

PREDICTIVE CONTROL OF A HEATEXCHANGER BASED ON LOCAL FUZZY MODELS AND NEURAL NETWORKS

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ABSTRACT

This paper deals with identification and control of a highly nonlinear real world application. The performance and applicability of the proposed methods are demonstrated for an industrial heat exchanger. The main difficulties for identification and control of this plant arise from the strongly nonlinear center. First, a neural network based predictive controller using Multi Layer Perceptron (MLP) is designed to govern the dynamics of a heat exchanger pilot plant. The performance of the proposed controller is compared with that of Local Linear Model Tree (LOLIMOT) through simulation studies.

Keywords: *Neural network control, Multi Layer Perceptron, Local Linear Model Tree, predictive control, heat exchanger pilot plant.*

1. INTRODUCTION

Predictive control is now widely used in industry and a large number of implementation algorithms. Most of the control algorithms use an explicit process model to predict the future behavior of a plant and because of this, the term model predictive control (MPC) is often utilized [1-2]. The most important advantage of the MPC technology comes from the process model itself, which allows the controller to deal with an exact replica of the real process dynamics, implying a much better control quality. The inclusion of the constraints is the feature that most clearly distinguishes MPC from other process control

techniques, leading to a tighter control and a more reliable controller. Another important characteristic, which contributes to the success of the MPC technology, is that the MPC algorithms consider plant behavior over a future horizon in time. Thus, the effects of both feedforward and feedback disturbances can be anticipated and eliminated, fact, which permits the controller to drive the process output more closely to the reference trajectory.

Although industrial processes usually contain complex nonlinearities, most of the MPC algorithms are based on a linear model of the process. Linear models such as step response and impulse response models derived from the

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convolution integral are preferred, because they can be identified in a straightforward manner from process test data. In addition, the goal for most of the applications is to maintain the system at a desired steady state, rather than moving rapidly between different operating points, so a precisely identified linear model is sufficiently accurate in the neighborhood of a single operating point. As linear models are reliable from this point of view, they will provide most of the benefits with MPC technology. Even so, if the process is highly nonlinear and subject to large frequent disturbances, a nonlinear model will be necessary to describe the behavior of the process. Also, in servo control problems where the operating point is frequently changing, a nonlinear model of the plant is indispensable [3-5].

In situations like the ones mentioned above, the task of obtaining a high-fidelity model is more difficult to build for nonlinear processes. Recently, neural networks have become an attractive tool in the construction of models for complex nonlinear systems [6-7]. A large number of control and identifications structures based on neural networks have been proposed [8-15].

Most of the nonlinear predictive control algorithms imply the minimization of a cost function, by using computational methods for obtaining the optimal command to be applied to the process. The implementation of the nonlinear predictive control algorithms becomes very difficult for real-time control because the minimization algorithm must converge at least to a sub-optimal solution and the operations involved must be completed in a very short time (corresponding to the sampling period). This paper analyzes an artificial neural network based nonlinear predictive controller for a heat exchanger, which is a highly nonlinear process.

The procedure is based on construction of a neural network model for the process and the proper use of that in the optimization process. The method eliminates the most significant obstacles for nonlinear MPC implementation by developing a nonlinear model, designing a neural predictor and providing a rapid, reliable solution for the control algorithm. Using the proposed controller, the output temperature tracking behavior of the plant is studied. Also, the

performance of the proposed neural network based predictive controller is compared with that of LOLIMOT, which the latter leads to better performance.

The organization of this paper is as follows: In Section II the structure of a heat exchanger pilot plant is briefly presented. Sections III and IV present the predictive control methodology based on MLP and the simulation results in heat exchanger using MLP. Section VI and VII present the predictive control methodology based on LOLIMOT and online learning of neural predictors. The simulation results are presented in section VIII. Finally, the paper is concluded in Section IX.

2.HEAT EXCHANGER PILOT PLANT

The problem of heat-exchanger control with sensors and actuators limitation represents a serious problem from the point of optimal energy consumption [16-18]. The problem lies in the nonlinearity of the system behavior [19-22]. There are a large number of phenomena associated with flow and heat transfer that are perhaps simple to solve singly, but when combined result in a system that is impossible to compute. Some of these are: complicated heat and fluid flow geometries, turbulence in the flow, existence of hydrodynamic and thermal entrance regions, non-uniform local heat transfer rates and fluid temperatures, secondary flows in the tube bends, vortices in the neighborhood of the tube-fin junctions, air-side flow development in fin passages, heat conduction along tube walls, natural convection within the tubes and between fins, and temperature dependence of fluid properties.

The objective of our investigation, a real temperature plant, consists of a plate heatexchanger, a reservoir with heated water, two thermocouples, and a motor driven valve. The plate heat exchanger, through which hot water from an electrically heated reservoir is continuously circulated in the counter-current flow to cold process fluid (cold water). The thermocouples are located in the inlet and outlet flows of the exchanger; both flow rates can be visually monitored. Power to the heater may be controlled by time proportioning control using

the external control loop. The flow of the heating fluid can be controlled by the proportional motor driven valve. A schematic diagram of the plant is shown in figure (1).

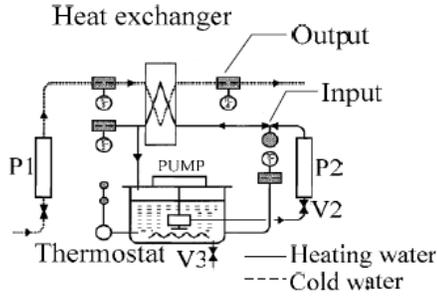


Fig. 1: The heat-exchanger pilot plant.

3. PREDICTIVE CONTROL METHODOLOGY BASED ON MULTI-LAYER PERCEPTRON

This section presents the role and architecture of the neural predictors resulting from the following nonlinear modeling techniques based on neural network principles.[26-28]

A network with $k+1$ layers and n_0, n_1, \dots, n_k points in each layer is recognized. Where, θ_k is the bias in the weigh vector of k^{th} layer. In zero and first layers, we mention x as input layer vector, w_1 as weight vector, z_1 as state vector and y_k as output vector. Thus we obtain:

$$X = \begin{bmatrix} x_1 \\ x_2 \\ \vdots \\ x_{n_0} \end{bmatrix}, W_1 = (w_{ij}^1)_{n_0 \times n_1}, Z_1 = \begin{bmatrix} z_1^1 \\ z_2^1 \\ \vdots \\ z_{n_1}^1 \end{bmatrix} = W_1^T X, Y_1 = \begin{bmatrix} y_1^1 \\ y_2^1 \\ \vdots \\ y_{n_1}^1 \end{bmatrix} = f(Z_1) \quad (1)$$

f is a function which is considered to be:

$$f(s) = \frac{1}{1 + \exp(-s)} \quad (2)$$

to implement BP algorithm we have to minimize the following cost function:

$$F(w) = \frac{1}{2} \sum_{i=1}^q e_i^T e_i = \frac{1}{2} \sum_{i=1}^q (R_i - Y_i)^T (R_i - Y_i) \quad (3)$$

w is a vector including bias and weights. Using steepest descent algorithm to minimize that cost function, we have:

$$w_{k+1} = w_k + \mu \left(-\frac{\partial e}{\partial w} \right)_{w=w_k} \quad (4)$$

where μ is the learning rate.

In a Multi Layer Perceptron (MLP) with Back propagation as training method with just one hidden layer, h neurons in hidden layer and p neurons in input layer, the output of MLP network becomes:

$$y(i) = \sum_{j=1}^h w_j f_j(z_j(i)) + b \quad (5)$$

$$z(j) = \sum_{k=1}^p w_{j,k} x(k) + b_j \quad (6)$$

and $y(i)$ is the output of the i^{th} neuron, f_j output function of j^{th} neuron in hidden layer, $z(j)$

Output function of j^{th} neuron, h the neuron number in hidden layer, p the number of input neurons, w_j the connecting weigh of j^{th} neuron of hidden layer to output neuron, $w_{j,k}$ connecting weigh of i^{th} input neuron to j^{th} neuron of hidden layer, b_j the bias of j^{th} neuron in hidden layer and b as the bias in output neuron.

A quadratic cost function is utilized to compute the prediction error and to derive the optimal predictive control strategy.

$$\begin{aligned} \text{Min}_{u(t)} J = \text{Min}_{u(t)} \left\{ \frac{1}{2} \sum_{i=N_1}^{N_2} \|y(t+i) - r(t+i)\|^2 \right. \\ \left. + \frac{1}{2} \sum_{i=0}^{N_u} \lambda_i \|u(t+i)\|^2 + \lambda'_i \|\Delta u(t+i)\|^2 \right\} \quad (7) \end{aligned}$$

$$\text{s.t.} \begin{cases} u_{\min} \leq u(t+i) \leq u_{\max} & i = 0, \dots, N_u \\ y_{\min} \leq y(t+i) \leq y_{\max} & i = N_1, \dots, N_2 \\ \|\Delta u(t+i)\| \leq \Delta u_{\max} & i = 0, \dots, N_u \\ \Delta u(t+i) = 0 & i > N_u - 1 \end{cases} \quad (8)$$

Where λ and λ' are weighting matrixes and N_1, N_2, N_u are the minimum, maximum of prediction horizon and control horizon, respectively.

Minimization of the cost function (j) occurs in each sampling time and ends in a control signal. But with the aim of receding horizon only the first element of it will be used as control signal..Using steepest descent strategy we have:

$$u^{i+1}(t) = u^i(t) - \alpha \frac{\partial J}{\partial u^i(t)} \quad (9)$$

Where $\alpha \in R^+$ is the optimization step.

This algorithm is continued until the variation of $u(t)$ becomes less than a small value of \mathcal{E} . The derivation of the cost function (j) in time of $t+h, (h=1,2,\dots, N_u)$ is as follows:

$$\frac{\partial J}{\partial u(t+h)} = -\sum_{i=N_1}^{N_u} [y(t+i) - r(t+i)] \frac{\partial y(t+i)}{\partial u(t+h)} + \sum_{i=0}^{N_u} \lambda_i u(t+i) \frac{\partial u(t+i)}{\partial u(t+h)} + \sum_{i=0}^{N_u} \lambda_i \Delta u(t+i) \frac{\partial \Delta u(t+i)}{\partial u(t+h)} \quad (10)$$

Possibly we write $\frac{\partial \Delta u(t+j)}{\partial u(t+h)}$ in the form of

$$\frac{\partial u(t+j)}{\partial u(t+h)} - \frac{\partial u(t+j-1)}{\partial u(t+h)} = \delta(h, j) - \delta(h, j-1) \quad (11)$$

While Kronecker delta function is

$$\delta(h, j) = \begin{cases} 1 & \text{if } h = j \\ 0 & \text{if } h \neq j \end{cases} \quad (12)$$

So, we have:

$$\frac{\partial u(t+j)}{\partial u(t+h)} = \delta(h, j) \quad (13)$$

In accordance to (5) and (6), we have:

$$y(t+i) = \sum_{j=1}^h w_j f_j(z_j(t+i)) + b \quad (14)$$

And $\frac{\partial y(t+j)}{\partial u(t+h)}$ can be written as:

$$\frac{\partial y(t+j)}{\partial u(t+h)} = \sum_{j=1}^h w_j \frac{\partial f_j(z_j(t+i))}{\partial u(t+h)} \quad (15)$$

Using Chain rule we obtain:

$$\frac{\partial f_j(z_j(t+i))}{\partial u(t+h)} = \frac{\partial f_j(z_j(t+i))}{\partial z_j(t+i)} \frac{\partial z_j(t+i)}{\partial u(t+h)} \quad (16)$$

$\frac{\partial f_j(z_j(t+i))}{\partial z_j(t+i)}$ Can be calculated using output

function deviation. $z_j(t+i)$ is depended on input $u(t+i)$, delayed inputs $u(t+i-1), u(t+i-2), \dots, u(t+i-n)$ and output $y(t+i-1)$, delayed output $y(t+i-2), y(t+i-3), \dots, y(t+i-m)$.

Suppose having k neurons as input while the first neurons from 1 to q introduce $u(t+i-n); n=0,1,\dots, q-1$ Neurons from

$q+1$ to K show $y(t+i-1-m); m=0,1,\dots, K-q-1$. So we have:

$$z_j(t+i) = \sum_{n=0}^{q-1} w_{j,n+1} \mathcal{L}(t+i-n) + \sum_{m=0}^{K-q-1} w_{j,m+q+1} y(t+i-1-m) \quad (17)$$

and $\frac{\partial z_j(t+j)}{\partial u(t+h)}$ can be calculated as follows:

$$\frac{\partial z_j(t+j)}{\partial u(t+h)} = \sum_{n=0}^{q-1} w_{j,n+1} \frac{\partial u(t+i-n)}{\partial u(t+h)} + \sum_{m=0}^{K-q-1} w_{j,m+q+1} \frac{\partial y(t+i-1-m)}{\partial u(t+h)} \quad (18)$$

Then,

$$\frac{\partial u(t+i-n)}{\partial u(t+h)} = \begin{cases} \delta(i-n, h) & \text{if } i-n < N_u \\ \delta(N_u, h) & \text{if } i-n > N_u \end{cases} \quad (19)$$

$\frac{\partial y(t+i-1-m)}{\partial u(t+h)}$ can be calculated through a repetitive calculation considering the case of $i-1-m < 1$ ending in zero as a result.

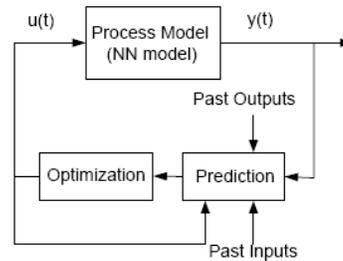


Fig. 2: The scheme of neural network based predictive control

4. SIMULATION RESULTS OF PREDICTIVE CONTROL IN THE HEAT-EXCHANGER WITH USE MLP

In this system we recognize flow as input and temperature as output. The input and output data [24] are shown in figure (3).

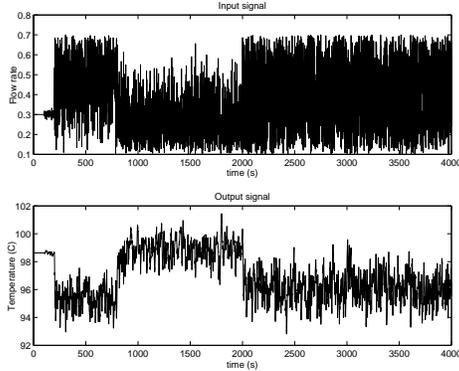


Fig. 3: Input and output signal

The set point tracking results of the simulation on the plant and the corresponding input signal are depicted in Figures 4 and 5. Clearly the system could track the set points with satisfactory performance using a numerical optimization the prediction and control horizons are 7 and 3, respectively also λ_i is 0.01 .

Next, the cost function J is constructed

$$Min_{u(t)} J = Min_{u(t)} \left\{ \frac{1}{2} \sum_{i=N1}^{N2} \|y(t+i) - r(t+i)\|^2 + \sum_{i=0}^N \lambda_i \|\Delta u(t+i)\|^2 \right\} \quad (20)$$

The minimization algorithm gives the control input vector $U=[u(t),u(t-1),u(t-2),y(t),y(t-1),y(t-2)]$ to be applied to the plant .

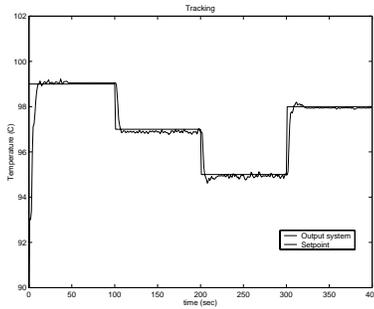


Fig. 4: Tracking

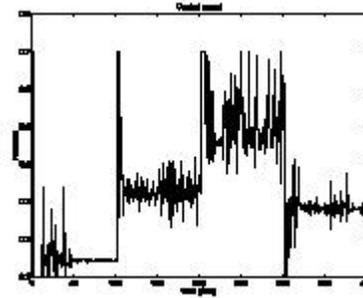


Fig. 5: Control signal

Clearly the system could track the set points with satisfactory performance.

5. AN INTRODUCTION TO LOCAL LINEAR MODEL TREE (LOLIMOT)

The network structure of a local linear neurofuzzy model is depicted in Fig.6. Each neuron realizes a local linear model (LLM) and an associated validity function that determines the region of validity of the LLM. The validity functions form a partition of unity, i.e., they are normalized such that

$$\sum_{i=1}^M \Phi_i(z) = 1 \quad (20)$$

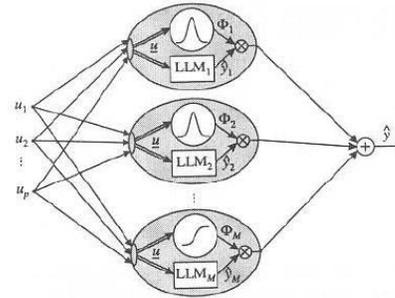


Fig. 6: Network structure of a local linear neuro fuzzy model with M neurons for n_x LLM inputs x and n_z validity function inputs z .

for any model input z . The output of a local linear neuro-fuzzy model is calculated as

$$\tilde{y} = \sum_{i=1}^M (w_{i,0} + w_{i,1}x_1 + \dots + w_{i,n_x}x_{n_x})\Phi_i(z) \quad (21)$$

where the local linear models depend on $\underline{x} = [x_1, x_2, \dots, x_{nz}]^T$ and the validity functions depend on $\underline{z} = [z_1, z_2, \dots, z_{nz}]^T$. Thus, the network output is calculated as a weighted sum of the outputs of the local linear models where the $\Phi_i(\cdot)$ are interpreted as the operating point dependent weighting factors. The network interpolates between different LLMs with the validity functions.

The weights w_{ij} are *linear* network parameters.

The validity functions are typically chosen as normalized Gaussians. If these Gaussians are furthermore axis-orthogonal the validity functions are

$$\Phi_i(\underline{z}) = \frac{\mu_i(\underline{z})}{\sum_{j=1}^M \mu_j(\underline{z})}$$

$$\mu_i(\underline{z}) = \exp\left(-\frac{1}{2}\left(\frac{(z_1 - c_{i1})^2}{\sigma_{i1}^2} + \dots + \frac{(z_{nz} - c_{inz})^2}{\sigma_{inz}^2}\right)\right)$$

$$= \exp\left(-\frac{1}{2}\frac{(z_1 - c_{i1})^2}{\sigma_{i1}^2}\right) \dots \exp\left(-\frac{1}{2}\frac{(z_{nz} - c_{inz})^2}{\sigma_{inz}^2}\right)$$
(22)

The centers and standard deviations are *nonlinear* network parameters.

In the fuzzy system interpretation each neuron represents one rule. The validity functions represent the rule premise and the LLMs represent the rule consequents. One-dimensional Gaussian membership functions:

$$\mu_{ij}(z_j) = \exp\left(-\frac{1}{2}\frac{(z_j - c_{ij})^2}{\sigma_{ij}^2}\right)$$
(23)

can be combined by a t-norm (conjunction) realized with the product operator to form the multidimensional membership functions in (5). One of the major strengths of local linear neuro-fuzzy models is that premises and consequents do not have to depend on identical variables, i.e. z and x can be chosen independently.

6. PREDICTIVE CONTROL METHODOLOGY BASED ON LOIMOT ALGORITHM

The prediction output can be written as: [25]

$$\hat{y}_{t+d+i} = \bar{F}_i^T \bar{\Phi}_i + \sum_{j=0}^i \bar{G}_{ij}^T \bar{\Phi}_{ij} u_{t+j}$$
(24)

$\bar{\Phi}_i$ and $\bar{\Phi}_{ij}$ are basis functions, we can possibly define the weight and basis function vectors as:

$$\bar{F}_i = [f_{i1} \ f_{i2} \ \dots \ f_{iN}]^T$$

$$\bar{\Phi}_i = [\varphi_{i1}(x_t) \ \varphi_{i2}(x_t) \ \dots \ \varphi_{iN}(x_t)]^T$$
(25)

$$\bar{G}_{ij} = [g_{ij1} \ g_{ij2} \ \dots \ g_{ijN}]^T$$

$$\bar{\Phi}_{ij} = [\varphi_{ij1}(x_t) \ \varphi_{ij2}(x_t) \ \dots \ \varphi_{ijN}(x_t)]^T$$

to define how well the predicted process output tracks the reference trajectory, a number of cost functions are employed for predictive control, here we use a cost function which is of the following quadratic form:

$$J_{np} = \frac{1}{2} \|R_{t+d+L} - Y_{t+d+L}\|_2^2 + \frac{1}{2} \alpha \|\Delta U_{t+L}\|_2^2$$
(26)

$$J_{np} = \frac{1}{2} \|R_{t+d+L} - Y_{t+d+L}\|_2^2 + \frac{1}{2} \alpha \|\Delta U_{t+L}\|_2^2$$
(27)

R_{t+d+L} , Y_{t+d+L} and U_{t+L} are the future reference input, predicted output and control input vectors, respectively, L is the control horizon, $L+D$ is the prediction horizon, and $\alpha > 0$ is the weight.

The optimal controller output sequence over the prediction horizon is obtained by minimizing the performance index J_{np} with respect to U_{t+L} . This can be carried out by taking the derivative of the performance function J_{np} with respect to the control input vector U_{t+L} and results in:

$$\frac{\partial J_{np}}{\partial U_{t+L}} = 0 \Rightarrow \frac{\partial Y_{t+d+L}^T}{\partial U_{t+d+L}} (Y_{t+d+L} - R_{t+d+L}) + \alpha \frac{\partial \Delta U_{t+L}^T}{\partial U_{t+L}} \Delta U_{t+L} = 0$$
(28)

$$\frac{\partial Y_{t+d+L}^T}{\partial U_{t+d+L}} = Q^T I$$

$$= \begin{bmatrix} \bar{G}_{00}^T \bar{\Phi}_{00} & 0 & 0 & 0 \\ \bar{G}_{10}^T \bar{\Phi}_{10} & \bar{G}_{11}^T \bar{\Phi}_{11} & 0 & 0 \\ \vdots & \vdots & \ddots & 0 \\ \bar{G}_{L0}^T \bar{\Phi}_{L0} & \bar{G}_{L1}^T \bar{\Phi}_{L1} & \dots & \bar{G}_{LL}^T \bar{\Phi}_{LL} \end{bmatrix}^T$$
(29)

Let

$$H_L = [\bar{F}_0^T \bar{\Phi}_0 \quad \bar{F}_1^T \bar{\Phi}_1 \quad \dots \quad \bar{F}_L^T \bar{\Phi}_L]^T \quad (30)$$

Where $I_1 = [1, 0, \dots, 0]$ is an identity vector

and the matrix D_L is of the form

$$D_L = \begin{bmatrix} 1 & & & & 0 \\ -1 & 1 & & & \\ & \ddots & \ddots & & \\ 0 & & -1 & 1 & \end{bmatrix} \quad (31)$$

It is clear that the controller input vector U_{t+L} can be calculated by

$$U_{t+L} = (Q_L^T Q_L + \alpha D_L^T D_L)^{-1} (Q_L^T R_{t+d+L} - Q_L^T H_L + \alpha I_1^T u_{t-1}) \quad (32)$$

Thus, the control input u_t minimizing the performance function J_{np} is given by:

$$u_t = I_1 (Q_L^T Q_L + \alpha D_L^T D_L)^{-1} (Q_L^T R_{t+d+L} - Q_L^T H_L + \alpha I_1^T u_{t-1}) \quad (33)$$

7. On-LINE LEARNING OF NEURAL PREDICTORS

Here we consider the online adjustment of the weights of the i^{th} predictor.[25] The weight estimation of the other predictors are the same . It will be assumed that the basis functions which are used in the predictors are given and the required prediction accuracy can be achieved by adjusting the corresponding weights to those functions.

Using the available output data and the input data, the output of the i^{th} predictor at time t can be written as

$$y_t = (\bar{F}_i^*) \Phi(x_{t-d-i}) + \sum_{j=0}^i (\bar{G}_{ij}^*) \bar{\Phi}_{ij}(x_{t-d-i}) u_{t-d-i+j} + \varepsilon_t \quad (34)$$

Where, (\bar{F}_i^*) and (\bar{G}_{ij}^*) are the optimal estimates of the weight vectors (\bar{F}_i) and (\bar{G}_{ij})

for $j = 0, 1, 2, \dots$, respectively ε_t is the approximation error of the predictor using the neural network and is assumed to be bounded by a positive number of δ for all time, that is

$$\max_{t \in N} |\varepsilon_t| \leq \delta \quad (35)$$

Where the number N represents the prediction accuracy, which is known by assumption. The i^{th}

estimated predictor can also be compactly expressed by:

$$\hat{y}_t = W_t^T \Phi_{t-1}$$

Where the weight vector W_t and the basis function vector Φ_t are

$$\Phi_t = \begin{bmatrix} \bar{\Phi}_i(x_{t-d-i}) \\ \bar{\Phi}_{i0}(x_{t-d-i}) u_{t-d-i} \\ \bar{\Phi}_{i1}(x_{t-d-i}) u_{t-d-i+1} \\ \vdots \\ \bar{\Phi}_{ii}(x_{t-d-i}) u_{t-d} \end{bmatrix} \quad (36)$$

$$W_t = [\bar{F}_i^T \quad \bar{G}_{i0}^T \quad \bar{G}_{i1}^T \quad \dots \quad \bar{G}_{ii}^T]^T$$

Based on the recursive least squares algorithm, an on-line weight learning algorithm is developed for affine nonlinear predictors. The algorithm is given by the following theorem.

THEOREM: consider the i^{th} predictor and the learning algorithm:

$$\begin{aligned} W_t &= W_{t-1} + \alpha_t \beta_t P_{t-1} \Phi_t e_t \\ P_t &= P_{t-1} - \beta_t \gamma_t P_{t-1} \Phi_{t-1} \Phi_{t-1}^T P_{t-1} \\ \alpha_t &= (1 - \delta |e_t|^{-1}) (1 + \Phi_{t-1}^T P_{t-1} \Phi_{t-1})^{-1} \\ \gamma_t &= (|e_t| - \delta) (|e_t| + (2|e_t| - \delta) \Phi_{t-1}^T P_{t-1} \Phi_{t-1})^{-1} \\ e_t &= y_t - W_{t-1}^T \Phi_{t-1} \\ \beta_t &= \begin{cases} 1, & |e_t| > \delta \\ 0, & |e_t| \leq \delta \end{cases} \end{aligned} \quad (37)$$

$$(i) \lim_{t \rightarrow \infty} \frac{\beta_t (|e_t| - \delta)^2}{1 + \Phi_{t-1}^T P_{t-1} \Phi_{t-1}} = 0 \quad (38)$$

$$(ii) \lim_{t \rightarrow \infty} |W_t - W_{t-1}| = 0 \quad (39)$$

$$(iii) \|\tilde{W}_t\|_2 \leq \sqrt{\frac{\lambda_{\max}(P_0^{-1})}{\lambda_{\min}(P_0^{-1})}} \|\tilde{W}_0\|_2 \quad (40)$$

$$\text{where } \tilde{W}_t = W^* - W_t \quad (41)$$

$\lambda_{\max}(\cdot)$ and $\lambda_{\min}(\cdot)$ denote the maximum and the minimum eigenvalues of the matrix (\cdot) , respectively, and W^* is the optimal estimate of the weight vector W_t .

Property (i) of the theorem above shows that if $1 + \Phi_{t-1}^T P_{t-1} \Phi_{t-1}$ is finite for all time, which is true if the closed-loop system is stable, the estimation error e_t converges to δ . Also, it can be seen from property (ii) that the weights converge as time t approaches infinity. In addition, Property (iii) implies that the weights will never drift to infinity over time.

8. SIMULATION RESULTS OF PREDICTIVE CONTROL IN THE HEAT-EXCHANGER WITH USE OF LOLIMOT

The set point tracking results of the simulation on the plant and the corresponding input signal are depicted in Figures 7 and 8. One and two step ahead predictors are depicted in figure 9 as well. Clearly the system could track the set points with satisfactory performance. To implement the algorithm, 4 neurons have been used and the prediction and control horizon are both set at 2 with the control weight which is equal to 2500 and

$$x(t) = [u(t-1), u(t-2), u(t-3), y(t-1), y(t-2), y(t-3)]$$

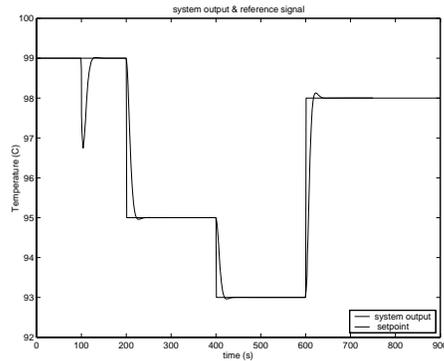


Fig. 7: System output and reference signal

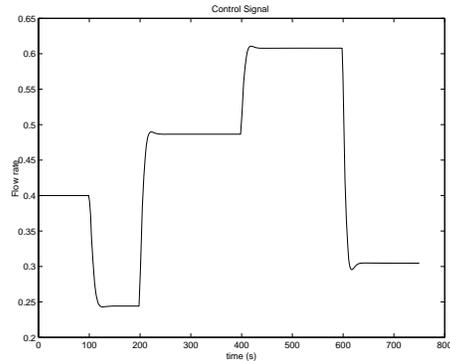


Fig. 8: Control signal

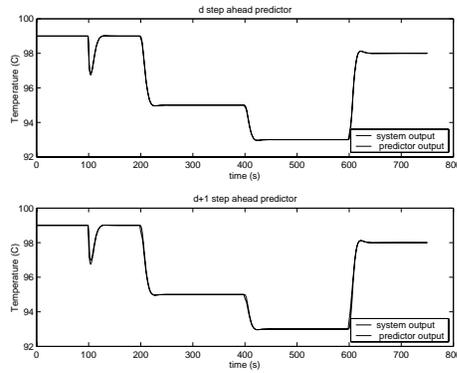


Fig. 9: 1 and 2 step ahead predictors

Based upon the above simulations, the following table is presented and we can conclude that LOLIMOT algorithm provides a better performance.

Table 1: Comparison between MLP and LOLIMOT

Method	Mean square error	Over shoot percentage	Settling time
MLP	0.6433	%6.66	22
LOLIMOT	0.3646	%2.4	27

It can be concluded from the table that the mean square error and overshoot percentage has been significantly decreased in LOLIMOT comparing with MLP resulting from the fact that in LOLIMOT an analytical optimization is used however a numerical optimization is used in MLP due to the fact of Sub-optimality problem.

9. CONCLUSIONS

A neural network based predictive control strategy was applied to a heat exchanger pilot plant. Heat exchanger is a highly nonlinear process; therefore, a nonlinear prediction method, e.g. neural network based methods, should be a better match in a predictive control strategy. Using the neuro predictive controller, the outlet liquid temperature of the plant tracked the desired set points by applying the liquid flow rate as a control signal. A neural network model for the plant was constructed. Once having such a model, i -step ahead predictions were obtained and a quadratic form cost function was utilized to compute the prediction error and to derive the optimal predictive control strategy. The performance of the proposed control strategy was

compared with that of LOLIMOT strategy when dealing with the tracking problem of output temperature, simulation results showed that the latter strategy performs much better than the former one in case of mean square error and the percent overshoot

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