in order to evaluate the use of nanoparticle materials in thermal insulation materials, which a new perspective on energy is saving. The heat transfer coefficients of  $\text{Al}_2\text{O}_3$  and CuO nanoparticles were found to be 34.2 and 65.4 W/mK, respectively. Uyar et al. [4] calculated that there was a 1.1% increase in thermal efficiency due to the MgO nanoparticle additive. Keklikcioğlu and Özceyhan [5] conducted a numerical analysis of the thermal performance of a hybrid nanofluid composed of graphene, iron oxide, and water, with varying concentrations between 0.5% and 1%. This analysis was performed within a flat heat exchanger tube featuring a circular cross-section, under conditions of constant surface heat flux, turbulent flow, and Reynolds numbers ranging from 10000 to 50000. The analysis revealed that the use of nanofluid significantly enhanced heat transfer while maintaining a relatively stable friction coefficient. The study found that using nanofluid instead of base fluid water increased the Nusselt number by up to 24%. The highest thermo hydraulic performance coefficient observed in this study was calculated as 1.2 for  $\text{Re}=10000$  in the use of 1% graphene-iron oxide-water hybrid nanofluid. An experimental investigation was carried out by Çiftçi et al. [6] to assess the thermal performance of a closed heat pipe, particularly focusing on a thermo siphon that employed titanium dioxide-water ( $\text{TiO}_2 - \text{H}_2\text{O}$ ) nanofluid. Three distinct cooling water flow rates ( $5 \text{ g s}^{-1}$ ,  $7.5 \text{ g s}^{-1}$ ,  $10 \text{ g s}^{-1}$ ) and three varying heater power levels (200 Watt, 300 Watt, and 400 Watt) were utilized in the evaporation section of the study. The

experiments employed both water and nanofluid as the working fluids. It was found that the titanium dioxide-water nanofluid enhanced thermal performance by 16.5% when subjected to a heating power of 200 Watt and a cooling water flow rate of 5 g/s. Kılınç et al. [7] conducted an experimental study to examine the cooling performance of vehicle radiators using nanofluids. This investigation incorporated pure water, along with graphene oxide-water and graphene nanoribbon-water nanofluids. The experimental setup included three different inlet temperatures and four varying flow rates as variable parameters. The experiments revealed an increase in the total heat transfer coefficient of 6.9% for a 0.001% GO-water solution, 32% for a 0.02% GO-water solution, and 18.9% for a 0.01% GNR-water solution. Kılınç [8] examined the thermal efficiency of a thermo syphon by employing nanofluid within a thermo syphon-type heat pipe. In the experiment, he used nanofluid containing 2% iron oxide particles and 0.2% surface activator in water. The cooling water flow rate of the condenser zone was used as  $3 \text{ g s}^{-1}$ ,  $6 \text{ g s}^{-1}$ ,  $9 \text{ g s}^{-1}$ , and two different parameters were used for the heat value given to heat the evaporator as 300 Watt and 400 Watt. As a result, it was observed that the magnetic nanofluid increased the thermal performance by 20%. Sadeghinezhad et al. [9] examined the thermal performance of fluid flow in the pipe in the range of  $5000 < \text{Re} < 22000$  using graphene-water nanofluid with various weight ratios ranging from 0.025% to 1%. In their research, they found that using nanofluid enhanced heat transfer and Nusselt number. The thermal performance of graphene and iron oxide nanoparticles separately and in hybrid nanofluids was examined by Askari et al. [10]. The nanofluids they prepared had three different weight ratios of 0.1%, 0.2% and 1.0%. As a result of the experiments, they found an improvement between 14% and 32% in the thermal conductivity coefficient compared to the base fluid. For the value of  $\text{Re}=4248$ , the heat transfer coefficient increased by 8.5% in the iron oxide-water nanofluid, while it increased by 14.5% in the iron oxide-graphene-water hybrid nanofluid. The thermal transfer properties of water-based nanofluids containing copper oxide and iron oxide were investigated by Peyghambarzadeh et al. [11], who suggested using them in place of conventional water in car radiators. Three distinct volumetric concentrations of 0.15%, 0.4%, 0.65% were used to prepare the nanofluids. The total heat transfer coefficient increased by 9% in this experimental investigation. A study on the heat transfer properties of nanofluids based on carbon nanotubes in a horizontal pipe was carried out by Ding et al. [12]. The pipe used for the study was 970 mm long with an inner diameter of 4.5 mm. Under laminar flow and fixed wall heat flux boundary conditions, they discovered that the convection heat transfer coefficient increased by more than 350% at  $\text{Re}=800$  and 0.5% nanofluid. Abreu et al. [13] observed a 23% increase in Nusselt number for 0.25% concentration under the condition of  $\text{Re}=1650$  for multilayer CNT with 80mm outer diameter and  $20 \times 10^{-3}$  nm length in a 6 mm inner diameter and 200 mm long pipe. Based on the research undertaken, it has been noted that the incorporation of nanofluids in heat transfer systems significantly improves efficiency. As global energy

resources continue to diminish at a rapid pace, the efficiency of current systems has gained paramount importance. Therefore, the high efficiency observed in nanofluids is anticipated to play a more significant role in our lives in the future.

This research examined the thermal performance of water-iron oxide  $H_2O - Fe_3O_4$  nanofluid at volumetric ratios of 0.5%, 1%, and 1.5%, across various flow rates, while maintaining a constant heat capacity. The study also considered the effects of a magnetic field and the subsequent removal of the magnetic field. The findings were analyzed in the context of the thermal performance of water.

## 2. MATERIAL AND METHOD

In this experimental study, the thermal performance of water and iron oxide-water ( $Fe_3O_4 - H_2O$ ) nanofluids (volume ratios; 0.5%, 1%, and 1.5%) flowing through a straight copper pipe at two different flow rates ( $10 \times 10^{-5} m^3 s^{-1}$ ,  $13 \times 10^{-5} m^3 s^{-1}$ ), under constant heat capacity ( $25,000 W m^{-2}$ ), constant inlet temperature ( $15^\circ C$ ), without a magnetic field and then under the influence of a magnetic field were investigated. During the experiments, the inlet temperature of all fluids was maintained constant. After each experiment, the fluids were cooled in refrigeration units, and the tests were repeated once the fluids returned to the specified inlet temperature conditions. Experiments were conducted for four different fluid types at two flow rates without a magnetic field. Following this, the identical experiments were conducted in the presence of a magnetic field. In total, 14 distinct experiments were carried out.

### 2.1. Nanofluid Preparation

In the experimental study, pure water and iron oxide-water nanofluids with three different volumetric ratios (0.5%, 1%, 1.5%) were used as fluids. Nanofluids were synthesized using a two-step approach. Iron oxide particles supplied in the form of nanoparticles were mixed in pure water and kept in an ultrasonic mixer for approximately 5 hours. As a result of the process, homogeneous and stable iron oxide-water nanofluids were prepared.

**Table 1.** Thermophysical properties of fluids

	$H_2O$ Water	%0.5 $Fe_3O_4 - H_2O$ Iron Oxide-Water	%1 $Fe_3O_4 - H_2O$ Iron Oxide-Water	%1.5 $Fe_3O_4 - H_2O$ Iron Oxide-Water	$Fe_3O_4$ Iron Oxide
Intensity ( $\rho$ ) $kg m^{-3}$	999.0	1019.9	1040.8	1061.7	5180
Specific Heat ( $c_p$ ) $J kgK^{-1}$	4186	4082	3982	3887	104
Dynamic Viscosity ( $\mu$ ) $kg ms^{-1}$	$1.120 \times 10^{-3}$	$1.134 \times 10^{-3}$	$1.148 \times 10^{-3}$	$1.162 \times 10^{-3}$	
Heat Conduction Coefficient ( $k$ ) $W mK^{-1}$	0.59	0.6007	0.6116	0.6226	17.65
Prandtl Number (Pr)	7.940	7.706	7.475	7.255	

### 2.2. Experimental Setup

To facilitate the flow, a two-stage circulation pump with a total power of 250 Watts was utilized. In the experimental setup, copper tubing was used to effectively

The formulas used to determine the thermal properties of fluids are as follows;

Volumetric concentration: Pak and Cho [14] proposed Equation 1;

$$\phi_v = \frac{1}{(100 \phi_m^{-1})(\rho_p \rho_f^{-1}) + 1} \times 100 \quad (1)$$

Density: Equation 2 was utilized for density calculations;

$$\rho_n = (1 - \phi)\rho_f + \phi x \rho_p \quad (2)$$

Specific heat: Bhimani et al. [15] employed Equation 3;

$$c_{p_n} = \frac{(1 - \phi)x\rho_f x c_{p_f} + \phi x \rho_p x c_{p_p}}{\rho_n} \quad (3)$$

Dynamic viscosity: Wen and Ding [16] provided Equation 4;

$$\mu_n = \mu_f(1 + 2.5\phi) \quad (4)$$

Thermal conductivity: Yu and Choi [17] used Equation 5;

$$k_n = \left[ \frac{k_p + 2k_f + \{2(k_p - k_f)(1 + \beta)^3 \phi\}}{k_p + 2k_f - \{(k_p - k_f)(1 + \beta)^3 \phi\}} \right] x k_f \quad (5)$$

Prandtl number showed in Equation 6;

$$Pr = \frac{\mu c_p}{k} \quad (6)$$

The formula includes the parameters:  $\rho_n$  for nanofluid density,  $\rho_f$  for base fluid density, and  $\rho_n$  for nanoparticle density.

The parameter  $\phi$  refers to the volumetric or mass fraction, while  $\phi_v$  signifies the volumetric fraction of the nanofluid, and  $\phi_m$  indicates the mass fraction of the nanofluid. The specific heat capacities are represented as  $c_{p_n}$  for the nanofluid,  $c_{p_f}$  for the base fluid, and  $c_{p_p}$  for the nanoparticles. Furthermore,  $\mu_n$  represents the dynamic viscosity of the nanofluid, while  $\mu_f$  denotes the dynamic viscosity of the base fluid,  $k_n$  stands for the thermal conductivity of the nanofluid,  $k_f$  symbolizes the thermal conductivity of the base fluid, and  $k_p$  refers to the thermal conductivity of the nanoparticles. The parameter  $\beta$  represents the ratio of the thickness of the nanoparticle layer to the original particle radius, with a determined value of 0.1 in this study.

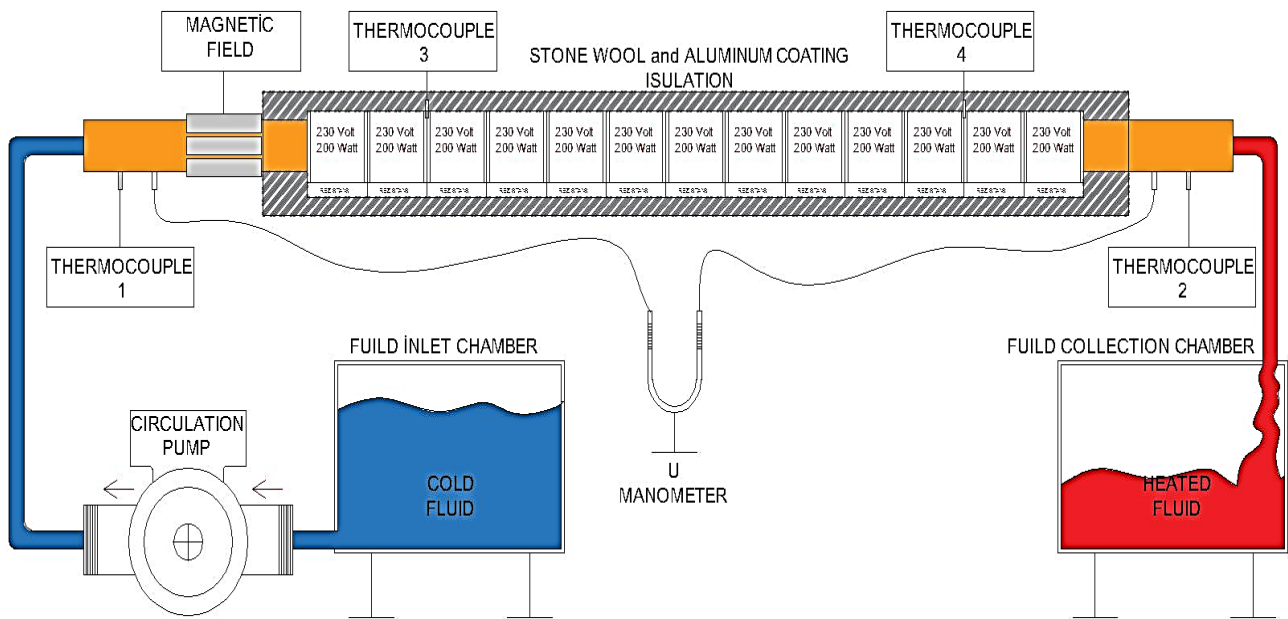
The thermophysical characteristics of the fluids were determined utilizing the designated formulas. These properties are detailed in Table 1.

transfer heat energy to the fluid. The copper tube has an outer diameter of 28 mm, an inner diameter of 26 mm, and a length of 75 cm. Clamp heaters are placed on a 50 cm section of the copper tube. The remaining sections are equipped with magnets, thermocouple probes and

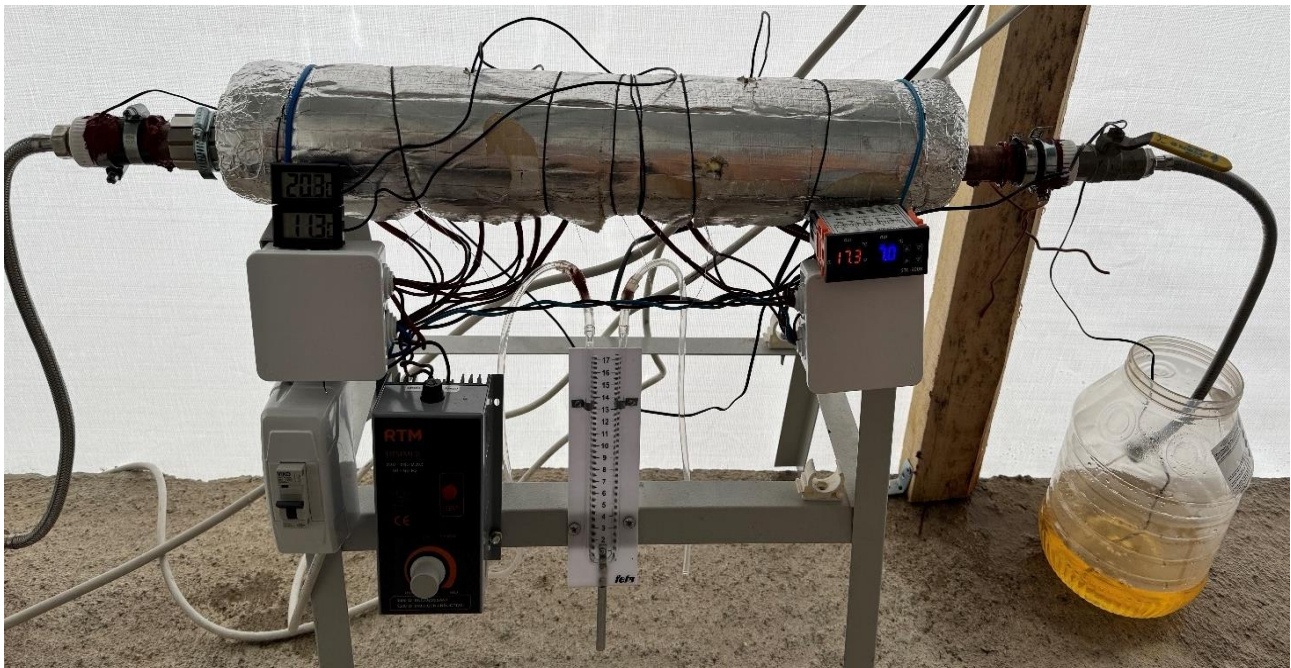
manometer inlets. Twelve clamp heaters are utilized, each having an outer diameter of 30 mm and a length of 40 mm, with a power rating of 200 Watts per heater. To achieve a consistent heat flux of  $25,000 \text{ W/m}^2$ , the system's electrical power is controlled using a 3000W-15A dimmer. For insulation, the heaters were first wrapped with rock wool and then covered with aluminum sheathing.

In the experimental setup, copper pipes were used to effectively give heat energy to the fluid. The copper pipe is length of  $l = 75 \text{ cm}$  and diameters of  $D_o = 28 \text{ mm}$ ,  $d_i = 26 \text{ mm}$ . At the starting position of the heaters, 10 neodymium magnets were placed to generate

a magnetic field. Each magnet had dimensions of  $50 \times 10 \times 5 \text{ mm}$  measurements with a gauss meter revealed that the total magnetic field intensity produced by the magnets was 1600 Gauss. Thermocouples were placed at the inlet and outlet of the copper tube to measure the fluid temperatures at both ends. Two more thermocouples were positioned between the heaters to monitor the surface temperature of the copper tube. Additionally, the pressure drops within the flow were investigated using a U-type manometer integrated into the system. The diagrammatic illustration of the experimental arrangement created using the computer software is presented in Figure 1, while the actual visual depiction of the experimental setup can be found in Figure 2.



**Figure 1.** Schematic representation of the experimental set prepared in the computer program



**Figure 2.** Visual of the experimental setup

### 3. CONCLUSION AND DISCUSSION

The thermal performance of an iron oxide-pure water nanofluid under the influence of a magnetic field was the main experimental focus of this study. Fourteen distinct experiments were conducted, and the outcomes were compared. Using the collected data, the necessary computations were carried out, and the thermal performance of nanofluids relative to pure water was evaluated. The formulas used in the calculations (Equation 7 to 15) are as follows;

Temperature difference;

$$\Delta T (K) = T_{\zeta} - T_g \tag{7}$$

Average temperature;

$$T_{ort}(K) = \frac{T_g + T_{\zeta}}{2} \tag{8}$$

Heat absorbed by the fluid;

$$\dot{Q}(W) = \dot{m}c_p(T_{\zeta} - T_g) \tag{9}$$

Heat transfer coefficient;

$$h (W mK^{-1}) = \frac{\dot{q}}{T_y - T_{ort}} \tag{10}$$

Thermal capacity;

$$\dot{q}(W m^{-1}) = \frac{\dot{Q}}{A} \tag{11}$$

Pressure drop;

$$\Delta P = (\rho_{Hg} - \rho)g \times \Delta h \tag{12}$$

Reynolds number;

$$Re = \frac{\rho * V * D_h}{\mu} \tag{13}$$

Nusselt number;

$$Nu = \frac{h * D_h}{k} \tag{14}$$

Friction factor;

$$f = \frac{P_{in} - P_{out}}{\left(\frac{L}{D}\right) \left(\frac{\rho V^2}{2}\right)} \tag{15}$$

The formulas indicate the following parameters:  $\Delta T$  represents the temperature difference between the inlet and outlet of the fluid;  $T_g$  denotes the inlet temperature of the fluid;  $T_{\zeta}$  signifies the outlet temperature of the fluid;  $T_y$  refers to the surface temperature of the copper pipe;  $T_{ort}$  is the average of the inlet and outlet temperatures; and  $\dot{m}$  indicates the mass flow rate,  $h$  heat convection coefficient,  $A$  Field,  $\rho_{Hg}$  density of mercury,  $\rho$  the density of the fluid,  $g$  Acceleration of gravity,  $\Delta h$  the difference in height on the pressure gauge,  $V$  velocity of the fluid,  $D_h$  hydrodynamic diameter,  $L$  characteristic length,  $P_{in}$  fluid inlet pressure,  $P_{out}$  the fluid outlet pressure.

#### 3.1. Experiments without Magnetic Field

The experiments were conducted at two distinct flow rates while maintaining a constant temperature capacity in the absence of a magnetic field. The ambient temperature, the copper pipe's surface temperature, and the fluids' inlet temperatures were maintained constant during the experiment. The results indicated that as the Reynolds number increased, the Nusselt numbers also increased. When compared to pure water, nanofluids show higher Nusselt number values at equivalent Reynolds numbers. Figure 3 displays the Re-Nu graph, which was produced by computations using the experimental data.

Furthermore, the graph of the computed friction factor is shown in Figure 4.

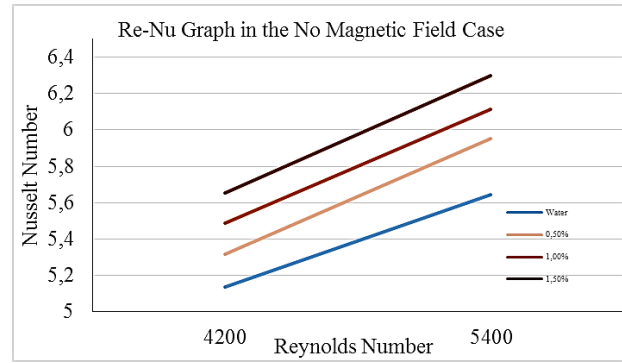


Figure 3. Re-Nu plot of fluids in the absence of magnetic field effect

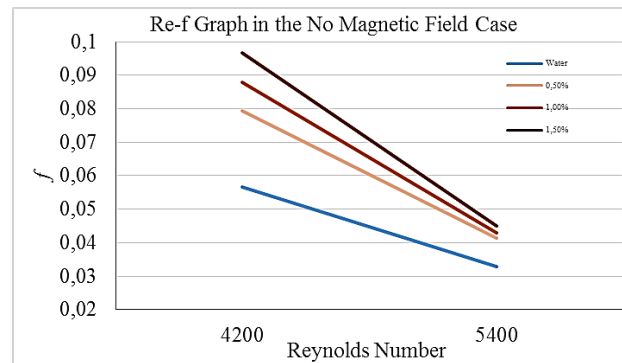


Figure 4. Re-f plot of fluids in the absence of magnetic field effect

#### 3.2. Experiments under Magnetic Field

The studies were carried out with two different flow rates and a constant temperature capacity while being affected by a magnetic field. Throughout the experimentation, the inlet temperatures of the fluids, the surface temperature of the copper pipe, and the ambient temperature were maintained at constant levels. The results yielded graph curves that resembled those obtained in the absence of a magnetic field. The same data was utilized for pure water, as the magnetic field is not expected to affect it. In the experiments performed within the magnetic field, an increase in the Nusselt number of nanofluids was observed. No significant variations were observed in the fluid's inlet and outlet pressure values. Therefore, there is no obvious difference in the coefficient of friction. The Re-Nu graph formed as a result of the calculations made according to the experimental data is shown in Figure 5. The calculated friction factor is illustrated in Figure 6.

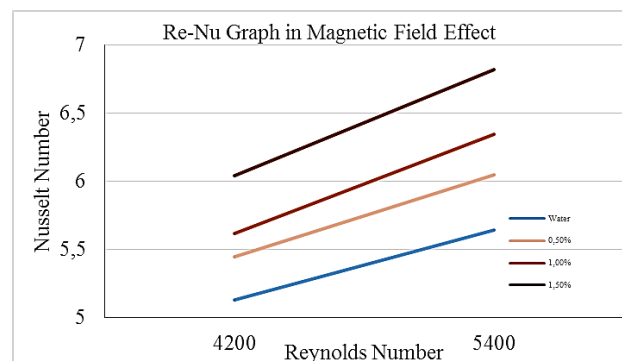


Figure 5. Re-Nu plot of fluids under magnetic field effect

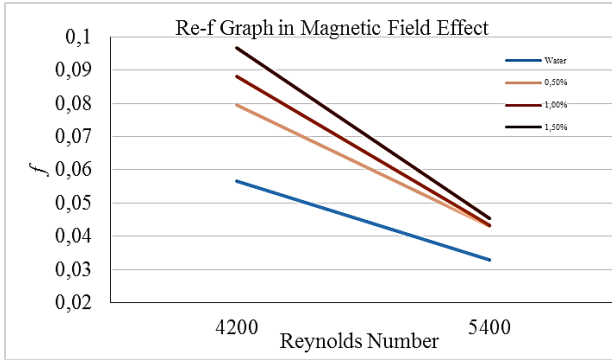


Figure 6. Re-f plot of fluids under magnetic field effect

### 3.3. Effect of Magnetic Field on Nanofluids

The experimental data collected without a magnetic field were compared to evaluate the effect of the magnetic field on nanofluids. Analysis of the results reveals that the magnetic field significantly influences the properties of the nanofluid. The Nusselt number increase value brought on by the magnetic field in the same nanofluid was compared with the graphs below in experiments conducted at two different Reynolds numbers. It is generally observed that the iron oxide-water nanofluid is affected by the magnetic field. Figure 7 and Figure 8 compare the Nusselt numbers of fluids with  $Re=4200$  and  $Re=5400$  values based on the magnetic field.

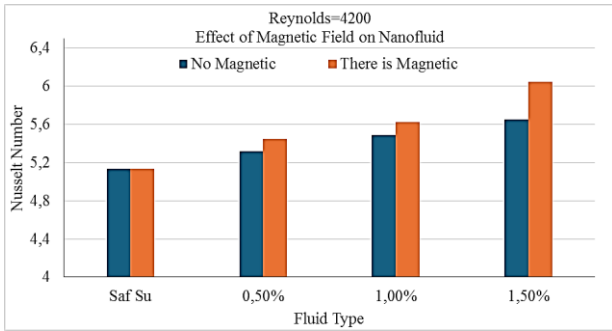


Figure 7. The effect of magnetic field at  $Re=4200$  on the Nusselt number of fluids

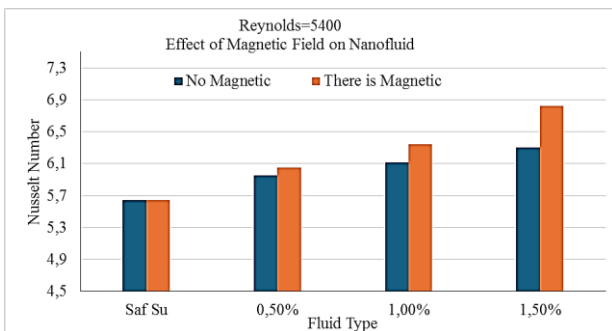


Figure 8. The effect of magnetic field at  $Re=5400$  on the Nusselt number of fluids

## 3. RESULTS

The experiments demonstrated that the Nusselt number increased as the Reynolds number rose for all the fluids tested. It was also observed that the Nusselt number was further increased when pure water was replaced with an iron oxide-water nanofluid. In the experiments conducted

without the influence of a magnetic field, it was noted that the Nusselt number rose as the volumetric ratio of the iron oxide-water nanofluid increased. In experiments conducted at  $Re=4200$ , the Nusselt number of pure water was 5.135, while the Nusselt number of 1.5% Iron oxide-water nanofluid increased by 10.1% and was found to be 5.653. In experiments conducted at  $Re=5400$ , the Nusselt number of pure water was 5.645, while the Nusselt number of 1.5% Iron oxide-water nanofluid increased by 11.6% and was found to be 6.299.

In experiments conducted under the influence of magnetic field, the Nusselt number of 1.5% Iron oxide-water nanofluid at  $Re=4200$  was found to be 6.043. This value is 17.7% higher than the Nusselt number of pure water. At a Reynolds number of 5400, the Nusselt number of the 1.5% iron oxide-water nanofluid increased by 20.8% compared to water, reaching a value of 6.819. The observation indicated that the application of a magnetic field enhanced the thermal performance of nanofluids. The greatest effect of the magnetic field occurred in the 1.5% iron oxide-water nanofluid. While the Nusselt number of a 1.5% iron oxide-water nanofluid without a magnetic field is 6.299, the Nusselt number increases by approximately 8.25% to 6.819 when a magnetic field is applied to this fluid. It has been observed that it increases the Nusselt number by creating a linear effect in nanofluids at other concentrations. When the results are compared with previous studies, parallel results are seen. Like many nanofluids, the iron oxide-water nanofluid has increased heat transfer. The Nusselt number increases when a magnetic field is added to the nanofluid. Thus, we can conclude that magnetic nanofluids benefit from the magnetic field. There are multiple reasons for the iron oxide-water nanofluid's improved heat transfer. Initially, the total heat transfer coefficient of the nanofluid is higher than that of water alone, as iron oxide nanoparticles have a greater heat transfer coefficient than water. Additionally, the heat transfer coefficient increases due to the random motion of the nanoparticles within the fluid, along with their interactions and collisions. Moreover, the impact of the magnetic field on the movement of nanoparticles adds complexity to the fluid dynamics, thereby improving the heat transfer coefficient. The fact that nanofluids increase the heat transfer coefficient shows that their use in heat transfer systems is inevitable in the future. In today's technology, nanofluids are not widely used due to their high production costs and not at the desired level of homogeneity/stability. With the developing technology, nanoparticles in smaller sizes can be produced and nanofluids with high homogeneity and stability levels can be produced. With these nanofluids produced, it will be possible to obtain more heat transfer coefficient.

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